



ARKANSAS

ENERGY & ENVIRONMENT

January 31, 2022

Via email to: dcaldwell@bigriversteel.com & First Class Mail

Dean Caldwell
Director Environmental
Big River Steel LLC
P.O. Box 707
Osceola, AR 72370

Re: Notice of Final Permitting Decision; Permit No. 2445-AOP-R0

Dear Mr. Caldwell,

After considering the application, any public comments, and other applicable materials as required by APC&EC Reg.8.211 and Ark. Code Ann. § 8-4-101 *et seq.*, this notice of final permitting decision is provided for:

Big River Steel LLC
1000 East County Road 860
Osceola, AR 72370-0248

Permit Number: 2445-AOP-R0

Permitting Decision: approval with permit conditions as set forth in final Permit No. 2445-AOP-R0

Accessing the Permitting Decision and Response to Comments, if any:
<https://www.adeq.state.ar.us/downloads/WebDatabases/PermitsOnline/Air/2445-AOP-R0.pdf>.

Accessing the Statement of Basis:
<https://www.adeq.state.ar.us/downloads/WebDatabases/PermitsOnline/Air/2445-AOP-R0-SOB.pdf>.

The permitting decision is effective on the date stated in the attached Certificate of Service unless a Commission review has been properly requested under Arkansas Pollution Control & Ecology Commission's Administrative Procedures, Regulation No. 8, within thirty (30) days after service of this decision.

The applicant or permittee and any other person submitting public comments on the record may request an adjudicatory hearing and Commission review of the final permitting decisions as provided under Chapter Six of Regulation No. 8. Such a request shall be in the form and manner

required by Reg.8.603, including filing a written Request for Hearing with the Commission secretary at 3800 Richards Rd, North Little Rock, Arkansas 72117. If you have any questions about filing the request, please call the Commission at 501-682-7890.

This permit is your authority to construct, operate, and maintain the equipment and control apparatus as set forth in your application initially received on 9/22/2021.

Sincerely,

William K. Montgomery
Associate Director, Office of Air Quality, Division of Environmental Quality
5301 Northshore Drive, North Little Rock, AR 72118-5317

Enclosure: Certificate of Service
cc: stevefrey@kennedyjenks.com

CERTIFICATE OF SERVICE

I, Cynthia Hook, hereby certify that the final permit decision notice has been mailed by first class mail to Big River Steel LLC, P.O. Box 707, Osceola, AR, 72370, on this 31st day of January, 2022.



Cynthia Hook, AA, Office of Air Quality

RESPONSE TO COMMENTS

BIG RIVER STEEL LLC PERMIT #2445-AOP-R0 AFIN: 47-01073

On December 19, 2021, the Director of the Arkansas Department of Energy and Environment, Division of Environmental Quality (“Division”) gave notice of a draft permitting decision for the above referenced facility. On January 14, 2022, written comments on the draft permitting decision were submitted by the facility. The Division’s response to these issues follows.

Note: The following page numbers and condition numbers refer to the draft permit. These references may have changed in the final permit based on changes made during the comment period.

Comment #1:

A blackline version of the Draft Operating Air Permit in Microsoft Word, is attached to this letter. This blackline permit shows (in trackchange) suggested changes to the draft permit language based on the following comments in this letter, or to otherwise provide clarity or correct typographical errors.

The changes shown in the attached blackline version reflect both (1) changes in text proposed to address each of the other comments proposed in this letter; and (2) where appropriate, additional changes needed to provide additional clarity and accuracy are included solely in the blackline, including grammatical type changes, or correction of typographical errors (e.g., removal of the word “not” as shown on page 11 of the attached blackline).

Response to Comment #1:

The Division has reviewed the changes shown in the blackline version of the permit submitted with these comments. Many of these changes are responded to specifically in Response to Comments #2 through #29. As a result of this comment, the following changes were made throughout the permit:

- Updated references referring to the “proposed project,” “proposed steel mill,” and other such identifiers to refer to the “Facility;”
- Updated some source names that were inconsistent throughout the permit;
- Added certain clarifying information to the Process Description and Source Descriptions throughout the permit;
- Added language to the Prevention of Significant Deterioration section of the permit to more clearly identify which modeling was performed for Class I or Class II purposes as well as additional descriptions of the dense grid modeling analysis; and
- Corrected various typographical and formatting errors throughout the permit.

Comment #2:

Street address should be changed to 1000 East County Road 860 in Osceola, AR. This change should be made to the cover sheet, and Section I Facility Information of the draft operating permit.

The initial draft operating permit had the address as 1000 East County Road. Including the reference to 860 more clearly defines the location of the Proposed Steel Mill Project. This full address is consistent with the location already specified in the September 2021 permit application (e.g., at Figure 5-1).

Response to Comment #2:

All references to the facility's address in the permit and Statement of Basis have been updated as requested.

Comment #3:

The Draft Permit includes references to the Proposed Steel Mill Project (hereinafter, the Facility) being a "new major source," but as discussed in the September 20, 2021 permit application, BRS understands U.S Environmental Protection Agency (EPA) guidance to require that the Facility be treated as a major modification. To clarify this, the following changes should be made to Section II: Introduction "Summary of Permit Activity":

- Big River Steel, LLC (BRS) is proposing to construct and operate a steel mill located at 1000 East County Road 860 in Osceola, AR (Facility). This new steel mill will be contiguous to an existing BRS steel mill, AFIN: 47-00991 (Existing Mill), and both are under common control of BRS or its parent company, and thus this new facility and the Existing Mill constitute a single stationary source under the Clean Air Act, and the Facility constitutes a major modification to the Existing Mill. At the request of BRS and for administrative convenience, this permit is being issued specific to the equipment located at the new Facility. This permit is the initial permit for a new steel mill and will include all the sources at the Facility. The Facility required a Prevention of Significant Deterioration (PSD) review to ensure the new emission sources associated with this major modification will not cause a significant deterioration of the local ambient air quality. PSD review was performed required for emissions of NO_x, CO, PM, PM₁₀, PM_{2.5}, SO₂, VOC, lead, and greenhouse gasses from the Facility.

And the following changes should be made to the first paragraph of Section II: Introduction "Prevention of Significant Deterioration":

- ~~Big River Steel~~The Facility is classified as a ~~new major source~~major modification to BRS's nearby Existing Mill under Prevention of Significant Deterioration (PSD) regulations. Due to the proposed emission rates, PSD review was performed is required for emissions of NO_x, CO, PM, PM₁₀, PM_{2.5}, SO₂, VOC, lead, and greenhouse gasses from the Facility.

The Facility will be a new stand-alone steel mill that will be independent from BRS' existing mill (hereinafter the Existing Mill) and will be a major source of emissions for purposes of PSD. However, because the Facility and the Existing Mill are located on adjacent property and are currently under common ownership, EPA guidance requires that they be treated as a single stationary source for purposes of the Clean Air Act and PSD regulations. Because both mills technically constitute a single source, the permit should note that the Facility is a PSD major modification to the Existing Mill rather than for a new source.

Notwithstanding the above analysis, please note that

1. Whether this Facility is treated as a new source or as a major modification will not affect the modeling conclusions that the Facility proposed emissions will result in compliance with the NAAQS and with Class I modeling requirements. For the sake of conservativeness, BRS modeled the Facility as a new source (e.g., not taking credit for the property boundary of the Existing Mill when defining ambient air for modeling purposes), and thus the modeled values are even more conservative than if it were modeled as a major modification to the existing source.
2. As a matter of administrative convenience, BRS has requested that the Facility be given a separate permit from the Existing Mill. This is a standard practice where two independent facilities or operators are grouped together due to EPA guidance on single source determinations. It is especially appropriate here because the Facility is intended to be a stand-alone project with separate operations, financing, and corporate management, and because the Facility is being permitted and designed to allow for the transfer of ownership and operational responsibilities to an entity other than BRS at some subsequent time without affecting ownership or operations of the Existing Mill.

Response to Comment #3:

The Summary of Permit Activity and initial paragraph of the Prevention of Significant Deterioration sections of the permit have been updated as requested.

Comment #4:

The summary results of the NAAQS analysis at page 10 of the draft permit should be revised, as shown in the attached redline, to be consistent with the updated modeling report provided by BRS, dated December 17, 2021. Specifically, the Maximum Modeled Impact for PM10 24-hour averaging time should be corrected from 68.21 ug/m³ to 57.30 ug/m³, and the Total Impact for PM10 24-hour averaging time should be corrected from 110.11 ug/m³ to 99.2 ug/m³.

This difference is being provided to ensure the Statement of Basis matched up with the technical information provided by BRS.

Response to Comment #4:

The Maximum Modeled Impact and Total Impact results for the PM₁₀ 24-hour NAAQS have been updated to match the modeling report submitted to the Division on December 17, 2021. The Maximum Modeled Impact for the 24-hour PM₁₀ Analysis is now 57.30 µg/m³. The Total Impact for the 24-hour PM₁₀ Analysis is now 99.20 µg/m³.

Comment #5:

SN-36 Pickle Galvanizing Line Tandem Cold Mill should be removed throughout the Operating Air Permit.

BRS previously notified AEEDEQ that it would no longer need a second Tandem Cold Mill to support the proposed Steel Mill project. Accordingly, we hereby request AEEDEQ to remove this source is consistent with BRS' prior request. Please note that this source was also excluded from the revised air quality impact assessment that was submitted to the AEEDEQ on December 17, 2021.

Response to Comment #5:

References left in the permit to SN-36 have been removed as requested.

Comment #6:

The nitrogen and sulfur deposition numbers under the "Maximum % of Threshold" row on page 12 of the draft permit should be corrected as shown in the attached redline.

This change is required so that the percentages provided match the percentages provided by BRS in the Class I technical report that supported the air permit application.

Response to Comment #6:

The Maximum Percent of Threshold value for Nitrogen Deposition has been updated from 36% to 72.8%. The Maximum Percent of Threshold value for Sulfur Deposition has been updated from 64% to 32.3%.

Comment #7:

BACT limits for the following sources should be included in BACT table included in the Draft Operating Air Permit

- SN-111 Paved Roadways
- SN-112 Unpaved Roadways
- SN-134 DRI Paved Road & Unpaved Fugitive Dust

BACT should be Best Work Practices which consists of the Development / Implementation of a Fugitive Dust Control Plan.

This change is required to properly address the regulatory requirement to implement BACT for Paved and Unpaved Roadways. EPA guidance stipulates that if technological or economic limitations in the application of a measurement technology to a particular emission unit would make an emission limit infeasible, a design, equipment, work practice, operation standard, or combination thereof, may be prescribed.

Response to Comment #7:

The BACT limits for SN-111, SN-112, and SN-134 were included in the permit but were not listed in the BACT Analysis Summary. These sources and their corresponding BACT limits have been included in the BACT Analysis Summary as a result of this comment.

Comment #8:

BACT limits for the CO₂e rate for SN-03 & SN-04 should be revised to account for the CO₂e emissions from the combustion of natural gas. Total rate is 11,132 tpy CO₂e and should be changed throughout the draft permit, accordingly.

This change is required to ensure that the CO₂e emission rate defined by BRS for this emission source in the initial application / supporting supplement information/data, is correctly referenced in the Operating Air Permit.

Response to Comment #8:

The BACT limit for CO₂e at SN-03 and SN-04 has been updated from 6,008 tpy total emissions of CO₂e to 11,132 tpy total emissions of CO₂e. Natural gas usage was already permitted but emissions were not updated for these sources. Each source's emissions have been individually updated from 3,004 tpy CO₂e to 5,566 tpy CO₂e throughout the permit.

Comment #9:

The lbs/hr limits should be removed for CO₂e for SN-03 and SN-04 under specific condition 1. Removal of the lbs/hr limit for CO₂e is required so that there is consistency throughout the permit with limits expressed for CO₂e. The limit is only expressed as tons/year for this and all other sources through the Operating Air Permit and we are not aware of any technical or legal basis that would necessitate the treatment of SN-03 and SN-04 differently from the other sources at the Facility.

Response to Comment #9:

The lb/hr limits for CO₂e have been removed for SN-03 and SN-04 as requested in Specific Condition #1.

Comment #10:

The Opacity limitation imposed on the following emission sources is 5%. This opacity limitation should be changed to 20%.

- SN-91 (charging Crane), SN-92 (Scrap Yard and Stockpiling) and SN-109 (Slag handling and Conveying); and
- Direct Reduction Iron (DRI) process sources: SN-116, SN-117, SN-118, SN-119, SN-120, SN-121, SN-122, SN-123, SN-124, SN-125, SN-126, SN-127, SN-128, SN-129

This change to SN-91, SN-92, and SN-109 is required to ensure that the opacity limitation properly identifies and is consistent with the opacity limitation required by the AEEDEQ on the BRS existing Osceola, Arkansas Mill, as well as other steel mills permitted in Arkansas. The DRI opacity limits for the emission source listed above should be set to 20%, which is consistent with AEEDEQ's Regulation 19.503 Visible Emission Regulation.

Response to Comment #10:

SN-91, SN-92, SN-109, and SN-116 have been updated as requested. The other DRI sources mentioned have a similar control technology to other permitted sources at the Facility that also have a 5% opacity limit. The opacity limit for all other listed sources remains unchanged.

Comment #11:

The draft permit did not address BACT for potential emissions of SO₂, VOC, CO, Lead, NO_x and CO_{2e} that may occur from seal gas used in the DRI process for emission sources SN-122 (Charge Hopper Dedusting), SN-124 (Furnace Dedusting) and SN-126 (Briquetter Dedusting). The BACT limits should be expressed as follows:

- 0.00317 lbs of NO_x / MMBtu
- 0.000376 lbs of SO₂ / MMBtu
- 0.08 lbs of CO / MMBtu
- 0.01 lbs of VOC / MMBtu
- 8.17 E-08 of Lead / MMBtu
- CO_{2e} should be 136,753 tons/year for SN-122, SN-124 and SN-126 combined
- The BACT Control Technology will be Good Combustion Practice, the combustion of natural gas only and a maximum heat input of 1591 MMBtu/hr.

This change is required to ensure that BACT is properly identified in the Operating Permit as it pertains to the use of seal gas in the DRI process. This information was provided to the AEEDEQ in the initial application dated September 20, 2021 and the Revised Proposed Steel Mill BACT demonstration submitted to AEEDEQ, dated October 11, 2021.

Response to Comment #11:

The sources and emissions associated with these sources were in the draft permit, however the BACT section was not updated with these BACT limits. The BACT Analysis Summary as well as Specific Condition #93 have been updated with this additional BACT information.

Comment #12:

The emission limits for the CO₂e rate for SN-03 & SN-04 should be revised to account for the CO₂e emissions from the combustion of natural gas. Total rate is 5,566 tpy CO₂e for SN-03 and SN-04, each and should be changed throughout the draft permit, accordingly.

This change is required to ensure that the CO₂e emission rate defined by BRS for this emission source in the initial application / supporting supplement information / data, is correctly referenced in the Operating Air Permit.

Response to Comment #12:

Please see Response to Comment #8.

Comment #13:

The emission limits for the single and combined HAPs in Permit Condition #3 and the Emission Summary table should be revised as reflected in the attached redline, because they do not include emissions of Lead. The estimated Lead emission rate for EAF 1 / LMF 1 and EAF 2 / LMF 2 is 0.57 tons/year for each, respectively. The Lead emission rate represents the maximum single HAP and the inclusion of Lead for the total HAP would change from 0.44 tons/year to 1.01 tons/year for both EAF / LMF 1 and EAF/ LMF 2.

The maximum estimated pounds per hour (lb/hr) for Lead was 0.14 for each EAF / LMF combination. This lb/hr rate would replace the lb/hr rate for the Single HAP and would be added to the total lb/hr rate for each Total HAP rate.

This change is required to ensure that the HAP emission rates defined by BRS for these emission sources in the initial application / supporting supplement information / data, is correctly referenced in the Operating Air Permit.

Response to Comment #13:

The emissions for lead are accounted for individually at these sources and thus it is unnecessary to include lead emissions in the Single HAP or Total HAP emission limits. As outlined in the footer of the Emission Summary Section, "HAPs included in the VOC totals. Other HAPs are not included in any other totals unless specifically stated." Lead is required to be listed separately as it is a non VOC HAP and also subject to PSD BACT review. There were no changes made to the permit as a result of this comment.

Comment #14:

The following stack testing requirement is contained in the Draft Operating Air Permit. BRS will conduct the required testing as defined in this permit condition. BRS would like to request that the following statement be included in the proposed permit limit as highlighted in red below.

29. The permittee shall perform stack testing of SN-01 and SN-02 for NO_x, SO₂, CO, CO₂ and VOC emissions to show compliance with the emissions limits in Specific Conditions #1 and #2. Testing shall be performed in accordance with Plantwide Conditions 3 and 4 and shall be repeated every six months (i.e., semi-annual) thereafter. The permittee may reduce the frequently of stack testing to every twelve months (i.e., annually) in the event testing over the initial three (3) year period shows compliance with the corresponding permitted emission limits.

The permittee shall measure NO_x, SO₂, CO₂ and CO emissions in accordance with EPA Reference Methods 7E, 6C, 3A and 10, respectively. The permittee shall measure the total VOC emissions using EPA Reference Method 25A, from which it will subtract out methane (CH₄) and ethane (C₂H₆) emissions from the EAF baghouse using EPA Reference Method 18 to arrive at applicable VOC levels for purposes of this permit. Semiannual stack testing for a pollutant is not required if the permittee elects to operate a CEMS for that pollutant at SN-01 and SN-02. Testing shall be conducted when the EAF is operated at or near its capacity based on the specific type of steel to be produced. A targeted capacity would be 250 tons/hour of steel. If the production rate is less than 250 tons/hour, the tested emission rates shall be scaled up to 250 ton/hour and compared to the permitted emission rates. If the production rate is above 250 tons/hour, the tested rate would be compared directly to the permitted emission rate. The capacity of SN-01 and SN-02 will vary based on the type of steel being produced. [[Reg.19.702 and 40 C.F.R. § 52 Subpart E].

This change is being requested to ensure that stack testing of SN-01 and SN-02 is on the same testing frequency for all regulated air pollutants to be tested for these two emission sources. Please note that draft permit condition #10 requires testing for PM/PM₁₀/PM_{2.5} to be conducted on an annual basis and this annual testing requirement is consistent with BRS' air permit for the Existing Mill and other steel mills in Arkansas.

Response to Comment #14:

Specific Condition #29 has been updated and now reads as follows:

“The permittee shall perform stack testing of SN-01 and SN-02 for NO_x, SO₂, CO, CO₂ and VOC emissions to show compliance with the emissions limits in Specific Conditions #1 and #2. Testing shall be performed in accordance with Plantwide Conditions 3 and 4 and shall be repeated every six months until six consecutive tests are passed. The permittee shall then conduct subsequent testing annually. The permittee shall measure NO_x, SO₂, CO₂ and CO emissions in accordance with EPA Reference Methods 7E, 6C, 3A and 10, respectively. The permittee shall measure the total VOC emissions using EPA Reference Method 25A, from which

it will subtract out methane (CH₄) and ethane (C₂H₆) emissions from the EAF baghouse using EPA Reference Method 18 to arrive at applicable VOC levels for purposes of this permit. Semiannual stack testing for a pollutant is not required if the permittee elects to operate a CEMS for that pollutant at SN-01 and SN-02. Testing shall be conducted when the EAF is operated at or near its capacity based on the specific type of steel to be produced. A targeted capacity would be 250 tons/hour of steel. If the production rate is less than 250 tons/hour, the tested emission rates shall be scaled up to 250 ton/hour and compared to the permitted emission rates. If the production rate is above 250 tons/hour, the tested rate would be compared directly to the permitted emission rate. [Reg.19.702 and 40 C.F.R. § 52 Subpart E]”

Comment #15:

Permit conditions #23, 24 and 25 discuss what should be done for installation of pressure monitoring devices for SN-01 and SN-02. Permit condition #17 allows BRS the ability to either install a pressure monitoring device or conduct daily observation of shop operation. As such permit conditions #23, 24 and 25 should be adjusted to state that they only apply “if the pressure monitoring devices is selected by BRS” under Permit condition #17, for SN-01 and SN-02.

This change is required since permit condition #17 required BRS to select the monitoring option to be used for SN-01 and SN-02, respectively. The permit conditions as written appears to presuppose selection of the pressure monitoring devices.

Response to Comment #15:

Specific Conditions #23, #24, #25, and #26 have been updated to clarify the conditions only apply if the pressure device option is chosen in Specific Condition #17.

Comment #16:

Permit condition #42 as provided below should be updated to reflect additional natural gas combustion devices associated with the Proposed Steel Mill Project.

Permit condition #42 (as drafted below) should include reference to the following natural gas fired combustion devices:

- SN-34 Batch Annealing furnaces
- SN-35 Natural Gas Space Heaters – Cold Mill
- SN-43 Coil Coating Line Chemical Dryer
- SN-44 Coil Coating Line Primer Oven
- SN-45 Coil Coating Line Finish Oven
- SN-46 Coil Coating Line RTO

This change to specific condition 42 could be reflected as shown below in the added red text below:

42 Visible emissions may not exceed the limits specified in the following table of this permit as measured by EPA Reference Method 9. The permittee shall show compliance with this condition by combustion of natural gas only at SN-24, SN-27, SN-28, SN-34, SN-35, SN-37, SN-43, SN-44, SN-45 and SN-46, compliance with Specific Condition 43 Error! Reference source not found., and Plantwide Condition 5.

Source	Limit	Regulatory Citation
SN-22, SN-23a, SN-23b, SN-24, SN-25, SN-26, SN-27, SN-28, SN-29, SN-30, SN-31, SN-32, SN-33, SN-34, SN-35, SN-36, SN-37, SN-38, SN-39, SN-40, SN-41, SN-42, SN-43, SN-44, SN-45, SN-46	5%	Reg.19.901 <i>et seq.</i> and 40 C.F.R. § 52 Subpart E

This change is required to maintain consistency between the method of determining compliance with visible emission limits for the natural gas combustion devices identified in specific condition 42.

Response to Comment #16:

These sources are present in the draft permit but were not listed under the natural gas sources that may show compliance by combustion of only natural gas. Specific Condition #42 has been updated as requested to clarify this.

Comment #17:

Draft permit condition #72 states the following:

72 The permittee shall not operate the emergency generators SN-69 through SN-90, SN-135, and SN-136 in excess of 100 total hours each (emergency and non-emergency) per calendar year in order to demonstrate compliance with the annual emission rate limits. Emergency operation in excess of these hours may be allowable but shall be reported and will be evaluated in accordance with Reg.19.602 and other applicable regulations. [Reg.19.705, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 70.6]

BRS is requesting that the above permit condition be revised as provided below. The permit language provided below was extracted from the Operating Air Permit issued to BRS for the Existing Mill in Osceola, Arkansas:

72 The permittee shall not operate any single emergency engine, SN-69 through SN-90, SN-135 and SN-136 more than 100 hours, for maintenance and readiness testing, in any consecutive 12-month period. The permittee shall maintain records of the hours of operation of each generator each month. These records shall be updated by the fifteenth day of the month following the month that the records represent, kept on site, made available to Department personnel upon request and submitted in accordance with General Provision 7. [Reg.19.705, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, 40 C.F.R. § 70.6, and 40 C.F.R. § 60 Subpart III]”

This change is required to be consistent with current permit language contained in the Operating Air Permit issued to the BRS Existing Mill.

Response to Comment #17:

As a result of this comment, Specific Condition #72 has been updated as follows:

“The permittee shall not operate the emergency generators SN-69 through SN-90, SN-135, and SN-136 in excess of 100 total hours each, for maintenance and readiness testing, per calendar year in order to demonstrate compliance with the annual emission rate limits. Emergency operation in excess of these hours may be allowable but shall be reported and will be evaluated in accordance with Reg.19.602 and other applicable regulations. [Reg.19.705, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 70.6]”

Comment #18:

Revision to the BACT limits listed for SN-111 (Paved roadways), SN-112 (Unpaved roadways) and SN-134 (DRI Paved Road & Unpaved Fugitive Dust) under permit condition 89.

Due to the nature of these emission source, being intermittent, BRS is requesting that the emission rate limits in tons/year be removed as BACT and replaced with Best Work Practices – Development / Implementation of a Fugitive Dust Control Plan.

Response to Comment #18:

The BACT limits themselves refer to a permitted limit that is determined on the basis of the control technology. Due to the intermittent nature of the emissions from roadways sources, the yearly emissions were chosen as a good representative limit rather than one of a shorter term as seen in other sources at the facility. The requested change is a description of the control technology and would remove any numerical limit from the BACT evaluation. There were no changes made to Specific Condition #89 as a result of this comment.

Comment #19:

Remove reference to “Use of Water Sprays and Wetting Agents and Vehicle Restrictions” from SN-111, SN-112, and SN-134 under permit condition 89.

Since BRS is required to develop and implement a Fugitive Dust Control plan, that plan will outline the specific techniques to be utilized by BRS to control fugitive dust. As such it is not required to specifically list these items with the above referenced permit condition.

Response to Comment #19:

References to the control technology in Specific Condition #89 and the Prevention of Significant Deterioration section of the permit have been updated for SN-111, SN-112, and SN-134 to read “Development and Implementation of Fugitive Dust Control Plan.”

Comment #20:

In permit condition 90, add the specification that “Implementation of the fugitive dust control plan is a demonstration of compliance with the referenced BACT limits.” Inclusion of the language noted above is required to clearly define the method of compliance.

Response to Comment #20:

Specific Condition #90 has been updated as requested. Further, the last sentence of Specific Condition #89 has been updated to read “Compliance with these emission limits shall be demonstrated by compliance with Specific Condition #**Error! Reference source not found.**”

Comment #21:

The SO₂ emission rate for SN-124 (Furnace Dedusting) in the emission summary and permit condition 92 should be corrected from 0.9 to 1.1 tons/year. This change is required to be consistent with the engineering estimate provided by BRS in the emission estimation spreadsheet in the September 2021 application.

Response to Comment #21:

This emission rate has been updated as requested to match the information submitted by the facility.

Comment #22:

The NO_x rate for SN-16 through SN-21 in the BACT Summary and permit condition 35 should be revised from 0.095 to 0.097 lb/MMBtu. This change is required so that the lbs/MMBtu rates match the rates provided by BRS in the initial air permit application submitted in September 2021 and the Revised Proposed Steel Mill BACT demonstration submitted to AEEDEQ, dated October 11, 2021.

Response to Comment #22:

This BACT limit for SN-16 through SN-21 has been updated as requested to match the information submitted by the facility.

Comment #23:

Request that the NO_x rate for SN-123 in the BACT Summary and permit condition 92 be revised to 388.3 tons/year. The permit referenced a NO_x rate of 3883.3 tons/year. This appears to be a typographical error. The NO_x rate of 388.3 tons/year was provided by BRS in the September 2021 application and the Revised Proposed Steel Mill BACT demonstration submitted to AEEDEQ, dated October 11, 2021.

Response to Comment #23:

The NO_x BACT limit has been updated for SN-123 to match the emission rate from the unit. This BACT limit is now 383.3 tons/year.

Comment #24:

The PM, PM₁₀ and PM_{2.5} rates for SN-39 in the Emission Summary and permit condition 39 should be revised from 1.3 to 1.2 tons/year. This change is required so that the ton/year rates match the rates provided by BRS in the initial air permit application submitted in September 2021 and the Revised Proposed Steel Mill BACT demonstration submitted to AEEDEQ, dated October 11, 2021.

Response to Comment #24:

The yearly emission rates for SN-39 have been updated as requested.

Comment #25:

Draft permit plantwide condition #8 in Section VI states the following:

- 8 The permittee must build the stacks for the following sources to the height listed. These stack heights are those supplied by the facility for the initial permit application. [Reg.19.303 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-31

Source	Stack Height (ft)
SN-01, SN-02, SN-36	240
SN-03, SN-04	165
SN-22, SN-24, SN-27, SN-28, SN-37, SN-40, SN-41	120
SN-23, SN-25	105
SN-29, SN-30, SN-38	140
SN-31, SN-32, SN-39	145
SN-33	250
SN-42, SN-43, SN-44, SN-45, SN-46	164
SN-118, SN-119, SN-120, SN-121, SN-128, SN-129	180
SN-122, SN-123, SN-124, SN-125, SN-126, SN-127	213
SN-130	66

BRS is requesting that the above permit condition be revised as provided below.

- 8 The permittee must build the stacks for the following sources to the height listed. These stack heights are those supplied by the facility for the initial permit application. [Reg.19.303 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

Source	Stack Height (ft)
SN-01, SN-02	240
SN-03, SN-04	165
SN-22	270
SN-24, SN-27, SN-28, SN-37	120
SN-23, SN-25	105
SN-29, SN-30, SN-38	140
SN-31, SN-32, SN-39	145
SN-40, SN41	121
SN-33	250
SN-42, SN-43, SN-44, SN-45, SN-46	164
SN-118, SN-119, SN-120, SN-121, SN-128, SN-129	180
SN-122, SN-123, SN-124, SN-125, SN-126, SN-127	213

This change is required to be consistent with the stack heights proposed by BRS and reflected in the air quality impact assessment that was submitted to AEEDEQ in the December 17, 2021 updated modeling report. Also, the reference to SN-130 was removed because it is not a stack.

Response to Comment #25:

Plantwide Condition #8 has been updated as requested.

Comment #26:

Draft plantwide permit condition #9 in Section VI states the following:

- 9 The permittee shall install, operate, and maintain air quality monitors for PM₁₀, PM_{2.5}, and NO₂. The permittee shall submit a monitoring protocol to the Department within 180 days of the anticipated startup date of the facility. The Department must approve of the monitoring protocol prior to installation of the monitors. The monitors shall be installed and operating within 180 days of the startup of the EAFs. [Reg.19.901 et seq. and 40 C.F.R. art 52, Subpart E]

BRS is requesting that the above permit condition be revised as provided below.

- 9 The permittee shall install, operate, and maintain air quality monitors for PM₁₀, PM_{2.5}, and NO₂ at the stationary source. Monitors shall be installed and operating at this stationary source within 180 days of the startup of the EAFs. This condition is satisfied by operation of the existing monitor at the existing BRS mill located in Osceola, Arkansas. In the event BRS ceases operation of such on-site air quality monitors, the permittee shall submit a monitoring protocol to the Department within 180 days after ceasing operation of the on-site air quality monitor. The Department must approve of the monitoring protocol prior to installation of the new monitors. [Reg.19.901 et seq. and 40 C.F.R. Part 52, Subpart E]

This change is required to support the fact that BRS currently operates and maintains air quality monitors at the existing BRS mill located in Osceola, Arkansas. Especially since the two facilities constitute a single source for Clean Air Act purposes, there is no need for additional on-site air quality monitors. Furthermore, these monitors are not technically “ambient air” monitors, since they are located on-site, and air within the property boundary of a source is excluded from the definition of ambient air under relevant EPA guidance.

Response to Comment #26:

Plantwide Condition #9 has been updated as follows:

9. The permittee shall install, operate, and maintain air quality monitors for PM₁₀, PM_{2.5}, and NO₂ at the stationary source. Monitors shall be installed and operating at this stationary source within 180 days of the startup of the EAFs. This condition is satisfied by operation of the existing monitor at the Existing Mill (Permit #2305-AOP-R7). In the event BRS ceases operation of such on-site air quality monitor, the permittee shall submit a monitoring protocol to the Division within 30 days after ceasing operation of the on-site air quality monitor at the Existing Mill. The Division must approve of the monitoring

protocol prior to installation of the new monitors. [Reg.19.901 et seq. and 40 C.F.R. Part 52, Subpart E]

Comment #27:

The Draft Operating Air Permit did not provide a Permit History in Section III. BRS has provided the permit history from Permit #2305-AOP-R7 that should be included in Section III of the Operating Air Permit.

This change is required to support the Facility being a major modification to the Existing Mill. The Facility and the Existing Mill are considered one major stationary source for regulatory applicability purposes.

Response to Comment #27:

The permit history has been updated to read as follows:

“This is the initial permit for the facility. The sources included in this permit and those of Permit #2305-AOP-R7 (AFIN 47-00991) are considered one stationary source under definition of the Clean Air Act. See the Permit History section of Permit #2305-AOP-R7 for all revisions to this stationary source.”

Comment #28:

BRS requests that the limit to HCL specified in the following Draft Operating Air Permit provision be removed since it would be captured in the summary of Emission Rates for the Single and total HAPs.

The change is being proposed to ensure the reference to HAPs is consistent throughout the Operating Air Permit.

Response to Comment #28:

HCl is considered a non-VOC HAP. As outlined in the footer of the Emission Summary Section, “HAPs included in the VOC totals. Other HAPs are not included in any other totals unless specifically stated.” Changing HCl to be included in the Single HAP and Total HAP limit would imply those emissions are included in the VOC totals when they are not. The sources which are permitted to emit HCl have no other HAP or VOC emissions, so these emissions are not currently accounted for in the Single HAP and Total HAP limits. There were no changes made to the permit as a result of this comment.

Comment #29:

BRS submits the following additional analysis in support of the Draft Operating Permit’s CO₂e BACT selection, specifically, the elimination of Carbon Capture and Sequestration (CCS) from consideration as BACT for CO₂e associated with the Facility.

CCS is discussed on page 4-14 et seq of the Revised Proposed Steel Mill BACT demonstration submitted to AEEDEQ, dated October 11, 2021. The primary outcome of that discussion on CCS is that it is not commercially available and used in actual practice for the primary sources of CO₂ from the Facility, specifically the EAFs (SN-01 and SN-02) and the Reformer from the proposed DRI process (SN-123). There are several fuel combustion (i.e., natural gas and diesel fuel) devices that also have the potential to generate emissions of CO₂ in amounts significantly less than the EAFs and Reformer. These devices would be located throughout the layout of the steel mill site. The two EAFs and Reformer processes are located at specific locations.

Guidance from EPA, titled “PSD and Title V Permitting Guidance for Greenhouse Gasses” (Document No. EPA457/B-II-001) (March 2011), hereafter “EPA 2011 Guidance,” specifically acknowledges that CCS may be eliminated in BACT step 2 as technically infeasible for a variety of reasons, including if:

- 1 the three components of CCS (capture and/or compression, transport, and storage) “working together are deemed technically infeasible for the proposed source, taking into account the integration of the CCS components with the base facility and site-specific considerations (e.g., space for CO₂ capture equipment at an existing facility, right-of-ways to build a pipeline or access to an existing pipeline, access to suitable geologic reservoirs for sequestration, or other storage options).” Or
- 2 “the temperature, pressure, pollutant concentration, or volume of the gas stream to be controlled, may differ so significantly from previous applications that it is uncertain the control device will work in the situation currently undergoing review.”

As explained below, both of the above reasons support eliminating CCS under BACT step 2 in this case.

With respect to the integration of CCS components with the proposed Facility (specific to the EAFs and Reformer), even if capture and compression were technically feasible, there is no existing infrastructure anywhere near the Facility to store, transport, or otherwise use CO₂. Based on the most recent official review of CO₂ pipeline infrastructure in the United States, it appears that the closest existing pipeline (the Delta pipeline near Tinsley MS, owned and operated by a third party) is over 200 miles south from the proposed Facility.

The fact that the nearest pipeline is over 200 miles away, by itself justifies concluding that CCS is infeasible at the site given the prohibitive logistics that would be associated with installation of a 200+ mile compressed CO₂ pipeline, including rights of way and permitting, neither of which can be guaranteed for such a distance, and the years of development required for the pipeline alone, which would jeopardize the viability of the Facility. In addition, even in the unlikely event that it were possible to accomplish a connection to that closest available CO₂ pipeline infrastructure, requiring use of a third party’s infrastructure as a condition of permit compliance would be problematic because a permit requirement that requires BRS to use a specific pipeline creates a potentially monopolistic situation, as the third party pipeline owner/operator could require arbitrary economic compensation in order for BRS to remain compliant with the permit.

Another important consideration is the characteristics of the CO₂ stream to be controlled. As noted in the October 11, 2021 updated BACT demonstration, metallurgical processes, including the EAFs and the DRI Reformer at the Facility, have relatively dilute CO₂ streams (meaning the exhaust gas streams contain other constituents in addition to CO₂) as compared to power plants which have exhaust gas streams that are higher in the presence of pure CO₂ and contain lesser amounts of other constituents. This matters because the quality of CO₂ in the exhaust gas streams (higher in pure CO₂) is key to defining the ability to implement CCS. Even if the total volume of CO₂ emissions from a power plant and the Facility are similar, CCS is only demonstrated on CO₂ streams of a far higher concentration/purity than those associated with the proposed EAF and DRI processes.

Accordingly, any demonstration of CCS in the context of other operations such as powerplants does not constitute a demonstration that CCS is technically feasible here, because the “pollutant concentration . . . differ[s] so significantly from previous applications [e.g., powerplants] that it is uncertain the control device will work in the situation currently undergoing review [steel mills].” (EPA 2011 Guidance).

This conclusion is supported by the fact that, to BRS’s knowledge (including review of the RACT/BACT/LAER Clearinghouse), no DRI (utilizing a Reformer) or steelmaking facility (incorporating EAFs) located in the United States, has ever proposed, been required to install, or successfully demonstrated in practice CCS technology.

Provided below is a summary of recent permit actions and the resultant outcome from evaluating BACT for GHG emission related to two permitted DRI facilities (i.e., IronUnits and Voestalpine) and a steelmaking facility (i.e., AM/NS), all supporting a finding that CCS is not technically feasible, and not cost feasible.

- IronUnits LLC, Toledo, Ohio HBR facility (Permit Number P0126975, dated 12/10/2019): As part of the final permit issued by the Ohio EPA for the IronUnits LLC, Toledo HBR facility, the use of CCS was not identified as a commercially available control technology for reducing potential GHG emissions from a DRI Reformer process. The outcome of the PSD evaluations resulted in the following limit for GHG emissions for the Reformer:
 - Carbon dioxide equivalent (CO₂e) emission from the reformer exhaust stack shall not exceed 1,554,047 tons per rolling, 12-month period.
 - BACT for the Reformer process was determined to be the nature of the operation without add-on controls, specifically: “Use of gaseous fuels, energy integrated design, and good combustion practices through proper operation and maintenance of the unit.”

- Voestalpine DRI facility, TX (Permit Number: PSD-TX-1344-GHG, dated April 24, 2014) The Voestalpine DRI facility obtained a PSD GHG permit from EPA Region 6. In the Statement of Basis, EPA Region 6 noted that:

- Voestalpine and EPA identified three prior DRI facilities that had evaluated BACT for CO₂ from a DRI process, and none had selected add on controls.
 - At BACT step 2, EPA acknowledged that, as of 2014, CCS was “not proven as technically feasible” because “Carbon capture and storage has not been demonstrated in practice for any commercial scale DRI facility.”
 - EPA acknowledged without dispute Voestalpine’s representation that “It is also possible to apply CCS to the main reformer firebox flue gas steam (92% of the emissions at the site), but that stream, as the products of combustion of natural gas, has a CO₂ concentration of approximately 5%, too low to practically capture by CCS.”
 - Voestalpine performed a cost analysis based on the Report of the Interagency Task Force on Carbon Capture and the fact that the nearest available pipeline infrastructure was 220 miles away, calculating a cost of \$339.21/ton of CO₂ controlled, and a total cost in excess of \$173 million. EPA concurred that this was a sufficiently high cost to eliminate from BACT consideration, and stated it was rejecting CCS as BACT for the site due to economic costs, “and the potential for increased energy requirements and the resultant criteria emission increases.”
- AM/NS Calvert, AL (Revised PSD Application filed Dec. 30, 2020) (ArcelorMittal and Nippon Steel Corp joint venture producing flat-rolled carbon steel products.). The BACT analysis:
 - Identified a single facility in the world which had installed CCS technology at a steelmaking facility (Al Reyadah, which in 2016 started operation of a greenfield CO₂ Compression Facility and other equipment installed at the Emirates Steel facility in Abu Dhabi, UAE, to support enhanced oil recovery at nearby oilfields).⁵ AM/NS noted that CCS was only technically feasible at that specific facility because the DRI process at that particular facility had a pure (i.e. 98%+) emission stream of CO₂ that was previously vented to the atmosphere and which provided a sufficiently concentrated CO₂ stream to support CCS.
 - AM/NS also noted that even if CCS was available, storage was not technically feasible due to lack of any CO₂ storage project being demonstrated beyond a pilot scale (notably, the Abu Dhabi CCS operations used the CO₂ for advanced oil recovery in nearby oilfields, not in permanent CO₂ sequestration). AM/NS noted that pilot scale testing cannot be considered an ‘available’ technology.
 - Finally, AM/NS performed an economic evaluation, concluding CCS would cost \$350,923,560 of capital expenditures, and an additional annual spend of \$47,217,897 between O&M and capital recovery.
 - Ultimately AM/NS selected BACT for GHGs of “energy efficiency measures” with no add-on controls.

Based on the following reasons, the use of CCS for the GHG emission related to CO₂e from the Facility has been eliminated from consideration under BACT:

- Installation and operation of CCS has not been demonstrated as technically feasible by any similar operation and has never been set as BACT for any facility in the iron or steelmaking industry.
- Currently there is no infrastructure available at the Facility to allow BRS to capture its CO₂ gas streams and pipe that gas stream to any nearby facility for further processing, such as a beverage plant or enhanced oil recovery (EOR) facility, or to store its CO₂ gas stream for future use in the event a EOR facility or beverage plant would be installed in the vicinity of the Facility site.
- CO₂ produced at the Facility would require significant enhancements to improve its quality prior to being used by another source to produce a product, if technically feasible at all.
- CCS capture, compression, and transport equipment would increase energy requirements and thus resultant criteria emission increases.
- CCS is economically infeasible for the Facility.

Please note that in the September 20, 2021 / October 11, 2021 BACT demonstrations, BRS did not include a cost analysis in support of removing CCS as a cost-effective control alternative under BACT step 4 because:

1. CCS should already be eliminated as technically infeasible under BACT step 2;
2. U.S. EPA has not provided any guidance or established thresholds on what cost, expressed as a dollar per ton would be considered cost excessive; and
3. No project in the steelmaking industry has ever found CCS to be cost justified, and every project and permitting authority to analyze its economic viability in the steelmaking industry has found it to be economically prohibitive.

However, even a preliminary look at some of the costs involved justifies also eliminating CCS from consideration as BACT for GHGs on the alternative ground that it is not cost justified. For example, viewing the transportation cost alone, Denbury's 10-K filing dated March 1, 2011 represents that it took four years and expenditure of approximately \$884 million to plan, develop, and construct the 325 mile Green Pipeline. Using these real world costs from the developer of the closest available CCS transport and use infrastructure to the proposed Facility:

- $(\$884 \text{ million}) / (325 \text{ miles}) = \$2.72 \text{ million/mile.}$
- $(\$2.72 \text{ million/mile}) \times (200 \text{ miles}) = \$544 \text{ million for a pipeline to the Facility alone (excluding recurring O\&M costs).}$

The estimated cost for the pipeline (as estimated above) of \$544 million is well above or reasonably equivalent to other cost estimates that the EPA has previously accepted as demonstrating CCS to be not cost justified. Furthermore, a delay of several years just to install the pipeline as a precondition of operating the proposed Facility could jeopardize the construction and operation of the proposed BRS Facility.

For the reasons noted above, BRS supports AEEDEQ setting BACT for CO₂e for the Facility as currently proposed in the Draft Operating Permit and consistent with the Revised Proposed Steel Mill BACT demonstration submitted to AEEDEQ, dated October 11, 2021.

Response to Comment #29:

The additional information related to the CO₂e BACT is noted. There were no changes made to the permit as a result of this comment.

Comment #30:

Section 2 of the Draft Statement of Basis “Applicant” the reference to the location of the Proposed Steel Mill Project should be 1000 East County Road 860. This change is required to ensure that the content of the Operating Permit agrees with the content of the Statement of Basis.

Response to Comment #30:

The Statement of Basis has been updated as requested.

Comment #31:

Section 6 of the Draft Statement of Basis “Reviewers Notes” the reference to the location of the Proposed Steel Mill Project should be 1000 East County Road 860. Also, the Facility is referenced as a ”new source.” The Proposed Steel Mill Project is a major modification to the existing BRS Steel Mill located in Osceola, Arkansas. BRS is request that this section be updated to reflect the change in address and that the project is a major modification, consistent with the wording proposed in BRS Comment 2 to the Draft Operating Air Permit .

This change is required to ensure that the content of the Operating Permit agree with the content of the Statement of Basis.

Response to Comment #31:

The reviewer’s notes have been updated to match the changes made to the Summary of Permit Activity.

Comment #32:

Section 14 of the Draft Statement of Basis “Ambient Air Evaluation” the reference to the highest concentration for PM₁₀ 24-hour averaging time was 110.11 ug/m³. The predicted concentration provided by BRS in the updated modeling report, dated December 17, 2021 was 99.2 ug/m³, which represents 66.1% of the NAAQS.

This difference is being provided to ensure the Statement of Basis matched up with the technical information provided by BRS.

Response to Comment #32:

The Ambient Air Evaluation section has been updated as requested.

Comment #33:

Section 19 of the Draft Statement of Basis “Opacity” makes reference to opacity limits imposed on individual emission units. The appropriate limits should be updated to reflect BRS Comment above to the Draft Operating Air Permit.

This change is required to ensure that the content of the Operating Permit agrees with the content of the Statement of Basis.

Response to Comment #33:

The Opacity section of the Statement of Basis has been updated to match the changes made to the permit in Response to Comment #10.



DIVISION OF ENVIRONMENTAL QUALITY

OPERATING AIR PERMIT

PERMIT NUMBER: 2445-AOP-R0

IS ISSUED TO:

Big River Steel LLC
1000 East County Road 860
Osceola, AR 72370-0248
Mississippi County
AFIN: 47-01073

PURSUANT TO THE REGULATIONS OF THE ARKANSAS OPERATING AIR PERMIT PROGRAM, REGULATION 26: THIS PERMIT AUTHORIZES THE ABOVE REFERENCED PERMITTEE TO INSTALL, OPERATE, AND MAINTAIN THE EQUIPMENT AND EMISSION UNITS DESCRIBED IN THE PERMIT APPLICATION AND ON THE FOLLOWING PAGES. THIS PERMIT IS VALID BETWEEN:

January 31, 2022

AND

January 30, 2027

THE PERMITTEE IS SUBJECT TO ALL LIMITS AND CONDITIONS CONTAINED HEREIN.

Signed:

William K. Montgomery
Associate Director, Office of Air Quality
Division of Environmental Quality

January 31, 2022

Date

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Appendix A - 40 CFR Part 60, Subpart Dc - *Standards of Performance for Small Industrial-Commercial-Institutional Steam Generating Units*

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Appendix C - 40 CFR Part 60, Subpart TT – *Standards of Performance for Metal Coil Surface Coating*

Appendix D - 40 CFR Part 60 Subpart IIII, *Standards of Performance for Stationary Compression Ignition Internal Combustion Engines*

Appendix E - 40 CFR Part 63 Subpart ZZZZ, *National Emission Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustions Engines*

Appendix F - 40 CFR Part 63 Subpart DDDDD, *National Emission Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters*

Appendix G - 40 CFR Part 63 Subpart SSSS, *National Emission Standards for Hazardous Air Pollutants: Surface Coating of Metal Coil*

Appendix H - 40 CFR Part 63 Subpart CCC, *National Emission Standards for Hazardous Air Pollutants for Steel Pickling – HCl Process Facilities and Hydrochloric Acid Regeneration Plants*

Appendix I - Case by Case Analysis for the Electric Arc Furnaces

Big River Steel LLC
Permit #: 2445-AOP-R0
AFIN: 47-01073

Appendix J - 40 CFR Part 63 Subpart B, Requirements for Control Technology Determinations for Major Sources in Accordance With Clean Air Act Sections, Sections 112(g) and 112(j)

Big River Steel LLC
Permit #: 2445-AOP-R0
AFIN: 47-01073

List of Acronyms and Abbreviations

Ark. Code Ann.	Arkansas Code Annotated
AFIN	Arkansas DEQ Facility Identification Number
C.F.R.	Code of Federal Regulations
CO	Carbon Monoxide
COMS	Continuous Opacity Monitoring System
HAP	Hazardous Air Pollutant
Hp	Horsepower
lb/hr	Pound Per Hour
NESHAP	National Emission Standards (for) Hazardous Air Pollutants
MVAC	Motor Vehicle Air Conditioner
No.	Number
NO _x	Nitrogen Oxide
NSPS	New Source Performance Standards
PM	Particulate Matter
PM ₁₀	Particulate Matter Equal To Or Smaller Than Ten Microns
PM _{2.5}	Particulate Matter Equal To Or Smaller Than 2.5 Microns
SNAP	Significant New Alternatives Program (SNAP)
SO ₂	Sulfur Dioxide
SSM	Startup, Shutdown, and Malfunction Plan
Tpy	Tons Per Year
UTM	Universal Transverse Mercator
VOC	Volatile Organic Compound

Big River Steel LLC
Permit #: 2445-AOP-R0
AFIN: 47-01073

SECTION I: FACILITY INFORMATION

PERMITTEE: Big River Steel LLC

AFIN: 47-01073

PERMIT NUMBER: 2445-AOP-R0

FACILITY ADDRESS: 1000 East County Road 860
Osceola, AR 72370-0248

MAILING ADDRESS: P.O. Box 707
Osceola, AR 72370

COUNTY: Mississippi County

CONTACT NAME: Dean Caldwell

CONTACT POSITION: Director Environmental

TELEPHONE NUMBER: (731) 234-4204

REVIEWING ENGINEER: Jesse Smith

UTM North South (Y): Zone 16: 3945486.420 m

UTM East West (X): Zone 16: 233260.820 m

SECTION II: INTRODUCTION

Summary of Permit Activity

Big River Steel, LLC (BRS) is proposing to construct and operate a steel mill located at 1000 East County Road 860 in Osceola, AR (Facility). This new steel mill will be contiguous to an existing BRS steel mill, AFIN: 47-00991 (Existing Mill), and both are under common control of BRS or its parent company, and thus this new facility and the Existing Mill constitute a single stationary source under the Clean Air Act, and the Facility constitutes a major modification to the Existing Mill. At the request of BRS and for administrative convenience, this permit is being issued specific to the equipment located at the new Facility. This permit will include all the sources at the Facility. The Facility required a Prevention of Significant Deterioration (PSD) review to ensure the new emission sources associated with this major modification will not cause a significant deterioration of the local ambient air quality. PSD review was performed for NO_x, CO, PM, PM₁₀, PM_{2.5}, SO₂, VOC, lead, and greenhouse gasses from the Facility.

Process Description

The steel mill project consists of five key process areas or supporting activities that will have equipment or operations that have the potential to emit emissions of regulated air pollutants. The five key process areas or supporting activities are:

- Direct Reduction Iron (DRI) process that takes iron oxide in a solid form and processes that iron oxide so that it meets the quality requirements to be used as a raw material (liquid or solid form) to be used in the EAF steel making process performed in the Melt Shop;
- Melt Shop that contains process equipment and operations that will be used to process scrap and supporting raw materials to produce liquid steel. Two Electric Arc Furnaces (EAFs) are utilized to produce the liquid steel;
- Casting Process (CP) that processes the liquid steel in a caster to produce steel in the form of coils;
- Cold Mill that will contain several process lines that are used to pickle, galvanize, and coat the steel; and
- Miscellaneous support activities, which include material handling and storage activities, emergency generators, emergency backup water pumps, scrap and slag processing areas, and process water cooling towers.

The Facility is capable of producing a variety of rolled steel products and utilizes two EAFs each having a maximum design production output volume of approximately 2,050,000 short tons per year. Specifics on each operation are found in the Specific Condition section of the permit.

Prevention of Significant Deterioration

The Facility is classified as a major modification to BRS's nearby Existing Mill under Prevention of Significant Deterioration (PSD) regulations. Due to the proposed emission rates, PSD review was performed for emissions of NO_x, CO, PM, PM₁₀, PM_{2.5}, SO₂, VOC, lead, and greenhouse gasses from the Facility.

An applicant for a Prevention of Significant Deterioration (PSD) permit is required to conduct an air quality analysis of the ambient impacts associated with the construction and operation of the proposed new source or modification. The primary purpose of the air quality analysis is to demonstrate that new emissions emitted from a major stationary source, in conjunction with other applicable emissions from existing sources (including secondary emissions from growth associated with the new project), will not cause or contribute to a violation of any applicable National Ambient Air Quality Standard (NAAQS) or PSD increment.

PSD modeling is performed in two stages: the significance analysis and the full impact analysis. The significance analysis considers the net emissions change associated with PSD affected emissions units to determine if the increased emissions will have a significant impact upon the surrounding area. If the results of the significance analysis are below the corresponding Modeling Significance Levels, the full impact analysis is not required. A summary of the results of the significance analysis is in the table below.

Pollutant	Averaging Period	Modeled Concentration (µg/m ³)	Significance Level (µg/m ³)
CO	1 – hour	460.69	2,000
	8 – hour	180.56	500
PM ₁₀	24 – hour	82.87	5
	Annual	8.18	1.0
PM _{2.5}	24 – hour	15.84	1.2
	Annual	3.15	0.3
SO ₂	1 – Hour	17.29	7.8
	3 – Hour	15.99	25
	24 – Hour	7.32	5
	Annual	0.29	1.0
NO ₂	1 – hour	96.15	7.52
	Annual	6.04	1.0

Based on the above modeled concentrations, a full impact analysis was required for emissions of PM_{2.5}, PM₁₀, SO₂, and NO₂ from the Facility. The full impact analysis modeling must show that the emissions from the Facility and surrounding existing sources will not cause or contribute to a violation of any applicable National Ambient Air Quality Standard (NAAQS) or PSD Class II increment.

Initial modeling from the Facility showed a possible exceedance in the PM₁₀ 24 hour Class II increment standard. The Facility performed dense grid (100 m receptor spacing) modeling around this possible exceedance to determine the maximum impact and has submitted the following conclusions:

The maximum PM₁₀ impact is 15.8 µg/m³ based on removal of the Bunge Grain Elevator emission sources in the AERMOD model run. Please note that the Bunge Grain Elevator is a unique emission source and does not operate on a 24-hour and 365-day basis. The Grain Elevator's primary operator time of year is during the crop harvesting time. As such very conservative assumption regarding the Grain Elevator's operation are included in the Class II PM₁₀ increment analysis. The PSD Class II Increment is 30 ug./m³.

The maximum PM₁₀ impact from the Bunge emission sources is 57.50 µg/m³, which is above the PSD Class II increment of 30 µg/m³. and represents more than 88% of the maximum overall predicted concentration of 65.1 µg/m³.

The maximum PM₁₀ impact from the BRS existing mill and the Facility is 14.1 ug/m³, which is also well below the PSD Class II increment of 30 µg/m³.

The above analysis shows that the Bunge emission source's predicted impacts appear to be overstated in the modeling analysis. Further refinement of the emission sources and taking into account Bunge's property boundary would reduce these impact significantly.

The above analysis also shows that all the other sources being evaluated result in a predicted impact of 11.6 µg/m³, which is well below the Class II increment of 30 µg/m³. That predicted concentration represents around 40% consumption of the Class II increment for the PM₁₀ 24-hour averaging period.

In conclusion, the predicted impacts from the Facility do not appear to significantly contribute to the maximum predicted Class II PM₁₀ 24-hour average concentrations. As such, the Facility does not appear to restrict or prohibit future industrial growth in the area for non-Facility source and does not significantly deteriorate air quality

The following table shows the results of the PSD Class II increment modeling for the Facility and reflects the discussion provided above.

Pollutant	Averaging Period	Maximum Predicted Increment Consumption (µg/m ³)	PSD Class II Increment (µg/m ³)	Percent of Class II Increment (%)
PM ₁₀	24 – hour	29.17	30	97.3%
	Annual	5.86	17	34.5%
PM _{2.5}	24 – hour	8.92	9	99.2%
	Annual	2.31	4	57.8%
SO ₂	24 – hour	10.33	91	11.4%

Pollutant	Averaging Period	Maximum Predicted Increment Consumption ($\mu\text{g}/\text{m}^3$)	PSD Class II Increment ($\mu\text{g}/\text{m}^3$)	Percent of Class II Increment (%)
NO ₂	Annual	10.82	25	43.3%

Arkansas Regulation 19 requires that if the issuance of a permit for any major stationary source or any major modification would result in the consumption of more than fifty percent of the available annual increment or eighty percent of any short term increment, the person applying for such a permit shall submit to the Division an assessment of the effects that the proposed consumption would have upon the industrial and economic development within the area of the proposed source and the alternatives to such consumption including alternate siting of the proposed source. To address this requirement the following was submitted by BRS in support of the Facility.

As stated in Arkansas Regulation 19.904, subsection (c) (1), where air quality impact analysis required under this subpart indicated that the issuance of a permit for any major stationary source or for any major modification would result in the consumption of more than fifty (50%) of any available annual increment or eighty percent (80%) of any short term increment, the person applying for such a permit shall submit to the Division an assessment of the following factors:

- (a) Effect that the proposed consumption would have upon the industrial and economic development within the area of the proposed sources; and
- (b) Alternatives to such consumption, including alternative siting of the proposed source or portion thereof.

The Facility will have potential emission of PM_{2.5} / PM₁₀ in and by itself that were predicted to be above 80% of the Class II increment (24-hour averaging period), but will be below the Class II Increment. Combined impacts from BRS and other increment consuming sources have shown predicted concentrations to be below the Class II increments for PM_{2.5} and PM₁₀, respectively. The specific point of maximum predicted concentrations reside within close proximity of the existing BRS Mill or in the case of the Facility along the property boundary or within a relative short distance of that boundary. Since the predicted concentration is representative of time and space, future growth in the area should not be limited. It is highly unlikely that future growth will take place near or in close proximity to the Facility's property boundary or the existing BRS Mill's property boundary. For any future project going through PSD review, a separate analysis will be required as part of that application process and primary point of increment consumption will also be based on time and space and will most likely occur in the immediate vicinity of that source as well.

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BRS has selected the location of the Facility based on the availability of land, close proximity to major road ways, as well as access to a major river. The Facility site has been zoned industrial and has access to infrastructure to support the steel mill operations being proposed. BRS, as part of the property selection process has evaluated this site and other sites as well. This site meets the criteria for this Facility and ranked the highest in terms of mill site selection. BRS does not have the ability to select an alternative site, since an alternative site would not meet the site qualifications for a project of this nature.

Also as demonstrated to the AEEDEQ, the Facility will meet the NAAQS established by EPA and as such will not be harmful to public health or the environment.

The full impact modeling analysis also requires modeling to show that the emissions from the Facility and surrounding existing sources will not cause or contribute to a violation of any applicable National Ambient Air Quality Standard (NAAQS).

The background concentration was determined by use of representative ambient air monitors in the area. BRS has a monitor onsite which is being used for NO₂, PM₁₀ and PM_{2.5} background concentrations. The SO₂ background monitor is located in Little Rock, AR (Pike Ave At River Road, ID 51-19-0007). This monitor is in an area with higher population density and more intensive land use than the area surrounding the Project. As such, the concentrations recorded here are expected to be conservative with respect to the ambient air in the vicinity of the Facility. The North Little Rock monitor exceeded 97 percent data completeness in each of the 20 quarterly periods considered in the background record. The North Little Rock data was chosen to develop the background SO₂ concentrations.

A summary of the results of the NAAQS analysis is in the table below.

Pollutant	Averaging Period	Maximum Modeled Impact (µg/m ³)	Background Concentration (µg/m ³)	Total Impact (µg/m ³)	NAAQS (µg/m ³)
PM ₁₀	24 – hour	57.30	41.90	99.20	150
PM _{2.5}	24 – hour	18.4	11.83	30.58	35
	Annual	3.8	7.69	11.50	12
SO ₂	1 – Hour	45.8	8.00	53.76	196
NO ₂	1 - Hour	134.6	43.11	177.72	188
	Annual	10.3	6.32	16.66	100
Lead	3 – month	0.00154	0.01	0.01154	0.15

A dense grid (100 m receptor spacing) modeling analysis was performed on the maximum predicted 1-hour NO₂ modeled concentration since the predicted concentration was in the vicinity of an existing non-BRS emission source.. The following finding was submitted by BRS:

As shown in Table 5-9 the maximum 1-hour impact (134.6 µg/m³) was located at a receptor in the vicinity of an off-site Non-BRS stationary source. As such, an updated NO₂ NAAQS analysis for the Facility, to determine the maximum impact based on 100-

meter spaced receptors was performed. A dense grid of receptors was created, with a spacing of 100-meters were located around that receptor point, and a separate model run was performed. The predicted concentrations increased from 134.6 $\mu\text{g}/\text{m}^3$ to 660.4 $\mu\text{g}/\text{m}^3$. The maximum predicted impact receptors were then evaluated using the MaxDcont output from AERMOD and it showed that the Facility does not have a significant impact on any receptor predicted to be above the 1-hour NO_2 NAAQS. The maximum predicted impacts from the Proposed Steel Mill Project were well below the significant impact concentration, for NO_2 , for a 1-hour averaging period, which is 7.5 $\mu\text{g}/\text{m}^3$.

Because of this minimal contribution, the Facility does not cause or contribute to predicted impacts above the 1-hour NO_2 NAAQS. The maximum predicted impacts predicted at other receptors point within the SIL area are below the initial concentration of 134.6 $\mu\text{g}/\text{m}^3$, as such when combined with the background concentration of 43.11 $\mu\text{g}/\text{m}^3$, resulted in a combined predicted impact below the 1-hour NO_2 NAAQS of 188 $\mu\text{g}/\text{m}^3$.

Additional Impact Review

An applicant for a Prevention of Significant Deterioration (PSD) permit must prepare additional impact analyses for each pollutant subject to the regulation under the Clean Air Act Amendments. Three areas constitute the Additional Impact Review: a growth analysis, a soil and vegetation analysis, and a visibility analysis.

Growth Analysis

The Growth Analysis estimates the impact of atmospheric emissions that will be generated by the projected growth from industrial, commercial, and residential growth associated with the project. The only increase in emissions from associated growth results from the increase in workers traveling to and from work. Emissions from this are assumed to be insignificant and would have a minor impact (if any) to the area.

Vegetation Analysis

A PSD applicant must also conduct a soil and vegetation air pollution impact analysis based on an inventory of the soils and vegetation types found in the impact area. For most types of soils and vegetation ambient concentrations of criteria pollutants below the secondary NAAQS will not result in harmful effects.

Class I Analysis

An analysis for visibility and deposition on the nearest Class I area (i.e., Mingo Wilderness Area) was conducted. Based on these results, no further analysis was required. The threshold for concern for visibility is an impact greater than a 5% change in light extinction at Rank 8. The CALPUFF predicted deposition fluxes were compared to the deposition thresholds of 0.005

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kg/ha/year for nitrogen and 0.01 kg/ha/year for sulfur. Results are summarized in the following tables.

Visibility Screening Results

Rank	Daily Light Extinction Change			Maximum % of Threshold
	2018	2019	2020	
1	2.32%	2.88%	2.10%	57.6%
2	2.06%	2.38%	1.82%	47.6%
3	1.88%	2.34%	1.60%	46.8%
4	1.78%	2.17%	1.58%	43.4%
5	1.73%	1.65%	1.47%	34.6%
6	1.52%	1.23%	1.46%	30.4%
7	1.52%	1.17%	1.36%	30.4%
8	1.36%	1.08%	1.33%	27.2%

Deposition

Year	Nitrogen Deposition kg/ha/yr	Sulfur Deposition kg/ha/yr
2018	0.0036	0.0029
2019	0.0032	0.0027
2020	0.0036	0.0032
DAT Threshold	0.005	0.010
Maximum % of Threshold	72.8%	32.3%

Class I increment SIL and Increment modeling was performed using AERMOD and CalPuff. Based on the modeling results, the Facility's potential emissions of regulated air pollutants were shown to be below the Class I SILs and thus no multisource analysis was required. The modeling performed for the Facility resulted in predicted impacts below the Class I Increments.

Best Available Control Technology

The PSD regulations mandate that a case-by-case Best Available Control Technology (BACT) analysis be performed on all new or modified affected sources at which a net emissions increase will occur. The following table is a summary of the BACT determinations made in this permit.

For more detailed discussion of BACT see the BACT analysis section of the permit application.

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
SN-01 and SN-	EAFs and LMFs	PM	Fabric Filter	0.0018 gr/dscf (filterable only)

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
02		PM ₁₀	Fabric Filter	0.0024 gr/dscf
		PM _{2.5}	Fabric Filter	0.0024 gr/dscf
		Opacity	Fabric Filter	3% as a 6 minute average from baghouse 6% from melt shop
		SO ₂	Scrap management plan	0.20 lb/ton of steel produced
		VOC	Scrap management plan and good operating practices	0.093 lb/ton steel produced
		CO		2.02 lb/ton of steel produced
		NO _x		0.35 lb/ton of steel produced
		Lead	Fabric Filter	0.00056 lb/ton of steel produced
		GHG	Good operating practices	747,098 tpy CO ₂ e
SN-03 and SN-04	VT Degassers	CO (from degasser)	Flare	0.04 lb/ton of steel produced
		PM	Combustion of natural gas and good combustion practice	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x		0.10 lb/MMBtu
		GHG		Good operating practices
SN-05 and SN-06	Lime Injector Burners	PM	Combustion of natural gas and good combustion practices	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
		CO		0.0824 lb/MMBtu
		NO _x	Low NOX burners Combustion of clean fuel Good Combustion Practices	0.095 lb/MMBtu
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu
SN-07 through SN-11	Horizontal Ladle Preheaters	PM	Combustion of Natural gas and Good Combustion Practices	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.095 lb/MMBtu
GHG	Good operating practices	117 lb CO ₂ e/MMBtu		
SN-12 through SN-15	Vertical Ladle Dryout Flash Preheater Stations	PM	Combustion of Natural gas and Good Combustion Practices	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.095 lb/MMBtu

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu
SN-16 through SN-21	Tundish Preheaters/ Dryout Stand	PM	Combustion of Natural gas and Good Combustion Practices	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.097 lb/MMBtu
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu
SN-22	Pickle Line Tandem Mill	PM	Mist Eliminator	0.0025 gr/dscf (filterable only)
		PM ₁₀		0.0066 gr/dscf
		PM _{2.5}		0.0066 gr/dscf
		Opacity		5%
SN-23	Push Pull Pickle Line (Tension Leveler & Pickling Section Fume Exhaust)	PM	Baghouse Scrubber	0.0022 gr/dscf
		PM ₁₀		0.0022 gr/dscf
		PM _{2.5}		0.0022 gr/dscf
		Opacity		5%
SN-24	Pickle Line Boiler	PM	Combustion of Natural gas and Good Combustion Practice	0.00186 lb/MMBTU
		PM ₁₀		0.00186 lb/MMBTU
		PM _{2.5}		0.00186 lb/MMBTU
		Opacity		5%
		SO ₂		0.0006 lb/MMBTU
		VOC		0.0054 lb/MMBTU
		CO		0.0824 lb/MMBTU

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.035 lb/MMBTU
		GHG	Good operating practices Minimum Boiler Efficiency	117 lb CO ₂ e/MMBtu
SN-25	Pickle Line Scale Dust	PM	Fabric Filter	0.0022 gr/dscf
		PM ₁₀		0.0022 gr/dscf
		PM _{2.5}		0.0022 gr/dscf
		Opacity		5%
SN-27 and SN-28	Galvanizing Line Boilers #1 and #2	PM	Combustion of Natural gas and Good Combustion Practice	0.00068 lb/MMBTU
		PM ₁₀		0.00068 lb/MMBTU
		PM _{2.5}		0.00068 lb/MMBTU
		Opacity		5%
		SO ₂		0.0006 lb/MMBTU
		VOC		0.0054 lb/MMBTU
		CO		0.0824 lb/MMBTU
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.035 lb/MMBTU
GHG	Good operating practices Minimum Boiler Efficiency	117 lb CO ₂ e/MMBtu		
SN-29 and SN-30	Galvanizing Line Caustic Cleaning #1 and #2	PM	Mist Eliminator	0.003 gr/dscf
		PM ₁₀		0.003 gr/dscf
		PM _{2.5}		0.003 gr/dscf
		Opacity		5%
SN-31 and SN-	Galvanizing Line Post	PM	Mist Eliminator	0.003 gr/dscf
		PM ₁₀		0.003 gr/dscf

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
32	Treatment #1 and #2	PM _{2.5}		0.003 gr/dscf
		Opacity		5%
SN-33	Skin Pass Mill	PM	Mist Eliminator	0.0025 gr/dscf (filterable only)
		PM ₁₀		0.0066 gr/dscf
		PM _{2.5}		0.0066 gr/dscf
		Opacity		5%
SN-34	Batch Annealing Furnaces	PM	Combustion of Natural gas and Good Combustion Practice	0.0075 lb/MMBtu
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂	0.0006 lb/MMBtu	
		VOC	0.0054 lb/MMBtu	
		CO	0.0824 lb/MMBtu	
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.1 lb/MMBtu
GHG	Good operating practices	117 lb CO ₂ e/MMBtu		
SN-35	Natural Gas Space Heaters – Cold Mill	PM	Combustion of Natural gas and Good Combustion Practice	0.0075 lb/MMBtu
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂	0.0006 lb/MMBtu	
		VOC	0.0054 lb/MMBtu	
		CO	0.0824 lb/MMBtu	
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.08 lb/MMBtu
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
SN-37	Pickle Galvanizing Line Boiler	PM	Combustion of Natural gas and Good Combustion Practice	0.0012 lb/MMBtu
		PM ₁₀		0.0012 lb/MMBtu
		PM _{2.5}		0.0012 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.035 lb/MMBtu
	GHG	Good operating practices	117 lb CO ₂ e/MMBtu	
SN-38	Pickle Galvanizing Line – Scale Dust and Pickling Section	PM	Fabric Filter Scrubber	0.0022 gr/dscf
		PM ₁₀		0.0022 gr/dscf
		PM _{2.5}		0.0022 gr/dscf
		Opacity		5%
SN-39	Pickle Galvanizing Line Cleaning Sections – Pre-Cleaning and Post Treatment	PM	Mist Eliminator	0.003 gr/dscf
		PM ₁₀		0.003 gr/dscf
		PM _{2.5}		0.003 gr/dscf
		Opacity		5%
SN-40	Coil Coating Line – Pre-cleaning Section	PM	Mist eliminator Good operating practices	0.003 gr/dscf
		PM ₁₀		0.003 gr/dscf
		PM _{2.5}		0.003 gr/dscf
		Opacity		5%
SN-41	Coil Coating Line – Cleaning Section	PM	Mist eliminator Good operating practices	0.003 gr/dscf
		PM ₁₀		0.003 gr/dscf
		PM _{2.5}		0.003 gr/dscf
		Opacity		5%

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
SN-42	Coil Coating Line – Prime/Finish Coating	VOC	Enclosed painting system Thermal oxidation Good work practices	152.6 tpy
SN-43	Coil Coating Line Chemical Dryer	PM	Good combustion practices Energy efficient burners Combustion of natural gas	0.0075 lb/MMBtu
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x		0.1 lb/MMBtu
		GHG	Good operating practices	117 lb CO _{2e} /MMBtu
SN-44	Coil Coating Line Primer Oven	PM	Good combustion practices Energy efficient burners Combustion of natural gas	0.0075 lb/MMBtu
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x		0.1 lb/MMBtu
		GHG	Good operating practices	117 lb CO _{2e} /MMBtu
SN-45	Coil Coating Line Finish Oven	PM	Good combustion practices Energy efficient burners Combustion of natural gas	0.0075 lb/MMBtu
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	0.1 lb/MMBtu	

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu
SN-46	Coil Coating Line RTO	PM	Good combustion practices Energy efficient burners Combustion of natural gas	0.009 lb/MMBtu
		PM ₁₀		0.009 lb/MMBtu
		PM _{2.5}		0.009 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x		0.25 lb/MMBtu
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu
SN-48 and SN-49	Casters	PM	Good operating practices	0.062 lb/ton steel produced
		PM ₁₀		
		PM _{2.5}		
SN-50	Casting Process Heating Source	PM	Combustion of Natural gas and Good Combustion Practices	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.095 lb/MMBtu
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu
SN-52 through SN-68 SN-133	Cooling Towers	PM	Drift Eliminators Low TDS	0.0005% drift loss
		PM ₁₀		
		PM _{2.5}		
		Opacity		5%
SN-69	Emergency	PM	Good Operating	0.1 g/bhp-hr

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
through SN-84, SN-135	Generators	PM ₁₀	Practices, limited hours of operation, Compliance with NSPS Subpart III	0.1 g/bhp-hr
		PM _{2.5}		0.1 g/bhp-hr
		Opacity		20%
		SO ₂		<15 ppm sulfur in fuel
		VOC		0.13 g/bhp-hr
		CO		0.9 g/bhp-hr
		NO _x		3.9 g/bhp-hr
		CO _{2e}	Good Combustion Practices	164 lb CO _{2e} /MMBtu
SN-85 through SN-90, SN-136	Emergency Water Pumps	PM	Good Operating Practices, limited hours of operation, Compliance with NSPS Subpart III	1 g/bhp-hr
		PM ₁₀		1 g/bhp-hr
		PM _{2.5}		1 g/bhp-hr
		Opacity		20%
		SO ₂		<15 ppm sulfur in fuel
		VOC		1.12 g/bhp-hr
		CO		3.03 g/bhp-hr
		NO _x		14.06 g/bhp-hr
		CO _{2e}	Good Combustion Practices	164 lb CO _{2e} /MMBtu
SN-91	Charging Crane	PM	Dust Control Plan	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-92	Scrap Yard Stockpiling	PM	Dust Control Plan	0.81 tpy
		PM ₁₀		0.38 tpy
		PM _{2.5}		0.06 tpy
		Opacity		20%
SN-93	EAF Flux Receiving System	PM	Dust Control Plan, Enclosed Receiving, System with Fabric Filter	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		5%
SN-94	EAF Flux Storage and	PM	Dust Control Plan, Enclosed	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
	Handling System	PM _{2.5}	Conveyors with Fabric Filters, Silos with Bin Vent Filters	0.01 gr/dscf
		Opacity		5%
SN-95	Carbon Injection Receiving System	PM	Dust Control Plan, Enclosed Receiving System with Fabric Filter	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		5%
SN-96	Carbon Injection Storage and Handling System	PM	Dust Control Plan, Enclosed Conveyors with Fabric Filters, Silos with Bin Vent Filters	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%
SN-97	LMF Flux Receiving System	PM	Dust Control Plan, Enclosed Receiving System with Fabric Filter	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		5%
SN-98	LMF Flux Storage and Handling System	PM	Dust Control Plan, Enclosed Conveyors with Fabric Filters, Silos with Bin Vent Filters	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%
SN-99	Alloy Receiving System	PM	Dust Control Plan, Enclosed Receiving System with Fabric Filter	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		5%
SN-100	Alloy Storage and Handling System	PM	Dust Control Plan, Enclosed Conveyors with Fabric Filters, Silos with Bin Vent Filters	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%
SN-101	Alloy Delivery System –	PM	Dust Control Plan, Enclosed Conveyors with	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
	LMF	Opacity	Fabric Filters, Enclosed Receiving System with Fabric Filter, Silos with Bin Vent Filters	5%
SN-102	Degasser Alloy Delivery System	PM	Dust Control Plan, Enclosed Conveyors with Fabric Filters, Enclosed Receiving System with Fabric Filter, Silos with Bin Vent Filters	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%
SN-103	EAF Lime Injection Receiving, Storage, and Handling System	PM	Fabric Filter Enclosed Conveyors with Compressed Air, Dust control Plan, Bin Vent Filter on Each Silo	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%
SN-104	Inside Drop Point – Spent Refractory and Other Waste	PM	Dust Control Plan	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-105	Outside Drop Point – Spent Refractory and Other Waste	PM	Dust Control Plan	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-106	Inside Drop Point – EAF Dust	PM	Dust Control Plan	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-107	Wind Erosion	PM	Dust Control Plan	3.7 tpy
		PM ₁₀		1.84 tpy
		PM _{2.5}		0.28 tpy
		Opacity		20%

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
SN-108	Drop Points Slag	PM	Dust Control Plan	3.39 tpy
		PM ₁₀		1.63 tpy
		PM _{2.5}		0.54 tpy
		Opacity		20%
SN-109	Slag Handling and Conveying	PM	Dust Control Plan	1.11 tpy
		PM ₁₀		0.37 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-110	Slag Storage Piles	PM	Dust Control Plan	0.58 tpy
		PM ₁₀		0.29 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-111	Paved Roadways	PM	Development and Implementation of Fugitive Dust Control Plan	2.8 tpy
		PM ₁₀		0.6 tpy
		PM _{2.5}		0.2 tpy
SN-112	Unpaved Roadways	PM	Development and Implementation of Fugitive Dust Control Plan	0.81 tpy
		PM ₁₀		0.38 tpy
		PM _{2.5}		0.06 tpy
SN-114	Hydrogen Plant #2 Reformer Furnace (PHG830)	PM	Combustion of Natural gas and Good Combustion Practice	0.0075 lb/MMBtu
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.1 lb/MMBtu
		CO _{2e}	Good Operating Practices	117 lb CO _{2e} /MMBtu

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
SN-115	Gasoline Storage Tanks and Dispensing Operation	VOC	Good Operating Practices, Vehicle On-Board Vapor Recovery or Stage II Vapor Recovery System	0.62 tpy
SN-116	Ore Unloading and Product Loading Gantry Crane	PM	Enclosed Conveyors and Water Sprays at the Transfer Points	5.7 tpy
		PM ₁₀		2.7 tpy
		PM _{2.5}		0.5 tpy
		Opacity		20%
SN-117	Oxide Unloading Bin and Dedusting	PM	Fabric Filter Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-118	Oxide Pellet Pile Transfer and Dedusting (Pre-Enclosed Storage)	PM	Fabric Filter Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-119	Oxide Transfer and Dedusting (Post-Enclosed Storage)	PM	Fabric Filter Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-120	Oxide and Remet Screening and Dedusting	PM	Fabric Filter Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-121	Furnace Charge Hopper Loading Silos	PM	Fabric Filter Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-122	Charge Hopper	PM	Fabric Filter Baghouse, Hooded	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
	Dedusting	PM _{2.5}	Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		Opacity		5%
		SO ₂	Combustion of Natural Gas and Good Combustion Practices	0.000376 lb/MMBtu
		VOC		0.01 lb/MMBtu
		CO		0.08 lb/MMBtu
		NO _x		0.00317 lb/MMBtu
		Lead		8.17E-08 lb/MMBtu
		CO _{2e}	Good Operating Practices	54,701 tpy CO _{2e}
SN-123	Reformer Natural Gas Fired (1591 MMBtu/hr)	PM	Scrubber, Low NOX Burners, Combustion of Natural Gas, and Good Combustion Practices	0.0044 gr/dscf
		PM ₁₀		0.0044 gr/dscf
		PM _{2.5}		0.0044 gr/dscf
		Opacity		5%
		SO ₂		32.2 tpy
		VOC		35.6 tpy
		CO		543.2 tpy
		NO _x		383.3 tpy
		Lead		0.01 tpy
		CO _{2e}	Good Operating Practices	1,680,207 tpy CO _{2e}
SN-124	Furnace Dedusting (BSG Dust Collection) Wet Scrubber	PM	Dust Collector and Scrubber	0.0079 gr/dscf
		PM ₁₀		0.0079 gr/dscf
		PM _{2.5}		0.0079 gr/dscf
		Opacity		5%
		SO ₂	Combustion of Natural Gas and Good Combustion Practices	0.000376 lb/MMBtu
		VOC		0.01 lb/MMBtu
		CO		0.08 lb/MMBtu
		NO _x		0.00317 lb/MMBtu
		Lead		8.17E-08 lb/MMBtu
		CO _{2e}	Good Operating Practices	54,701 tpy CO _{2e}
SN-125	Hot Pressure Relief Vent	PM	Flare, Scrubber, Good Combustion	0.0044 gr/dscf
		PM ₁₀		0.0044 gr/dscf

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
	(Flare)	PM _{2.5}	Practices, Low NO _x Fuel	0.0044 gr/dscf
		Opacity		5%
		SO ₂		0.1 tpy
		VOC		0.1 tpy
		CO		8.8 tpy
		NO _x		1.0 tpy
		Lead		9.855E-07 tpy
		CO _{2e}	Good Operating Practices	762 tpy CO _{2e}
SN-126	Briquetter Dedusting	PM	Scrubber	0.0079 gr/dscf
		PM ₁₀		0.0079 gr/dscf
		PM _{2.5}		0.0079 gr/dscf
		Opacity		5%
		SO ₂	Combustion of Natural Gas and Good Combustion Practices	0.000376 lb/MMBtu
		VOC		0.01 lb/MMBtu
		CO		0.08 lb/MMBtu
		NO _x		0.00317 lb/MMBtu
		Lead		8.17E-08 lb/MMBtu
		CO _{2e}	Good Operating Practices	27,350 tpy CO _{2e}
SN-127	HBI Cooling Conveyor #1 and #2	PM	Scrubber	0.0079 gr/dscf
		PM ₁₀		0.0079 gr/dscf
		PM _{2.5}		0.0079 gr/dscf
		Opacity		5%
SN-128	Transfer and Product Screening Station No. 1 (Pre Pile)	PM	Fabric Filter Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-129	Transfer and Product Screening Station No. 2 (Post Pile)	PM	Fabric Filter Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-130	HBI Product	PM	Dust Control Plan	1.2 tpy

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
	Storage Pile	PM ₁₀	and Use of Water Sprays and Wetting Agents and Vehicle Restrictions	0.6 tpy
		PM _{2.5}		0.2 tpy
		Opacity		20%
SN-131	Remet/Fines Storage	PM	Dust Control Plan and Use of Water Sprays and Wetting Agents and Vehicle Restrictions	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-132	Process Water Degasser	CO	Good Design Methods and Operating Practice	106.5 tpy
		CO _{2e}		2230 tpy CO _{2e}
SN-134	Vehicle Travel on In-Plant Paved and Unpaved Roads	PM	Development and Implementation of Fugitive Dust Control Plan	0.2 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy

Case by Case MACT Determination

The Facility has been determined to potentially require a case by case MACT determination for the electric arc furnaces (SN-01 and SN-02) for PM, PM₁₀, and PM_{2.5} and related HAP emissions. The following general principles are to be followed in selection of MACT on a case-by-case basis

- The MACT emission limit shall not be less stringent than the emission control which is achieved in practice by the best controlled similar sources;
- The maximum degree of reduction in emissions of HAP which can be achieved by utilizing those control technologies that can be identified from the available information, taking into consideration the costs of achieving such emission reduction and any non-air quality health and environmental impacts and energy requirements associated with the emission control; and
- If EPA has either proposed a relevant emission standard pursuant to section 112(d) or section 112(g) of the Act or adopted a presumptive MACT determination for the source category which includes the constructed major source.

BRS reviewed applicable requirements from NSPS and non-major source NESHAP standards as well as the BACT analysis already performed on these sources for PM, PM₁₀, and PM_{2.5} and submitted that information in a full analysis which can be found in Appendix I of this permit. The requirements on the Facility as a result of this analysis can be found in Specific Condition #34.

Regulations

The following table contains the regulations applicable to this permit.

Regulations
Arkansas Air Pollution Control Code, Regulation 18, effective March 14, 2016
Rules of the Arkansas Plan of Implementation for Air Pollution Control, Rule 19, effective August 6, 2020
Regulations of the Arkansas Operating Air Permit Program, Regulation 26, effective March 14, 2016
40 CFR 52.21, <i>Prevention of Significant Deterioration</i>
40 CFR Part 60, Subpart Dc - <i>Standards of Performance for Small Industrial-Commercial-Institutional Steam Generating Units</i>
40 CFR Part 60, Subpart AAa - <i>Standards of Performance for Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 7, 1983</i>
40 CFR Part 60, Subpart TT – <i>Standards of Performance for Metal Coil Surface Coating</i>
40 CFR Part 60 Subpart IIII, <i>Standards of Performance for Stationary Compression Ignition Internal Combustion Engines</i>
40 CFR Part 63 Subpart ZZZZ, <i>National Emission Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustions Engines</i>
40 CFR Part 63 Subpart DDDDD, <i>National Emission Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters</i>
40 CFR Part 63 Subpart SSSS, <i>National Emission Standards for Hazardous Air Pollutants: Surface Coating of Metal Coil</i>
40 CFR Part 63 Subpart CCC, <i>National Emission Standards for Hazardous Air Pollutants for Steel Pickling – HCl Process Facilities and Hydrochloric Acid Regeneration Plants</i>
40 CFR Part 63 Subpart B, <i>Requirements for Control Technology Determinations for Major Sources in Accordance With Clean Air Act Sections, Sections 112(g) and 112(j)</i>

Emission Summary

The following table is a summary of emissions from the facility. This table, in itself, is not an enforceable condition of the permit.

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
Total Allowable Emissions		PM	107.8	357.2
		PM ₁₀	122.3	423.7
		PM _{2.5}	119.9	414.9
		SO ₂	121.9	451.7
		VOC	122.3	406.7
		CO	1720.0	5250.2
		NO _x	983.4	1470.4
		Lead	0.352741	1.455309
		CO _{2e}	--	2,984,214
HAPs*		Single HAP	6.85	27.75
		Total Other HAPs	14.18	59.60
		HCl	0.43	1.84
SN-01	EAF 1 and LMF 1	PM	16.2	71.0
		PM ₁₀	21.6	94.6
		PM _{2.5}	21.6	94.6
		SO ₂	50.0	205.0
		VOC	23.3	95.3
		CO	505.0	2070.5
		NO _x	87.5	358.8
		Lead	0.14	0.57
		CO _{2e}	-	373,549
		Single HAP	0.08	0.08
		Total Other HAPs	0.11	0.44
SN-02	EAF 2 and LMF 2	PM	16.2	71.0
		PM ₁₀	21.6	94.6
		PM _{2.5}	21.6	94.6
		SO ₂	50.0	205.0
		VOC	23.3	95.3
		CO	505.0	2070.5

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		NO _x	87.5	358.8
		Lead	0.14	0.57
		CO ₂ e	-	373,549
		Single HAP	0.08	0.08
		Total Other HAPs	0.11	0.44
SN-03	Vacuum Tank Degasser 1	PM	0.1	0.2
		PM ₁₀	0.1	0.2
		PM _{2.5}	0.1	0.2
		SO ₂	0.1	0.1
		VOC	0.1	0.2
		CO	9.8	40.1
		NO _x	0.5	2.2
		Lead	2.45E-06	1.07E-05
		CO ₂ e	-	5,566
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-04	Vacuum Tank Degasser 2	PM	0.1	0.2
		PM ₁₀	0.1	0.2
		PM _{2.5}	0.1	0.2
		SO ₂	0.1	0.1
		VOC	0.1	0.2
		CO	9.8	40.1
		NO _x	0.5	2.2
		Lead	2.45E-06	1.07E-05
		CO ₂ e	-	5,566
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-05	Lime Injector Burner 1	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
		SO ₂	0.1	0.1
		VOC	0.2	0.6
		CO	1.9	8.1
		NO _x	2.2	9.3
		Lead	1.09E-05	4.77E-05
		CO ₂ e	-	11,377
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-06	Lime Injector Burner 2	PM	0.2	0.8
		PM ₁₀	0.2	0.8

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		PM _{2.5}	0.2	0.8
		SO ₂	0.1	0.1
		VOC	0.2	0.6
		CO	1.9	8.1
		NO _x	2.2	9.3
		Lead	1.09E-05	4.77E-05
		CO _{2e}	-	11,377
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-07	Horizontal Ladle Preheater 1	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
		Single HAP	0.01	0.01
SN-08	Horizontal Ladle Preheater 2	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
		Single HAP	0.01	0.01
SN-09	Horizontal Ladle Preheater 3	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
		Single HAP	0.01	0.01

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-10	Horizontal Ladle Preheater 4	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-11	Horizontal Ladle Preheater 5	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-12	Vertical Ladle Dryout Flash Preheater Station 1	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-13	Vertical Ladle Dryout Flash Preheater Station 2	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-14	Vertical Ladle Dryout Flash Preheater Station 3	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-15	Vertical Ladle Dryout Flash Preheater Station 4	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-16	Tundish Preheaters/Dryout Stand 1	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
SN-17	Tundish Preheaters/Dryout Stand 2	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-18	Tundish Preheaters/Dryout Stand 3	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-19	Tundish Preheaters/Dryout Stand 4	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-20	Tundish Preheaters/Dryout Stand 5	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-21	Tundish Preheaters/Dryout Stand 6	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
				Single HAP
		Total Other HAPs	0.01	0.01
SN-22	Pickle Line Tandem Cold Mill	PM	4.8	20.7
		PM ₁₀	12.5	54.7
		PM _{2.5}	12.5	54.7
SN-23a	Push Pull Pickle Line – Tension Leveler Scale Dust Exhaust	PM	0.4	1.7
		PM ₁₀	0.4	1.7
		PM _{2.5}	0.4	1.7
SN-23b	Push Pull Pickle Line – Pickling Section	HCl	0.18	0.79
SN-24	Pickle Line Boiler	PM	0.1	0.5
		PM ₁₀	0.1	0.5
		PM _{2.5}	0.1	0.5
		SO ₂	0.1	0.2
		VOC	0.3	1.3
		CO	4.5	19.4
		NO _x	1.9	8.3
		Lead	2.63E-05	1.15E-04
		CO _{2e}	--	27,530
				Single HAP
		Total Other HAPs	0.01	0.02
SN-25	Pickle Line Scale Dust	PM	1.0	4.4
		PM ₁₀	1.0	4.4
		PM _{2.5}	1.0	4.4
SN-26	Pickling Section	HCl	0.12	0.51
SN-27	Galvanizing Line Boiler	PM	0.1	0.2

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
	#1	PM ₁₀	0.1	0.2
		PM _{2.5}	0.1	0.2
		SO ₂	0.1	0.2
		VOC	0.3	1.3
		CO	4.5	19.4
		NO _x	1.9	8.3
		Lead	2.63E-05	1.15E-04
		CO _{2e}	-	27,530
		Single HAP	0.01	0.02
		Total Other HAPs	0.01	0.02
		PM	0.1	0.2
		PM ₁₀	0.1	0.2
		PM _{2.5}	0.1	0.2
		SO ₂	0.1	0.2
		VOC	0.3	1.3
		CO	4.5	19.4
		NO _x	1.9	8.3
		Lead	2.63E-05	1.15E-04
		CO _{2e}	-	27,530
		Single HAP	0.01	0.02
		Total Other HAPs	0.01	0.02
		PM	0.2	0.9
		PM ₁₀	0.2	0.9
		PM _{2.5}	0.2	0.9
		PM	0.2	0.9
		PM ₁₀	0.2	0.9
		PM _{2.5}	0.2	0.9
		PM	0.1	0.3
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.3
		PM	0.1	0.3
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.3
		PM	0.6	2.5
		PM ₁₀	1.5	6.6
		PM _{2.5}	1.5	6.6
		PM	0.9	3.9
		PM ₁₀	0.9	3.9
		PM _{2.5}	0.9	3.9
		SO ₂	0.1	0.3

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		VOC	0.7	2.8
		CO	9.8	42.6
		NO _x	11.8	51.7
		Lead	5.78E-05	2.53E-04
		CO _{2e}	-	60,421
		Single HAP	0.01	0.04
		Total Other HAPs	0.01	0.05
SN-35	Natural Gas Space Heaters – Cold Mill	PM	1.3	5.6
		PM ₁₀	1.3	5.6
		PM _{2.5}	1.3	5.6
		SO ₂	0.1	0.5
		VOC	1.0	4.1
		CO	14.1	61.4
		NO _x	13.6	59.6
		Lead	8.33E-05	3.65E-04
		CO _{2e}	-	87,121
				Single HAP
		Total Other HAPs	0.01	0.07
SN-37	Pickle Galvanizing Line Boiler	PM	0.1	0.3
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.3
		SO ₂	0.1	0.2
		VOC	0.3	1.3
		CO	4.5	19.4
		NO _x	1.9	8.3
		Lead	2.63E-05	1.15E-04
		CO _{2e}	-	27,530
				Single HAP
		Total Other HAPs	0.01	0.02
SN-38	Pickle Galvanizing Line – Scale Dust & Pickling Section	PM	1.0	4.4
		PM ₁₀	1.0	4.4
		PM _{2.5}	1.0	4.4
		HCl	0.12	0.51
SN-39	Pickle Galvanizing Line – Pre-Cleaning & Post Treatment	PM	0.3	1.2
		PM ₁₀	0.3	1.2
		PM _{2.5}	0.3	1.2
SN-40	Coil Coating Line – Pre-Cleaning Section	PM	0.3	1.2
		PM ₁₀	0.3	1.2
		PM _{2.5}	0.3	1.2

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
SN-41	Coil Coating Line – Cleaning Section	PM	0.3	1.2
		PM ₁₀	0.3	1.2
		PM _{2.5}	0.3	1.2
SN-42	Coil Coating Line – Prime/Finish Coating	VOC	34.9	152.7
		Single HAP	6.1	26.8
		Total Other HAPs	13.2	57.9
SN-43	Coil Coating Line Chemical Dryer	PM	0.1	0.2
		PM ₁₀	0.1	0.2
		PM _{2.5}	0.1	0.2
		SO ₂	0.1	0.1
		VOC	0.1	0.2
		CO	0.4	1.8
		NO _x	0.5	2.2
		Lead	2.41E-06	1.05E-05
		CO _{2e}	-	2,520
		Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-44	Coil Coating Line Primer Oven	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
		SO ₂	0.1	0.1
		VOC	0.2	0.6
		CO	1.9	8.3
		NO _x	2.3	10.1
		Lead	1.12E-05	4.91E-05
		CO _{2e}	-	11,709
		Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-45	Coil Coating Line Finish Oven	PM	0.2	0.6
		PM ₁₀	0.2	0.6
		PM _{2.5}	0.2	0.6
		SO ₂	0.1	0.1
		VOC	0.1	0.5
		CO	1.5	6.3
		NO _x	1.8	7.6
		Lead	8.49E-06	3.72E-05
		CO _{2e}	-	8,880
		Single HAP Total Other HAPs	0.01 0.01	0.01 0.01

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
SN-46	Coil Coating Line RTO	PM	0.2	0.5
		PM ₁₀	0.2	0.5
		PM _{2.5}	0.2	0.5
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	5.6	24.2
		NO _x	3.1	13.4
		Lead	6.00E-06	2.63E-05
		CO _{2e}	-	6,273
		Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-48	Caster 1	PM	0.4	1.3
		PM ₁₀	0.4	1.3
		PM _{2.5}	0.4	1.3
SN-49	Caster 2	PM	0.4	1.3
		PM ₁₀	0.4	1.3
		PM _{2.5}	0.4	1.3
SN-50	Casting Process Heating Source	PM	0.3	1.0
		PM ₁₀	0.3	1.0
		PM _{2.5}	0.3	1.0
		SO ₂	0.1	0.1
		VOC	0.2	0.8
		CO	2.5	10.9
		NO _x	2.9	12.5
		Lead	1.47E-05	6.44E-05
		CO _{2e}	-	15,374
		Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-51	Casting Process Cooling Tower 1	PM	0.8	3.3
		PM ₁₀	0.8	3.3
		PM _{2.5}	0.8	3.3
SN-52	Casting Process Cooling Tower 2	PM	0.8	3.3
		PM ₁₀	0.8	3.3
		PM _{2.5}	0.8	3.3
SN-53	Casting Process Cooling Tower 3	PM	0.8	3.3
		PM ₁₀	0.8	3.3
		PM _{2.5}	0.8	3.3
SN-54	Casting Process Cooling Tower 4	PM	0.8	3.3
		PM ₁₀	0.8	3.3
		PM _{2.5}	0.8	3.3

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
SN-55	Melt Shop Cooling Tower 1	PM	0.1	0.5
		PM ₁₀	0.1	0.5
		PM _{2.5}	0.1	0.5
SN-56	Melt Shop Cooling Tower 2: Gas Cleaning Plant (GCP)	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
SN-57	Caster Cooling Tower 1	PM	0.3	1.0
		PM ₁₀	0.3	1.0
		PM _{2.5}	0.3	1.0
SN-58	Caster Cooling Tower 2	PM	0.6	2.5
		PM ₁₀	0.6	2.5
		PM _{2.5}	0.6	2.5
SN-59	Cold Mill Cooling Tower 1	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
SN-60	Cold Mill Cooling Tower 2	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
SN-61	Cold Mill Cooling Tower 3	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
SN-62	Melt Shop Cooling Tower 3: Spray Cooled EAF (Dcut Only)	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
SN-63	Melt Shop Cooling Tower 4: EAF/LMF 1 and DOC Spray	PM	1.0	4.1
		PM ₁₀	1.0	4.1
		PM _{2.5}	1.0	4.1
SN-64	Melt Shop Cooling Tower 5: EAF Closed Loop for Electrode Arms	PM	0.2	0.6
		PM ₁₀	0.2	0.6
		PM _{2.5}	0.2	0.6
SN-65	Melt Shop Cooling Tower 6: Vacuum Tank Degasser	PM	0.1	0.3
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.3
SN-66	Caster Cooling Tower 3	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
SN-67	Caster Cooling Tower 4	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
SN-68	Cold Mill Cooling Tower 4: Coil Coating Line	PM	0.1	0.3
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.3
SN-69	Emergency Generator 1	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
		Single HAP	0.01	0.01
Total Other HAPs	0.02	0.01		
SN-70	Emergency Generator 2	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
		Single HAP	0.01	0.01
Total Other HAPs	0.02	0.01		
SN-71	Emergency Generator 3	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
		Single HAP	0.01	0.01
Total Other HAPs	0.02	0.01		
SN-72	Emergency Generator 4	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-73	Emergency Generator 5	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-74	Emergency Generator 6	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-75	Emergency Generator 7	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-76	Emergency Generator 8	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-77	Emergency Generator 9	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-78	Emergency Generator 10	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-79	Emergency Generator 11	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-80	Emergency Generator 12	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-81	Emergency Generator 13	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-82	Emergency Generator 14	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-83	Emergency Generator 15	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-84	Emergency Generator 16	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		CO ₂ e	-	195
		Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-85	Emergency Water Pump 1	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO ₂ e	-	8
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-86	Emergency Water Pump 2	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO ₂ e	-	8
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-87	Emergency Water Pump 3	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO ₂ e	-	8
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-88	Emergency Water Pump 4	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		CO ₂ e	-	8
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-89	Emergency Water Pump 5	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO ₂ e	-	8
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-90	Emergency Water Pump 6	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO ₂ e	-	8
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-91	Charging Crane	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-92	Scrap Yard Stockpiling	PM	0.2	0.9
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.1
SN-93	EAF Flux Receiving System	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-94	EAF Flux Storage and Handling System	PM	0.3	1.3
		PM ₁₀	0.3	1.0
		PM _{2.5}	0.2	0.8
SN-95	Carbon Injection Receiving System	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-96	Carbon Injection Storage and Handling System	PM	0.2	0.5
		PM ₁₀	0.1	0.4

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		PM _{2.5}	0.1	0.4
SN-97	LMF Flux Receiving System	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-98	LMF Flux Storage and Handling System	PM	0.3	1.0
		PM ₁₀	0.2	0.7
		PM _{2.5}	0.2	0.5
SN-99	Alloy Receiving System	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-100	Alloy Storage and Handling System	PM	0.2	0.6
		PM ₁₀	0.2	0.6
		PM _{2.5}	0.2	0.6
SN-101	Alloy Delivery System – LMF	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-102	Degasser Alloy Delivery System	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-103	EAF Lime Injection Receiving, Storage, and Handling System	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
SN-104	Inside Drop Point – Spent Refractory and Other Waste	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-105	Outside Drop Point – Spent Refractory and Other Waste	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-106	Inside Drop Point – EAF Dust	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-107	Wind Erosion	PM	0.9	3.7
		PM ₁₀	0.5	1.9
		PM _{2.5}	0.1	0.3
SN-108	Drop Points Slag	PM	1.1	3.4
		PM ₁₀	0.5	1.7
		PM _{2.5}	0.1	0.6
SN-109	Slag Handling and Conveying	PM	1.1	1.2
		PM ₁₀	0.4	0.4

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
		PM _{2.5}	0.1	0.1
SN-110	Wind Erosion – Slag Storage Piles	PM	0.2	0.6
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.1
SN-111	Paved Roadways	PM	0.7	2.8
		PM ₁₀	0.2	0.6
		PM _{2.5}	0.1	0.2
SN-112	Unpaved Roadways	PM	2.2	9.7
		PM ₁₀	0.6	2.6
		PM _{2.5}	0.1	0.3
SN-113	HCl Storage Tanks	HCl	0.01	0.03
SN-114	Hydrogen Plant #1 Reformer Furnace	PM	0.6	2.5
		PM ₁₀	0.6	2.5
		PM _{2.5}	0.6	2.5
		SO ₂	0.1	0.2
		VOC	0.4	1.8
		CO	6.2	27.1
		NO _x	7.5	32.9
		Lead	3.68E-05	1.61E-04
		Single HAP Total Other HAPs	0.01 0.01	0.03 0.03
SN-115	Gasoline Storage Tanks and Dispensing Operations	VOC	0.2	0.7
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-116	Ore Unloading and Product Loading Gantry Crane	PM	1.3	5.7
		PM ₁₀	0.7	2.7
		PM _{2.5}	0.1	0.5
		Lead	6.51E-03	2.85E-02
SN-117	Oxide Unloading Bin and Dedusting	PM	0.2	0.5
		PM ₁₀	0.2	0.5
		PM _{2.5}	0.2	0.5
		Lead	5.54E-04	2.43E-03
SN-118	Oxide Pellet Pile Transfer and Dedusting (Pre-Enclosed Storage)	PM	0.3	1.1
		PM ₁₀	0.3	1.1
		PM _{2.5}	0.3	1.1
		Lead	1.26E-03	5.52E-03
SN-119	Oxide Unloading Bin and Dedusting Oxide Transfer and Dedusting (Post	PM	0.2	0.5
		PM ₁₀	0.2	0.5
		PM _{2.5}	0.2	0.5

EMISSION SUMMARY						
Source Number	Description	Pollutant	Emission Rates			
			lb/hr	tpy		
	Domes)	Lead	5.54E-04	2.43E-03		
SN-120	Oxide and Remet Screening and Dedusting	PM	0.8	3.1		
		PM ₁₀	0.8	3.1		
		PM _{2.5}	0.8	3.1		
		Lead	3.53E-03	1.54E-02		
SN-121	Furnace Charge Hopper Loading Silos	PM	0.1	0.1		
		PM ₁₀	0.1	0.1		
		PM _{2.5}	0.1	0.1		
		Lead	7.05E-05	3.09E-04		
SN-122	Charge Hopper Dedusting	PM	0.1	0.5		
		PM ₁₀	0.1	0.5		
		PM _{2.5}	0.1	0.5		
		SO ₂	0.3	1.1		
		VOC	0.2	0.9		
		CO	2.9	12.4		
		NO _x	2.1	8.9		
		Lead	5.56E-04	2.43E-03		
		CO _{2e}	-	54,701		
SN-123	Reformer Natural Gas Fired (1591 MMBtu/hr)	PM	8.1	35.3		
		PM ₁₀	8.1	35.3		
		PM _{2.5}	8.1	35.3		
		SO ₂	10.6	32.2		
		VOC	8.2	35.6		
		CO	124.1	543.2		
		NO _x	88.7	388.3		
		Lead	2.29E-03	7.00E-03		
				CO _{2e}	-	1,680,207
				Single HAP	0.02	0.08
		Total Other HAPs	0.02	0.09		
SN-124	Furnace Dedusting (BSG Dust Collection)	PM	2.5	11.0		
		PM ₁₀	2.5	11.0		
		PM _{2.5}	2.5	11.0		
		SO ₂	0.3	1.1		
		VOC	0.2	0.9		
		CO	2.9	12.4		
		NO _x	2.1	8.9		
		Lead	1.26E-02	5.50E-02		
		CO _{2e}	-	54,701		
SN-125	Hot Pressure Relief Vent	PM	0.6	0.1		

EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
	(Flare)	PM ₁₀	0.6	0.1
		PM _{2.5}	0.6	0.1
		SO ₂	0.1	0.1
		VOC	0.1	0.1
		CO	316.0	8.8
		NO _x	24.9	1.0
		Lead	2.25E-07	9.86E-07
		CO _{2e}	-	762
		Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-126	Briquetter Dedusting	PM	4.0	17.4
		PM ₁₀	4.0	17.4
		PM _{2.5}	4.0	17.4
		SO ₂	0.2	0.6
		VOC	0.1	0.4
		CO	1.5	6.2
		NO _x	1.1	4.5
		Lead	1.99E-02	8.70E-02
		CO _{2e}	-	27,350
SN-127	HBI Cooling Conveyor 1 and 2	PM	1.9	8.4
		PM ₁₀	1.9	8.4
		PM _{2.5}	1.9	8.4
		Lead	1.90E-02	8.34E-02
SN-128	Transfer and Product Screening Station No 1	PM	0.4	1.8
		PM ₁₀	0.4	1.8
		PM _{2.5}	0.4	1.8
		Lead	2.02E-03	8.83E-03
SN-129	Transfer and Product Screening Station No 1	PM	0.4	1.8
		PM ₁₀	0.4	1.8
		PM _{2.5}	0.4	1.8
		Lead	2.02E-03	8.83E-03
SN-130	HBI Product Storage Pile	PM	0.3	1.2
		PM ₁₀	0.2	0.6
		PM _{2.5}	0.2	0.6
		Lead	1.29E-03	5.66E-03
SN-131	Remet/Fines Storage	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
		Lead	1.60E-04	7.01E-04

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EMISSION SUMMARY				
Source Number	Description	Pollutant	Emission Rates	
			lb/hr	tpy
SN-132	Process Water Degasser	CO	24.3	106.5
		CO _{2e}	-	2230
SN-133	DRI Process Water Cooling Tower	PM	0.7	3.0
		PM ₁₀	0.7	3.0
		PM _{2.5}	0.7	3.0
SN-134	Vehicle Travel on In-Plant Paved and Unpaved Roads	PM	0.1	0.2
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-135	DRI Diesel Fired Emergency Generator	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
		Single HAP	0.01	0.01
Total Other HAPs	0.02	0.01		
SN-136	DRI Emergency Water Pump	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO _{2e}	-	8
		Single HAP	0.01	0.01
Total Other HAPs	0.01	0.01		

*HAPs included in the VOC totals. Other HAPs are not included in any other totals unless specifically stated.

**Air Contaminants such as ammonia, acetone, and certain halogenated solvents are not VOCs or HAPs.

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SECTION III: PERMIT HISTORY

This is the initial permit for the facility. The sources included in this permit and those of Permit #2305-AOP-R7 (AFIN 47-00991) are considered one stationary source under definition of the Clean Air Act. See the Permit History section of Permit #2305-AOP-R7 for all revisions to this stationary source.

SECTION IV: SPECIFIC CONDITIONS

Melt Shop

SN-01 Electric Arc Furnace (EAF) 1 and Ladle Metallurgy Furnace (LMF) 1
SN-02 01 Electric Arc Furnace (EAF) 2 and Ladle Metallurgy Furnace (LMF) 2

SN-03 Vacuum Tank Degasser 1
SN-04 Vacuum Tank Degasser 2

SN-48 Caster 1
SN-49 Caster 2

Source Description

The facility receives scrap iron and steel by rail and truck. The scrap is unloaded and stockpiled on site. The scrap will be moved from the storage piles and placed in charging buckets. These charging buckets will be used to load the Electric Arc Furnaces (EAF). Additional raw materials will be added through various feed systems and the charged steel will be melted using electric arc applied through carbon electrodes. The EAF will be capable of typically producing 250 tons per hour of liquid steel. The liquid steel will be transferred to the Ladle Metallurgy Furnaces (LMF) and, depending upon the grade of steel being produced, the Vacuum Tank Degasser (VTD) for further refinement.

At the LMFs, the steel is subjected to additional heating by electrical energy to maintain its molten state and is further refined by the addition of raw materials (alloys). At the VTD the steel is further refined by the injection of oxygen and the addition of raw materials (alloys). Occasional stirring of the steel in the ladle may be required. Fugitive emissions will be captured by the LMF roof or hood, as required. Once the molten steel reaches the desired temperature and chemistry at the LMF or VTD, the ladle transports the molten steel to a caster, where it is poured into water cooled molds which are considered part of the Casting Process.

The EAF operations are enclosed in a structure with total enclosure in the Melt Shop structure. The Melt Shop is equipped with a deep storage canopy hood to cover the EAF operations. Air captured in the dedicated hoods is conveyed to the Melt Shop Baghouse.

Slag is formed in the EAFs and LMFs during the melting, and refining processes. The slag generated in these processes will be transferred to the slag processing area, where it will be quenched, processed, stored (outside) and eventually transported off-site by truck for sale to customers.

As the steel passes through the molds in the caster, it is cooled and formed. Dry powder will be applied in the caster mold for lubrication. Negligible (insignificant) emissions are assumed to occur while using the dry powder material. The casters also generate emissions of particulates.

The Casting Process (CP) involves operations and equipment that are designed to process liquid steel from the Melt Shop to produce a slab or coiled steel. The liquid from the Melt Shop is poured out from a ladle via a tundish into molds and coiled by a down coiler. The primary emission sources associated with the CP are two Casters, SN-48 and SN-49.

A portion of the steel is further refined in one of the two vacuum tank degassers (VTD). Ladles are placed directly into the VTD for processing. Once the ladle is enclosed in the VTD, mechanical pumps are used to draw a vacuum on the ladle.

The VTD is designed to reduce the dissolved carbon gasses through oxidation when refining stainless steel grades. The gas from the VTD is captured and first directed through a particulate filter to protect the mechanical pumps from the PM. The gas is then directed to a flare to control the excess carbon emissions, mainly CO. The VTDs share a single set of mechanical pumps. Therefore, only one degasser can operate at any given time. Emissions are generated from the flare combustion of natural gas and the oxidation of CO in the waste gas to CO₂.

Specific Conditions

- The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific Conditions #6 through #8 and #10 through #34. [Reg.19.501 *et seq.* and 40 C.F.R. § 52 Subpart E]

SN	Description	Pollutant	lb/hr	tpy
SN-01	EAF 1 and LMF 1	PM	16.2	71.0
		PM ₁₀	21.6	94.6
		PM _{2.5}	21.6	94.6
		SO ₂	50.0	205.0
		VOC	23.3	95.3
		CO	505.0	2070.5
		NO _x	87.5	358.8
		Lead	0.14	0.57
		CO _{2e}	-	373,549
SN-02	EAF 2 and LMF 2	PM	16.2	71.0
		PM ₁₀	21.6	94.6
		PM _{2.5}	21.6	94.6

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SN	Description	Pollutant	lb/hr	tpy
		SO ₂	50.0	205.0
		VOC	23.3	95.3
		CO	505.0	2070.5
		NO _x	87.5	358.8
		Lead	0.14	0.57
		CO ₂ e	-	373,549
SN-03	VTD 1	PM	0.1	0.2
		PM ₁₀	0.1	0.2
		PM _{2.5}	0.1	0.2
		SO ₂	0.1	0.1
		VOC	0.1	0.2
		CO	9.8	40.1
		NO _x	0.5	2.2
		Lead	2.45E-06	1.07E-05
		CO ₂ e	-	5,566
SN-04	VTD 2	PM	0.1	0.2
		PM ₁₀	0.1	0.2
		PM _{2.5}	0.1	0.2
		SO ₂	0.1	0.1
		VOC	0.1	0.2
		CO	9.8	40.1
		NO _x	0.5	2.2
		Lead	2.45E-06	1.07E-05
		CO ₂ e	-	5,566
SN-48	Caster 1	PM	0.4	1.3
		PM ₁₀	0.4	1.3
		PM _{2.5}	0.4	1.3

SN	Description	Pollutant	lb/hr	tpy
SN-49	Caster 2	PM	0.4	1.3
		PM ₁₀	0.4	1.3
		PM _{2.5}	0.4	1.3

2. The permittee shall not exceed the emission rates set forth in the following table and must install the control devices or implement the pollution prevention measures set forth in the following table. Compliance with these emission limits shall be demonstrated by compliance with Specific Conditions #6 through #8 and #10 through #34

Source	Description	Pollutant	Control Technology	BACT Limit
SN-01 and SN-02	EAFs and LMFs	PM	Fabric Filter	0.0018 gr/dscf (filterable only)
		PM ₁₀		0.0024 gr/dscf
		PM _{2.5}		0.0024 gr/dscf
		Opacity		3% as a 6 minute average from baghouse 6% from melt shop
		SO ₂	Scrap management plan	0.20 lb/ton of steel produced
		VOC	Scrap management plan and good operating practices	0.093 lb/ton steel produced
		CO		2.02 lb/ton of steel produced
		NO _x		0.35 lb/ton of steel produced
		Lead	Fabric Filter	0.00056 lb/ton of steel produced
		GHG	Good operating practices	747,098 tpy CO ₂ e
SN-03 and SN-04	VT Degassers	CO (from degasser)	Flare	0.04 lb/ton of steel produced
		PM	Combustion of natural gas and good combustion practice	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
Opacity		5%		

Source	Description	Pollutant	Control Technology	BACT Limit
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x		0.10 lb/MMBtu
		GHG	Good operating practices	11,132 tpy CO ₂ e
SN-48 and SN-49	Casters	PM	Good operating practices	0.062 lb/ton steel produced
		PM ₁₀		
		PM _{2.5}		

3. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific Conditions #6 through #8 and #10 through #34. [Reg.18.801 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

SN	Description	Pollutant	lb/hr	tpy
SN-01	EAF 1 and LMF 1	Single HAP	0.08	0.08
		Total Other HAPs	0.11	0.44
SN-02	EAF 2 and LMF 2	Single HAP	0.08	0.08
		Total Other HAPs	0.11	0.44
SN-03	VTD 1	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-04	VTD 2	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01

4. Visible emissions may not exceed the limits specified in the following table of this permit as measured by EPA Reference Method 9. Compliance with this condition will be shown by compliance with Specific Condition #5.

SN	Limit	Regulatory Citation
SN-03 SN-04	5%	Reg.19.901 <i>et seq.</i> and 40 C.F.R. § 52 Subpart E

5. The permittee shall conduct weekly observations of the opacity from SN-03 and SN-04 flares, when VTD 1 and/or VTD 2 is in operation. If visible emissions are detected, then the permittee shall immediately conduct a 6-minute opacity reading in accordance with EPA Reference Method 9. The result of these observations or readings shall be recorded in a log that shall be kept on site and made available for inspection upon request. [Reg.19.705 and 40 C.F.R. § 52 Subpart E]

6. The permittee shall install and operate alarm system to notify the operator of the presence of a pilot flame or other possible flare malfunction for SN-03 and SN-04. The permittee shall perform monthly visual confirmation of the pilot lights, semi-annually remove the strainer and check for debris, and annual test fire to ensure pilot light. The permittee shall maintain logs of all flare inspection and maintenance activities. These logs shall be kept on site and made available to Division personnel upon request. [Reg.19.702, Reg.19.304, 40 C.F.R. § 52 Subpart E, and 40 C.F.R. § 64]
7. The permittee shall test the VTDs, SN-03 and SN-04, to show the flare is designed and operated in accordance with 40 C.F.R. 60.18(b) through (f). This test includes a Method 22 for opacity, measurement of the actual gas flow rate and, calculations of the heating value of the gas (if complying with 60.18(c)(3)(ii) and (c)(4)). This test shall be conducted in accordance with Plantwide Condition 3. [Reg.19.702 and 40 C.F.R. § 52 Subpart E]
8. The permittee shall not process more than 2,050,000 tons of steel through each VTD, SN-03 and SN-04, in any consecutive rolling 12-month period. [Reg.19.901 *et seq.* and 40 C.F.R. § 52 Subpart E]
9. The permittee shall maintain monthly records of the amount of steel processed in SN-03 and SN-04. These records shall include the monthly total of steel processed and the 12-month rolling total of steel processed. These records shall be updated by the 15th day of the month following the month to which the records pertain, kept on site, made available to Division personnel upon request, and submitted in accordance with General Provision 7. [Reg.19.901 *et seq.* and 40 C.F.R. § 52 Subpart E]
10. The permittee shall perform stack testing of SN-01 and SN-02 fabric filters to show compliance with the emissions limits in Specific Conditions #1, #2, and NSPS Subpart AAa. Testing shall be performed initially and annually thereafter in accordance Plantwide Condition 3 and 4, and EPA Reference Method 5D as found in 40 CFR, Part 60, Appendix A. The sampling time and sampling volume for each run shall be at least 4 hours and 4.50 dscm (160 dscf). The permittee shall report all emissions measured using Method 5D as filterable PM, PM₁₀, or PM_{2.5} or may conduct separate filterable PM₁₀ testing using EPA Reference Method 201 or 201A. The permittee shall also conduct test for condensable particulate emissions concurrently using EPA reference Method 202 and include these results in PM₁₀ and PM_{2.5} values for compliance with emission rates. The report shall include information specified in § 60.276a(f) of 40 CFR, Part 60, Subpart AAa. Testing shall be conducted when the EAF is operated at or near its capacity based on the specific type of steel to be produced. A targeted capacity would be 250 tons/hour of steel. If the production rate is less than 250 tons/hour, the tested emission rates shall be scaled up to 250 ton/hour and compared to the permitted emission rates. If the production rate is above 250 tons/hour, the tested rate would be compared directly to the permitted emission rate. [Reg.19.304 and 40 C.F.R. §§ 60.275a(e)(1) Subpart AAa and Reg.19.702 and 40 C.F.R. § 52 Subpart E]

11. Unless the presence of inclement weather makes concurrent testing infeasible, the permittee shall conduct the performance tests required by Specific Conditions #5, #14, and, #20 concurrently. [Reg.19.304 and 40 C.F.R. §§ 60.275a(e)(4) and 60.275a(j)]
12. The permittee shall submit to the Division a written report of the results of the performance test required by Specific Condition 10. The report shall include information specified in §60.276a(f) of 40 CFR, Part 60, Subpart AAa, and the information required under Plantwide Condition 4. [Reg.19.705 and 40 C.F.R. § 52 Subpart E and Reg.19.304 and 40 C.F.R. § 60. 276a(f)]
13. The permittee shall not discharge into the atmosphere any gases from the EAF Baghouses, SN-01 and SN-02, exhibiting 3 percent opacity or greater. [Reg.19.304 and 40 C.F.R. § 60.272a(a)(2)]
14. The permittee shall perform observations of the opacity of the visible emissions from EAF Baghouses, SN-01 and SN-02 by a certified visible emission observer as follows: Visible emission observations are conducted at least once per day when the furnace is operating in the melting and refining period. These observations shall be taken in accordance with Method 9, and, for at least three 6-minute periods, the opacity shall be recorded for any point(s) where visible emissions are observed. Where it is possible to determine that a number of visible emission sites relate to only one incident of the visible emissions, only one set of three 6-minute observations will be required. In this case, Method 9 observations must be made for the site of highest opacity that directly relates to the cause (or location) of visible emissions observed during a single incident. Records shall be maintained of any 6-minute average that is in excess of 3% opacity. Reports of exceedances shall be submitted in accordance with Specific Condition 15. Should the permittee install a single stack to its melt shop baghouse the permittee shall install and operate a bag leak detection system in accordance with § 60.273a(c), (e), (f), and (g). The permittee shall maintain records for each bag leak detection system as outlined in § 60.276a(h). [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
15. The permittee shall submit a written report of exceedances of the EAF baghouse opacity and the EAF Melt Shop opacity to the Division semi-annually in accordance with General Provision 7. For the purposes of these reports, exceedances are defined as all 6-minute periods during which the average opacity is 3 percent or greater at the EAF baghouse, and all 6-minute periods during which the average opacity is 6 percent or greater at the EAF Melt Shop due solely to the operations of the EAF. Opacity observations shall be recorded on a visible emissions observation form. The information presented in Figures 9-1 and 9-2 to EPA Method 9 shall be recorded. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
16. The permittee shall not discharge into the atmosphere any gases which exit from EAF Melt Shop which exceed 6 percent opacity or greater due solely to the operations of the EAF. Exceedances shall be defined as all 6-minute periods during which the average opacity is 6 percent or greater. This opacity limit shall apply at all times that either of the

EAFs is in operation and due solely to the operations of the electric arc furnace.
[Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]

17. The permittee shall either (a) install, calibrate, and maintain a monitoring device that allows the pressure in the free space inside each EAF baghouse to be monitored, pursuant to 40 CFR § 60.274a(f), or (b) perform daily observations of shop opacity, pursuant to 40 CFR § 60.273a(d). The permittee shall notify the Division which method it elects within 180 days before startup of SN-01 or 02. If the permittee elects to conduct opacity observations or in the case of a failure of the monitoring device, the permittee must perform daily observations of shop opacity, pursuant to 40 C.F.R. § 60.273a(d) until the monitoring device is back in operation. The permittee shall conduct these daily opacity readings on the EAF Melt Shop as follows: Shop opacity observations shall be conducted at least once per day when the furnace(s) is operating in the meltdown and refining period. Shop opacity shall be determined as the arithmetic average of 24 or more consecutive 15-second opacity observations of emissions from the shop taken in accordance with Method 9. Shop opacity shall be recorded for any point(s) where visible emissions are observed in proximity to an affected EAF. Where it is possible to determine that a number of visible emission sites relate to only one incident of visible emissions, only one observation of shop opacity will be required. In this case, the shop opacity observations must be made for the site of highest opacity that directly relates to the cause (or location) of visible emissions observed during a single incident. Records of these opacity observations shall be kept on site and made available for inspection upon request. Reports of exceedances shall be submitted in accordance with Specific Condition #15. If the permittee elects to install a monitoring device in lieu of continuing to perform opacity observations, the permittee must notify the Division of this change within 30 days of installing a monitoring device that allows the pressure inside the free space inside each EAF to be monitored. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
18. The permittee shall check and record the control system fan motor amperes and damper positions on a once per shift basis. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
19. The permittee shall comply with 40 C.F.R. § 60.274a(c), and shall conduct a compliance test to re-establish these parameters as specified in 40 C.F.R. § 60.274a(c) within 180 days after the effective date of Permit #2445-AOP-R0. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
20. The permittee shall determine baseline values of the fan motor amperes and damper positions during annual performance testing in accordance with Specific Condition #5 to demonstrate compliance with the operating parameters monitored by the permittee pursuant to Specific Condition #18. The values of these parameters as determined during the most recent demonstration of compliance shall be maintained at the appropriate level for each applicable period. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
21. The permittee shall perform monthly operational status inspections of the equipment that is important to the performance of the total capture system (i.e., pressure sensors,

- dampers, and damper switches). This inspection shall include observations of the physical appearance of the equipment (e.g., presence of holes in ductwork or hoods, flow constrictions caused by dents or accumulated dust in ductwork, and fan erosion). Any deficiencies shall be noted and proper maintenance performed. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
22. The permittee shall maintain records of all data obtained under Specific Condition #20 and all monthly operational status inspections performed under Specific Condition #21. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
 23. If the pressure device option in Specific Condition #17 is selected, the pressure shall be recorded as 15-minute integrated averages. The monitoring device may be installed in any appropriate location in the EAF duct prior to the introduction of ambient air such that reproducible results will be obtained. The pressure monitoring device shall have an accuracy of ± 5 mm of water gauge over its normal operating range and shall be calibrated according to the manufacturer's instructions. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
 24. If the pressure device option in Specific Condition #17 is selected, during each performance testing conducted in accordance with Specific Condition #5, the permittee shall determine baseline values of the pressure in the free space inside the furnace during the meltdown and refining period(s). The pressure determined during the most recent demonstration of particulate emission compliance shall be maintained at all times when the EAF is operating in a meltdown and refining period. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
 25. If the pressure device option in Specific Condition #17 is selected, operation of the EAFs at a furnace static pressure that exceeds the value established under Specific Condition #24 will require the permittee to perform an opacity reading at the Melt Shop. Operation of the EAFs at this rate may be considered by the Division to be unacceptable operation and maintenance of the affected facility, if operation at such rates results in opacity readings at the Melt Shop Building greater than 6%. Operation at such values shall be reported to the Division semiannually. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
 26. If the pressure device option in Specific Condition #17 is selected, the permittee shall maintain records which demonstrate compliance with Specific Condition #24 and may be used by the Division for enforcement purposes. The records shall be updated on a daily basis, shall be kept on site, and shall be provided to Division personnel upon request. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
 27. During any performance test conducted in accordance with Specific Condition #5, the owner or operator shall monitor the following information for all heats covered by the test:
 - (1) Charge weights and materials, tap weights and materials;

- (2) Heat times, including start and stop times, and a log of process operation, including periods of no operation during testing and, the pressure inside an EAF when direct-shell evacuation control systems are used;
- (3) Control device operation log; and
- (4) Continuous monitor or Reference Method 9 data.

[Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]

28. The permittee shall retain all records of the measurements required by Specific Conditions #17 through #27 for at least two years following the date of the measurement. [Reg.19.304 and 40 C.F.R. § 60 Subpart AAa]
29. The permittee shall perform stack testing of SN-01 and SN-02 for NO_x, SO₂, CO, CO₂ and VOC emissions to show compliance with the emissions limits in Specific Conditions #1 and #2. Testing shall be performed in accordance with Plantwide Conditions 3 and 4 and shall be repeated every six months until six consecutive tests are passed. The permittee shall then conduct subsequent testing annually. The permittee shall measure NO_x, SO₂, CO₂ and CO emissions in accordance with EPA Reference Methods 7E, 6C, 3A and 10, respectively. The permittee shall measure the total VOC emissions using EPA Reference Method 25A, from which it will subtract out methane (CH₄) and ethane (C₂H₆) emissions from the EAF baghouse using EPA Reference Method 18 to arrive at applicable VOC levels for purposes of this permit. Semiannual stack testing for a pollutant is not required if the permittee elects to operate a CEMS for that pollutant at SN-01 and SN-02. Testing shall be conducted when the EAF is operated at or near its capacity based on the specific type of steel to be produced. A targeted capacity would be 250 tons/hour of steel. If the production rate is less than 250 tons/hour, the tested emission rates shall be scaled up to 250 ton/hour and compared to the permitted emission rates. If the production rate is above 250 tons/hour, the tested rate would be compared directly to the permitted emission rate. [Reg.19.702 and 40 C.F.R. § 52 Subpart E]
30. The permittee shall keep record of the total number of tons of steel tapped from the EAFs during each of the previous twelve months updated on a monthly basis and submitted in accordance with General Provision #7. For each month, the emission factor from the nearest preceding stack test shall be multiplied by the total tons of steel tapped during that month, to establish the amount of each pollutant emitted during that month. The emissions so calculated for each of the last twelve months shall be added together and expressed as tons of pollutant per year. The sum of the last twelve months shall not exceed the ton per year limits for SN-01 and SN-02 in Specific Condition #1. If more than one stack test is conducted during a month, the calculation for that month shall be modified so that the total number of tons of steel tapped during the period between two consecutive stack tests shall be multiplied by the emission factor established by the stack test at the beginning of any such period. This record must be updated by the 15th day of the following month. [Reg.19.705, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 70.6]

31. The permittee shall perform stack testing of SN-01 and SN-02 for lead (Pb) emissions. Testing shall be performed in accordance with Plantwide Conditions 3 and 4 and shall be repeated annually thereafter. The permittee shall measure lead emissions in accordance with EPA Reference Method 12 or other alternate method, provided the Division approves the alternate method prior to use. Testing shall be conducted when the EAF is operated at or near its capacity based on the specific type of steel to be produced. A targeted capacity would be 250 tons/hour of steel. If the production rate is less than 250 tons/hour, the tested emission rates shall be scaled up to 250 ton/hour and compared to the permitted emission rates. If the production rate is above 250 tons/hour, the tested rate would be compared directly to the permitted emission rate. [Reg.19.702 and 40 C.F.R. § 52 Subpart E]
32. In lieu of, or in addition to calculating an emission factor for NO_x, SO₂, CO, CO₂ and VOC, reporting EAF production each month as provided in Specific Condition #30, and the semiannual testing required in Specific Condition #29, the permittee may install and operate a monitoring device that continuously monitors and records NO_x, SO₂, CO, CO₂ and/or VOC concentration of gases in the duct leading to the EAF baghouses. The NO_x and SO₂ monitors shall be operated in accordance with performance specification #2 which is found in 40 CFR Part 60, Appendix B, and the CEMS conditions in Attachment A of this permit. The CO monitor shall be operated in accordance with performance specification #4, which is found in 40 CFR Part 60, Appendix B, and the CEMS conditions in Attachment A of this permit. The CO₂ monitor shall be operated in accordance with performance specification #3, which is found in 40 CFR Part 60, Appendix B, and the CEMS conditions in Attachment A of this permit. For purposes of measuring VOCs, the permittee may use an adjustment factor which will assume that the VOCs are 30% less than THC or, may take actual measurements of methane concentrations to subtract from the THC measurement to arrive at the VOC concentration. The VOC monitor shall be operated in accordance with the CEMS conditions in Attachment A of this permit. The permittee shall provide reporting from the CEMS in parts per million (ppm) and also in pounds per hour (lb/hr). The permittee must install monitors for the flow rate through the EAF Baghouses in order to calculate the lb/hr, lb/ton of steel, and tpy emission rates. The permittee shall indicate the methodology used to determine the lb/hr figure in the required reporting. Both ppm and lb/hr data shall be used for compliance purposes. The lb/hr value shall be determined using 3-hour block averages for compliance purposes for the emissions limits in Specific Conditions #1 and #2. [Reg.19.703, 40 C.F.R. Part 52, Subpart E, and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]
33. If the permittee elects to install CEMS, it shall give the Division 15 days advanced written notice. Thereafter, the permittee shall demonstrate compliance either by providing monthly production reports pursuant to Specific Condition #30, or quarterly CEMS excess emission reports. If the permittee elects to discontinue use of CEMS, it shall give the Division 15 days advance written notice and shall resume or continue compliance with Specific Condition #30. [Reg.19.703, 40 C.F.R. Part 52, Subpart E, and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

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34. The facility has been determined to be subject to a Case by Case Maximum Achievable Control Technology (MACT) determination for the EAFs associated with the Steel Mill Project (SN-01 and SN-02). As a result of this Case by Case analysis, the facility must meet the following requirements:
- a. Install, operate, and maintain a capture system that collects emissions from each EAF and conveys the collected emissions to a control device for the removal of particulate matter (PM);
 - b. An EAF must not discharge from a control device and contain in excess of 0.0018 grains of PM per dry standard cubic foot (gr/dscf);
 - c. Any exit from a Melt Shop using an EAF is not allowed to exhibit 6% opacity or greater; and
 - d. The requirements of 40 C.F.R. § 63.10685 which identifies specific requirements for the control of contaminants from scrap. The primary requirement is to prepare / implement a plan to minimize scrap steel containing mercury.

[Reg.19.304, 40 C.F.R. § 63.43, and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

Melt Shop Natural Gas Sources

SN-05 Lime Injection Burner 1
SN-06 Lime Injection Burner 2

SN-07 Horizontal Ladle Preheater 1
SN-08 Horizontal Ladle Preheater 2
SN-09 Horizontal Ladle Preheater 3
SN-10 Horizontal Ladle Preheater 4
SN-11 Horizontal Ladle Preheater 5

SN-12 Vertical Ladle Dryout Flash Preheater Station 1
SN-13 Vertical Ladle Dryout Flash Preheater Station 2
SN-14 Vertical Ladle Dryout Flash Preheater Station 3
SN-15 Vertical Ladle Dryout Flash Preheater Station 4

SN-16 Tundish Preheaters/Dryout Stand 1
SN-17 Tundish Preheaters/Dryout Stand 2
SN-18 Tundish Preheaters/Dryout Stand 3
SN-19 Tundish Preheaters/Dryout Stand 4
SN-20 Tundish Preheaters/Dryout Stand 5
SN-21 Tundish Preheaters/Dryout Stand 6

SN-50 Casting Process Heating Source

Source Description

In order to support the Melt Shop operations, several natural gas fired combustion devices are installed at the facility and are summarized as follows:

- Each EAF is equipped with a natural gas fired Lime Injection Burner, SN-05 and SN-06, rated at 22.5 MMBtu/hr each
- The Horizontal Ladle Preheaters, SN-07 through SN-11, are natural gas fired burners used to raise the temperature of ladles prior to the transfer of molten steel from the EAFs. Each Horizontal Ladle Preheater is rated at 9.6 MMBtu/hr.
- The Vertical Ladle Dryout Flash Preheater Stations, SN-12 through SN-15, are natural gas fired heaters used to cure new refractory linings after they are replaced. Each Vertical Ladle Dryout Flash Preheater Station is rated at 9.6 MMBtu/hr.
- The Tundish Preheaters/Dryout Stand, SN-16 through SN-21, are natural gas fired heaters used to raise the temperature of tundishes prior to transfer of molten steel to the ladles. Each Tundish Preheater/Dryout Stand is rated at 10.8 MMBtu/hr.

- The Casting Process Heating Source, SN-50, includes natural gas fired combustion devices that will support the casting process. SN-50 has a total estimated heat input of 30 MMBtu/hr.

Specific Conditions

35. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Plantwide Condition #5. [Reg.19.501 *et seq.* and 40 C.F.R. § 52 Subpart E]

SN	Description	Pollutant	lb/hr	tpy
SN-05	Lime Injection Burner 1	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
		SO ₂	0.1	0.1
		VOC	0.2	0.6
		CO	1.9	8.1
		NO _x	2.2	9.3
		Lead	1.09E-05	4.77E-05
		CO _{2e}	-	11,377
SN-06	Lime Injection Burner 2	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
		SO ₂	0.1	0.1
		VOC	0.2	0.6
		CO	1.9	8.1
		NO _x	2.2	9.3
		Lead	1.09E-05	4.77E-05
		CO _{2e}	-	11,377
SN-07	Horizontal Ladle Preheater 1	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4

SN	Description	Pollutant	lb/hr	tpy
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
SN-08	Horizontal Ladle Preheater 2	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
SN-09	Horizontal Ladle Preheater 3	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
SN-10	Horizontal Ladle Preheater 4	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4

SN	Description	Pollutant	lb/hr	tpy
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
SN-11	Horizontal Ladle Preheater 5	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
SN-12	Vertical Ladle Dryout Flash Preheater Station 1	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
SN-13	Vertical Ladle Dryout Flash Preheater Station 2	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4

SN	Description	Pollutant	lb/hr	tpy
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
SN-14	Vertical Ladle Dryout Flash Preheater Station 3	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
SN-15	Vertical Ladle Dryout Flash Preheater Station 4	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.8	3.5
		NO _x	1.0	4.0
		Lead	4.71E-06	2.06E-05
		CO _{2e}	-	4,920
SN-16	Tundish Preheaters/Dryout Stand 1	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4

SN	Description	Pollutant	lb/hr	tpy
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
SN-17	Tundish Preheaters/Dryout Stand 2	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
SN-18	Tundish Preheaters/Dryout Stand 3	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
SN-19	Tundish Preheaters/Dryout Stand 4	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4

SN	Description	Pollutant	lb/hr	tpy
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
SN-20	Tundish Preheaters/Dryout Stand 5	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
SN-21	Tundish Preheaters/Dryout Stand 6	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	0.9	3.9
		NO _x	1.1	4.6
		Lead	5.29E-06	2.32E-05
		CO _{2e}	-	5,535
SN-50	Casting Process Heating Source	PM	0.3	1.0
		PM ₁₀	0.3	1.0
		PM _{2.5}	0.3	1.0

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SN	Description	Pollutant	lb/hr	tpy
		SO ₂	0.1	0.1
		VOC	0.2	0.8
		CO	2.5	10.9
		NO _x	2.9	12.5
		Lead	1.47E-05	6.44E-05
		CO _{2e}	-	15,374

36. The permittee shall not exceed the emission rates set forth in the following table and must install the control devices or implement the pollution prevention measures set forth in the following table. Compliance with these emission limits shall be demonstrated by compliance with Plantwide Condition #5

Source	Description	Pollutant	Control Technology	BACT Limit
SN-05 and SN-06	Lime Injection Burners	PM	Combustion of natural gas and good combustion practices	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NOX burners Combustion of clean fuel Good Combustion Practices	0.095 lb/MMBtu
	GHG	Good operating practices	117 lb CO _{2e} /MMBtu	
SN-07 through SN-11	Horizontal Ladle Preheaters	PM	Combustion of Natural gas and Good Combustion Practices	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu

Source	Description	Pollutant	Control Technology	BACT Limit
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.095 lb/MMBtu
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu
SN-12 through SN-15	Vertical Ladle Dryout Flash Preheater Stations	PM	Combustion of Natural gas and Good Combustion Practices	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.095 lb/MMBtu
	GHG	Good operating practices	117 lb CO ₂ e/MMBtu	
SN-16 through SN-21	Tundish Preheaters/Dryout Stand	PM	Combustion of Natural gas and Good Combustion Practices	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.097 lb/MMBtu
	GHG	Good operating practices	117 lb CO ₂ e/MMBtu	

Source	Description	Pollutant	Control Technology	BACT Limit
SN-50	Casting Process Heating Source	PM	Combustion of Natural gas and Good Combustion Practices	0.0075 lb/MMBtu (filterable only)
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.095 lb/MMBtu
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu

37. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Plantwide Condition #5. [Reg.18.801 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

SN	Description	Pollutant	lb/hr	tpy
SN-05	Lime Injector Burner 1	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-06	Lime Injector Burner 2	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-07	Horizontal Ladle Preheater 1	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-08	Horizontal Ladle Preheater 2	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-09	Horizontal Ladle Preheater 3	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-10	Horizontal Ladle Preheater 4	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-11	Horizontal Ladle Preheater 5	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-12	Vertical Ladle Dryout Flash Preheater Station 1	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-13	Vertical Ladle Dryout	Single HAP	0.01	0.01

SN	Description	Pollutant	lb/hr	tpy
	Flash Preheater Station 2	Total Other HAPs	0.01	0.01
SN-14	Vertical Ladle Dryout Flash Preheater Station 3	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-15	Vertical Ladle Dryout Flash Preheater Station 4	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-16	Tundish Preheaters/Dryout Stand 1	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-17	Tundish Preheaters/Dryout Stand 2	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-18	Tundish Preheaters/Dryout Stand 3	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-19	Tundish Preheaters/Dryout Stand 4	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-20	Tundish Preheaters/Dryout Stand 5	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-21	Tundish Preheaters/Dryout Stand 6	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-50	Casting Process Heating Source	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01

38. Visible emissions may not exceed the limits specified in the following table of this permit as measured by EPA Reference Method 9. Compliance with this condition will be shown by combustion of natural gas only and Plantwide Condition 5.

Source	Limit	Regulatory Citation
SN-07, SN-08, SN-09, SN-10, SN-11, SN-12, SN-13, SN-14, SN-15, SN-16, SN-17, SN-18, SN-19, SN-20, SN-21, SN-50	5%	Reg.19.901 <i>et seq.</i> and 40 C.F.R. § 52 Subpart E

Cold Mill Operations

SN-22 Pickle Line Tandem Mill
SN-23a Push Pull Pickle Line – Tension Leveler Scale Dust Exhaust
SN-23b Push Pull Pickle Line – Pickling Section
SN-24 Pickle Line Boiler
SN-25 Pickle Line Scale Dust
SN-26 Pickling Section

SN-27 Galvanizing Line Boiler 1
SN-28 Galvanizing Line Boiler 2
SN-29 Galvanizing Line Caustic Cleaning 1
SN-30 Galvanizing Line Caustic Cleaning 2
SN-31 Galvanizing Line Post Treatment 1
SN-32 Galvanizing Line Post Treatment 2

SN-33 Skin Pass Mill

SN-34 Batch Annealing Furnaces

SN-35 Natural Gas Space Heaters – Cold Mill

SN-37 Pickle Galvanizing Line Boiler
SN-38 Pickle Galvanizing Line – Scale Dust & Pickling Section
SN-39 Pickle Galvanizing Line Cleaning Sections – Pre-Cleaning & Post Treatment

SN-40 Coil Coating Line – Pre-cleaning Section
SN-41 Coil Coating Line – Cleaning Section
SN-42 Coil Coating Line – Prime/Finish Coating
SN-43 Coil Coating Line Chemical Dryer
SN-44 Coil Coating Line Primer Oven
SN-45 Coil Coating Line Finish Oven
SN-46 Coil Coating Line RTO

Source Description

The cold mill contains several operations designed to produce various different types of steel products. Provided below is a brief description of each of the individual operations to be performed in the Cold Mill.

Pickling Line

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Pickling is the process that cleans a steel coil of its rust, dirt, and oil so the metal can further processed. The steel will be uncoiled and sent through a series of hydrochloric acid baths that remove the oxides. The steel sheet is then rinsed and dried. A wet scrubber is used to control any potential hydrochloric acid emission generated from the pickling line process. This process is identified as the Pickling Section, SN-26, in the permit.

The Pickling Line Tandem Cold Mill, SN-22, is a cold rolling process directly coupled with the pickling line. The process consists of removal of hot strip scale and a rolling operation to final material thickness. The steel coil is unwound and passed between a set of work rolls which will be pressed together by hydraulically forced backup rolls.

A Push Pull Pickle Line, SN-23, removes scale and other surface impurities from rolled steel. This line processes coils without strip joining and has two potential emissions points: the tension leveler exhaust (SN-23a) with a fabric filter baghouse with an exhaust stack to reduce potential PM emissions and the Fume Exhaust (SN-23b) with a wet scrubber with an exhaust stack to reduce potential HCl emissions.

Pickle Line Scale Dust, SN-25, scale dust can be generated from the uncoiling, flattening and scale breaking of the steel. The scale dust emissions from this operations are controlled by a fabric filter baghouse.

The Pickle Line Boiler, SN-24, is a 53.7 MMBtu/hr natural gas fired boiler that provides steam to the pickling line.

Galvanizing Lines

The cold mill incorporates two continuous galvanizing lines to produce galvanized strips. The sources below are part of the Galvanizing Line:

- The Galvanizing Line Boilers 1 and 2, SN-27 and SN-28, are 53.7 MMBtu/hr each and combust natural gas only to provide steam to the galvanizing lines.
- The Galvanizing Line Caustic Cleaning 1 and 2, SN-29 and SN-30, and the Galvanizing Line Post Treatment 1 and 2, SN-31 and SN-32, are in the post treatment sections of the two galvanizing lines. Each line is equipped with a mist eliminator to reduce the emissions of particulate matter from caustic cleaning
- The Off-line Skin Pass Mill, SN-33, adjusts the final mechanical properties, flatness, and surface finish of the cold rolled strip. A mist eliminator is used to reduce the particulate matter from the emulsion applied to the rolling material. The Skin Pass Mill is capable of processing 160 tons of steel per hour.

Batch Annealing Furnaces

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The Batch Annealing Furnaces, SN-34, are fifteen (15) annealing furnace bases for a total heat input of 117.9 MMBtu/hr. Eleven (11) annealing furnace bases are installed to provide cooling. These bases are not natural gas fired.

Cold Mill Space Heaters

Natural Gas Fired Cold Mill / Supporting Building Structures Space Heaters, SN-35, are utilized to provide localized heating within the Cold Mill building structure. The total heat input is 170 MMBtu/hr.

Pickle Galvanizing Line

The cold mill also incorporates a pickle galvanizing line which contains the sources listed below:

- The Pickle Galvanizing Line Boiler, SN-37, is a 53.7 MMBtu/hr natural gas fired boiler that provides steam to the galvanizing portion of the Pickle Galvanizing Line.
- Pickle Galvanizing Line - Scale Dust & Pickling Section, SN-38, includes scale dust that is generated from the uncoiling, flattening and scale breaking of the steel. The scale dust emissions are controlled by a fabric filter. This source also includes pickling, which is the process that cleans a steel coil of its rust, dirt and oil so the metal can be further processed. The steel coil is unwound and sent through a series of hydrochloric acid baths that remove the oxides. The steel sheet is then rinsed and dried. A wet scrubber is used to control the HCl emissions
- Pickle Galvanizing Line Cleaning Sections, SN-39, includes the pre-cleaning and post treatment sections of the galvanizing process. These sources are equipped with mist eliminators to reduce the emissions of particulate matter.

Coil Coating Line

The Coil Coating Line (CCL) involves several pieces of equipment designed to take a steel coil, prep the steel, coat the steel with a prime and finish coat, dry those coatings, and rewind the steel for shipment to the customer. The potential emission sources from the Coil Coating Line are as follows:

- The Coil Coating Line – Cleaning Section (SN-41) consists of a two-stage alkaline spray cleaning section with an additional brushing stage in-between followed by a three-cascade rinsing unit. After the chemical cleaning section, the strip proceeds through conversion coating and dunk conversion coating processes followed by a final spray rinse.
- The Coil Coating Line – Prime/Finish Coating (SN-42) is comprised of both a vertical chemical coater and a paint roller coating machine with the primer and finish coaters for coating both sides of the strip.

- The Coil Coating Line Chemical Dryer, SN-43, is a natural gas fired chemical dryer to assist with the prime/finish coating section of the process. SN-43 has a heat input of 4.9 MMBtu/hr.
- The Coil Coating Line Primer Oven and Coil Coating Line Finish Oven, SN-44 and SN-45, are designed to cure the coatings on the metal strip. SN-44 has a heat input of 22.8 MMBtu/hr and SN-45 has a heat input of 17.3 MMBtu/hr
- Depending on the production, the curing oven exhaust air could be highly loaded by organic solvents. These solvents are purified by a regenerative thermal oxidizer system or thermal oxidizer, Coil Coating Line RTO, (SN-46) with a heat input of 12.2 MMBtu/hr.

Specific Conditions

39. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific Conditions #42 through #62. [Reg.19.501 *et seq.* and 40 C.F.R. § 52 Subpart E]

SN	Description	Pollutant	lb/hr	tpy
SN-22	Pickle Line Tandem Cold Mill	PM	4.8	20.7
		PM ₁₀	12.5	54.7
		PM _{2.5}	12.5	54.7
SN-23a	Push Pull Pickle Line – Tension Leveler Scale Dust Exhaust	PM	0.4	1.7
		PM ₁₀	0.4	1.7
		PM _{2.5}	0.4	1.7
SN-24	Pickle Line Boiler	PM	0.1	0.5
		PM ₁₀	0.1	0.5
		PM _{2.5}	0.1	0.5
		SO ₂	0.1	0.2
		VOC	0.3	1.3
		CO	4.5	19.4
		NO _x	1.9	8.3
		Lead	2.63E-05	1.15E-04

SN	Description	Pollutant	lb/hr	tpy
		CO ₂ e	--	27,530
SN-25	Pickle Line Scale Dust	PM	1.0	4.4
		PM ₁₀	1.0	4.4
		PM _{2.5}	1.0	4.4
SN-27	Galvanizing Line Boiler #1	PM	0.1	0.2
		PM ₁₀	0.1	0.2
		PM _{2.5}	0.1	0.2
		SO ₂	0.1	0.2
		VOC	0.3	1.3
		CO	4.5	19.4
		NO _x	1.9	8.3
		Lead	2.63E-05	1.15E-04
		CO ₂ e	-	27,530
SN-28	Galvanizing Line Boiler #2	PM	0.1	0.2
		PM ₁₀	0.1	0.2
		PM _{2.5}	0.1	0.2
		SO ₂	0.1	0.2
		VOC	0.3	1.3
		CO	4.5	19.4
		NO _x	1.9	8.3
		Lead	2.63E-05	1.15E-04
		CO ₂ e	-	27,530
SN-29	Galvanizing Line Caustic Cleaning #1	PM	0.2	0.9
		PM ₁₀	0.2	0.9
		PM _{2.5}	0.2	0.9
SN-30	Galvanizing Line Caustic Cleaning #2	PM	0.2	0.9
		PM ₁₀	0.2	0.9

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SN	Description	Pollutant	lb/hr	tpy
		PM _{2.5}	0.2	0.9
SN-31	Galvanizing Line Post Treatment #1	PM	0.1	0.3
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.3
SN-32	Galvanizing Line Post Treatment #2	PM	0.1	0.3
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.3
SN-33	Skin Pass Mill	PM	0.6	2.5
		PM ₁₀	1.5	6.6
		PM _{2.5}	1.5	6.6
SN-34	Batch Annealing Furnaces	PM	0.9	3.9
		PM ₁₀	0.9	3.9
		PM _{2.5}	0.9	3.9
		SO ₂	0.1	0.3
		VOC	0.7	2.8
		CO	9.8	42.6
		NO _x	11.8	51.7
		Lead	5.78E-05	2.53E-04
SN-35	Natural Gas Space Heaters – Cold Mill	PM	1.3	5.6
		PM ₁₀	1.3	5.6
		PM _{2.5}	1.3	5.6
		SO ₂	0.1	0.5
		VOC	1.0	4.1
		CO	14.1	61.4
		NO _x	13.6	59.6
		Lead	8.33E-05	3.65E-04

SN	Description	Pollutant	lb/hr	tpy
		CO ₂ e	-	87,121
SN-37	Pickle Galvanizing Line Boiler	PM	0.1	0.3
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.3
		SO ₂	0.1	0.2
		VOC	0.3	1.3
		CO	4.5	19.4
		NO _x	1.9	8.3
		Lead	2.63E-05	1.15E-04
		CO ₂ e	-	27,530
SN-38	Pickle Galvanizing Line – Scale Dust & Pickling Section	PM	1.0	4.4
		PM ₁₀	1.0	4.4
		PM _{2.5}	1.0	4.4
SN-39	Pickle Galvanizing Line – Pre-Cleaning & Post Treatment	PM	0.3	1.2
		PM ₁₀	0.3	1.2
		PM _{2.5}	0.3	1.2
SN-40	Coil Coating Line – Pre-Cleaning Section	PM	0.3	1.2
		PM ₁₀	0.3	1.2
		PM _{2.5}	0.3	1.2
SN-41	Coil Coating Line – Cleaning Section	PM	0.3	1.2
		PM ₁₀	0.3	1.2
		PM _{2.5}	0.3	1.2
SN-42	Coil Coating Line – Prime/Finish Coating	VOC	34.9	152.7
SN-43	Coil Coating Line Chemical Dryer	PM	0.1	0.2
		PM ₁₀	0.1	0.2
		PM _{2.5}	0.1	0.2

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SN	Description	Pollutant	lb/hr	tpy
		SO ₂	0.1	0.1
		VOC	0.1	0.2
		CO	0.4	1.8
		NO _x	0.5	2.2
		Lead	2.41E-06	1.05E-05
		CO _{2e}	-	2,520
SN-44	Coil Coating Line Primer Oven	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
		SO ₂	0.1	0.1
		VOC	0.2	0.6
		CO	1.9	8.3
		NO _x	2.3	10.1
		Lead	1.12E-05	4.91E-05
		CO _{2e}	-	11,709
SN-45	Coil Coating Line Finish Oven	PM	0.2	0.6
		PM ₁₀	0.2	0.6
		PM _{2.5}	0.2	0.6
		SO ₂	0.1	0.1
		VOC	0.1	0.5
		CO	1.5	6.3
		NO _x	1.8	7.6
		Lead	8.49E-06	3.72E-05
		CO _{2e}	-	8,880
SN-46	Coil Coating Line RTO	PM	0.2	0.5
		PM ₁₀	0.2	0.5
		PM _{2.5}	0.2	0.5

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SN	Description	Pollutant	lb/hr	tpy
		SO ₂	0.1	0.1
		VOC	0.1	0.3
		CO	5.6	24.2
		NO _x	3.1	13.4
		Lead	6.00E-06	2.63E-05
		CO _{2e}	-	6,273

40. The permittee shall not exceed the emission rates set forth in the following table and must install the control devices or implement the pollution prevention measures set forth in the following table. Compliance with these emission limits shall be demonstrated by compliance with Specific Conditions #42 through #62.

Source	Description	Pollutant	Control Technology	BACT Limit
SN-22	Pickle Line Tandem Mill	PM	Mist Eliminator	0.0025 gr/dscf (filterable only)
		PM ₁₀		0.0066 gr/dscf
		PM _{2.5}		0.0066 gr/dscf
		Opacity		5%
SN-23	Push Pull Pickle Line (Tension Leveler & Pickling Section Fume Exhaust)	PM	Baghouse Scrubber	0.0022 gr/dscf
		PM ₁₀		0.0022 gr/dscf
		PM _{2.5}		0.0022 gr/dscf
		Opacity		5%
SN-24	Pickle Line Boiler	PM	Combustion of Natural gas and Good Combustion Practice	0.00186 lb/MMBTU
		PM ₁₀		0.00186 lb/MMBTU
		PM _{2.5}		0.00186 lb/MMBTU
		Opacity		5%
		SO ₂		0.0006 lb/MMBTU
		VOC		0.0054 lb/MMBTU
		CO		0.0824 lb/MMBTU
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.035 lb/MMBTU

Source	Description	Pollutant	Control Technology	BACT Limit
		GHG	Good operating practices Minimum Boiler Efficiency	117 lb CO ₂ e/MMBtu
SN-25	Pickle Line Scale Dust	PM	Fabric Filter	0.0022 gr/dscf
		PM ₁₀		0.0022 gr/dscf
		PM _{2.5}		0.0022 gr/dscf
		Opacity		5%
SN-27 and SN-28	Galvanizing Line Boilers #1 and #2	PM	Combustion of Natural gas and Good Combustion Practice	0.00068 lb/MMBTU
		PM ₁₀		0.00068 lb/MMBTU
		PM _{2.5}		0.00068 lb/MMBTU
		Opacity		5%
		SO ₂		0.0006 lb/MMBTU
		VOC		0.0054 lb/MMBTU
		CO	0.0824 lb/MMBTU	
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.035 lb/MMBTU
		GHG	Good operating practices Minimum Boiler Efficiency	117 lb CO ₂ e/MMBTU
SN-29 and SN-30	Galvanizing Line Caustic Cleaning #1 and #2	PM	Mist Eliminator	0.003 gr/dscf
		PM ₁₀		0.003 gr/dscf
		PM _{2.5}		0.003 gr/dscf
		Opacity		5%
SN-31 and SN-32	Galvanizing Line Post Treatment #1 and #2	PM	Mist Eliminator	0.003 gr/dscf
		PM ₁₀		0.003 gr/dscf
		PM _{2.5}		0.003 gr/dscf
		Opacity		5%
SN-33	Skin Pass Mill	PM	Mist Eliminator	0.0025 gr/dscf (filterable only)
		PM ₁₀		0.0066 gr/dscf
		PM _{2.5}		0.0066 gr/dscf
		Opacity		5%

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Source	Description	Pollutant	Control Technology	BACT Limit
SN-34	Batch Annealing Furnaces	PM	Combustion of Natural gas and Good Combustion Practice	0.0075 lb/MMBtu
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.1 lb/MMBtu
	GHG	Good operating practices	117 lb CO ₂ e/MMBtu	
SN-35	Natural Gas Space Heaters – Cold Mill	PM	Combustion of Natural gas and Good Combustion Practice	0.0075 lb/MMBtu
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.08 lb/MMBtu
	GHG	Good operating practices	117 lb CO ₂ e/MMBtu	
SN-37	Pickle Galvanizing Line Boiler	PM	Combustion of Natural gas and Good Combustion Practice	0.0012 lb/MMBtu
		PM ₁₀		0.0012 lb/MMBtu
		PM _{2.5}		0.0012 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO	0.0824 lb/MMBtu	

Source	Description	Pollutant	Control Technology	BACT Limit
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.035 lb/MMBtu
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu
SN-38	Pickle Galvanizing Line – Scale Dust and Pickling Section	PM	Fabric Filter	0.0022 gr/dscf
		PM ₁₀	Scrubber	0.0022 gr/dscf
		PM _{2.5}		0.0022 gr/dscf
		Opacity		5%
SN-39	Pickle Galvanizing Line Cleaning Sections – Pre-Cleaning and Post Treatment	PM	Mist Eliminator	0.003 gr/dscf
		PM ₁₀		0.003 gr/dscf
		PM _{2.5}		0.003 gr/dscf
		Opacity		5%
SN-40	Coil Coating Line – Pre-cleaning Section	PM	Mist eliminator	0.003 gr/dscf
		PM ₁₀	Good operating practices	0.003 gr/dscf
		PM _{2.5}		0.003 gr/dscf
		Opacity		5%
SN-41	Coil Coating Line – Cleaning Section	PM	Mist eliminator	0.003 gr/dscf
		PM ₁₀	Good operating practices	0.003 gr/dscf
		PM _{2.5}		0.003 gr/dscf
		Opacity		5%
SN-42	Coil Coating Line – Prime/Finish Coating	VOC	Enclosed painting system Thermal oxidation Good work practices	152.6 tpy
SN-43	Coil Coating Line Chemical Dryer	PM	Good combustion practices	0.0075 lb/MMBtu
		PM ₁₀	Energy efficient burners	0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity	Combustion of natural gas	5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x		0.1 lb/MMBtu

Source	Description	Pollutant	Control Technology	BACT Limit
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu
SN-44	Coil Coating Line Primer Oven	PM	Good combustion practices Energy efficient burners Combustion of natural gas	0.0075 lb/MMBtu
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	0.1 lb/MMBtu	
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu
SN-45	Coil Coating Line Finish Oven	PM	Good combustion practices Energy efficient burners Combustion of natural gas	0.0075 lb/MMBtu
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	0.1 lb/MMBtu	
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu
SN-46	Coil Coating Line RTO	PM	Good combustion practices Energy efficient burners Combustion of natural gas	0.009 lb/MMBtu
		PM ₁₀		0.009 lb/MMBtu
		PM _{2.5}		0.009 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	0.25 lb/MMBtu	
		GHG	Good operating practices	117 lb CO ₂ e/MMBtu

41. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific

Conditions #42 through #62. [Reg.18.801 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

SN	Description	Pollutant	lb/hr	tpy
SN-23b	Push Pull Pickle Line – Pickling Section	HCl	0.18	0.79
SN-24	Pickle Line Boiler	Single HAP Total Other HAPs	0.01 0.01	0.02 0.02
SN-26	Pickling Section	HCl	0.12	0.51
SN-27	Galvanizing Line Boiler #1	Single HAP Total Other HAPs	0.01 0.01	0.02 0.02
SN-28	Galvanizing Line Boiler #2	Single HAP Total Other HAPs	0.01 0.01	0.02 0.02
SN-34	Batch Annealing Furnaces	Single HAP Total Other HAPs	0.01 0.01	0.04 0.05
SN-35	Natural Gas Space Heaters – Cold Mill	Single HAP Total Other HAPs	0.01 0.01	0.06 0.07
SN-37	Pickle Galvanizing Line Boiler	Single HAP Total Other HAPs	0.01 0.01	0.02 0.02
SN-38	Pickle Galvanizing Line – Scale Dust & Pickling Section	HCl	0.12	0.51
SN-42	Coil Coating Line – Prime/Finish Coating	Single HAP Total Other HAPs	6.1 13.2	26.8 57.9
SN-43	Coil Coating Line Chemical Dryer	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-44	Coil Coating Line Primer Oven	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-45	Coil Coating Line Finish Oven	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01
SN-46	Coil Coating Line RTO	Single HAP Total Other HAPs	0.01 0.01	0.01 0.01

42. Visible emissions may not exceed the limits specified in the following table of this permit as measured by EPA Reference Method 9. The permittee shall show compliance with this condition by combustion of natural gas only at SN-24, SN-27, SN-28, SN-34, SN-35, SN-37, SN-43, SN-44, SN-45, and SN-46, compliance with Specific Condition #43, and Plantwide Condition 5.

Source	Limit	Regulatory Citation
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SN-22, SN-23a, SN-23b, SN-24, SN-25, SN-26, SN-27, SN-28, SN-29, SN-30, SN-31, SN-32, SN-33, SN-34, SN-35, SN-37, SN-38, SN-39, SN-40, SN-41, SN-42, SN-43, SN-44, SN-45, SN-46	5%	Reg.19.901 <i>et seq.</i> and 40 C.F.R. § 52 Subpart E
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43. The permittee shall conduct weekly observations of the opacity from the buildings and/or process stacks containing the sources listed in Specific Condition 42 except specifically SN-24, SN-27, SN-28, and SN-37. If visible emissions are detected, then the permittee shall immediately conduct a 6-minute opacity reading in accordance with EPA Reference Method 9. The result of these observations or readings shall be recorded in a log that shall be kept on site and made available for inspection upon request. [Reg.19.705 and 40 C.F.R. 52, Subpart E]
44. The permittee shall record and maintain records of the amounts of natural gas combusted in the boilers, SN-24, SN-27, SN-28, and SN-37, during each month. These records shall be kept on site and available for inspection upon request. [Reg.19.304 and 40 C.F.R. § 60 Subpart Dc]
45. The permittee, for the coil coating line, SN-40 through SN-46, on and after the compliance date on which 40 C.F.R. § 60.8 requires the performance test to be completed shall not cause to be discharged to the atmosphere more than: 0.14 kg VOC/l of coating solids applied or 10% of the VOCs applied (90% emissions reduction) for each calendar month operated at the most recently demonstrated overall efficiency. [Reg.19.304 and 40 C.F.R. § 60 Subpart TT]
46. The permittee shall conduct an initial performance test as required under 40 C.F.R. § 60.8(a) and thereafter a performance test every calendar month for the coil coating line (SN-40 through SN-46) according to the procedures of 40 C.F.R. § 60.463. The permittee shall use the procedures specified in 40 C.F.R. § 60.463(c) (1) for determining the monthly volume-weighted average emissions of VOCs in kg/l of coating solids applied. The permittee shall use the procedures specified in 40 C.F.R. § 60.463(c) (2) to show compliance with the emission limits specified under 40 C.F.R. § 60.462(a)(2) or (3) and Specific Condition 45. The permittee shall use the method and procedures outlined in 40 C.F.R. § 60.466 during these tests as appropriate. NSPS Subpart TT states section 40 C.F.R. § 60.8 (d) and (f) do not apply to this testing. The initial testing must be

conducted in accordance with General Provision 3 of this permit. [Reg.19.304 and 40 C.F.R. § 60 Subpart TT]

47. The permittee shall compute and record the average VOC content of the coatings applied during each calendar month for coil coating line (SN-40 through SN-46) according the equations in 40 C.F.R. § 60.463 in compliance with the numerical limits specified in § 60.462(a)(2). [Reg.19.304 and 40 C.F.R. § 60 Subpart TT]
48. The permittee shall install, calibrate, operate, and maintain a device that continuously records the combustion temperature of the effluent gasses of the RTO on SN-46. This device shall have an accuracy $\pm 2.5^{\circ}\text{C}$ or ± 0.75 percent of the temperature being measured expressed in degrees Celsius, whichever is greater. The permittee shall record all periods (during actual coating operations) in excess of 3 hours duration which the average temperature in the RTO remains more than 28°C below the temperature at which the compliance was measured in the most recent measurement of the RTOs efficiency required in Specific Condition 46. [Reg.19.304 and 40 C.F.R. § 60 Subpart TT]
49. The permittee shall in the initial compliance report required by 40 C.F.R. § 60.8 include the weighted average of the VOC content of coatings used during a period of one calendar month for the coil coating line (SN-40 through SN-46). The permittee shall also include the data outlined in 40 CFR § 60.465(b). [Reg.19.304 and 40 C.F.R. § 60 Subpart TT]
50. Each coil coating line (SN-40 through SN-46) affected source subject to NESHAP Subpart SSSS must limit organic HAP emissions to the level specified below:
 - a. No more than 2 percent of the organic HAP applied for each month during the each 12-month compliance period (98 percent reduction); or
 - b. No more than 0.046 kilogram of organic HAP per liter of solids applied during each 12-month compliance period; or
 - c. If the permittee uses an oxidizer to control organic HAP emissions, operate the oxidizer such that an outlet organic HAP concentration of no greater than 20 parts per million by volume (ppmv) on a dry basis is achieved and the efficiency of the capture system is 100 percent.

[Reg.19.304 and 40 C.F.R. § 63.5120]

51. The permittee must demonstrate compliance with on these following standards for the coil coating line (SN-40 through SN-46)
 - a. Use of “as purchased” compliant coatings – Each coating material used during the 12- month compliance period does not exceed 0.046 kg HAP per liter solids.

- b. Use of “as applied” compliant coatings – Each coating material used does not exceed 0.046 kg HAP per liter solids on a rolling 12-month average as applied basis, determined monthly, or average of all coating materials used does not exceed 0.046 kg HAP per liter solids on a rolling 12-month average as applied basis, determined monthly.
- c. Use of a capture system and control device – Overall organic HAP control efficiency is at least 98 percent on a monthly basis for individual or groups of coil coating lines, or overall organic HAP control efficiency is at least 98 percent during performance tests conducted according to Table 1 to § 63.5170 and operating limits are achieved continuously for individual coil coating lines, or oxidizer outlet HAP concentration is no greater than 20 ppmv and there is 100-percent capture efficiency during performance tests conducted according to Table 1 to § 63.5170 and operating limits are achieved continuously for individual coil coating lines.
- d. Use of a combination of compliant coatings and control devices and maintaining an acceptable equivalent emission rate – Average equivalent emission rate does not exceed 0.046 kg HAP per liter solids on a rolling 12-month average as applied basis, determined monthly.

[Reg.19.304 and Table 1 to NESHAP Subpart SSSS]

- 52. The permittee must submit the reports and notifications specified in § 63.5180 for the coil coating line (SN-40 through SN-46). The facility must submit these notifications and reports to EPA through CEDRI as outlined in § 63.5181. The permittee must maintain all records specified in § 63.5190. [Reg.19.702 and 40 C.F.R. § 63 Subpart SSSS]
- 53. The facility is subject to the requirements of 40 C.F.R. § 63 Subpart CCC. The requirements of this subpart apply to, at minimum, the following sources: SN-23b, SN-26, and SN-38. [Reg.19.702 and 40 C.F.R. 63 Subpart CCC]
- 54. No owner or operator of a new or reconstructed affected continuous pickling line at a steel pickling facility shall cause or allow to be discharged into the atmosphere from the affected pickling line any gases that contain HCl in a concentration in excess of 6 ppmv or HCl at a mass emission rate that corresponds to a collection efficiency of less than 99 percent. [Reg.19.702 and 40 C.F.R. § 63.1158(a)]
- 55. The permittee must prepare an operation and maintenance plan for each emission control device associated with SN-23b, SN-26, and SN-38 as outlined in § 63.1160 (b) including an inspection of each scrubber at intervals of no less than 3 months. The permittee shall conduct an initial performance test for each process or emission control device to determine and demonstrate compliance with the emission limitation according to the requirements in § 63.7 of subpart A. Performance tests shall be conducted using the test methods specified in § 63.1161(d). [Reg.19.702 and 40 C.F.R. § 63 Subpart CCC]

56. The permittee must submit the reports and notifications specified in § 63.1163 for SN-23b, SN-26, and SN-38. The facility must submit these notifications and reports to EPA through CEDRI as outlined in § 63.1164. The permittee must maintain all records specified in § 63.1165. [Reg.19.702 and 40 C.F.R. § 63 Subpart CCC]
57. The permittee shall test the Boilers SN-24, SN-27, SN-28, and SN-37 for PM_{2.5}, CO, and NO_x emissions. This test shall be conducted in accordance with Plantwide Condition 3 and EPA Reference Method 202, 10, and 7E for PM_{2.5}, CO, and NO_x respectively and repeated every 5 years after the initial test. The test for PM_{2.5} shall include filterable and condensable emissions. [Reg.19.702 and 40 C.F.R. § 52 Subpart E]
58. The permittee shall test SN-23b, SN-26, and SN-38 for HCl emissions. This test shall be conducted in accordance with Plantwide Condition 3 and EPA Reference Method 26. [Reg.18.1002 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]
59. The facility is subject to the requirements of 40 C.F.R. § 63 Subpart DDDDD. The requirements of this subpart apply to, at minimum, the following sources: SN-24, SN-27, SN-28, and SN-37. [Reg.19.702 and 40 C.F.R. § 63 Subpart DDDDD]
60. The permittee shall conduct a tune-up of the boilers (SN-24, SN-27, SN-28, and SN-37) or process heaters annually as specified in § 63.7540. Units in either the Gas 1 or Metal Process Furnace subcategories will conduct this tune-up as a work practice for all regulated emissions under this subpart. Units in all other subcategories will conduct this tune-up as a work practice for dioxins/furans. [Reg.19.702, 40 C.F.R. § 63.7500(a)(1) and Table 3 to Subpart DDDDD]
61. The permittee must conduct each annual tune-up of each boiler, (SN-24, SN-27, SN-28, and SN-37) no more than 13 months after the previous tune-up. The tune-up must be conducted as follows:
 - a. While burning the type of fuel that provided the majority of the heat input to the boiler over the 12 months prior to the tune-up.
 - b. As applicable, inspect the burner, and clean or replace any components of the burner as necessary.
 - c. Inspect the flame pattern, as applicable, and adjust the burner as necessary to optimize the flame pattern. The adjustment should be consistent with the manufacturer's specifications, if available.
 - d. Inspect the system controlling the air-to-fuel ratio as applicable and ensure that it is correctly calibrated and functioning properly.

- e. Optimize total emissions of CO. The optimization should be consistent with the manufacturer's specifications, if available, and with any NOX requirement to which the unit is subject.
- f. Measure the concentrations in the effluent stream of CO in parts per million, by volume, and oxygen in volume percent, before and after the adjustments are made (measurements may be either on a dry or wet basis, as long as it is the same basis before and after the adjustments are made). Measurements may be taken using a portable CO analyzer
- g. Maintain on-site and submit, if requested by the Division, a report containing the following information:
 - i. The concentrations of CO in the effluent stream in parts per million by volume, and oxygen in volume percent, measured at high fire or typical operating load, before and after the tune-up of the boiler or process heater;
 - ii. A description of any corrective actions taken as a part of the tune-up; and
 - iii. The type and amount of fuel used over the 12 months prior to the tune-up, but only if the unit was physically and legally capable of using more than one type of fuel during that period. Units sharing a fuel meter may estimate the fuel used by each unit.

[Reg.19.702 and 40 C.F.R. § 63.7540]

62. The permittee must submit all notifications and reports as outlined in 40 C.F.R. §§ 63.7545 and 63.7550 respectively for SN-24, SN-27, SN-28, and SN-37. The permittee must keep a record of each notification and report submitted, including all documentation supporting any notifications or semiannual compliance reports. The records must be in a form suitable and ready for expeditious review and kept for a period of 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record. The permittee must keep each record on site, or they must be accessible from on site, for at least 2 years after the date of each occurrence, measurement, corrective action, report, or record. Records may be kept offsite for the remaining 3 years. [Reg.19.702 and 40 C.F.R. § 63 Subpart DDDDD]

Cooling Towers

SN-51 Casting Process Cooling Tower 1
SN-52 Casting Process Cooling Tower 2
SN-53 Casting Process Cooling Tower 3
SN-54 Casting Process Cooling Tower 4

SN-55 Melt Shop Cooling Tower 1
SN-56 Melt Shop Cooling Tower 2: Gas Cleaning Plant (GCP)
SN-62 Melt Shop Cooling Tower 3: Spray Cooled EAF (Duct Only)
SN-63 Melt Shop Cooling Tower 4: EAF/LMF 1 and DOC Spray
SN-64 Melt Shop Cooling Tower 5: EAF Closed Loop for Electrode Arms
SN-65 Melt Shop Cooling Tower 6: Vacuum Tank Degasser

SN-57 Caster Cooling Tower 1
SN-58 Caster Cooling Tower 2
SN-66 Caster Cooling Tower 3
SN-67 Caster Cooling Tower 4

SN-59 Cold Mill Cooling Tower 1
SN-60 Cold Mill Cooling Tower 2
SN-61 Cold Mill Cooling Tower 3

SN-68 Cold Mill Cooling Tower 4: Coil Coating Line Cooling Tower

SN-133 DRI Process Water Cooling Tower

Source Description

SN-51 through SN-54 includes four cooling towers used to support the Casting Process. Each cooling tower has a circulation rate of approximately 2,000,000 gallons per hour.

SN-55 is a 499,800 gallon per hour Non-Contact Induced Draft Cooling Tower.

SN-56 is an 885,000 gallon per hour Non-Contact Induced Draft Cooling Tower.

SN-57 is a 1,104,240 gallon per hour Non-Contact Induced Draft Cooling Tower.

SN-58 is a 1,500,000 gallon per hour Non-Contact Induced Draft Cooling Tower.

SN-59 through SN-61 are 806,780 gallon per hour Non-Contact Induced Draft Cooling Towers.

SN-62 is a 813,125 gallon per hour Non-Contact Induced Draft Cooling Tower.

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SN-63 is a 2,500,000 gallon per hour Non-Contact Induced Draft Cooling Tower.

SN-64 is a 600,000 gallon per hour Non-Contact Induced Draft Cooling Tower.

SN-65 is a 274,740 gallon per hour Contact Induced Draft Cooling Tower.

SN-66 is a 307,800 gallon per hour Contact Induced Draft Cooling Tower.

SN-67 is a 450,000 gallon per hour Contact Induced Draft Cooling Tower.

SN-68 is a 75,000 gallon per hour Contact Induced Draft Cooling Tower

SN-133 is a 1,200,000 gallon per hour Contact Induced Draft Cooling Tower

Specific Conditions

63. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific Conditions #65 and #66. [Reg.19.501 *et seq.* and 40 C.F.R. § 52 Subpart E]

SN	Description	Pollutant	lb/hr	tpy
SN-51	Casting Process Cooling Tower 1	PM	0.8	3.3
		PM ₁₀	0.8	3.3
		PM _{2.5}	0.8	3.3
SN-52	Casting Process Cooling Tower 2	PM	0.8	3.3
		PM ₁₀	0.8	3.3
		PM _{2.5}	0.8	3.3
SN-53	Casting Process Cooling Tower 3	PM	0.8	3.3
		PM ₁₀	0.8	3.3
		PM _{2.5}	0.8	3.3
SN-54	Casting Process Cooling Tower 4	PM	0.8	3.3
		PM ₁₀	0.8	3.3
		PM _{2.5}	0.8	3.3
SN-55	Melt Shop Cooling Tower 1	PM	0.1	0.5
		PM ₁₀	0.1	0.5

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SN	Description	Pollutant	lb/hr	tpy
		PM _{2.5}	0.1	0.5
SN-56	Melt Shop Cooling Tower 2: Gas Cleaning Plant (GCP)	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
SN-57	Caster Cooling Tower 1	PM	0.3	1.0
		PM ₁₀	0.3	1.0
		PM _{2.5}	0.3	1.0
SN-58	Caster Cooling Tower 2	PM	0.6	2.5
		PM ₁₀	0.6	2.5
		PM _{2.5}	0.6	2.5
SN-59	Cold Mill Cooling Tower 1	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
SN-60	Cold Mill Cooling Tower 2	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
SN-61	Cold Mill Cooling Tower 3	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
SN-62	Melt Shop Cooling Tower 3: Spray Cooled EAF (Dcut Only)	PM	0.2	0.8
		PM ₁₀	0.2	0.8
		PM _{2.5}	0.2	0.8
SN-63	Melt Shop Cooling Tower 4: EAF/LMF 1 and DOC Spray	PM	1.0	4.1
		PM ₁₀	1.0	4.1
		PM _{2.5}	1.0	4.1
SN-64	Melt Shop Cooling Tower 5: EAF Closed Loop for	PM	0.2	0.6
		PM ₁₀	0.2	0.6

SN	Description	Pollutant	lb/hr	tpy
	Electrode Arms	PM _{2.5}	0.2	0.6
SN-65	Melt Shop Cooling Tower 6: Vacuum Tank Degasser	PM	0.1	0.3
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.3
SN-66	Caster Cooling Tower 3	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
SN-67	Caster Cooling Tower 4	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
SN-68	Cold Mill Cooling Tower 4: Coil Coating Line	PM	0.1	0.3
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.3
SN-133	DRI Process Water Cooling Tower	PM	0.7	3.0
		PM ₁₀	0.7	3.0
		PM _{2.5}	0.7	3.0

64. The permittee shall not exceed the emission rates set forth in the following table and must install the control devices or implement the pollution prevention measures set forth in the following table. Compliance with these emission limits shall be demonstrated by compliance with Specific Conditions #65 and #66.

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
SN-52 through SN-68 SN-133	Cooling Towers	PM	Drift Eliminators	0.0005% drift loss
		PM ₁₀	Low TDS	
		PM _{2.5}		
		Opacity		5%

65. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific Condition 66. [Reg.19.901 *et seq.* and 40 C.F.R. § 52 Subpart E]

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SN	Description	TDS Limit
SN-51	Casting Process Cooling Tower 1	8800
SN-52	Casting Process Cooling Tower 2	8800
SN-53	Casting Process Cooling Tower 3	8800
SN-54	Casting Process Cooling Tower 4	8800
SN-55	Melt Shop Cooling Tower 1	4800
SN-56	Melt Shop Cooling Tower 2: Gas Cleaning Plant (GCP)	4800
SN-57	Caster Cooling Tower 1	4800
SN-58	Caster Cooling Tower 2	8800
SN-59	Cold Mill Cooling Tower 1	4800
SN-60	Cold Mill Cooling Tower 2	4800
SN-61	Cold Mill Cooling Tower 3	4800
SN-62	Melt Shop Cooling Tower 3: Spray Cooled EAF (Duct Only)	4800
SN-63	Melt Shop Cooling Tower 4: EAF/LMF 1 and DOC Spray	8800
SN-64	Melt Shop Cooling Tower 5: EAF Closed Loop for Electrode Arms	4800
SN-65	Melt Shop Cooling Tower 6: Vacuum Tank Degasser	5600
SN-66	Caster Cooling Tower 3	6800
SN-67	Caster Cooling Tower 4	4800

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SN	Description	TDS Limit
SN-68	Cold Mill Cooling Tower 4: Coil Coating Line	4800
SN-133	DRI Process Water Cooling Tower	2200

66. The permittee test the TDS of each of the cooling towers initially and every 6 months thereafter. This testing shall be conducted in accordance with Plantwide Condition 3 with a method approved by the Division before the first test is performed. [Reg.19.705, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 70.6]
67. Visible emissions may not exceed the limits specified in the following table of this permit as measured by EPA Reference Method 9. Compliance with this condition will be shown by proper maintenance according to the defined maintenance procedures and Plantwide Condition 5.

Source	Limit	Regulatory Citation
SN-51, SN-52, SN-53, SN-54, SN-55, SN-56, SN-57, SN-58, SN-59, SN-60, SN-61, SN-62, SN-63, SN-64, SN-65, SN-66, SN-67, SN-68, SN-133	5%	Reg.19.901 <i>et seq.</i> and 40 C.F.R. § 52 Subpart E

Emergency Operations

SN-69 Emergency Generator 1
SN-70 Emergency Generator 2
SN-71 Emergency Generator 3
SN-72 Emergency Generator 4
SN-73 Emergency Generator 5
SN-74 Emergency Generator 6
SN-75 Emergency Generator 7
SN-76 Emergency Generator 8
SN-77 Emergency Generator 9
SN-78 Emergency Generator 10

SN-79 Emergency Generator 11
SN-80 Emergency Generator 12
SN-81 Emergency Generator 13
SN-82 Emergency Generator 14
SN-83 Emergency Generator 15
SN-84 Emergency Generator 16

SN-85 Emergency Water Pump 1
SN-86 Emergency Water Pump 2
SN-87 Emergency Water Pump 3
SN-88 Emergency Water Pump 4
SN-89 Emergency Water Pump 5
SN-90 Emergency Water Pump 6

SN-135 DRI Process Emergency Generator
SN-136 DRI Process Emergency Water Pump

Source Description

The steel mill project requires emergency generators and water pumps for emergency support. The emergency equipment is fueled with ultra-low sulfur diesel oil and will operate only a limited number of hours (100 hours per year or less) for testing purposes under normal conditions. The seventeen emergency generators, SN-69 through SN-84 and SN-135, are rated at 2700 kW (3621 HP) each. The seven emergency water pumps, SN-85 through SN-90 and SN-136, are rated at 281 kW (376 HP) each.

Specific Conditions

68. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific Conditions #72 and #75 through #78. [Reg.19.501 *et seq.* and 40 C.F.R. § 52 Subpart E]

SN	Description	Pollutant	lb/hr	tpy
SN-69	Emergency Generator 1	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-70	Emergency Generator 2	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-71	Emergency Generator 3	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-72	Emergency Generator 4	PM	0.9	0.1
		PM ₁₀	0.9	0.1

SN	Description	Pollutant	lb/hr	tpy
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-73	Emergency Generator 5	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-74	Emergency Generator 6	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-75	Emergency Generator 7	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1

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SN	Description	Pollutant	lb/hr	tpy
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-76	Emergency Generator 8	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-77	Emergency Generator 9	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-78	Emergency Generator 10	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195

SN	Description	Pollutant	lb/hr	tpy
SN-79	Emergency Generator 11	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-80	Emergency Generator 12	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-81	Emergency Generator 13	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-82	Emergency Generator 14	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1

SN	Description	Pollutant	lb/hr	tpy
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-83	Emergency Generator 15	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-84	Emergency Generator 16	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-85	Emergency Water Pump 1	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2

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SN	Description	Pollutant	lb/hr	tpy
		NO _x	11.7	0.6
		CO _{2e}	-	8
SN-86	Emergency Water Pump 2	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO _{2e}	-	8
SN-87	Emergency Water Pump 3	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO _{2e}	-	8
SN-88	Emergency Water Pump 4	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO _{2e}	-	8
SN-89	Emergency Water	PM	0.9	0.1

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SN	Description	Pollutant	lb/hr	tpy
	Pump 5	PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO _{2e}	-	8
SN-90	Emergency Water Pump 6	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO _{2e}	-	8
SN-135	DRI Diesel Fired Emergency Generator	PM	0.8	0.1
		PM ₁₀	0.8	0.1
		PM _{2.5}	0.8	0.1
		SO ₂	0.1	0.1
		VOC	1.1	0.1
		CO	7.3	0.4
		NO _x	31.5	1.6
		CO _{2e}	-	195
SN-136	DRI Emergency Water Pump	PM	0.9	0.1
		PM ₁₀	0.9	0.1
		PM _{2.5}	0.9	0.1
		SO ₂	0.8	0.1

SN	Description	Pollutant	lb/hr	tpy
		VOC	1.0	0.1
		CO	2.6	0.2
		NO _x	11.7	0.6
		CO ₂ e	-	8

69. The permittee shall not exceed the emission rates set forth in the following table and must install the control devices or implement the pollution prevention measures set forth in the following table. Compliance with these emission limits shall be demonstrated by compliance with Specific Conditions #72 and #75 through #78

BACT Analysis Summary				
Source	Description	Pollutant	Control Technology	BACT Limit
SN-69 through SN-84, SN-135	Emergency Generators	PM	Good Operating Practices, limited hours of operation, Compliance with NSPS Subpart III	0.1 g/bhp-hr
		PM ₁₀		0.1 g/bhp-hr
		PM _{2.5}		0.1 g/bhp-hr
		Opacity		20%
		SO ₂		<15 ppm sulfur in fuel
		VOC		0.13 g/bhp-hr
		CO		0.9 g/bhp-hr
		NO _x	3.9 g/bhp-hr	
		CO ₂ e	Good Combustion Practices	164 lb CO ₂ e/MMBtu
SN-85 through SN-90, SN-136	Emergency Water Pumps	PM	Good Operating Practices, limited hours of operation, Compliance with NSPS Subpart III	1 g/bhp-hr
		PM ₁₀		1 g/bhp-hr
		PM _{2.5}		1 g/bhp-hr
		Opacity		20%
		SO ₂		<15 ppm sulfur in fuel
		VOC		1.12 g/bhp-hr
		CO		3.03 g/bhp-hr
		NO _x	14.06 g/bhp-hr	
		CO ₂ e	Good Combustion Practices	164 lb CO ₂ e/MMBtu

70. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific

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Conditions #72 and #75 through #78. [Reg.18.801 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

SN	Description	Pollutant	lb/hr	tpy
SN-69	Emergency Generator 1	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-70	Emergency Generator 2	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-71	Emergency Generator 3	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-72	Emergency Generator 4	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-73	Emergency Generator 5	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-74	Emergency Generator 6	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-75	Emergency Generator 7	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-76	Emergency Generator 8	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-77	Emergency Generator 9	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-78	Emergency Generator 10	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-79	Emergency Generator 11	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-80	Emergency Generator 12	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-81	Emergency Generator 13	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-82	Emergency Generator 14	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-83	Emergency Generator 15	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-84	Emergency Generator 16	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-85	Emergency Water Pump 1	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-86	Emergency Water Pump 2	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-87	Emergency Water Pump 3	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-88	Emergency Water Pump 4	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01

SN	Description	Pollutant	lb/hr	tpy
SN-89	Emergency Water Pump 5	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-90	Emergency Water Pump 6	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01
SN-135	DRI Diesel Fired Emergency Generator	Single HAP	0.01	0.01
		Total Other HAPs	0.02	0.01
SN-136	DRI Emergency Water Pump	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01

71. The permittee shall not exceed 20% opacity from the Sources SN-69 through SN-90, SN-135, and SN-136. Compliance with this condition will be shown by combustion of low sulfur diesel fuel only and Plantwide Condition 5. [Reg.19.901 *et seq.* and 40 C.F.R. § 52 Subpart E]
72. The permittee shall not operate the emergency generators SN-69 through SN-90, SN-135, and SN-136 in excess of 100 total hours each, for maintenance and readiness testing, per calendar year in order to demonstrate compliance with the annual emission rate limits. Emergency operation in excess of these hours may be allowable but shall be reported and will be evaluated in accordance with Reg.19.602 and other applicable regulations. [Reg.19.705, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 70.6]
73. The permittee shall maintain monthly records to demonstrate compliance with Specific Condition #72. The permittee shall update these records by the fifteenth day of the month following the month to which the records pertain. The calendar year totals and each individual month's data shall be maintained on-site, made available to Division of Environmental Quality personnel upon request, and submitted in accordance with General Provision #7. [Reg.19.705 and 40 C.F.R. § 52 Subpart E]
74. The permittee shall comply with the provisions of 40 C.F.R. Part 63 Subpart ZZZZ for SN-69 through SN-90, SN-135, and SN-136 by complying with the provisions of 40 C.F.R. Part 60 Subpart IIII. [Reg.19.304 and 40 C.F.R. § 63 Subpart ZZZZ]
75. The permittee shall comply with the emissions standards specified in § 60.4202 of 40 C.F.R. Part 60 Subpart IIII for SN-69 through SN-90, SN-135, and SN-136. The permittee shall operate and maintain the emergency equipment, SN-69 through SN-90, SN-135, and SN-136 according to the manufacturer's written instruction or procedures developed by the permittee and approved by the generator manufacturer, over the life of the entire engine. [Reg.19.304 and 40 C.F.R. § 60 Subpart IIII]
76. The permittee shall install a non-resettable hour meter on the emergency equipment, SN-69 through SN-90, SN-135, and SN-136. [Reg.19.304 and 40 C.F.R. § 60 Subpart IIII]

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77. The permittee shall use a diesel fuel that meets the requirements of 40 C.F.R. 80.510(b) in the emergency equipment, SN-69 through SN-90, SN-135, and SN-136. [Reg.19.304 and 40 C.F.R. § 60 Subpart III]

78. If the emergency equipment, SN-69 through SN-90, SN-135, and SN-136 are equipped with a diesel particulate filter to comply with emission standards, the diesel particulate filter must be installed with a back pressure monitor that notifies the permittee when the high backpressure limit of the engine is approached. [Reg.19.304 and 40 C.F.R. § 60 Subpart III]

Miscellaneous Operations

SN-91 Charging Crane
SN-92 Scrap Yard Stockpiling

SN-93 EAF Flux Receiving System
SN-94 EAF Flux Storage and Handling System
SN-95 Carbon Injection Receiving System
SN-96 Carbon Injection Storage and Handling System
SN-97 LMF Flux Receiving System
SN-98 LMF Flux Storage and Handling System
SN-99 Alloy Receiving System
SN-100 Alloy Storage and Handling System
SN-101 Alloy Delivery System – LMF
SN-102 Degasser Alloy Delivery System
SN-103 EAF Lime Injection Receiving, Storage, and Handling System

SN-104 Inside Drop Point – Spent Refractory and Other Waste
SN-105 Outside Drop Point – Spent Refractory and Other Waste
SN-106 Inside Drop Point – EAF Dust
SN-107 Wind Erosion
SN-108 Drop Points Slag
SN-109 Slag Handling and Conveying
SN-110 Slag Storage Piles

SN-113 HCl Storage Tanks
SN-114 Hydrogen Plant #1 Reformer Furnace (PHG830)
SN-115 Gasoline Storage Tanks and Dispensing Operation

Source Description

The Charging Crane, SN-91, loads scrap from the scrap yard for charging into the EAF. The Scrap Yard Stockpiling, SN-92, is the emissions from loading of scrap steel from trucks or railcars to the scrapyards.

The EAF Flux Receiving System, SN-93, includes the truck and rail unloading of the flux materials for the EAF. The EAF Flux Storage and Handling System, SN-94, includes the transport and storage of the flux materials for the EAF. A total of 10 silos will store HBI/DRI, dolomite, and lime. Each silo has a capacity of 9,000 cubic feet and will be equipped with bin vent filters.

The Carbon Injection Receiving System, SN-95, includes the truck and rail unloading of the carbon for the carbon injection into the EAF. The Carbon Injection Storage and Handling

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System, SN-96, includes the transport of the carbon for the EAF. There are four storage silos each with a capacity of 8,000 cubic feet.

The LMF Flux Receiving System, SN-97, includes the truck and rail loading of the flux materials for the LMF. The LMF Flux Storage and Handling System, SN-98, includes the transport and storage of the flux materials for the EAF. Six silos store bauxite, CAL/A, dolomite, and lime. Each silo has a capacity of 9,000 cubic feet and are equipped with bin vent filters.

The Alloy Receiving System, SN-99, includes the truck and rail unloading of the alloy materials for the LMF. The Alloy Storage and Handling System, SN-100, includes the transport and storage of the alloy materials for the EAF. A total of seven silos store FeSn, SiMn, and FeCr. Each silo has a capacity of 9,000 cubic feet and is equipped with bin vent filters.

The Alloy Delivery System – LMF, SN-101, delivers alloy materials to support the LMF operations. A stocking pocket belt conveyor is used to transfer the materials from the silos to weight hoppers to be loaded into the LMF stations. The Degasser Alloy Delivery System, SN-102, delivers alloy materials into the degasser. A stocking pocket conveyor is used to transfer materials to the feed hoppers that feed the degasser.

The EAF Lime Injection Receiving, Storage, and Handling System, SN-103, accounts for emissions from the transport and storage of the various types of lime for the EAFs. The Drop Points and Storage Piles Sources, SN-104 through SN-110, account for emissions from the placement of materials into indoor and outdoor storage piles as well as wind erosion.

The Hydrogen Plant #1 Reformer Furnace, SN-114, includes six natural gas fired units with a heat input of 12.5 MMBtu/hr each or 75 MMBtu/hr total. Five units operate on a normal basis and the sixth unit is for backup purposes and will not operate unless one of the five is down for maintenance.

The gasoline storage and gasoline dispensing operation, SN-115, includes several tanks which vary in size from a few hundred gallons up to several thousand gallons. This source also includes a 500 gallon gasoline storage tank and dispensing operation associated with the steel mills slag handling operation.

Specific Conditions

79. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific Conditions #82 and #83 and Plantwide Condition #5. [Reg.19.501 *et seq.* and 40 C.F.R. § 52 Subpart E]

SN	Description	Pollutant	lb/hr	tpy
SN-91	Charging Crane	PM	0.1	0.1

SN	Description	Pollutant	lb/hr	tpy
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-92	Scrap Yard Stockpiling	PM	0.2	0.9
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.1
SN-93	EAF Flux Receiving System Fabric Filter	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-94	EAF Flux Storage and Handling System Bin Vent Filter	PM	0.3	1.3
		PM ₁₀	0.3	1.0
		PM _{2.5}	0.2	0.8
SN-95	Carbon Injection Receiving System Fabric Filter	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-96	Carbon Injection Storage and Handling System Bin Vent Filter	PM	0.2	0.5
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
SN-97	LMF Flux Receiving System Fabric Filter	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-98	LMF Flux Storage and Handling System Fabric and Bin Vent Filters	PM	0.3	1.0
		PM ₁₀	0.2	0.7
		PM _{2.5}	0.2	0.5
SN-99	Alloy Receiving System Fabric Filter	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-100	Alloy Storage and	PM	0.2	0.6

SN	Description	Pollutant	lb/hr	tpy
	Handling System Fabric and Bin Vent Filters	PM ₁₀	0.2	0.6
		PM _{2.5}	0.2	0.6
SN-101	Alloy Delivery System – LMF Fabric and Bin Vent Filters	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-102	Degasser Alloy Delivery System Fabric and Bin Vent Filters	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-103	EAF Lime Injection Receiving, Storage, and Handling System Fabric and Bin Vent Filters	PM	0.1	0.4
		PM ₁₀	0.1	0.4
		PM _{2.5}	0.1	0.4
SN-104	Inside Drop Point – Spent Refractory and Other Waste	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-105	Outside Drop Point – Spent Refractory and Other Waste	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-106	Inside Drop Point – EAF Dust	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
SN-107	Wind Erosion	PM	0.9	3.7
		PM ₁₀	0.5	1.9
		PM _{2.5}	0.1	0.3
SN-108	Drop Points Slag	PM	1.1	3.4
		PM ₁₀	0.5	1.7

SN	Description	Pollutant	lb/hr	tpy
		PM _{2.5}	0.1	0.6
SN-109	Slag Handling and Conveying	PM	1.1	1.2
		PM ₁₀	0.4	0.4
		PM _{2.5}	0.1	0.1
SN-110	Wind Erosion – Slag Storage Piles	PM	0.2	0.6
		PM ₁₀	0.1	0.3
		PM _{2.5}	0.1	0.1
SN-114	Hydrogen Plant #1 Reformer Furnace	PM	0.6	2.5
		PM ₁₀	0.6	2.5
		PM _{2.5}	0.6	2.5
		SO ₂	0.1	0.2
		VOC	0.4	1.8
		CO	6.2	27.1
		NO _x	7.5	32.9
Lead	3.68E-05	1.61E-04		
SN-115	Gasoline Storage Tanks and Dispensing Operations	VOC	0.2	0.7

80. The permittee shall not exceed the emission rates set forth in the following table and must install the control devices or implement the pollution prevention measures set forth in the following table. Compliance with these emission limits shall be demonstrated by compliance with Specific Conditions #82 and #83 and Plantwide Condition #5.

Source	Description	Pollutant	Control Technology	BACT Limit
SN-91	Charging Crane	PM	Dust Control Plan	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-92	Scrap Yard Stockpiling	PM	Dust Control Plan	0.81 tpy
		PM ₁₀		0.38 tpy

Source	Description	Pollutant	Control Technology	BACT Limit
		PM _{2.5}		0.06 tpy
		Opacity		20%
SN-93	EAF Flux Receiving System	PM	Dust Control Plan, Enclosed Receiving, System with Fabric Filter	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		5%
SN-94	EAF Flux Storage and Handling System	PM	Dust Control Plan, Enclosed Conveyors with Fabric Filters, Silos with Bin Vent Filters	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%
SN-95	Carbon Injection Receiving System	PM	Dust Control Plan, Enclosed Receiving, System with Fabric Filter	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		5%
SN-96	Carbon Injection Storage and Handling System	PM	Dust Control Plan, Enclosed Conveyors with Fabric Filters, Silos with Bin Vent Filters	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%
SN-97	LMF Flux Receiving System	PM	Dust Control Plan, Enclosed Receiving, System with Fabric Filter	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		5%
SN-98	LMF Flux Storage and Handling System	PM	Dust Control Plan, Enclosed Conveyors with Fabric Filters, Silos with Bin Vent Filters	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%
SN-99	Alloy Receiving System	PM	Dust Control Plan, Enclosed Receiving, System with Fabric Filter	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		5%
SN-100	Alloy Storage and Handling System	PM	Dust Control Plan, Enclosed Conveyors with Fabric Filters, Silos with Bin Vent Filters	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%

Source	Description	Pollutant	Control Technology	BACT Limit
SN-101	Alloy Delivery System – LMF	PM	Dust Control Plan, Enclosed Conveyors with Fabric Filters, Enclosed Receiving System with Fabric Filter, Silos with Bin Vent Filters	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%
SN-102	Degasser Alloy Delivery System	PM	Dust Control Plan, Enclosed Conveyors with Fabric Filters, Enclosed Receiving System with Fabric Filter, Silos with Bin Vent Filters	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%
SN-103	EAF Lime Injection Receiving, Storage, and Handling System	PM	Fabric Filter Enclosed Conveyors with Compressed Air, Dust control Plan, Bin Vent Filter on Each Silo	0.01 gr/dscf
		PM ₁₀		0.01 gr/dscf
		PM _{2.5}		0.01 gr/dscf
		Opacity		5%
SN-104	Inside Drop Point – Spent Refractory and Other Waste	PM	Dust Control Plan	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-105	Outside Drop Point – Spent Refractory and Other Waste	PM	Dust Control Plan	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-106	Inside Drop Point – EAF Dust	PM	Dust Control Plan	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-107	Wind Erosion	PM	Dust Control Plan	3.7 tpy
		PM ₁₀		1.84 tpy
		PM _{2.5}		0.28 tpy
		Opacity		20%
SN-108	Drop Points Slag	PM	Dust Control Plan	3.39 tpy
		PM ₁₀		1.63 tpy

Source	Description	Pollutant	Control Technology	BACT Limit
		PM _{2.5}		0.54 tpy
		Opacity		20%
SN-109	Slag Handling and Conveying	PM	Dust Control Plan	1.11 tpy
		PM ₁₀		0.37 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-110	Slag Storage Piles	PM	Dust Control Plan	0.58 tpy
		PM ₁₀		0.29 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-114	Hydrogen Plant #1 Reformer Furnace (PHG830)	PM	Combustion of Natural gas and Good Combustion Practice	0.0075 lb/MMBtu
		PM ₁₀		0.0075 lb/MMBtu
		PM _{2.5}		0.0075 lb/MMBtu
		Opacity		5%
		SO ₂		0.0006 lb/MMBtu
		VOC		0.0054 lb/MMBtu
		CO		0.0824 lb/MMBtu
		NO _x	Low NO _x burners Combustion of clean fuel Good Combustion Practices	0.1 lb/MMBtu
		CO ₂ e	Good Operating Practices	117 lb CO ₂ e/MMBtu
SN-115	Gasoline Storage Tanks and Dispensing Operation	VOC	Good Operating Practices, Vehicle On-Board Vapor Recovery or Stage II Vapor Recovery System	0.62 tpy

81. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific Conditions #82 and #83 and Plantwide Condition #5. [Reg.18.801 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

SN	Description	Pollutant	lb/hr	tpy
SN-113	HCl Storage Tanks	HCl	0.01	0.03

SN	Description	Pollutant	lb/hr	tpy
SN-114	Hydrogen Plant #1 Reformer Furnace	Single HAP	0.01	0.03
		Total Other HAPs	0.01	0.03
SN-115	Gasoline Storage Tanks and Dispensing Operations	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01

82. The permittee shall not receive more than material than in the table below in any consecutive rolling 12 month period. [Reg.19.901 *et seq.* and 40 C.F.R. § 52 Subpart E]

Source	Consecutive rolling 12 month limit (tons/year)
SN-93	175,830
SN-95	79,204
SN-97	175,830
SN-99	680,000
SN-103	210,240

83. The permittee shall maintain monthly records of the amount of materials received in the sources in Specific Condition 82. These records shall include the monthly total of material received and the rolling 12 month total of material received. These records shall be updated by the 15th day of the month following the month to which the records pertain, kept on site, made available to Division personnel upon request, and submitted in accordance with General Provision 7. [Reg.19.901 *et seq.* and 40 C.F.R. § 52 Subpart E]
84. Visible emissions may not exceed the limits specified in the following table of this permit as measured by EPA Reference Method 9. For SN-114, the opacity requirement is met by combustion of natural gas only. For all other listed sources, compliance with this condition will be shown by compliance with Specific Condition #85 and Plantwide Condition 5.

Source	Limit	Regulatory Citation
SN-93, SN-94, SN-95, SN-96, SN-97, SN-98, SN-99, SN-100, SN-101, SN-102, SN-103, SN-113, SN-114, SN-115	5%	Reg.19.901 <i>et seq.</i> and 40 C.F.R. § 52 Subpart E

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SN-91, SN-92, SN-104, SN-105, SN-106, SN-107, SN-108, SN-109, SN-110	20%	Reg.19.901 <i>et seq.</i> and 40 C.F.R. § 52 Subpart E
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85. The permittee shall conduct weekly observations of the opacity from the sources listed in Specific Condition #84. If visible emissions are detected, the permittee shall conduct a 6-minute opacity reading in accordance with Method 9 at the point where visible emissions were detected. The results of these observations shall be recorded in a log which shall be kept on site and made available for inspection upon request. [Reg.19.901 *et seq.* and 40 C.F.R. § 52 Subpart E]

86. The permittee may install sealed conveyors or sealed pneumatic conveyors that have no vents to the atmosphere. The permittee is not required to vent the conveyors to a baghouse if no vent is needed. [Reg.19.705, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 70.6]

87. The permittee shall implement a fugitive emission dust control plan to control dust emissions from the sources specified to require a dust control plan in Specific Condition 80. The fugitive emission dust control plan shall be maintained on-site, made available to Division of Environmental Quality personnel upon request, and submitted in accordance with General Provision #7. [Reg.19.705, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 70.6]

Roadway Sources

SN-111 Paved Roads
 SN-112 Unpaved Roads
 SN-134 Vehicle Travel on In-Plant Paved and Unpaved Roads

Source Description

SN-111 accounts for emissions from paved roadways and SN-112 accounts for emissions from unpaved roadways. SN-134 accounts for vehicle traffic on in-plant paved and unpaved roads associated with the DRI processes.

Specific Conditions

88. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by application of dust suppressant as necessary to control dust emissions. [Reg.19.501 *et seq.* and 40 C.F.R. § 52 Subpart E]

SN	Description	Pollutant	lb/hr	tpy
SN-111	Paved Roadways	PM	0.7	2.8
		PM ₁₀	0.2	0.6
		PM _{2.5}	0.1	0.2
SN-112	Unpaved Roadways	PM	2.2	9.7
		PM ₁₀	0.6	2.6
		PM _{2.5}	0.1	0.3
SN-134	Vehicle Travel on In-Plant Paved and Unpaved Roads	PM	0.1	0.2
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1

89. The permittee shall not exceed the emission rates set forth in the following table and must install the control devices or implement the pollution prevention measures set forth in the following table. Compliance with these emission limits shall be demonstrated by compliance with Specific Condition #90.

Source	Description	Pollutant	Control Technology	BACT Limit
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Source	Description	Pollutant	Control Technology	BACT Limit
SN-111	Paved Roadways	PM	Development and Implementation of Fugitive Dust Control Plan	2.8 tpy
		PM ₁₀		0.6 tpy
		PM _{2.5}		0.2 tpy
SN-112	Unpaved Roadways	PM	Development and Implementation of Fugitive Dust Control Plan	0.81 tpy
		PM ₁₀		0.38 tpy
		PM _{2.5}		0.06 tpy
SN-134	Vehicle Travel on In-Plant Paved and Unpaved Roads	PM	Development and Implementation of Fugitive Dust Control Plan	0.2 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy

90. The permittee shall implement a fugitive emission dust control plan to control dust emissions from the roadways. Implementation of the fugitive dust control plan is a demonstration of compliance with the referenced BACT limits. The fugitive emission dust control plan shall be maintained on-site, made available to Division of Environmental Quality personnel upon request, and submitted in accordance with General Provision #7. [Reg.19.705, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 70.6]

91. Nothing in this permit shall be construed to authorize a violation of the Arkansas Water and Air Pollution Control Act or the federal National Pollutant Discharge Elimination System (NPDES). [Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

DRI Process

SN-116 Ore Unloading and Product Loading Gantry Crane
SN-117 Oxide Unloading Bin and Dedusting
SN-118 Oxide Pellet Pile Transfer and Dedusting (Pre-Enclosed Storage)
SN-119 Oxide Transfer and Dedusting (Post-Enclosed Storage)
SN-120 Oxide and Remet Screening and Dedusting
SN-121 Furnace Charge Hopper Loading Silos
SN-122 Charge Hopper Dedusting

SN-123 Reformer Natural Gas Fired (1591 MMBtu/hr)
SN-124 Furnace Dedusting (BSG Dust Collection) Wet Scrubber
SN-125 Hot Pressure Relief Vent (Flare)
SN-126 Briquetter Dedusting
SN-127 HBI Cooling Conveyor 1 & 2

SN-128 Transfer & Product Screening Station No. 1 (Pre Pile)
SN-129 Transfer & Product Screening Station No. 2 (Post Pile)
SN-130 HBI Product Storage Pile
SN-131 Remet/Fines Storage

SN-132 Process Water Degasser

Source Description

The DRI process involves operations and equipment that are designed to produce an iron ore that can be used in the EAFs. The process primarily involves taking a solid form of iron ore and processing that iron ore through a tower reactor to produce the iron ore into a briquette form that can be used directly in the EAF to assist in achieving the specific type of steel grade. The process includes receiving, conveying, processing, and storing of the original form of the iron ore. The iron ore is processed through a tower reactor with a reducing gas from reformed natural gas. The product from the tower reactor is called Hot-briquetted iron (HBI) and is pressed into briquettes. The briquettes are stored and sent over to the Melt Shop for use in the two EAFs. The DRI is designed to produce approximately 2,200,000 tons of briquette. Amount of iron ore throughput is approximately 3,000,000 tons per year.

Specific Conditions

92. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific Conditions #97, #98, and #102 and Plantwide Condition #5. [Reg.19.501 *et seq.* and 40 C.F.R. § 52 Subpart E]

SN	Description	Pollutant	lb/hr	tpy
SN-116	Ore Unloading and Product Loading Gantry Crane	PM	1.3	5.7
		PM ₁₀	0.7	2.7
		PM _{2.5}	0.1	0.5
		Lead	6.51E-03	2.85E-02
SN-117	Oxide Unloading Bin and Dedusting Fabric Filter	PM	0.2	0.5
		PM ₁₀	0.2	0.5
		PM _{2.5}	0.2	0.5
		Lead	5.54E-04	2.43E-03
SN-118	Oxide Pellet Pile Transfer and Dedusting (Pre-Enclosed Storage) Fabric Filter	PM	0.3	1.1
		PM ₁₀	0.3	1.1
		PM _{2.5}	0.3	1.1
		Lead	1.26E-03	5.52E-03
SN-119	Oxide Unloading Bin and Dedusting Oxide Transfer and Dedusting (Post Domes) Fabric Filter	PM	0.2	0.5
		PM ₁₀	0.2	0.5
		PM _{2.5}	0.2	0.5
		Lead	5.54E-04	2.43E-03
SN-120	Oxide and Remet Screening and Dedusting Fabric Filter	PM	0.8	3.1
		PM ₁₀	0.8	3.1
		PM _{2.5}	0.8	3.1
		Lead	3.53E-03	1.54E-02
SN-121	Furnace Charge Hopper Loading Silos Fabric Filter	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
		Lead	7.05E-05	3.09E-04
SN-122	Charge Hopper Dedusting Fabric Filter	PM	0.1	0.5
		PM ₁₀	0.1	0.5
		PM _{2.5}	0.1	0.5

SN	Description	Pollutant	lb/hr	tpy
		SO ₂	0.3	1.1
		VOC	0.2	0.9
		CO	2.9	12.4
		NO _x	2.1	8.9
		Lead	5.56E-04	2.43E-03
		CO _{2e}	-	54,701
SN-123	Reformer Natural Gas Fired (1591 MMBtu/hr) Scrubber	PM	8.1	35.3
		PM ₁₀	8.1	35.3
		PM _{2.5}	8.1	35.3
		SO ₂	10.6	32.2
		VOC	8.2	35.6
		CO	124.1	543.2
		NO _x	88.7	388.3
		Lead	2.29E-03	7.00E-03
		CO _{2e}	-	1,680,207
SN-124	Furnace Dedusting (BSG Dust Collection) Scrubber	PM	2.5	11.0
		PM ₁₀	2.5	11.0
		PM _{2.5}	2.5	11.0
		SO ₂	0.3	1.1
		VOC	0.2	0.9
		CO	2.9	12.4
		NO _x	2.1	8.9
		Lead	1.26E-02	5.50E-02
		CO _{2e}	-	54,701
SN-125	Hot Pressure Relief Vent (Flare) Scrubber	PM	0.6	0.1
		PM ₁₀	0.6	0.1
		PM _{2.5}	0.6	0.1

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SN	Description	Pollutant	lb/hr	tpy
		SO ₂	0.1	0.1
		VOC	0.1	0.1
		CO	316.0	8.8
		NO _x	24.9	1.0
		Lead	2.25E-07	9.86E-07
		CO _{2e}	-	762
SN-126	Briquetter Dedusting Scrubber	PM	4.0	17.4
		PM ₁₀	4.0	17.4
		PM _{2.5}	4.0	17.4
		SO ₂	0.2	0.6
		VOC	0.1	0.4
		CO	1.5	6.2
		NO _x	1.1	4.5
		Lead	1.99E-02	8.70E-02
		CO _{2e}	-	27,350
SN-127	HBI Cooling Conveyor 1 and 2 Scrubber	PM	1.9	8.4
		PM ₁₀	1.9	8.4
		PM _{2.5}	1.9	8.4
		Lead	1.90E-02	8.34E-02
SN-128	Transfer and Product Screening Station No 1 Fabric Filter	PM	0.4	1.8
		PM ₁₀	0.4	1.8
		PM _{2.5}	0.4	1.8
		Lead	2.02E-03	8.83E-03
SN-129	Transfer and Product Screening Station No 1 Fabric Filter	PM	0.4	1.8
		PM ₁₀	0.4	1.8
		PM _{2.5}	0.4	1.8
		Lead	2.02E-03	8.83E-03

SN	Description	Pollutant	lb/hr	tpy
SN-130	HBI Product Storage Pile	PM	0.3	1.2
		PM ₁₀	0.2	0.6
		PM _{2.5}	0.2	0.6
		Lead	1.29E-03	5.66E-03
SN-131	Remet/Fines Storage	PM	0.1	0.1
		PM ₁₀	0.1	0.1
		PM _{2.5}	0.1	0.1
		Lead	1.60E-04	7.01E-04
SN-132	Process Water Degasser	CO	24.3	106.5
		CO _{2e}	-	2230

93. The permittee shall not exceed the emission rates set forth in the following table and must install the control devices or implement the pollution prevention measures set forth in the following table. Compliance with these emission limits shall be demonstrated by compliance with Specific Conditions #97, #98, and #102 and Plantwide Condition #5.

Source	Description	Pollutant	Control Technology	BACT Limit
SN-116	Ore Unloading and Product Loading Gantry Crane	PM	Enclosed Conveyors and Water Sprays at the Transfer Points	5.7 tpy
		PM ₁₀		2.7 tpy
		PM _{2.5}		0.5 tpy
		Opacity		20%
SN-117	Oxide Unloading Bin and Dedusting	PM	Fabric Filter Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-118	Oxide Pellet Pile Transfer and Dedusting (Pre-Enclosed Storage)	PM	Fabric Filter Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-119	Oxide Transfer and Dedusting (Post-Enclosed Storage)	PM	Fabric Filter Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%

Source	Description	Pollutant	Control Technology	BACT Limit
SN-120	Oxide and Remet Screening and Dedusting	PM	Fabric Filter	0.002 gr/dscf
		PM ₁₀	Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-121	Furnace Charge Hopper Loading Silos	PM	Fabric Filter	0.002 gr/dscf
		PM ₁₀	Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-122	Charge Hopper Dedusting	PM	Fabric Filter	0.002 gr/dscf
		PM ₁₀	Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
		SO ₂	Combustion of Natural Gas and Good Combustion Practices	0.000376 lb/MMBtu
		VOC		0.01 lb/MMBtu
		CO		0.08 lb/MMBtu
		NO _x		0.00317 lb/MMBtu
		Lead		8.17E-08 lb/MMBtu
CO _{2e}	Good Operating Practices	54,701 tpy CO _{2e}		
SN-123	Reformer Natural Gas Fired (1591 MMBtu/hr)	PM	Scrubber, Low NOX Burners, Combustion of Natural Gas, and Good Combustion Practices	0.0044 gr/dscf
		PM ₁₀		0.0044 gr/dscf
		PM _{2.5}		0.0044 gr/dscf
		Opacity		5%
		SO ₂		32.2 tpy
		VOC		35.6 tpy
		CO		543.2 tpy
		NO _x		383.3 tpy
		Lead		0.01 tpy
CO _{2e}	Good Operating Practices	1,680,207 tpy CO _{2e}		
SN-124	Furnace Dedusting (BSG Dust Collection) Wet Scrubber	PM	Dust Collector and Scrubber	0.0079 gr/dscf
		PM ₁₀		0.0079 gr/dscf
		PM _{2.5}		0.0079 gr/dscf
		Opacity		5%
		SO ₂	Combustion of	0.000376 lb/MMBtu

Source	Description	Pollutant	Control Technology	BACT Limit
		VOC	Natural Gas and Good Combustion Practices	0.01 lb/MMBtu
		CO		0.08 lb/MMBtu
		NO _x		0.00317 lb/MMBtu
		Lead		8.17E-08 lb/MMBtu
		CO _{2e}	Good Operating Practices	54,701 tpy CO _{2e}
SN-125	Hot Pressure Relief Vent (Flare)	PM	Flare, Scrubber, Good Combustion Practices, Low NO _x Fuel	0.0044 gr/dscf
		PM ₁₀		0.0044 gr/dscf
		PM _{2.5}		0.0044 gr/dscf
		Opacity		5%
		SO ₂		0.1 tpy
		VOC		0.1 tpy
		CO		8.8 tpy
		NO _x		1.0 tpy
		Lead		9.855E-07 tpy
		CO _{2e}	Good Operating Practices	762 tpy CO _{2e}
SN-126	Briquetter Dedusting	PM	Scrubber	0.0079 gr/dscf
		PM ₁₀		0.0079 gr/dscf
		PM _{2.5}		0.0079 gr/dscf
		Opacity		5%
		SO ₂	Combustion of Natural Gas and Good Combustion Practices	0.000376 lb/MMBtu
		VOC		0.01 lb/MMBtu
		CO		0.08 lb/MMBtu
		NO _x		0.00317 lb/MMBtu
		Lead		8.17E-08 lb/MMBtu
		CO _{2e}	Good Operating Practices	27,350 tpy CO _{2e}
SN-127	HBI Cooling Conveyor #1 and #2	PM	Scrubber	0.0079 gr/dscf
		PM ₁₀		0.0079 gr/dscf
		PM _{2.5}		0.0079 gr/dscf
		Opacity		5%
SN-128	Transfer and Product Screening Station No. 1 (Pre	PM	Fabric Filter Baghouse, Hooded Conveyors, and	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf

Source	Description	Pollutant	Control Technology	BACT Limit
	Pile)	Opacity	Enclosed Transfer Points	5%
SN-129	Transfer and Product Screening Station No. 2 (Post Pile)	PM	Fabric Filter Baghouse, Hooded Conveyors, and Enclosed Transfer Points	0.002 gr/dscf
		PM ₁₀		0.002 gr/dscf
		PM _{2.5}		0.002 gr/dscf
		Opacity		5%
SN-130	HBI Product Storage Pile	PM	Dust Control Plan and Use of Water Sprays and Wetting Agents and Vehicle Restrictions	1.2 tpy
		PM ₁₀		0.6 tpy
		PM _{2.5}		0.2 tpy
		Opacity		20%
SN-131	Remet/Fines Storage	PM	Dust Control Plan and Use of Water Sprays and Wetting Agents and Vehicle Restrictions	0.1 tpy
		PM ₁₀		0.1 tpy
		PM _{2.5}		0.1 tpy
		Opacity		20%
SN-132	Process Water Degasser	CO	Good Design Methods and Operating Practice	106.5 tpy
		CO _{2e}		2230 tpy CO _{2e}

94. The permittee shall not exceed the emission rates set forth in the following table. The permittee shall demonstrate compliance with this condition by compliance with Specific Condition #102 and Plantwide Condition #5. [Reg.18.801 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

SN	Description	Pollutant	lb/hr	tpy
SN-123	Reformer Natural Gas Fired (1591 MMBtu/hr)	Single HAP	0.02	0.08
		Total Other HAPs	0.02	0.09
SN-125	Hot Pressure Relief Vent (Flare)	Single HAP	0.01	0.01
		Total Other HAPs	0.01	0.01

95. Visible emissions may not exceed the limits specified in the following table of this permit as measured by EPA Reference Method 9. For SN-123, the opacity requirement is met by combustion of natural gas only. For all other listed sources, compliance with this condition will be shown by compliance with Specific Condition #96 and Plantwide Condition 5.

Source	Limit	Regulatory Citation
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SN-117, SN-118, SN-119, SN-120, SN-121, SN-122, SN-123, SN-124, SN-125, SN-126, SN-127, SN-128, SN-129	5%	Reg.19.901 <i>et seq.</i> and 40 C.F.R. § 52 Subpart E
SN-116, SN-130, SN-131	20%	Reg.19.901 <i>et seq.</i> and 40 C.F.R. § 52 Subpart E

96. The permittee shall conduct weekly observations of the opacity from the sources listed in Specific Condition #95. If visible emissions are detected, the permittee shall conduct a 6-minute opacity reading in accordance with Method 9 at the point where visible emissions were detected. The results of these observations shall be recorded in a log which shall be kept on site and made available for inspection upon request. [Reg.19.901 *et seq.* and 40 C.F.R. § 52 Subpart E]
97. The permittee shall not receive more than material than in the table below in any consecutive rolling 12 month period. [Reg.19.901 *et seq.* and 40 C.F.R. § 52 Subpart E]

Source	Consecutive rolling 12 month limit (tons/year)
SN-116	9,591,750
SN-130	2,830,033
SN-131	273,014

98. The permittee shall maintain monthly records of the amount of materials received in the sources in Specific Condition #97. These records shall include the monthly total of material received and the rolling 12 month total of material received. These records shall be updated by the 15th day of the month following the month to which the records pertain, kept on site, made available to Division personnel upon request, and submitted in accordance with General Provision 7. [Reg.19.901 *et seq.* and 40 C.F.R. § 52 Subpart E]
99. The permittee may install sealed conveyors or sealed pneumatic conveyors that have no vents to the atmosphere. The permittee is not required to vent the conveyors to a baghouse if no vent is needed. [Reg.19.705, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 70.6]
100. The permittee shall implement a fugitive emission dust control plan to control dust emissions from the sources specified to require a dust control plan in Specific Condition 93. The fugitive emission dust control plan shall be maintained on-site, made available to Division of Environmental Quality personnel upon request, and submitted in accordance with General Provision #7. [Reg.19.705, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 70.6]

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101. Nothing in this permit shall be construed to authorize a violation of the Arkansas Water and Air Pollution Control Act or the federal National Pollutant Discharge Elimination System (NPDES). [Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]
102. The permittee shall install and operate alarm system on the Hot Pressure Relief Vent Flare, SN-125, to notify the operator of the presence of a pilot flame or other possible flare malfunction. The permittee shall perform monthly visual confirmation of the pilot lights, semi-annually remove the strainer and check for debris, and annual test fire to ensure pilot light. The permittee shall maintain logs of all flare inspection and maintenance activities. These logs shall be kept on site and made available to Division personnel upon request. [Reg.19.702, Reg.19.304, 40 C.F.R. § 52 Subpart E, and 40 C.F.R. § 64]
103. The permittee shall test the Hot Pressure Relief Vent, SN-125, to show the flare is designed and operated in accordance with 40 C.F.R. 60.18(b) through (f). This test includes a Method 22 for opacity, measurement of the actual gas flow rate and, calculations of the heating value of the gas (if complying with 60.18(c)(3)(ii) and (c)(4)). This test shall be conducted in accordance with Plantwide Condition 3. [Reg.19.702 and 40 C.F.R. § 52 Subpart E]

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SECTION V: COMPLIANCE PLAN AND SCHEDULE

Big River Steel LLC will continue to operate in compliance with those identified regulatory provisions. The facility will examine and analyze future regulations that may apply and determine their applicability with any necessary action taken on a timely basis.

SECTION VI: PLANTWIDE CONDITIONS

1. The permittee shall notify the Director in writing within thirty (30) days after commencing construction, completing construction, first placing the equipment and/or facility in operation, and reaching the equipment and/or facility target production rate. [Reg.19.704, 40 C.F.R. § 52 Subpart E, and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]
2. If the permittee fails to start construction within eighteen months or suspends construction for eighteen months or more, the Director may cancel all or part of this permit. [Reg.19.410(B) and 40 C.F.R. § 52 Subpart E]
3. The permittee must test any equipment scheduled for testing, unless otherwise stated in the Specific Conditions of this permit or by any federally regulated requirements, within the following time frames: (1) new equipment or newly modified equipment within sixty (60) days of achieving the maximum production rate, but no later than 180 days after initial start up of the permitted source or (2) operating equipment according to the time frames set forth by the Division of Environmental Quality or within 180 days of permit issuance if no date is specified. The permittee must notify the Division of Environmental Quality of the scheduled date of compliance testing at least fifteen (15) business days in advance of such test. The permittee shall submit the compliance test results to the Division of Environmental Quality within sixty (60) calendar days after completing the testing. [Reg.19.702 and/or Reg.18.1002 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]
4. The permittee must provide:
 - a. Sampling ports adequate for applicable test methods;
 - b. Safe sampling platforms;
 - c. Safe access to sampling platforms; and
 - d. Utilities for sampling and testing equipment.

[Reg.19.702 and/or Reg.18.1002 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]
5. The permittee must operate the equipment, control apparatus and emission monitoring equipment within the design limitations. The permittee shall maintain the equipment in good condition at all times. [Reg.19.303 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]
6. This permit subsumes and incorporates all previously issued air permits for this facility. [Reg. 26 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

7. Unless otherwise specified in the permit, approval to construct any new major stationary source or a major modification subject to 40 C.F.R. § 52.21 shall become invalid if construction is not commenced within 18 months after receipt of such approval, if construction is discontinued for a period of 18 months or more, or if construction is not completed within a reasonable time. The Division of Environmental Quality may extend the 18-month period upon a satisfactory showing that an extension is justified. [Reg.19.901 *et seq.* and 40 C.F.R. § 52 Subpart E]
8. The permittee must build the stacks for the following sources to the height listed. These stack heights are those supplied by the facility for the initial permit application. [Reg.19.303 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

Source	Stack Height (ft)
SN-01, SN-02	240
SN-03, SN-04	165
SN-22	270
SN-24, SN-27, SN-28, SN-37	120
SN-23, SN-25	105
SN-29, SN-30, SN-38	140
SN-31, SN-32, SN-39	145
SN-33	250
SN-40, SN-41	121
SN-42, SN-43, SN-44, SN-45, SN-46	164
SN-118, SN-119, SN-120, SN- 121, SN-128, SN-129	180
SN-122, SN-123, SN-124, SN- 125, SN-126, SN-127	213

9. The permittee shall install, operate, and maintain air quality monitors for PM₁₀, PM_{2.5}, and NO₂ at the stationary source. Monitors shall be installed and operating at this stationary source within 180 days of the startup of the EAFs. This condition is satisfied by operation of the existing monitor at the Existing Mill (Permit #2305-AOP-R7). In the event BRS ceases operation of such on-site air quality monitor, the permittee shall submit a monitoring protocol to the Division within 30 days after ceasing operation of the on-site air quality monitor at the Existing Mill. The Division must approve of the monitoring protocol prior to installation of the new monitors. [Reg.19.901 *et seq.* and 40 C.F.R. Part 52, Subpart E]

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SECTION VII: INSIGNIFICANT ACTIVITIES

The Division of Environmental Quality deems the following types of activities or emissions as insignificant on the basis of size, emission rate, production rate, or activity in accordance with Group A of the Insignificant Activities list found in Regulation 18 and Regulation 19 Appendix A. Group B insignificant activities may be listed but are not required to be listed in permits. Insignificant activity emission determinations rely upon the information submitted by the permittee in an application dated September 20, 2021. [Reg.26.304 and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

Description	Category
N/A	

SECTION VIII: GENERAL PROVISIONS

1. Any terms or conditions included in this permit which specify and reference Arkansas Pollution Control & Ecology Commission Regulation 18 or the Arkansas Water and Air Pollution Control Act (Ark. Code Ann. § 8-4-101 *et seq.*) as the sole origin of and authority for the terms or conditions are not required under the Clean Air Act or any of its applicable requirements, and are not federally enforceable under the Clean Air Act. Arkansas Pollution Control & Ecology Commission Regulation 18 was adopted pursuant to the Arkansas Water and Air Pollution Control Act (Ark. Code Ann. § 8-4-101 *et seq.*). Any terms or conditions included in this permit which specify and reference Arkansas Pollution Control & Ecology Commission Regulation 18 or the Arkansas Water and Air Pollution Control Act (Ark. Code Ann. § 8-4-101 *et seq.*) as the origin of and authority for the terms or conditions are enforceable under this Arkansas statute. [40 C.F.R. § 70.6(b)(2)]
2. This permit shall be valid for a period of five (5) years beginning on the date this permit becomes effective and ending five (5) years later. [40 C.F.R. § 70.6(a)(2) and Reg.26.701(B)]
3. The permittee must submit a complete application for permit renewal at least six (6) months before permit expiration. Permit expiration terminates the permittee's right to operate unless the permittee submitted a complete renewal application at least six (6) months before permit expiration. If the permittee submits a complete application, the existing permit will remain in effect until the Division of Environmental Quality takes final action on the renewal application. The Division of Environmental Quality will not necessarily notify the permittee when the permit renewal application is due. [Reg.26.406]
4. Where an applicable requirement of the Clean Air Act, as amended, 42 U.S.C. 7401, *et seq.* (Act) is more stringent than an applicable requirement of regulations promulgated under Title IV of the Act, the permit incorporates both provisions into the permit, and the Director or the Administrator can enforce both provisions. [40 C.F.R. § 70.6(a)(1)(ii) and Reg.26.701(A)(2)]
5. The permittee must maintain the following records of monitoring information as required by this permit.
 - a. The date, place as defined in this permit, and time of sampling or measurements;
 - b. The date(s) analyses performed;
 - c. The company or entity performing the analyses;
 - d. The analytical techniques or methods used;
 - e. The results of such analyses; and
 - f. The operating conditions existing at the time of sampling or measurement.

[40 C.F.R. § 70.6(a)(3)(ii)(A) and Reg.26.701(C)(2)]

6. The permittee must retain the records of all required monitoring data and support information for at least five (5) years from the date of the monitoring sample, measurement, report, or application. Support information includes all calibration and maintenance records and all original strip chart recordings for continuous monitoring instrumentation, and copies of all reports required by this permit. [40 C.F.R. § 70.6(a)(3)(ii)(B) and Reg.26.701(C)(2)(b)]
7. The permittee must submit reports of all required monitoring every six (6) months. If the permit establishes no other reporting period, the reporting period shall end on the last day of the month six months after the issuance of the initial Title V permit and every six months thereafter. The report is due on the first day of the second month after the end of the reporting period. The first report due after issuance of the initial Title V permit shall contain six months of data and each report thereafter shall contain 12 months of data. The report shall contain data for all monitoring requirements in effect during the reporting period. If a monitoring requirement is not in effect for the entire reporting period, only those months of data in which the monitoring requirement was in effect are required to be reported. The report must clearly identify all instances of deviations from permit requirements. A responsible official as defined in Reg.26.2 must certify all required reports. The permittee will send the reports electronically using <https://portal.adeq.state.ar.us> or mail them to the address below:

Division of Environmental Quality
Office of Air Quality
ATTN: Compliance Inspector Supervisor
5301 Northshore Drive
North Little Rock, AR 72118-5317

[40 C.F.R. § 70.6(a)(3)(iii)(A) and Reg.26.701(C)(3)(a)]

8. The permittee shall report to the Division of Environmental Quality all deviations from permit requirements, including those attributable to upset conditions as defined in the permit.
 - a. For all upset conditions (as defined in Reg.19.601), the permittee will make an initial report to the Division of Environmental Quality by the next business day after the discovery of the occurrence. The initial report may be made by telephone and shall include:
 - i. The facility name and location;
 - ii. The process unit or emission source deviating from the permit limit;
 - iii. The permit limit, including the identification of pollutants, from which deviation occurs;
 - iv. The date and time the deviation started;
 - v. The duration of the deviation;

- vi. The emissions during the deviation;
- vii. The probable cause of such deviations;
- viii. Any corrective actions or preventive measures taken or being taken to prevent such deviations in the future; and
- ix. The name of the person submitting the report.

The permittee shall make a full report in writing to the Division of Environmental Quality within five (5) business days of discovery of the occurrence. The report must include, in addition to the information required by the initial report, a schedule of actions taken or planned to eliminate future occurrences and/or to minimize the amount the permit's limits were exceeded and to reduce the length of time the limits were exceeded. The permittee may submit a full report in writing (by facsimile, overnight courier, or other means) by the next business day after discovery of the occurrence, and the report will serve as both the initial report and full report.

- b. For all deviations, the permittee shall report such events in semi-annual reporting and annual certifications required in this permit. This includes all upset conditions reported in 8a above. The semi-annual report must include all the information as required by the initial and full reports required in 8a.

[Reg.19.601, Reg.19.602, Reg.26.701(C)(3)(b), and 40 C.F.R. § 70.6(a)(3)(iii)(B)]

9. If any provision of the permit or the application thereof to any person or circumstance is held invalid, such invalidity will not affect other provisions or applications hereof which can be given effect without the invalid provision or application, and to this end, provisions of this Regulation are declared to be separable and severable. [40 C.F.R. § 70.6(a)(5), Reg.26.701(E), and Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]
10. The permittee must comply with all conditions of this Part 70 permit. Any permit noncompliance with applicable requirements as defined in Regulation 26 constitutes a violation of the Clean Air Act, as amended, 42 U.S.C. § 7401, *et seq.* and is grounds for enforcement action; for permit termination, revocation and reissuance, for permit modification; or for denial of a permit renewal application. [40 C.F.R. § 70.6(a)(6)(i) and Reg.26.701(F)(1)]
11. It shall not be a defense for a permittee in an enforcement action that it would have been necessary to halt or reduce the permitted activity to maintain compliance with the conditions of this permit. [40 C.F.R. § 70.6(a)(6)(ii) and Reg.26.701(F)(2)]
12. The Division of Environmental Quality may modify, revoke, reopen and reissue the permit or terminate the permit for cause. The filing of a request by the permittee for a permit modification, revocation and reissuance, termination, or of a notification of planned changes or anticipated noncompliance does not stay any permit condition. [40 C.F.R. § 70.6(a)(6)(iii) and Reg.26.701(F)(3)]

13. This permit does not convey any property rights of any sort, or any exclusive privilege. [40 C.F.R. § 70.6(a)(6)(iv) and Reg.26.701(F)(4)]
14. The permittee must furnish to the Director, within the time specified by the Director, any information that the Director may request in writing to determine whether cause exists for modifying, revoking and reissuing, or terminating the permit or to determine compliance with the permit. Upon request, the permittee must also furnish to the Director copies of records required by the permit. For information the permittee claims confidentiality, the Division of Environmental Quality may require the permittee to furnish such records directly to the Director along with a claim of confidentiality. [40 C.F.R. § 70.6(a)(6)(v) and Reg.26.701(F)(5)]
15. The permittee must pay all permit fees in accordance with the procedures established in Regulation 9. [40 C.F.R. § 70.6(a)(7) and Reg.26.701(G)]
16. No permit revision shall be required, under any approved economic incentives, marketable permits, emissions trading and other similar programs or processes for changes provided for elsewhere in this permit. [40 C.F.R. § 70.6(a)(8) and Reg.26.701(H)]
17. If the permit allows different operating scenarios, the permittee shall, contemporaneously with making a change from one operating scenario to another, record in a log at the permitted facility a record of the operational scenario. [40 C.F.R. § 70.6(a)(9)(i) and Reg.26.701(I)(1)]
18. The Administrator and citizens may enforce under the Act all terms and conditions in this permit, including any provisions designed to limit a source's potential to emit, unless the Division of Environmental Quality specifically designates terms and conditions of the permit as being federally unenforceable under the Act or under any of its applicable requirements. [40 C.F.R. § 70.6(b) and Reg.26.702(A) and (B)]
19. Any document (including reports) required by this permit pursuant to 40 C.F.R. § 70 must contain a certification by a responsible official as defined in Reg.26.2. [40 C.F.R. § 70.6(c)(1) and Reg.26.703(A)]
20. The permittee must allow an authorized representative of the Division of Environmental Quality, upon presentation of credentials, to perform the following: [40 C.F.R. § 70.6(c)(2) and Reg.26.703(B)]
 - a. Enter upon the permittee's premises where the permitted source is located or emissions related activity is conducted, or where records must be kept under the conditions of this permit;
 - b. Have access to and copy, at reasonable times, any records required under the conditions of this permit;

- c. Inspect at reasonable times any facilities, equipment (including monitoring and air pollution control equipment), practices, or operations regulated or required under this permit; and
 - d. As authorized by the Act, sample or monitor at reasonable times substances or parameters for assuring compliance with this permit or applicable requirements.

- 21. The permittee shall submit a compliance certification with the terms and conditions contained in the permit, including emission limitations, standards, or work practices. The permittee must submit the compliance certification annually. If the permit establishes no other reporting period, the reporting period shall end on the last day of the anniversary month of the initial Title V permit. The report is due on the first day of the second month after the end of the reporting period. The permittee must also submit the compliance certification to the Administrator as well as to the Division of Environmental Quality. All compliance certifications required by this permit must include the following: [40 C.F.R. § 70.6(c)(5) and Reg.26.703(E)(3)]
 - a. The identification of each term or condition of the permit that is the basis of the certification;
 - b. The compliance status;
 - c. Whether compliance was continuous or intermittent;
 - d. The method(s) used for determining the compliance status of the source, currently and over the reporting period established by the monitoring requirements of this permit; and
 - e. Such other facts as the Division of Environmental Quality may require elsewhere in this permit or by § 114(a)(3) and § 504(b) of the Act.

- 22. Nothing in this permit will alter or affect the following: [Reg.26.704(C)]
 - a. The provisions of Section 303 of the Act (emergency orders), including the authority of the Administrator under that section;
 - b. The liability of the permittee for any violation of applicable requirements prior to or at the time of permit issuance;
 - c. The applicable requirements of the acid rain program, consistent with § 408(a) of the Act; or
 - d. The ability of EPA to obtain information from a source pursuant to § 114 of the Act.

- 23. This permit authorizes only those pollutant emitting activities addressed in this permit. [Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311]

- 24. The permittee may request in writing and at least 15 days in advance of the deadline, an extension to any testing, compliance or other dates in this permit. No such extensions are authorized until the permittee receives written Division of Environmental Quality approval. The Division of Environmental Quality may grant such a request, at its discretion in the following circumstances:

- a. Such an extension does not violate a federal requirement;
- b. The permittee demonstrates the need for the extension; and
- c. The permittee documents that all reasonable measures have been taken to meet the current deadline and documents reasons it cannot be met.

[Reg.18.314(A), Reg.19.416(A), Reg.26.1013(A), Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 52 Subpart E]

25. The permittee may request in writing and at least 30 days in advance, temporary emissions and/or testing that would otherwise exceed an emission rate, throughput requirement, or other limit in this permit. No such activities are authorized until the permittee receives written Division of Environmental Quality approval. Any such emissions shall be included in the facility's total emissions and reported as such. The Division of Environmental Quality may grant such a request, at its discretion under the following conditions:

- a. Such a request does not violate a federal requirement;
- b. Such a request is temporary in nature;
- c. Such a request will not result in a condition of air pollution;
- d. The request contains such information necessary for the Division of Environmental Quality to evaluate the request, including but not limited to, quantification of such emissions and the date/time such emission will occur;
- e. Such a request will result in increased emissions less than five tons of any individual criteria pollutant, one ton of any single HAP and 2.5 tons of total HAPs; and
- f. The permittee maintains records of the dates and results of such temporary emissions/testing.

[Reg.18.314(B), Reg.19.416(B), Reg.26.1013(B), Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 52 Subpart E]

26. The permittee may request in writing and at least 30 days in advance, an alternative to the specified monitoring in this permit. No such alternatives are authorized until the permittee receives written Division of Environmental Quality approval. The Division of Environmental Quality may grant such a request, at its discretion under the following conditions:

- a. The request does not violate a federal requirement;
- b. The request provides an equivalent or greater degree of actual monitoring to the current requirements; and
- c. Any such request, if approved, is incorporated in the next permit modification application by the permittee.

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[Reg.18.314(C), Reg.19.416(C), Reg.26.1013(C), Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 52 Subpart E]

27. Any credible evidence based on sampling, monitoring, and reporting may be used to determine violations of applicable emission limitations. [Reg.18.1001, Reg.19.701, Ark. Code Ann. § 8-4-203 as referenced by Ark. Code Ann. §§ 8-4-304 and 8-4-311, and 40 C.F.R. § 52 Subpart E]

Appendix A

40 C.F.R. Part 60 Subpart Dc

***Standards of Performance for Small Industrial-Commercial-Institutional Steam Generating
Units***

Subpart Dc - Standards of Performance for Small Industrial-Commercial-Institutional Steam Generating Units

Source: [72 FR 32759](#), June 13, 2007, unless otherwise noted.

§ 60.40c Applicability and delegation of authority.

- (a) Except as provided in [paragraphs \(d\), \(e\), \(f\), and \(g\)](#) of this section, the affected facility to which this subpart applies is each steam generating unit for which construction, modification, or reconstruction is commenced after June 9, 1989 and that has a maximum design heat input capacity of 29 megawatts (MW) (100 million British thermal units per hour (MMBtu/h)) or less, but greater than or equal to 2.9 MW (10 MMBtu/h).
- (b) In delegating implementation and enforcement authority to a State under section 111(c) of the Clean Air Act, [§ 60.48c\(a\)\(4\)](#) shall be retained by the Administrator and not transferred to a State.
- (c) Steam generating units that meet the applicability requirements in [paragraph \(a\)](#) of this section are not subject to the sulfur dioxide (SO₂) or particulate matter (PM) emission limits, performance testing requirements, or monitoring requirements under this subpart ([§ 60.42c](#), [§ 60.43c](#), [§ 60.44c](#), [§ 60.45c](#), [§ 60.46c](#), or [§ 60.47c](#)) during periods of combustion research, as defined in [§ 60.41c](#).
- (d) Any temporary change to an existing steam generating unit for the purpose of conducting combustion research is not considered a modification under [§ 60.14](#).
- (e) Affected facilities (*i.e.* heat recovery steam generators and fuel heaters) that are associated with stationary combustion turbines and meet the applicability requirements of [subpart KKKK of this part](#) are not subject to this subpart. This subpart will continue to apply to all other heat recovery steam generators, fuel heaters, and other affected facilities that are capable of combusting more than or equal to 2.9 MW (10 MMBtu/h) heat input of fossil fuel but less than or equal to 29 MW (100 MMBtu/h) heat input of fossil fuel. If the heat recovery steam generator, fuel heater, or other affected facility is subject to this subpart, only emissions resulting from combustion of fuels in the steam generating unit are subject to this subpart. (The stationary combustion turbine emissions are subject to subpart GG or KKKK, as applicable, of this part.)
- (f) Any affected facility that meets the applicability requirements of and is subject to subpart AAAA or [subpart CCCC of this part](#) is not subject to this subpart.
- (g) Any facility that meets the applicability requirements and is subject to an EPA approved State or Federal section 111(d)/129 plan implementing [subpart BBBB of this part](#) is not subject to this subpart.

(h) Affected facilities that also meet the applicability requirements under subpart J or [subpart Ja of this part](#) are subject to the PM and NO_x standards under this subpart and the SO₂ standards under subpart J or [subpart Ja of this part](#), as applicable.

(i) Temporary boilers are not subject to this subpart.

[[72 FR 32759](#), June 13, 2007, as amended at [74 FR 5090](#), Jan. 28, 2009; [77 FR 9461](#), Feb. 16, 2012]

§ 60.41c Definitions.

As used in this subpart, all terms not defined herein shall have the meaning given them in the Clean Air Act and in [subpart A of this part](#).

Annual capacity factor means the ratio between the actual heat input to a steam generating unit from an individual fuel or combination of fuels during a period of 12 consecutive calendar months and the potential heat input to the steam generating unit from all fuels had the steam generating unit been operated for 8,760 hours during that 12-month period at the maximum design heat input capacity. In the case of steam generating units that are rented or leased, the actual heat input shall be determined based on the combined heat input from all operations of the affected facility during a period of 12 consecutive calendar months.

Coal means all solid fuels classified as anthracite, bituminous, subbituminous, or lignite by the American Society of Testing and Materials in ASTM D388 (incorporated by reference, see [§ 60.17](#)), coal refuse, and petroleum coke. Coal-derived synthetic fuels derived from coal for the purposes of creating useful heat, including but not limited to solvent refined coal, gasified coal not meeting the definition of natural gas, coal-oil mixtures, and coal-water mixtures, are also included in this definition for the purposes of this subpart.

Coal refuse means any by-product of coal mining or coal cleaning operations with an ash content greater than 50 percent (by weight) and a heating value less than 13,900 kilojoules per kilogram (kJ/kg) (6,000 Btu per pound (Btu/lb) on a dry basis.

Combined cycle system means a system in which a separate source (such as a stationary gas turbine, internal combustion engine, or kiln) provides exhaust gas to a steam generating unit.

Combustion research means the experimental firing of any fuel or combination of fuels in a steam generating unit for the purpose of conducting research and development of more efficient combustion or more effective prevention or control of air pollutant emissions from combustion, provided that, during these periods of research and development, the heat generated is not used for any purpose other than preheating combustion air for use by that steam generating unit (*i.e.*, the heat generated is released to the atmosphere without being used for space heating, process heating, driving pumps, preheating combustion air for other units, generating electricity, or any other purpose).

Conventional technology means wet flue gas desulfurization technology, dry flue gas desulfurization technology, atmospheric fluidized bed combustion technology, and oil hydrodesulfurization technology.

Distillate oil means fuel oil that complies with the specifications for fuel oil numbers 1 or 2, as defined by the American Society for Testing and Materials in ASTM D396 (incorporated by reference, see [§ 60.17](#)), diesel fuel oil numbers 1 or 2, as defined by the American Society for Testing and Materials in ASTM D975 (incorporated by reference, see [§ 60.17](#)), kerosine, as defined by the American Society of Testing and Materials in ASTM D3699 (incorporated by reference, see [§ 60.17](#)), biodiesel as defined by the American Society of Testing and Materials in ASTM D6751 (incorporated by reference, see [§ 60.17](#)), or biodiesel blends as defined by the American Society of Testing and Materials in ASTM D7467 (incorporated by reference, see [§ 60.17](#)).

Dry flue gas desulfurization technology means a SO₂ control system that is located between the steam generating unit and the exhaust vent or stack, and that removes sulfur oxides from the combustion gases of the steam generating unit by contacting the combustion gases with an alkaline reagent and water, whether introduced separately or as a premixed slurry or solution and forming a dry powder material. This definition includes devices where the dry powder material is subsequently converted to another form. Alkaline reagents used in dry flue gas desulfurization systems include, but are not limited to, lime and sodium compounds.

Duct burner means a device that combusts fuel and that is placed in the exhaust duct from another source (such as a stationary gas turbine, internal combustion engine, kiln, etc.) to allow the firing of additional fuel to heat the exhaust gases before the exhaust gases enter a steam generating unit.

Emerging technology means any SO₂ control system that is not defined as a conventional technology under this section, and for which the owner or operator of the affected facility has received approval from the Administrator to operate as an emerging technology under [§ 60.48c\(a\)\(4\)](#).

Federally enforceable means all limitations and conditions that are enforceable by the Administrator, including the requirements of [40 CFR parts 60 and 61](#), requirements within any applicable State implementation plan, and any permit requirements established under [40 CFR 52.21](#) or under [40 CFR 51.18](#) and [51.24](#).

Fluidized bed combustion technology means a device wherein fuel is distributed onto a bed (or series of beds) of limestone aggregate (or other sorbent materials) for combustion; and these materials are forced upward in the device by the flow of combustion air and the gaseous products of combustion. Fluidized bed combustion technology includes, but is not limited to, bubbling bed units and circulating bed units.

Fuel pretreatment means a process that removes a portion of the sulfur in a fuel before combustion of the fuel in a steam generating unit.

Heat input means heat derived from combustion of fuel in a steam generating unit and does not include the heat derived from preheated combustion air, recirculated flue gases, or exhaust gases from other sources (such as stationary gas turbines, internal combustion engines, and kilns).

Heat transfer medium means any material that is used to transfer heat from one point to another point.

Maximum design heat input capacity means the ability of a steam generating unit to combust a stated maximum amount of fuel (or combination of fuels) on a steady state basis as determined by the physical design and characteristics of the steam generating unit.

Natural gas means:

- (1) A naturally occurring mixture of hydrocarbon and nonhydrocarbon gases found in geologic formations beneath the earth's surface, of which the principal constituent is methane; or
- (2) Liquefied petroleum (LP) gas, as defined by the American Society for Testing and Materials in ASTM D1835 (incorporated by reference, see [§ 60.17](#)); or
- (3) A mixture of hydrocarbons that maintains a gaseous state at ISO conditions. Additionally, natural gas must either be composed of at least 70 percent methane by volume or have a gross calorific value between 34 and 43 megajoules (MJ) per dry standard cubic meter (910 and 1,150 Btu per dry standard cubic foot).

Noncontinental area means the State of Hawaii, the Virgin Islands, Guam, American Samoa, the Commonwealth of Puerto Rico, or the Northern Mariana Islands.

Oil means crude oil or petroleum, or a liquid fuel derived from crude oil or petroleum, including distillate oil and residual oil.

Potential sulfur dioxide emission rate means the theoretical SO₂ emissions (nanograms per joule (ng/J) or lb/MMBtu heat input) that would result from combusting fuel in an uncleaned state and without using emission control systems.

Process heater means a device that is primarily used to heat a material to initiate or promote a chemical reaction in which the material participates as a reactant or catalyst.

Residual oil means crude oil, fuel oil that does not comply with the specifications under the definition of distillate oil, and all fuel oil numbers 4, 5, and 6, as defined by the American Society for Testing and Materials in ASTM D396 (incorporated by reference, see [§ 60.17](#)).

Steam generating unit means a device that combusts any fuel and produces steam or heats water or heats any heat transfer medium. This term includes any duct burner that combusts fuel and is part of a combined cycle system. This term does not include process heaters as defined in this subpart.

Steam generating unit operating day means a 24-hour period between 12:00 midnight and the following midnight during which any fuel is combusted at any time in the steam generating unit. It is not necessary for fuel to be combusted continuously for the entire 24-hour period.

Temporary boiler means a steam generating unit that combusts natural gas or distillate oil with a potential SO₂ emissions rate no greater than 26 ng/J (0.060 lb/MMBtu), and the unit is designed to, and is capable of, being carried or moved from one location to another by means of, for example, wheels, skids, carrying handles, dollies, trailers, or platforms. A steam generating unit is not a temporary boiler if any one of the following conditions exists:

- (1) The equipment is attached to a foundation.
- (2) The steam generating unit or a replacement remains at a location for more than 180 consecutive days. Any temporary boiler that replaces a temporary boiler at a location and performs the same or similar function will be included in calculating the consecutive time period.
- (3) The equipment is located at a seasonal facility and operates during the full annual operating period of the seasonal facility, remains at the facility for at least 2 years, and operates at that facility for at least 3 months each year.
- (4) The equipment is moved from one location to another in an attempt to circumvent the residence time requirements of this definition.

Wet flue gas desulfurization technology means an SO₂ control system that is located between the steam generating unit and the exhaust vent or stack, and that removes sulfur oxides from the combustion gases of the steam generating unit by contacting the combustion gases with an alkaline slurry or solution and forming a liquid material. This definition includes devices where the liquid material is subsequently converted to another form. Alkaline reagents used in wet flue gas desulfurization systems include, but are not limited to, lime, limestone, and sodium compounds.

Wet scrubber system means any emission control device that mixes an aqueous stream or slurry with the exhaust gases from a steam generating unit to control emissions of PM or SO₂.

Wood means wood, wood residue, bark, or any derivative fuel or residue thereof, in any form, including but not limited to sawdust, sanderdust, wood chips, scraps, slabs, millings, shavings, and processed pellets made from wood or other forest residues.

[[72 FR 32759](#), June 13, 2007, as amended at [74 FR 5090](#), Jan. 28, 2009; [77 FR 9461](#), Feb. 16, 2012]

§ 60.42c Standard for sulfur dioxide (SO₂).

- (a) Except as provided in [paragraphs \(b\), \(c\), and \(e\)](#) of this section, on and after the date on which the performance test is completed or required to be completed under [§ 60.8](#), whichever

date comes first, the owner or operator of an affected facility that combusts only coal shall neither: cause to be discharged into the atmosphere from the affected facility any gases that contain SO₂ in excess of 87 ng/J (0.20 lb/MMBtu) heat input or 10 percent (0.10) of the potential SO₂ emission rate (90 percent reduction), nor cause to be discharged into the atmosphere from the affected facility any gases that contain SO₂ in excess of 520 ng/J (1.2 lb/MMBtu) heat input. If coal is combusted with other fuels, the affected facility shall neither: cause to be discharged into the atmosphere from the affected facility any gases that contain SO₂ in excess of 87 ng/J (0.20 lb/MMBtu) heat input or 10 percent (0.10) of the potential SO₂ emission rate (90 percent reduction), nor cause to be discharged into the atmosphere from the affected facility any gases that contain SO₂ in excess of the emission limit is determined pursuant to [paragraph \(e\)\(2\)](#) of this section.

(b) Except as provided in [paragraphs \(c\)](#) and [\(e\)](#) of this section, on and after the date on which the performance test is completed or required to be completed under [§ 60.8](#), whichever date comes first, the owner or operator of an affected facility that:

(1) Combusts only coal refuse alone in a fluidized bed combustion steam generating unit shall neither:

(i) Cause to be discharged into the atmosphere from that affected facility any gases that contain SO₂ in excess of 87 ng/J (0.20 lb/MMBtu) heat input or 20 percent (0.20) of the potential SO₂ emission rate (80 percent reduction); nor

(ii) Cause to be discharged into the atmosphere from that affected facility any gases that contain SO₂ in excess of SO₂ in excess of 520 ng/J (1.2 lb/MMBtu) heat input. If coal is fired with coal refuse, the affected facility subject to [paragraph \(a\)](#) of this section. If oil or any other fuel (except coal) is fired with coal refuse, the affected facility is subject to the 87 ng/J (0.20 lb/MMBtu) heat input SO₂ emissions limit or the 90 percent SO₂ reduction requirement specified in [paragraph \(a\)](#) of this section and the emission limit is determined pursuant to [paragraph \(e\)\(2\)](#) of this section.

(2) Combusts only coal and that uses an emerging technology for the control of SO₂ emissions shall neither:

(i) Cause to be discharged into the atmosphere from that affected facility any gases that contain SO₂ in excess of 50 percent (0.50) of the potential SO₂ emission rate (50 percent reduction); nor

(ii) Cause to be discharged into the atmosphere from that affected facility any gases that contain SO₂ in excess of 260 ng/J (0.60 lb/MMBtu) heat input. If coal is combusted with other fuels, the affected facility is subject to the 50 percent SO₂ reduction requirement specified in this paragraph and the emission limit determined pursuant to [paragraph \(e\)\(2\)](#) of this section.

(c) On and after the date on which the initial performance test is completed or required to be completed under [§ 60.8](#), whichever date comes first, no owner or operator of an affected

facility that combusts coal, alone or in combination with any other fuel, and is listed in [paragraphs \(c\)\(1\), \(2\), \(3\), or \(4\)](#) of this section shall cause to be discharged into the atmosphere from that affected facility any gases that contain SO₂ in excess of the emission limit determined pursuant to [paragraph \(e\)\(2\)](#) of this section. Percent reduction requirements are not applicable to affected facilities under paragraphs (c)(1), (2), (3), or (4).

- (1) Affected facilities that have a heat input capacity of 22 MW (75 MMBtu/h) or less;
- (2) Affected facilities that have an annual capacity for coal of 55 percent (0.55) or less and are subject to a federally enforceable requirement limiting operation of the affected facility to an annual capacity factor for coal of 55 percent (0.55) or less.
- (3) Affected facilities located in a noncontinental area; or
- (4) Affected facilities that combust coal in a duct burner as part of a combined cycle system where 30 percent (0.30) or less of the heat entering the steam generating unit is from combustion of coal in the duct burner and 70 percent (0.70) or more of the heat entering the steam generating unit is from exhaust gases entering the duct burner.

(d) On and after the date on which the initial performance test is completed or required to be completed under [§ 60.8](#), whichever date comes first, no owner or operator of an affected facility that combusts oil shall cause to be discharged into the atmosphere from that affected facility any gases that contain SO₂ in excess of 215 ng/J (0.50 lb/MMBtu) heat input from oil; or, as an alternative, no owner or operator of an affected facility that combusts oil shall combust oil in the affected facility that contains greater than 0.5 weight percent sulfur. The percent reduction requirements are not applicable to affected facilities under this paragraph.

(e) On and after the date on which the initial performance test is completed or required to be completed under [§ 60.8](#), whichever date comes first, no owner or operator of an affected facility that combusts coal, oil, or coal and oil with any other fuel shall cause to be discharged into the atmosphere from that affected facility any gases that contain SO₂ in excess of the following:

- (1) The percent of potential SO₂ emission rate or numerical SO₂ emission rate required under [paragraph \(a\)](#) or [\(b\)\(2\)](#) of this section, as applicable, for any affected facility that
 - (i) Combusts coal in combination with any other fuel;
 - (ii) Has a heat input capacity greater than 22 MW (75 MMBtu/h); and
 - (iii) Has an annual capacity factor for coal greater than 55 percent (0.55); and
- (2) The emission limit determined according to the following formula for any affected facility that combusts coal, oil, or coal and oil with any other fuel:

$$E_s = \frac{(K_a H_a + K_b H_b + K_c H_c)}{(H_a + H_b + H_c)}$$

Where:

E_s = SO₂ emission limit, expressed in ng/J or lb/MMBtu heat input;

K_a = 520 ng/J (1.2 lb/MMBtu);

K_b = 260 ng/J (0.60 lb/MMBtu);

K_c = 215 ng/J (0.50 lb/MMBtu);

H_a = Heat input from the combustion of coal, except coal combusted in an affected facility subject to [paragraph \(b\)\(2\)](#) of this section, in Joules (J) [MMBtu];

H_b = Heat input from the combustion of coal in an affected facility subject to [paragraph \(b\)\(2\)](#) of this section, in J (MMBtu); and

H_c = Heat input from the combustion of oil, in J (MMBtu).

(f) Reduction in the potential SO₂ emission rate through fuel pretreatment is not credited toward the percent reduction requirement under [paragraph \(b\)\(2\)](#) of this section unless:

(1) Fuel pretreatment results in a 50 percent (0.50) or greater reduction in the potential SO₂ emission rate; and

(2) Emissions from the pretreated fuel (without either combustion or post-combustion SO₂ control) are equal to or less than the emission limits specified under [paragraph \(b\)\(2\)](#) of this section.

(g) Except as provided in [paragraph \(h\)](#) of this section, compliance with the percent reduction requirements, fuel oil sulfur limits, and emission limits of this section shall be determined on a 30-day rolling average basis.

(h) For affected facilities listed under [paragraphs \(h\)\(1\), \(2\), \(3\), or \(4\)](#) of this section, compliance with the emission limits or fuel oil sulfur limits under this section may be determined based on a certification from the fuel supplier, as described under [§ 60.48c\(f\)](#), as applicable.

(1) Distillate oil-fired affected facilities with heat input capacities between 2.9 and 29 MW (10 and 100 MMBtu/hr).

(2) Residual oil-fired affected facilities with heat input capacities between 2.9 and 8.7 MW (10 and 30 MMBtu/hr).

(3) Coal-fired affected facilities with heat input capacities between 2.9 and 8.7 MW (10 and 30 MMBtu/h).

(4) Other fuels-fired affected facilities with heat input capacities between 2.9 and 8.7 MW (10 and 30 MMBtu/h).

(i) The SO₂ emission limits, fuel oil sulfur limits, and percent reduction requirements under this section apply at all times, including periods of startup, shutdown, and malfunction.

(j) For affected facilities located in noncontinental areas and affected facilities complying with the percent reduction standard, only the heat input supplied to the affected facility from the combustion of coal and oil is counted under this section. No credit is provided for the heat input to the affected facility from wood or other fuels or for heat derived from exhaust gases from other sources, such as stationary gas turbines, internal combustion engines, and kilns.

[[72 FR 32759](#), June 13, 2007, as amended at [74 FR 5090](#), Jan. 28, 2009; [77 FR 9462](#), Feb. 16, 2012]

§ 60.43c Standard for particulate matter (PM).

(a) On and after the date on which the initial performance test is completed or required to be completed under [§ 60.8](#), whichever date comes first, no owner or operator of an affected facility that commenced construction, reconstruction, or modification on or before February 28, 2005, that combusts coal or combusts mixtures of coal with other fuels and has a heat input capacity of 8.7 MW (30 MMBtu/h) or greater, shall cause to be discharged into the atmosphere from that affected facility any gases that contain PM in excess of the following emission limits:

(1) 22 ng/J (0.051 lb/MMBtu) heat input if the affected facility combusts only coal, or combusts coal with other fuels and has an annual capacity factor for the other fuels of 10 percent (0.10) or less.

(2) 43 ng/J (0.10 lb/MMBtu) heat input if the affected facility combusts coal with other fuels, has an annual capacity factor for the other fuels greater than 10 percent (0.10), and is subject to a federally enforceable requirement limiting operation of the affected facility to an annual capacity factor greater than 10 percent (0.10) for fuels other than coal.

(b) On and after the date on which the initial performance test is completed or required to be completed under [§ 60.8](#), whichever date comes first, no owner or operator of an affected facility that commenced construction, reconstruction, or modification on or before February 28, 2005, that combusts wood or combusts mixtures of wood with other fuels (except coal) and has a heat input capacity of 8.7 MW (30 MMBtu/h) or greater, shall cause to be discharged into the atmosphere from that affected facility any gases that contain PM in excess of the following emissions limits:

(1) 43 ng/J (0.10 lb/MMBtu) heat input if the affected facility has an annual capacity factor for wood greater than 30 percent (0.30); or

(2) 130 ng/J (0.30 lb/MMBtu) heat input if the affected facility has an annual capacity factor for wood of 30 percent (0.30) or less and is subject to a federally enforceable requirement limiting operation of the affected facility to an annual capacity factor for wood of 30 percent (0.30) or less.

(c) On and after the date on which the initial performance test is completed or required to be completed under [§ 60.8](#), whichever date comes first, no owner or operator of an affected facility that combusts coal, wood, or oil and has a heat input capacity of 8.7 MW (30 MMBtu/h) or greater shall cause to be discharged into the atmosphere from that affected facility any gases that exhibit greater than 20 percent opacity (6-minute average), except for one 6-minute period per hour of not more than 27 percent opacity. Owners and operators of an affected facility that elect to install, calibrate, maintain, and operate a continuous emissions monitoring system (CEMS) for measuring PM emissions according to the requirements of this subpart and are subject to a federally enforceable PM limit of 0.030 lb/MMBtu or less are exempt from the opacity standard specified in this [paragraph \(c\)](#).

(d) The PM and opacity standards under this section apply at all times, except during periods of startup, shutdown, or malfunction.

(e)

(1) On and after the date on which the initial performance test is completed or is required to be completed under [§ 60.8](#), whichever date comes first, no owner or operator of an affected facility that commences construction, reconstruction, or modification after February 28, 2005, and that combusts coal, oil, wood, a mixture of these fuels, or a mixture of these fuels with any other fuels and has a heat input capacity of 8.7 MW (30 MMBtu/h) or greater shall cause to be discharged into the atmosphere from that affected facility any gases that contain PM in excess of 13 ng/J (0.030 lb/MMBtu) heat input, except as provided in [paragraphs \(e\)\(2\)](#), [\(e\)\(3\)](#), and [\(e\)\(4\)](#) of this section.

(2) As an alternative to meeting the requirements of [paragraph \(e\)\(1\)](#) of this section, the owner or operator of an affected facility for which modification commenced after February 28, 2005, may elect to meet the requirements of this paragraph. On and after the date on which the initial performance test is completed or required to be completed under [§ 60.8](#), whichever date comes first, no owner or operator of an affected facility that commences modification after February 28, 2005 shall cause to be discharged into the atmosphere from that affected facility any gases that contain PM in excess of both:

(i) 22 ng/J (0.051 lb/MMBtu) heat input derived from the combustion of coal, oil, wood, a mixture of these fuels, or a mixture of these fuels with any other fuels; and

(ii) 0.2 percent of the combustion concentration (99.8 percent reduction) when combusting coal, oil, wood, a mixture of these fuels, or a mixture of these fuels with any other fuels.

(3) On and after the date on which the initial performance test is completed or is required to be completed under [§ 60.8](#), whichever date comes first, no owner or operator of an affected facility that commences modification after February 28, 2005, and that combusts over 30 percent wood (by heat input) on an annual basis and has a heat input capacity of 8.7 MW (30 MMBtu/h) or greater shall cause to be discharged into the atmosphere from that affected facility any gases that contain PM in excess of 43 ng/J (0.10 lb/MMBtu) heat input.

(4) An owner or operator of an affected facility that commences construction, reconstruction, or modification after February 28, 2005, and that combusts only oil that contains no more than 0.50 weight percent sulfur or a mixture of 0.50 weight percent sulfur oil with other fuels not subject to a PM standard under [§ 60.43c](#) and not using a post-combustion technology (except a wet scrubber) to reduce PM or SO₂ emissions is not subject to the PM limit in this section.

[[72 FR 32759](#), June 13, 2007, as amended at [74 FR 5091](#), Jan. 28, 2009; [77 FR 9462](#), Feb. 16, 2012]

§ 60.44c Compliance and performance test methods and procedures for sulfur dioxide.

(a) Except as provided in [paragraphs \(g\) and \(h\)](#) of this section and [§ 60.8\(b\)](#), performance tests required under [§ 60.8](#) shall be conducted following the procedures specified in [paragraphs \(b\), \(c\), \(d\), \(e\), and \(f\)](#) of this section, as applicable. [Section 60.8\(f\)](#) does not apply to this section. The 30-day notice required in [§ 60.8\(d\)](#) applies only to the initial performance test unless otherwise specified by the Administrator.

(b) The initial performance test required under [§ 60.8](#) shall be conducted over 30 consecutive operating days of the steam generating unit. Compliance with the percent reduction requirements and SO₂ emission limits under [§ 60.42c](#) shall be determined using a 30-day average. The first operating day included in the initial performance test shall be scheduled within 30 days after achieving the maximum production rate at which the affect facility will be operated, but not later than 180 days after the initial startup of the facility. The steam generating unit load during the 30-day period does not have to be the maximum design heat input capacity, but must be representative of future operating conditions.

(c) After the initial performance test required under [paragraph \(b\)](#) of this section and [§ 60.8](#), compliance with the percent reduction requirements and SO₂ emission limits under [§ 60.42c](#) is based on the average percent reduction and the average SO₂ emission rates for 30 consecutive steam generating unit operating days. A separate performance test is completed at the end of each steam generating unit operating day, and a new 30-day average percent reduction and SO₂ emission rate are calculated to show compliance with the standard.

(d) If only coal, only oil, or a mixture of coal and oil is combusted in an affected facility, the procedures in Method 19 of [appendix A of this part](#) are used to determine the hourly SO₂ emission rate (E_{ho}) and the 30-day average SO₂ emission rate (E_{ao}). The hourly averages used

to compute the 30-day averages are obtained from the CEMS. Method 19 of [appendix A of this part](#) shall be used to calculate E_{ao} when using daily fuel sampling or Method 6B of [appendix A of this part](#).

(e) If coal, oil, or coal and oil are combusted with other fuels:

(1) An adjusted E_{ho} (E_{hoO}) is used in Equation 19-19 of Method 19 of [appendix A of this part](#) to compute the adjusted E_{ao} (E_{aoO}). The E_{hoO} is computed using the following formula:

$$E_{hoO} = \frac{E_{ho} - E_w (1 - X_k)}{X_k}$$

Where:

E_{hoO} = Adjusted E_{ho} , ng/J (lb/MMBtu);

E_{ho} = Hourly SO_2 emission rate, ng/J (lb/MMBtu);

E_w = SO_2 concentration in fuels other than coal and oil combusted in the affected facility, as determined by fuel sampling and analysis procedures in Method 9 of [appendix A of this part](#), ng/J (lb/MMBtu). The value E_w for each fuel lot is used for each hourly average during the time that the lot is being combusted. The owner or operator does not have to measure E_w if the owner or operator elects to assume $E_w = 0$.

X_k = Fraction of the total heat input from fuel combustion derived from coal and oil, as determined by applicable procedures in Method 19 of [appendix A of this part](#).

(2) The owner or operator of an affected facility that qualifies under the provisions of [§ 60.42c\(c\)](#) or [\(d\)](#) (where percent reduction is not required) does not have to measure the parameters E_w or X_k if the owner or operator of the affected facility elects to measure emission rates of the coal or oil using the fuel sampling and analysis procedures under Method 19 of [appendix A of this part](#).

(f) Affected facilities subject to the percent reduction requirements under [§ 60.42c\(a\)](#) or [\(b\)](#) shall determine compliance with the SO_2 emission limits under [§ 60.42c](#) pursuant to [paragraphs \(d\)](#) or [\(e\)](#) of this section, and shall determine compliance with the percent reduction requirements using the following procedures:

(1) If only coal is combusted, the percent of potential SO_2 emission rate is computed using the following formula:

$$\%P_s = 100 \left(1 - \frac{\%R_g}{100} \right) \left(1 - \frac{\%R_f}{100} \right)$$

Where:

$\%P_s$ = Potential SO₂ emission rate, in percent;

$\%R_g$ = SO₂ removal efficiency of the control device as determined by Method 19 of [appendix A of this part](#), in percent; and

$\%R_f$ = SO₂ removal efficiency of fuel pretreatment as determined by Method 19 of [appendix A of this part](#), in percent.

(2) If coal, oil, or coal and oil are combusted with other fuels, the same procedures required in [paragraph \(f\)\(1\)](#) of this section are used, except as provided for in the following:

(i) To compute the $\%P_s$, an adjusted $\%R_g$ ($\%R_{gO}$) is computed from E_{aoO} from [paragraph \(e\)\(1\)](#) of this section and an adjusted average SO₂ inlet rate (E_{aiO}) using the following formula:

$$\%R_{gO} = 100 \left(1 - \frac{E_{aoO}^o}{E_{aiO}^o} \right)$$

Where:

$\%R_{gO}$ = Adjusted $\%R_g$, in percent;

E_{aoO} = Adjusted E_{ao} , ng/J (lb/MMBtu); and

E_{aiO} = Adjusted average SO₂ inlet rate, ng/J (lb/MMBtu).

(ii) To compute E_{aiO} , an adjusted hourly SO₂ inlet rate (E_{hiO}) is used. The E_{hiO} is computed using the following formula:

$$E_{hiO} = \frac{E_{hi} - E_w (1 - X_k)}{X_k}$$

Where:

E_{hi0} = Adjusted E_{hi} , ng/J (lb/MMBtu);

E_{hi} = Hourly SO_2 inlet rate, ng/J (lb/MMBtu);

E_w = SO_2 concentration in fuels other than coal and oil combusted in the affected facility, as determined by fuel sampling and analysis procedures in Method 19 of [appendix A of this part](#), ng/J (lb/MMBtu). The value E_w for each fuel lot is used for each hourly average during the time that the lot is being combusted. The owner or operator does not have to measure E_w if the owner or operator elects to assume $E_w = 0$; and

X_k = Fraction of the total heat input from fuel combustion derived from coal and oil, as determined by applicable procedures in Method 19 of [appendix A of this part](#).

(g) For oil-fired affected facilities where the owner or operator seeks to demonstrate compliance with the fuel oil sulfur limits under [§ 60.42c](#) based on shipment fuel sampling, the initial performance test shall consist of sampling and analyzing the oil in the initial tank of oil to be fired in the steam generating unit to demonstrate that the oil contains 0.5 weight percent sulfur or less. Thereafter, the owner or operator of the affected facility shall sample the oil in the fuel tank after each new shipment of oil is received, as described under [§ 60.46c\(d\)\(2\)](#).

(h) For affected facilities subject to [§ 60.42c\(h\)\(1\)](#), [\(2\)](#), or [\(3\)](#) where the owner or operator seeks to demonstrate compliance with the SO_2 standards based on fuel supplier certification, the performance test shall consist of the certification from the fuel supplier, as described in [§ 60.48c\(f\)](#), as applicable.

(i) The owner or operator of an affected facility seeking to demonstrate compliance with the SO_2 standards under [§ 60.42c\(c\)\(2\)](#) shall demonstrate the maximum design heat input capacity of the steam generating unit by operating the steam generating unit at this capacity for 24 hours. This demonstration shall be made during the initial performance test, and a subsequent demonstration may be requested at any other time. If the demonstrated 24-hour average firing rate for the affected facility is less than the maximum design heat input capacity stated by the manufacturer of the affected facility, the demonstrated 24-hour average firing rate shall be used to determine the annual capacity factor for the affected facility; otherwise, the maximum design heat input capacity provided by the manufacturer shall be used.

(j) The owner or operator of an affected facility shall use all valid SO_2 emissions data in calculating $\%P_s$ and E_{ho} under [paragraphs \(d\)](#), [\(e\)](#), or [\(f\)](#) of this section, as applicable, whether or not the minimum emissions data requirements under [§ 60.46c\(f\)](#) are achieved. All valid emissions data, including valid data collected during periods of startup, shutdown, and malfunction, shall be used in calculating $\%P_s$ or E_{ho} pursuant to [paragraphs \(d\)](#), [\(e\)](#), or [\(f\)](#) of this section, as applicable.

[[72 FR 32759](#), June 13, 2007, as amended at [74 FR 5091](#), Jan. 28, 2009]

§ 60.45c Compliance and performance test methods and procedures for particulate matter.

(a) The owner or operator of an affected facility subject to the PM and/or opacity standards under [§ 60.43c](#) shall conduct an initial performance test as required under [§ 60.8](#), and shall conduct subsequent performance tests as requested by the Administrator, to determine compliance with the standards using the following procedures and reference methods, except as specified in [paragraph \(c\)](#) of this section.

(1) Method 1 of [appendix A of this part](#) shall be used to select the sampling site and the number of traverse sampling points.

(2) Method 3A or 3B of appendix A-2 of this part shall be used for gas analysis when applying Method 5 or 5B of appendix A-3 of this part or 17 of appendix A-6 of this part.

(3) Method 5, 5B, or 17 of [appendix A of this part](#) shall be used to measure the concentration of PM as follows:

(i) Method 5 of [appendix A of this part](#) may be used only at affected facilities without wet scrubber systems.

(ii) Method 17 of [appendix A of this part](#) may be used at affected facilities with or without wet scrubber systems provided the stack gas temperature does not exceed a temperature of 160 °C (320 °F). The procedures of Sections 8.1 and 11.1 of Method 5B of [appendix A of this part](#) may be used in Method 17 of [appendix A of this part](#) only if Method 17 of [appendix A of this part](#) is used in conjunction with a wet scrubber system. Method 17 of [appendix A of this part](#) shall not be used in conjunction with a wet scrubber system if the effluent is saturated or laden with water droplets.

(iii) Method 5B of [appendix A of this part](#) may be used in conjunction with a wet scrubber system.

(4) The sampling time for each run shall be at least 120 minutes and the minimum sampling volume shall be 1.7 dry standard cubic meters (dscm) [60 dry standard cubic feet (dscf)] except that smaller sampling times or volumes may be approved by the Administrator when necessitated by process variables or other factors.

(5) For Method 5 or 5B of [appendix A of this part](#), the temperature of the sample gas in the probe and filter holder shall be monitored and maintained at 160 ±14 °C (320±25 °F).

(6) For determination of PM emissions, an oxygen (O₂) or carbon dioxide (CO₂) measurement shall be obtained simultaneously with each run of Method 5, 5B, or 17 of [appendix A of this part](#) by traversing the duct at the same sampling location.

(7) For each run using Method 5, 5B, or 17 of [appendix A of this part](#), the emission rates expressed in ng/J (lb/MMBtu) heat input shall be determined using:

- (i) The O₂ or CO₂ measurements and PM measurements obtained under this section,
- (ii) The dry basis F factor, and
- (iii) The dry basis emission rate calculation procedure contained in Method 19 of [appendix A of this part](#).

(8) Method 9 of appendix A-4 of this part shall be used for determining the opacity of stack emissions.

(b) The owner or operator of an affected facility seeking to demonstrate compliance with the PM standards under [§ 60.43c\(b\)\(2\)](#) shall demonstrate the maximum design heat input capacity of the steam generating unit by operating the steam generating unit at this capacity for 24 hours. This demonstration shall be made during the initial performance test, and a subsequent demonstration may be requested at any other time. If the demonstrated 24-hour average firing rate for the affected facility is less than the maximum design heat input capacity stated by the manufacturer of the affected facility, the demonstrated 24-hour average firing rate shall be used to determine the annual capacity factor for the affected facility; otherwise, the maximum design heat input capacity provided by the manufacturer shall be used.

(c) In place of PM testing with Method 5 or 5B of appendix A-3 of this part or Method 17 of appendix A-6 of this part, an owner or operator may elect to install, calibrate, maintain, and operate a CEMS for monitoring PM emissions discharged to the atmosphere and record the output of the system. The owner or operator of an affected facility who elects to continuously monitor PM emissions instead of conducting performance testing using Method 5 or 5B of appendix A-3 of this part or Method 17 of appendix A-6 of this part shall install, calibrate, maintain, and operate a CEMS and shall comply with the requirements specified in [paragraphs \(c\)\(1\) through \(c\)\(14\)](#) of this section.

(1) Notify the Administrator 1 month before starting use of the system.

(2) Notify the Administrator 1 month before stopping use of the system.

(3) The monitor shall be installed, evaluated, and operated in accordance with [§ 60.13](#) of [subpart A of this part](#).

(4) The initial performance evaluation shall be completed no later than 180 days after the date of initial startup of the affected facility, as specified under [§ 60.8](#) of [subpart A of this part](#) or within 180 days of notification to the Administrator of use of CEMS if the owner or operator was previously determining compliance by Method 5, 5B, or 17 of [appendix A of this part](#) performance tests, whichever is later.

(5) The owner or operator of an affected facility shall conduct an initial performance test for PM emissions as required under [§ 60.8 of subpart A of this part](#). Compliance with the PM emission limit shall be determined by using the CEMS specified in [paragraph \(d\)](#) of this section to measure PM and calculating a 24-hour block arithmetic average emission concentration using EPA Reference Method 19 of [appendix A of this part, section 4.1](#).

(6) Compliance with the PM emission limit shall be determined based on the 24-hour daily (block) average of the hourly arithmetic average emission concentrations using CEMS outlet data.

(7) At a minimum, valid CEMS hourly averages shall be obtained as specified in [paragraph \(c\)\(7\)\(i\)](#) of this section for 75 percent of the total operating hours per 30-day rolling average.

(i) At least two data points per hour shall be used to calculate each 1-hour arithmetic average.

(ii) [Reserved]

(8) The 1-hour arithmetic averages required under [paragraph \(c\)\(7\)](#) of this section shall be expressed in ng/J or lb/MMBtu heat input and shall be used to calculate the boiler operating day daily arithmetic average emission concentrations. The 1-hour arithmetic averages shall be calculated using the data points required under [§ 60.13\(e\)\(2\) of subpart A of this part](#).

(9) All valid CEMS data shall be used in calculating average emission concentrations even if the minimum CEMS data requirements of [paragraph \(c\)\(7\)](#) of this section are not met.

(10) The CEMS shall be operated according to Performance Specification 11 in [appendix B of this part](#).

(11) During the correlation testing runs of the CEMS required by Performance Specification 11 in [appendix B of this part](#), PM and O₂ (or CO₂) data shall be collected concurrently (or within a 30- to 60-minute period) by both the continuous emission monitors and performance tests conducted using the following test methods.

(i) For PM, Method 5 or 5B of appendix A-3 of this part or Method 17 of appendix A-6 of this part shall be used; and

(ii) For O₂ (or CO₂), Method 3A or 3B of appendix A-2 of this part, as applicable shall be used.

(12) Quarterly accuracy determinations and daily calibration drift tests shall be performed in accordance with procedure 2 in [appendix F of this part](#). Relative Response Audit's must be performed annually and Response Correlation Audits must be performed every 3 years.

(13) When PM emissions data are not obtained because of CEMS breakdowns, repairs, calibration checks, and zero and span adjustments, emissions data shall be obtained by using

other monitoring systems as approved by the Administrator or EPA Reference Method 19 of [appendix A of this part](#) to provide, as necessary, valid emissions data for a minimum of 75 percent of total operating hours on a 30-day rolling average.

(14) As of January 1, 2012, and within 90 days after the date of completing each performance test, as defined in [§ 60.8](#), conducted to demonstrate compliance with this subpart, you must submit relative accuracy test audit (*i.e.*, reference method) data and performance test (*i.e.*, compliance test) data, except opacity data, electronically to EPA's Central Data Exchange (CDX) by using the Electronic Reporting Tool (ERT)

(see http://www.epa.gov/ttn/chief/ert/ert_tool.html/) or other compatible electronic spreadsheet. Only data collected using test methods compatible with ERT are subject to this requirement to be submitted electronically into EPA's WebFIRE database.

(d) The owner or operator of an affected facility seeking to demonstrate compliance under [§ 60.43c\(e\)\(4\)](#) shall follow the applicable procedures under [§ 60.48c\(f\)](#). For residual oil-fired affected facilities, fuel supplier certifications are only allowed for facilities with heat input capacities between 2.9 and 8.7 MW (10 to 30 MMBtu/h).

[[72 FR 32759](#), June 13, 2007, as amended at [74 FR 5091](#), Jan. 28, 2009; [76 FR 3523](#), Jan. 20, 2011; [77 FR 9463](#), Feb. 16, 2012]

§ 60.46c Emission monitoring for sulfur dioxide.

(a) Except as provided in [paragraphs \(d\) and \(e\)](#) of this section, the owner or operator of an affected facility subject to the SO₂ emission limits under [§ 60.42c](#) shall install, calibrate, maintain, and operate a CEMS for measuring SO₂ concentrations and either O₂ or CO₂ concentrations at the outlet of the SO₂ control device (or the outlet of the steam generating unit if no SO₂ control device is used), and shall record the output of the system. The owner or operator of an affected facility subject to the percent reduction requirements under [§ 60.42c](#) shall measure SO₂ concentrations and either O₂ or CO₂ concentrations at both the inlet and outlet of the SO₂ control device.

(b) The 1-hour average SO₂ emission rates measured by a CEMS shall be expressed in ng/J or lb/MMBtu heat input and shall be used to calculate the average emission rates under [§ 60.42c](#). Each 1-hour average SO₂ emission rate must be based on at least 30 minutes of operation, and shall be calculated using the data points required under [§ 60.13\(h\)\(2\)](#). Hourly SO₂ emission rates are not calculated if the affected facility is operated less than 30 minutes in a 1-hour period and are not counted toward determination of a steam generating unit operating day.

(c) The procedures under [§ 60.13](#) shall be followed for installation, evaluation, and operation of the CEMS.

(1) All CEMS shall be operated in accordance with the applicable procedures under Performance Specifications 1, 2, and 3 of [appendix B of this part](#).

(2) Quarterly accuracy determinations and daily calibration drift tests shall be performed in accordance with Procedure 1 of [appendix F of this part](#).

(3) For affected facilities subject to the percent reduction requirements under [§ 60.42c](#), the span value of the SO₂ CEMS at the inlet to the SO₂ control device shall be 125 percent of the maximum estimated hourly potential SO₂ emission rate of the fuel combusted, and the span value of the SO₂ CEMS at the outlet from the SO₂ control device shall be 50 percent of the maximum estimated hourly potential SO₂ emission rate of the fuel combusted.

(4) For affected facilities that are not subject to the percent reduction requirements of [§ 60.42c](#), the span value of the SO₂ CEMS at the outlet from the SO₂ control device (or outlet of the steam generating unit if no SO₂ control device is used) shall be 125 percent of the maximum estimated hourly potential SO₂ emission rate of the fuel combusted.

(d) As an alternative to operating a CEMS at the inlet to the SO₂ control device (or outlet of the steam generating unit if no SO₂ control device is used) as required under [paragraph \(a\)](#) of this section, an owner or operator may elect to determine the average SO₂ emission rate by sampling the fuel prior to combustion. As an alternative to operating a CEMS at the outlet from the SO₂ control device (or outlet of the steam generating unit if no SO₂ control device is used) as required under [paragraph \(a\)](#) of this section, an owner or operator may elect to determine the average SO₂ emission rate by using Method 6B of [appendix A of this part](#). Fuel sampling shall be conducted pursuant to either [paragraph \(d\)\(1\)](#) or [\(d\)\(2\)](#) of this section. Method 6B of [appendix A of this part](#) shall be conducted pursuant to [paragraph \(d\)\(3\)](#) of this section.

(1) For affected facilities combusting coal or oil, coal or oil samples shall be collected daily in an as-fired condition at the inlet to the steam generating unit and analyzed for sulfur content and heat content according the Method 19 of [appendix A of this part](#). Method 19 of [appendix A of this part](#) provides procedures for converting these measurements into the format to be used in calculating the average SO₂ input rate.

(2) As an alternative fuel sampling procedure for affected facilities combusting oil, oil samples may be collected from the fuel tank for each steam generating unit immediately after the fuel tank is filled and before any oil is combusted. The owner or operator of the affected facility shall analyze the oil sample to determine the sulfur content of the oil. If a partially empty fuel tank is refilled, a new sample and analysis of the fuel in the tank would be required upon filling. Results of the fuel analysis taken after each new shipment of oil is received shall be used as the daily value when calculating the 30-day rolling average until the next shipment is received. If the fuel analysis shows that the sulfur content in the fuel tank is greater than 0.5 weight percent sulfur, the owner or operator shall ensure that the sulfur content of subsequent oil shipments is low enough to cause the 30-day rolling average sulfur content to be 0.5 weight percent sulfur or less.

(3) Method 6B of [appendix A of this part](#) may be used in lieu of CEMS to measure SO₂ at the inlet or outlet of the SO₂ control system. An initial stratification test is required to verify the adequacy of the Method 6B of [appendix A of this part](#) sampling location. The stratification test shall consist of three paired runs of a suitable SO₂ and CO₂ measurement

train operated at the candidate location and a second similar train operated according to the procedures in [§ 3.2](#) and the applicable procedures in section 7 of Performance Specification 2 of [appendix B of this part](#). Method 6B of [appendix A of this part](#), Method 6A of [appendix A of this part](#), or a combination of Methods 6 and 3 of [appendix A of this part](#) or Methods 6C and 3A of [appendix A of this part](#) are suitable measurement techniques. If Method 6B of [appendix A of this part](#) is used for the second train, sampling time and timer operation may be adjusted for the stratification test as long as an adequate sample volume is collected; however, both sampling trains are to be operated similarly. For the location to be adequate for Method 6B of [appendix A of this part](#) 24-hour tests, the mean of the absolute difference between the three paired runs must be less than 10 percent (0.10).

(e) The monitoring requirements of [paragraphs \(a\)](#) and [\(d\)](#) of this section shall not apply to affected facilities subject to [§ 60.42c\(h\) \(1\), \(2\), or \(3\)](#) where the owner or operator of the affected facility seeks to demonstrate compliance with the SO₂ standards based on fuel supplier certification, as described under [§ 60.48c\(f\)](#), as applicable.

(f) The owner or operator of an affected facility operating a CEMS pursuant to [paragraph \(a\)](#) of this section, or conducting as-fired fuel sampling pursuant to [paragraph \(d\)\(1\)](#) of this section, shall obtain emission data for at least 75 percent of the operating hours in at least 22 out of 30 successive steam generating unit operating days. If this minimum data requirement is not met with a single monitoring system, the owner or operator of the affected facility shall supplement the emission data with data collected with other monitoring systems as approved by the Administrator.

§ 60.47c Emission monitoring for particulate matter.

(a) Except as provided in [paragraphs \(c\), \(d\), \(e\), and \(f\)](#) of this section, the owner or operator of an affected facility combusting coal, oil, or wood that is subject to the opacity standards under [§ 60.43c](#) shall install, calibrate, maintain, and operate a continuous opacity monitoring system (COMS) for measuring the opacity of the emissions discharged to the atmosphere and record the output of the system. The owner or operator of an affected facility subject to an opacity standard in [§ 60.43c\(c\)](#) that is not required to use a COMS due to [paragraphs \(c\), \(d\), \(e\), or \(f\)](#) of this section that elects not to use a COMS shall conduct a performance test using Method 9 of appendix A-4 of this part and the procedures in [§ 60.11](#) to demonstrate compliance with the applicable limit in [§ 60.43c](#) by April 29, 2011, within 45 days of stopping use of an existing COMS, or within 180 days after initial startup of the facility, whichever is later, and shall comply with either [paragraphs \(a\)\(1\), \(a\)\(2\), or \(a\)\(3\)](#) of this section. The observation period for Method 9 of appendix A-4 of this part performance tests may be reduced from 3 hours to 60 minutes if all 6-minute averages are less than 10 percent and all individual 15-second observations are less than or equal to 20 percent during the initial 60 minutes of observation.

(1) Except as provided in [paragraph \(a\)\(2\)](#) and [\(a\)\(3\)](#) of this section, the owner or operator shall conduct subsequent Method 9 of appendix A-4 of this part performance tests using the procedures in [paragraph \(a\)](#) of this section according to the applicable schedule in [paragraphs](#)

[\(a\)\(1\)\(i\)](#) through [\(a\)\(1\)\(iv\)](#) of this section, as determined by the most recent Method 9 of appendix A-4 of this part performance test results.

(i) If no visible emissions are observed, a subsequent Method 9 of appendix A-4 of this part performance test must be completed within 12 calendar months from the date that the most recent performance test was conducted or within 45 days of the next day that fuel with an opacity standard is combusted, whichever is later;

(ii) If visible emissions are observed but the maximum 6-minute average opacity is less than or equal to 5 percent, a subsequent Method 9 of appendix A-4 of this part performance test must be completed within 6 calendar months from the date that the most recent performance test was conducted or within 45 days of the next day that fuel with an opacity standard is combusted, whichever is later;

(iii) If the maximum 6-minute average opacity is greater than 5 percent but less than or equal to 10 percent, a subsequent Method 9 of appendix A-4 of this part performance test must be completed within 3 calendar months from the date that the most recent performance test was conducted or within 45 days of the next day that fuel with an opacity standard is combusted, whichever is later; or

(iv) If the maximum 6-minute average opacity is greater than 10 percent, a subsequent Method 9 of appendix A-4 of this part performance test must be completed within 45 calendar days from the date that the most recent performance test was conducted.

(2) If the maximum 6-minute opacity is less than 10 percent during the most recent Method 9 of appendix A-4 of this part performance test, the owner or operator may, as an alternative to performing subsequent Method 9 of appendix A-4 of this part performance tests, elect to perform subsequent monitoring using Method 22 of appendix A-7 of this part according to the procedures specified in [paragraphs \(a\)\(2\)\(i\)](#) and [\(ii\)](#) of this section.

(i) The owner or operator shall conduct 10 minute observations (during normal operation) each operating day the affected facility fires fuel for which an opacity standard is applicable using Method 22 of appendix A-7 of this part and demonstrate that the sum of the occurrences of any visible emissions is not in excess of 5 percent of the observation period (*i.e.*, 30 seconds per 10 minute period). If the sum of the occurrence of any visible emissions is greater than 30 seconds during the initial 10 minute observation, immediately conduct a 30 minute observation. If the sum of the occurrence of visible emissions is greater than 5 percent of the observation period (*i.e.*, 90 seconds per 30 minute period), the owner or operator shall either document and adjust the operation of the facility and demonstrate within 24 hours that the sum of the occurrence of visible emissions is equal to or less than 5 percent during a 30 minute observation (*i.e.*, 90 seconds) or conduct a new Method 9 of appendix A-4 of this part performance test using the procedures in [paragraph \(a\)](#) of this section within 45 calendar days according to the requirements in [§ 60.45c\(a\)\(8\)](#).

(ii) If no visible emissions are observed for 10 operating days during which an opacity standard is applicable, observations can be reduced to once every 7 operating days during

which an opacity standard is applicable. If any visible emissions are observed, daily observations shall be resumed.

(3) If the maximum 6-minute opacity is less than 10 percent during the most recent Method 9 of appendix A-4 of this part performance test, the owner or operator may, as an alternative to performing subsequent Method 9 of appendix A-4 performance tests, elect to perform subsequent monitoring using a digital opacity compliance system according to a site-specific monitoring plan approved by the Administrator. The observations shall be similar, but not necessarily identical, to the requirements in [paragraph \(a\)\(2\)](#) of this section. For reference purposes in preparing the monitoring plan, see OAQPS “Determination of Visible Emission Opacity from Stationary Sources Using Computer-Based Photographic Analysis Systems.” This document is available from the U.S. Environmental Protection Agency (U.S. EPA); Office of Air Quality and Planning Standards; Sector Policies and Programs Division; Measurement Policy Group (D243-02), Research Triangle Park, NC 27711. This document is also available on the Technology Transfer Network (TTN) under Emission Measurement Center Preliminary Methods.

(b) All COMS shall be operated in accordance with the applicable procedures under Performance Specification 1 of [appendix B of this part](#). The span value of the opacity COMS shall be between 60 and 80 percent.

(c) Owners and operators of an affected facilities that burn only distillate oil that contains no more than 0.5 weight percent sulfur and/or liquid or gaseous fuels with potential sulfur dioxide emission rates of 26 ng/J (0.060 lb/MMBtu) heat input or less and that do not use a post-combustion technology to reduce SO₂ or PM emissions and that are subject to an opacity standard in [§ 60.43c\(c\)](#) are not required to operate a COMS if they follow the applicable procedures in [§ 60.48c\(f\)](#).

(d) Owners or operators complying with the PM emission limit by using a PM CEMS must calibrate, maintain, operate, and record the output of the system for PM emissions discharged to the atmosphere as specified in [§ 60.45c\(c\)](#). The CEMS specified in [paragraph § 60.45c\(c\)](#) shall be operated and data recorded during all periods of operation of the affected facility except for CEMS breakdowns and repairs. Data is recorded during calibration checks, and zero and span adjustments.

(e) Owners and operators of an affected facility that is subject to an opacity standard in [§ 60.43c\(c\)](#) and that does not use post-combustion technology (except a wet scrubber) for reducing PM, SO₂, or carbon monoxide (CO) emissions, burns only gaseous fuels or fuel oils that contain less than or equal to 0.5 weight percent sulfur, and is operated such that emissions of CO discharged to the atmosphere from the affected facility are maintained at levels less than or equal to 0.15 lb/MMBtu on a boiler operating day average basis is not required to operate a COMS. Owners and operators of affected facilities electing to comply with this paragraph must demonstrate compliance according to the procedures specified in [paragraphs \(e\)\(1\) through \(4\)](#) of this section; or

(1) You must monitor CO emissions using a CEMS according to the procedures specified in [paragraphs \(e\)\(1\)\(i\) through \(iv\)](#) of this section.

(i) The CO CEMS must be installed, certified, maintained, and operated according to the provisions in [§ 60.58b\(i\)\(3\)](#) of [subpart Eb of this part](#).

(ii) Each 1-hour CO emissions average is calculated using the data points generated by the CO CEMS expressed in parts per million by volume corrected to 3 percent oxygen (dry basis).

(iii) At a minimum, valid 1-hour CO emissions averages must be obtained for at least 90 percent of the operating hours on a 30-day rolling average basis. The 1-hour averages are calculated using the data points required in [§ 60.13\(h\)\(2\)](#).

(iv) Quarterly accuracy determinations and daily calibration drift tests for the CO CEMS must be performed in accordance with procedure 1 in [appendix F of this part](#).

(2) You must calculate the 1-hour average CO emissions levels for each steam generating unit operating day by multiplying the average hourly CO output concentration measured by the CO CEMS times the corresponding average hourly flue gas flow rate and divided by the corresponding average hourly heat input to the affected source. The 24-hour average CO emission level is determined by calculating the arithmetic average of the hourly CO emission levels computed for each steam generating unit operating day.

(3) You must evaluate the preceding 24-hour average CO emission level each steam generating unit operating day excluding periods of affected source startup, shutdown, or malfunction. If the 24-hour average CO emission level is greater than 0.15 lb/MMBtu, you must initiate investigation of the relevant equipment and control systems within 24 hours of the first discovery of the high emission incident and, take the appropriate corrective action as soon as practicable to adjust control settings or repair equipment to reduce the 24-hour average CO emission level to 0.15 lb/MMBtu or less.

(4) You must record the CO measurements and calculations performed according to [paragraph \(e\)](#) of this section and any corrective actions taken. The record of corrective action taken must include the date and time during which the 24-hour average CO emission level was greater than 0.15 lb/MMBtu, and the date, time, and description of the corrective action.

(f) An owner or operator of an affected facility that is subject to an opacity standard in [§ 60.43c\(c\)](#) is not required to operate a COMS provided that the affected facility meets the conditions in either [paragraphs \(f\)\(1\), \(2\), or \(3\)](#) of this section.

(1) The affected facility uses a fabric filter (baghouse) as the primary PM control device and, the owner or operator operates a bag leak detection system to monitor the performance of the fabric filter according to the requirements in section [§ 60.48Da of this part](#).

(2) The affected facility uses an ESP as the primary PM control device, and the owner or operator uses an ESP predictive model to monitor the performance of the ESP developed in accordance and operated according to the requirements in section [§ 60.48Da of this part](#).

(3) The affected facility burns only gaseous fuels and/or fuel oils that contain no greater than 0.5 weight percent sulfur, and the owner or operator operates the unit according to a written site-specific monitoring plan approved by the permitting authority. This monitoring plan must include procedures and criteria for establishing and monitoring specific parameters for the affected facility indicative of compliance with the opacity standard. For testing performed as part of this site-specific monitoring plan, the permitting authority may require as an alternative to the notification and reporting requirements specified in [§§ 60.8](#) and [60.11](#) that the owner or operator submit any deviations with the excess emissions report required under [§ 60.48c\(c\)](#).

[[72 FR 32759](#), June 13, 2007, as amended at [74 FR 5091](#), Jan. 28, 2009; [76 FR 3523](#), Jan. 20, 2011; [77 FR 9463](#), Feb. 16, 2012]

§ 60.48c Reporting and recordkeeping requirements.

(a) The owner or operator of each affected facility shall submit notification of the date of construction or reconstruction and actual startup, as provided by [§ 60.7 of this part](#). This notification shall include:

(1) The design heat input capacity of the affected facility and identification of fuels to be combusted in the affected facility.

(2) If applicable, a copy of any federally enforceable requirement that limits the annual capacity factor for any fuel or mixture of fuels under [§ 60.42c](#), or [§ 60.43c](#).

(3) The annual capacity factor at which the owner or operator anticipates operating the affected facility based on all fuels fired and based on each individual fuel fired.

(4) Notification if an emerging technology will be used for controlling SO₂ emissions. The Administrator will examine the description of the control device and will determine whether the technology qualifies as an emerging technology. In making this determination, the Administrator may require the owner or operator of the affected facility to submit additional information concerning the control device. The affected facility is subject to the provisions of [§ 60.42c\(a\)](#) or [\(b\)\(1\)](#), unless and until this determination is made by the Administrator.

(b) The owner or operator of each affected facility subject to the SO₂ emission limits of [§ 60.42c](#), or the PM or opacity limits of [§ 60.43c](#), shall submit to the Administrator the performance test data from the initial and any subsequent performance tests and, if applicable, the performance evaluation of the CEMS and/or COMS using the applicable performance specifications in [appendix B of this part](#).

(c) In addition to the applicable requirements in [§ 60.7](#), the owner or operator of an affected facility subject to the opacity limits in [§ 60.43c\(c\)](#) shall submit excess emission reports for any excess emissions from the affected facility that occur during the reporting period and maintain records according to the requirements specified in [paragraphs \(c\)\(1\)](#) through [\(3\)](#) of this section, as applicable to the visible emissions monitoring method used.

(1) For each performance test conducted using Method 9 of appendix A-4 of this part, the owner or operator shall keep the records including the information specified in [paragraphs \(c\)\(1\)\(i\)](#) through [\(iii\)](#) of this section.

(i) Dates and time intervals of all opacity observation periods;

(ii) Name, affiliation, and copy of current visible emission reading certification for each visible emission observer participating in the performance test; and

(iii) Copies of all visible emission observer opacity field data sheets;

(2) For each performance test conducted using Method 22 of appendix A-4 of this part, the owner or operator shall keep the records including the information specified in [paragraphs \(c\)\(2\)\(i\)](#) through [\(iv\)](#) of this section.

(i) Dates and time intervals of all visible emissions observation periods;

(ii) Name and affiliation for each visible emission observer participating in the performance test;

(iii) Copies of all visible emission observer opacity field data sheets; and

(iv) Documentation of any adjustments made and the time the adjustments were completed to the affected facility operation by the owner or operator to demonstrate compliance with the applicable monitoring requirements.

(3) For each digital opacity compliance system, the owner or operator shall maintain records and submit reports according to the requirements specified in the site-specific monitoring plan approved by the Administrator

(d) The owner or operator of each affected facility subject to the SO₂ emission limits, fuel oil sulfur limits, or percent reduction requirements under [§ 60.42c](#) shall submit reports to the Administrator.

(e) The owner or operator of each affected facility subject to the SO₂ emission limits, fuel oil sulfur limits, or percent reduction requirements under [§ 60.42c](#) shall keep records and submit reports as required under [paragraph \(d\)](#) of this section, including the following information, as applicable.

(1) Calendar dates covered in the reporting period.

(2) Each 30-day average SO₂ emission rate (ng/J or lb/MMBtu), or 30-day average sulfur content (weight percent), calculated during the reporting period, ending with the last 30-day period; reasons for any noncompliance with the emission standards; and a description of corrective actions taken.

(3) Each 30-day average percent of potential SO₂ emission rate calculated during the reporting period, ending with the last 30-day period; reasons for any noncompliance with the emission standards; and a description of the corrective actions taken.

(4) Identification of any steam generating unit operating days for which SO₂ or diluent (O₂ or CO₂) data have not been obtained by an approved method for at least 75 percent of the operating hours; justification for not obtaining sufficient data; and a description of corrective actions taken.

(5) Identification of any times when emissions data have been excluded from the calculation of average emission rates; justification for excluding data; and a description of corrective actions taken if data have been excluded for periods other than those during which coal or oil were not combusted in the steam generating unit.

(6) Identification of the F factor used in calculations, method of determination, and type of fuel combusted.

(7) Identification of whether averages have been obtained based on CEMS rather than manual sampling methods.

(8) If a CEMS is used, identification of any times when the pollutant concentration exceeded the full span of the CEMS.

(9) If a CEMS is used, description of any modifications to the CEMS that could affect the ability of the CEMS to comply with Performance Specifications 2 or 3 of [appendix B of this part](#).

(10) If a CEMS is used, results of daily CEMS drift tests and quarterly accuracy assessments as required under appendix F, Procedure 1 of this part.

(11) If fuel supplier certification is used to demonstrate compliance, records of fuel supplier certification as described under [paragraph \(f\)\(1\), \(2\), \(3\), or \(4\)](#) of this section, as applicable. In addition to records of fuel supplier certifications, the report shall include a certified statement signed by the owner or operator of the affected facility that the records of fuel supplier certifications submitted represent all of the fuel combusted during the reporting period.

(f) Fuel supplier certification shall include the following information:

(1) For distillate oil:

(i) The name of the oil supplier;

(ii) A statement from the oil supplier that the oil complies with the specifications under the definition of distillate oil in [§ 60.41c](#); and

(iii) The sulfur content or maximum sulfur content of the oil.

(2) For residual oil:

(i) The name of the oil supplier;

(ii) The location of the oil when the sample was drawn for analysis to determine the sulfur content of the oil, specifically including whether the oil was sampled as delivered to the affected facility, or whether the sample was drawn from oil in storage at the oil supplier's or oil refiner's facility, or other location;

(iii) The sulfur content of the oil from which the shipment came (or of the shipment itself); and

(iv) The method used to determine the sulfur content of the oil.

(3) For coal:

(i) The name of the coal supplier;

(ii) The location of the coal when the sample was collected for analysis to determine the properties of the coal, specifically including whether the coal was sampled as delivered to the affected facility or whether the sample was collected from coal in storage at the mine, at a coal preparation plant, at a coal supplier's facility, or at another location. The certification shall include the name of the coal mine (and coal seam), coal storage facility, or coal preparation plant (where the sample was collected);

(iii) The results of the analysis of the coal from which the shipment came (or of the shipment itself) including the sulfur content, moisture content, ash content, and heat content; and

(iv) The methods used to determine the properties of the coal.

(4) For other fuels:

(i) The name of the supplier of the fuel;

(ii) The potential sulfur emissions rate or maximum potential sulfur emissions rate of the fuel in ng/J heat input; and

(iii) The method used to determine the potential sulfur emissions rate of the fuel.

(g)

(1) Except as provided under [paragraphs \(g\)\(2\)](#) and [\(g\)\(3\)](#) of this section, the owner or operator of each affected facility shall record and maintain records of the amount of each fuel combusted during each operating day.

(2) As an alternative to meeting the requirements of [paragraph \(g\)\(1\)](#) of this section, the owner or operator of an affected facility that combusts only natural gas, wood, fuels using fuel certification in [§ 60.48c\(f\)](#) to demonstrate compliance with the SO₂ standard, fuels not subject to an emissions standard (excluding opacity), or a mixture of these fuels may elect to record and maintain records of the amount of each fuel combusted during each calendar month.

(3) As an alternative to meeting the requirements of [paragraph \(g\)\(1\)](#) of this section, the owner or operator of an affected facility or multiple affected facilities located on a contiguous property unit where the only fuels combusted in any steam generating unit (including steam generating units not subject to this subpart) at that property are natural gas, wood, distillate oil meeting the most current requirements in [§ 60.42C](#) to use fuel certification to demonstrate compliance with the SO₂ standard, and/or fuels, excluding coal and residual oil, not subject to an emissions standard (excluding opacity) may elect to record and maintain records of the total amount of each steam generating unit fuel delivered to that property during each calendar month.

(h) The owner or operator of each affected facility subject to a federally enforceable requirement limiting the annual capacity factor for any fuel or mixture of fuels under [§ 60.42c](#) or [§ 60.43c](#) shall calculate the annual capacity factor individually for each fuel combusted. The annual capacity factor is determined on a 12-month rolling average basis with a new annual capacity factor calculated at the end of the calendar month.

(i) All records required under this section shall be maintained by the owner or operator of the affected facility for a period of two years following the date of such record.

(j) The reporting period for the reports required under this subpart is each six-month period. All reports shall be submitted to the Administrator and shall be postmarked by the 30th day following the end of the reporting period.

[[72 FR 32759](#), June 13, 2007, as amended at [74 FR 5091](#), Jan. 28, 2009]

Appendix B

40 C.F.R. Part 60 Subpart AAa

***Standards of Performance for Electric Arc Furnaces and Argon-Oxygen Decarburization
Vessels Constructed After August 7, 1983***

Subpart AAa - Standards of Performance for Steel Plants: Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 17, 1983

Source: [49 FR 43845](#), Oct. 31, 1984, unless otherwise noted.

§ 60.270a Applicability and designation of affected facility.

(a) The provisions of this subpart are applicable to the following affected facilities in steel plants that produce carbon, alloy, or specialty steels: electric arc furnaces, argon-oxygen decarburization vessels, and dust-handling systems.

(b) The provisions of this subpart apply to each affected facility identified in [paragraph \(a\)](#) of this section that commences construction, modification, or reconstruction after August 17, 1983.

§ 60.271a Definitions.

As used in this subpart, all terms not defined herein shall have the meaning given them in the Act and in [subpart A of this part](#).

Argon-oxygen decarburization vessel (AOD vessel) means any closed-bottom, refractory-lined converter vessel with submerged tuyeres through which gaseous mixtures containing argon and oxygen or nitrogen may be blown into molten steel for further refining.

Bag leak detection system means a system that is capable of continuously monitoring relative particulate matter (dust) loadings in the exhaust of a baghouse to detect bag leaks and other conditions that result in increases in particulate loadings. A bag leak detection system includes, but is not limited to, an instrument that operates on triboelectric, electrodynamic, light scattering, light transmittance, or other effect to continuously monitor relative particulate matter loadings.

Capture system means the equipment (including ducts, hoods, fans, dampers, etc.) used to capture or transport particulate matter generated by an electric arc furnace or AOD vessel to the air pollution control device.

Charge means the addition of iron and steel scrap or other materials into the top of an electric arc furnace or the addition of molten steel or other materials into the top of an AOD vessel.

Control device means the air pollution control equipment used to remove particulate matter from the effluent gas stream generated by an electric arc furnace or AOD vessel.

Direct-shell evacuation control system (DEC system) means a system that maintains a negative pressure within the electric arc furnace above the slag or metal and ducts emissions to the control device.

Dust-handling system means equipment used to handle particulate matter collected by the control device for an electric arc furnace or AOD vessel subject to this subpart. For the purposes

of this subpart, the dust-handling system shall consist of the control device dust hoppers, the dust-conveying equipment, any central dust storage equipment, the dust-treating equipment (e.g., pug mill, pelletizer), dust transfer equipment (from storage to truck), and any secondary control devices used with the dust transfer equipment.

Electric arc furnace (EAF) means a furnace that produces molten steel and heats the charge materials with electric arcs from carbon electrodes. For the purposes of this subpart, an EAF shall consist of the furnace shell and roof and the transformer. Furnaces that continuously feed direct-reduced iron ore pellets as the primary source of iron are not affected facilities within the scope of this definition.

Heat cycle means the period beginning when scrap is charged to an empty EAF and ending when the EAF tap is completed or beginning when molten steel is charged to an empty AOD vessel and ending when the AOD vessel tap is completed.

Meltdown and refining period means the time period commencing at the termination of the initial charging period and ending at the initiation of the tapping period, excluding any intermediate charging periods and times when power to the EAF is off.

Melting means that phase of steel production cycle during which the iron and steel scrap is heated to the molten state.

Negative-pressure fabric filter means a fabric filter with the fans on the downstream side of the filter bags.

Positive-pressure fabric filter means a fabric filter with the fans on the upstream side of the filter bags.

Refining means that phase of the steel production cycle during which undesirable elements are removed from the molten steel and alloys are added to reach the final metal chemistry.

Shop means the building which houses one or more EAF's or AOD vessels.

Shop opacity means the arithmetic average of 24 observations of the opacity of emissions from the shop taken in accordance with Method 9 of [appendix A of this part](#).

Tap means the pouring of molten steel from an EAF or AOD vessel.

Tapping period means the time period commencing at the moment an EAF begins to pour molten steel and ending either three minutes after steel ceases to flow from an EAF, or six minutes after steel begins to flow, whichever is longer.

[[49 FR 43845](#), Oct. 31, 1984, as amended at [64 FR 10110](#), Mar. 2, 1999; [70 FR 8532](#), Feb. 22, 2005]

§ 60.272a Standard for particulate matter.

(a) On and after the date of which the performance test required to be conducted by [§ 60.8](#) is completed, no owner or operator subject to the provisions of this subpart shall cause to be discharged into the atmosphere from an EAF or an AOD vessel any gases which:

(1) Exit from a control device and contain particulate matter in excess of 12 mg/dscm (0.0052 gr/dscf);

(2) Exit from a control device and exhibit 3 percent opacity or greater; and

(3) Exit from a shop and, due solely to the operations of any affected EAF(s) or AOD vessel(s), exhibit 6 percent opacity or greater.

(b) On and after the date on which the performance test required to be conducted by [§ 60.8](#) is completed, no owner or operator subject to the provisions of this subpart shall cause to be discharged into the atmosphere from the dust-handling system any gases that exhibit 10 percent opacity or greater.

§ 60.273a Emission monitoring.

(a) Except as provided under [paragraphs \(b\)](#) and [\(c\)](#) of this section, a continuous monitoring system for the measurement of the opacity of emissions discharged into the atmosphere from the control device(s) shall be installed, calibrated, maintained, and operated by the owner or operator subject to the provisions of this subpart.

(b) No continuous monitoring system shall be required on any control device serving the dust-handling system.

(c) A continuous monitoring system for the measurement of the opacity of emissions discharged into the atmosphere from the control device(s) is not required on any modular, multi-stack, negative-pressure or positive-pressure fabric filter if observations of the opacity of the visible emissions from the control device are performed by a certified visible emission observer; or on any single-stack fabric filter if visible emissions from the control device are performed by a certified visible emission observer and the owner installs and continuously operates a bag leak detection system according to [paragraph \(e\)](#) of this section. Visible emission observations shall be conducted at least once per day for at least three 6-minute periods when the furnace is operating in the melting and refining period. All visible emissions observations shall be conducted in accordance with Method 9. If visible emissions occur from more than one point, the opacity shall be recorded for any points where visible emissions are observed. Where it is possible to determine that a number of visible emission sites relate to only one incident of the visible emission, only one set of three 6-minute observations will be required. In that case, the Method 9 observations must be made for the site of highest opacity that directly relates to the cause (or location) of visible emissions observed during a single incident. Records shall be maintained of any 6-minute average that is in excess of the emission limit specified in [§ 60.272a\(a\)](#).

(d) A furnace static pressure monitoring device is not required on any EAF equipped with a DEC system if observations of shop opacity are performed by a certified visible emission observer as follows: Shop opacity observations shall be conducted at least once per day when the furnace is operating in the meltdown and refining period. Shop opacity shall be determined as the arithmetic average of 24 consecutive 15-second opacity observations of emissions from the shop taken in accordance with Method 9. Shop opacity shall be recorded for any point(s) where visible emissions are observed. Where it is possible to determine that a number of visible emission sites relate to only one incident of visible emissions, only one observation of shop opacity will be required. In this case, the shop opacity observations must be made for the site of highest opacity that directly relates to the cause (or location) of visible emissions observed during a single incident.

(e) A bag leak detection system must be installed and continuously operated on all single-stack fabric filters if the owner or operator elects not to install and operate a continuous opacity monitoring system as provided for under [paragraph \(c\)](#) of this section. In addition, the owner or operator shall meet the visible emissions observation requirements in [paragraph \(c\)](#) of this section. The bag leak detection system must meet the specifications and requirements of [paragraphs \(e\)\(1\)](#) through [\(8\)](#) of this section.

(1) The bag leak detection system must be certified by the manufacturer to be capable of detecting particulate matter emissions at concentrations of 1 milligram per actual cubic meter (0.00044 grains per actual cubic foot) or less.

(2) The bag leak detection system sensor must provide output of relative particulate matter loadings and the owner or operator shall continuously record the output from the bag leak detection system using electronic or other means (*e.g.*, using a strip chart recorder or a data logger.)

(3) The bag leak detection system must be equipped with an alarm system that will sound when an increase in relative particulate loading is detected over the alarm set point established according to [paragraph \(e\)\(4\)](#) of this section, and the alarm must be located such that it can be heard by the appropriate plant personnel.

(4) For each bag leak detection system required by [paragraph \(e\)](#) of this section, the owner or operator shall develop and submit to the Administrator or delegated authority, for approval, a site-specific monitoring plan that addresses the items identified in paragraphs (i) through (v) of this [paragraph \(e\)\(4\)](#). For each bag leak detection system that operates based on the triboelectric effect, the monitoring plan shall be consistent with the recommendations contained in the U.S. Environmental Protection Agency guidance document “Fabric Filter Bag Leak Detection Guidance” (EPA-454/R-98-015). The owner or operator shall operate and maintain the bag leak detection system according to the site-specific monitoring plan at all times. The plan shall describe the following:

(i) Installation of the bag leak detection system;

(ii) Initial and periodic adjustment of the bag leak detection system including how the alarm set-point will be established;

(iii) Operation of the bag leak detection system including quality assurance procedures;

(iv) How the bag leak detection system will be maintained including a routine maintenance schedule and spare parts inventory list; and

(v) How the bag leak detection system output shall be recorded and stored.

(5) The initial adjustment of the system shall, at a minimum, consist of establishing the baseline output by adjusting the sensitivity (range) and the averaging period of the device, and establishing the alarm set points and the alarm delay time (if applicable).

(6) Following initial adjustment, the owner or operator shall not adjust the averaging period, alarm set point, or alarm delay time without approval from the Administrator or delegated authority except as provided for in [paragraphs \(e\)\(6\)\(i\)](#) and [\(ii\)](#) of this section.

(i) Once per quarter, the owner or operator may adjust the sensitivity of the bag leak detection system to account for seasonal effects including temperature and humidity according to the procedures identified in the site-specific monitoring plan required under [paragraphs \(e\)\(4\)](#) of this section.

(ii) If opacities greater than zero percent are observed over four consecutive 15-second observations during the daily opacity observations required under [paragraph \(c\)](#) of this section and the alarm on the bag leak detection system does not sound, the owner or operator shall lower the alarm set point on the bag leak detection system to a point where the alarm would have sounded during the period when the opacity observations were made.

(7) For negative pressure, induced air baghouses, and positive pressure baghouses that are discharged to the atmosphere through a stack, the bag leak detection sensor must be installed downstream of the baghouse and upstream of any wet scrubber.

(8) Where multiple detectors are required, the system's instrumentation and alarm may be shared among detectors.

(f) For each bag leak detection system installed according to [paragraph \(e\)](#) of this section, the owner or operator shall initiate procedures to determine the cause of all alarms within 1 hour of an alarm. Except as provided for under [paragraph \(g\)](#) of this section, the cause of the alarm must be alleviated within 3 hours of the time the alarm occurred by taking whatever corrective action(s) are necessary. Corrective actions may include, but are not limited to, the following:

(1) Inspecting the baghouse for air leaks, torn or broken bags or filter media, or any other condition that may cause an increase in particulate emissions;

(2) Sealing off defective bags or filter media;

(3) Replacing defective bags or filter media or otherwise repairing the control device;

(4) Sealing off a defective baghouse compartment;

(5) Cleaning the bag leak detection system probe or otherwise repairing the bag leak detection system; and

(6) Shutting down the process producing the particulate emissions.

(g) In approving the site-specific monitoring plan required in [paragraph \(e\)\(4\)](#) of this section, the Administrator or delegated authority may allow owners or operators more than 3 hours to alleviate specific conditions that cause an alarm if the owner or operator identifies the condition that could lead to an alarm in the monitoring plan, adequately explains why it is not feasible to alleviate the condition within 3 hours of the time the alarm occurred, and demonstrates that the requested additional time will ensure alleviation of the condition as expeditiously as practicable.

[[49 FR 43845](#), Oct. 31, 1984, as amended at [54 FR 6672](#), Feb. 14, 1989; [64 FR 10111](#), Mar. 2, 1999; [70 FR 8532](#), Feb. 22, 2005]

§ 60.274a Monitoring of operations.

(a) The owner or operator subject to the provisions of this subpart shall maintain records of the following information:

(1) All data obtained under [paragraph \(b\)](#) of this section; and

(2) All monthly operational status inspections performed under [paragraph \(c\)](#) of this section.

(b) Except as provided under [paragraph \(e\)](#) of this section, the owner or operator subject to the provisions of this subpart shall check and record on a once-per-shift basis the furnace static pressure (if DEC system is in use, and a furnace static pressure gauge is installed according to [paragraph \(f\)](#) of this section) and either: check and record the control system fan motor amperes and damper position on a once-per-shift basis; install, calibrate, and maintain a monitoring device that continuously records the volumetric flow rate through each separately ducted hood; or install, calibrate, and maintain a monitoring device that continuously records the volumetric flow rate at the control device inlet and check and record damper positions on a once-per-shift basis. The monitoring device(s) may be installed in any appropriate location in the exhaust duct such that reproducible flow rate monitoring will result. The flow rate monitoring device(s) shall have an accuracy of ± 10 percent over its normal operating range and shall be calibrated according to the manufacturer's instructions. The Administrator may require the owner or operator to demonstrate the accuracy of the monitoring device(s) relative to Methods 1 and 2 of [appendix A of this part](#).

(c) When the owner or operator of an affected facility is required to demonstrate compliance with the standards under [§ 60.272a\(a\)\(3\)](#) and at any other time that the Administrator may

require (under section 114 of the CAA, as amended) either: the control system fan motor amperes and all damper positions, the volumetric flow rate through each separately ducted hood, or the volumetric flow rate at the control device inlet and all damper positions shall be determined during all periods in which a hood is operated for the purpose of capturing emissions from the affected facility subject to [paragraph \(b\)](#) of this section. The owner or operator may petition the Administrator for reestablishment of these parameters whenever the owner or operator can demonstrate to the Administrator's satisfaction that the affected facility operating conditions upon which the parameters were previously established are no longer applicable. The values of these parameters as determined during the most recent demonstration of compliance shall be maintained at the appropriate level for each applicable period. Operation at other than baseline values may be subject to the requirements of [§ 60.276a\(c\)](#).

(d) Except as provided under [paragraph \(e\)](#) of this section, the owner or operator shall perform monthly operational status inspections of the equipment that is important to the performance of the total capture system (*i.e.*, pressure sensors, dampers, and damper switches). This inspection shall include observations of the physical appearance of the equipment (e.g., presence of holes in ductwork or hoods, flow constrictions caused by dents or accumulated dust in ductwork, and fan erosion). Any deficiencies shall be noted and proper maintenance performed.

(e) The owner or operator may petition the Administrator to approve any alternative to either the monitoring requirements specified in [paragraph \(b\)](#) of this section or the monthly operational status inspections specified in [paragraph \(d\)](#) of this section if the alternative will provide a continuous record of operation of each emission capture system.

(f) Except as provided for under [§ 60.273a\(d\)](#), if emissions during any phase of the heat time are controlled by the use of a DEC system, the owner or operator shall install, calibrate, and maintain a monitoring device that allows the pressure in the free space inside the EAF to be monitored. The pressure shall be recorded as 15-minute integrated averages. The monitoring device may be installed in any appropriate location in the EAF or DEC duct prior to the introduction of ambient air such that reproducible results will be obtained. The pressure monitoring device shall have an accuracy of ± 5 mm of water gauge over its normal operating range and shall be calibrated according to the manufacturer's instructions.

(g) Except as provided for under [§ 60.273a\(d\)](#), when the owner or operator of an EAF controlled by a DEC is required to demonstrate compliance with the standard under [§ 60.272a\(a\)\(3\)](#), and at any other time the Administrator may require (under section 114 of the Clean Air Act, as amended), the pressure in the free space inside the furnace shall be determined during the meltdown and refining period(s) using the monitoring device required under [paragraph \(f\)](#) of this section. The owner or operator may petition the Administrator for reestablishment of the pressure whenever the owner or operator can demonstrate to the Administrator's satisfaction that the EAF operating conditions upon which the pressures were previously established are no longer applicable. The pressure determined during the most recent demonstration of compliance shall be maintained at all times when the EAF is operating in a meltdown and refining period. Operation at higher pressures may be considered by the Administrator to be unacceptable operation and maintenance of the affected facility.

(h) During any performance test required under [§ 60.8](#), and for any report thereof required by [§ 60.276a\(f\) of this subpart](#), or to determine compliance with [§ 60.272a\(a\)\(3\) of this subpart](#), the owner or operator shall monitor the following information for all heats covered by the test:

- (1) Charge weights and materials, and tap weights and materials;
- (2) Heat times, including start and stop times, and a log of process operation, including periods of no operation during testing and the pressure inside an EAF when direct-shell evacuation control systems are used;
- (3) Control device operation log; and
- (4) Continuous opacity monitor or Method 9 data.

[[49 FR 43845](#), Oct. 31, 1984, as amended at [64 FR 10111](#), Mar. 2, 1999; [65 FR 61758](#), Oct. 17, 2000; [70 FR 8533](#), Feb. 22, 2005]

§ 60.275a Test methods and procedures.

(a) During performance tests required in [§ 60.8](#), the owner or operator shall not add gaseous diluents to the effluent gas stream after the fabric in any pressurized fabric filter collector, unless the amount of dilution is separately determined and considered in the determination of emissions.

(b) When emissions from any EAF(s) or AOD vessel(s) are combined with emissions from facilities not subject to the provisions of this subpart but controlled by a common capture system and control device, the owner or operator shall use either or both of the following procedures during a performance test (see also [§ 60.276a\(e\)](#)):

- (1) Determine compliance using the combined emissions.
- (2) Use a method that is acceptable to the Administrator and that compensates for the emissions from the facilities not subject to the provisions of this subpart.

(c) When emission from any EAF(s) or AOD vessel(s) are combined with emissions from facilities not subject to the provisions of this subpart, the owner or operator shall demonstrate compliance with [§ 60.272\(a\)\(3\)](#) based on emissions from only the affected facility(ies).

(d) In conducting the performance tests required in [§ 60.8](#), the owner or operator shall use as reference methods and procedures the test methods in [appendix A of this part](#) or other methods and procedures as specified in this section, except as provided in [§ 60.8\(b\)](#).

(e) The owner or operator shall determine compliance with the particulate matter standards in [§ 60.272a](#) as follows:

(1) Method 5 shall be used for negative-pressure fabric filters and other types of control devices and Method 5D shall be used for positive-pressure fabric filters to determine the particulate matter concentration and volumetric flow rate of the effluent gas. The sampling time and sample volume for each run shall be at least 4 hours and 4.50 dscm (160 dscf) and, when a single EAF or AOD vessel is sampled, the sampling time shall include an integral number of heats.

(2) When more than one control device serves the EAF(s) being tested, the concentration of particulate matter shall be determined using the following equation:

$$c_{st} = \left[\sum_{i=1}^n (c_{si} Q_{sdi}) \right] \sum_{i=1}^n Q_{sdi}$$

where:

c_{st} = average concentration of particulate matter, mg/dscm (gr/dscf).

c_{si} = concentration of particulate matter from control device “i”, mg/dscm (gr/dscf).

n = total number of control devices tested.

Q_{sdi} = volumetric flow rate of stack gas from control device “i”, dscm/hr (dscf/hr).

(3) Method 9 and the procedures of [§ 60.11](#) shall be used to determine opacity.

(4) To demonstrate compliance with [§ 60.272a\(a\) \(1\)](#), [\(2\)](#), and [\(3\)](#), the Method 9 test runs shall be conducted concurrently with the particulate matter test runs, unless inclement weather interferes.

(f) To comply with [§ 60.274a \(c\)](#), [\(f\)](#), [\(g\)](#), and [\(h\)](#), the owner or operator shall obtain the information required in these paragraphs during the particulate matter runs.

(g) Any control device subject to the provisions of the subpart shall be designed and constructed to allow measurement of emissions using applicable test methods and procedures.

(h) Where emissions from any EAF(s) or AOD vessel(s) are combined with emissions from facilities not subject to the provisions of this subpart but controlled by a common capture system and control device, the owner or operator may use any of the following procedures during a performance test:

(1) Base compliance on control of the combined emissions;

(2) Utilize a method acceptable to the Administrator that compensates for the emissions from the facilities not subject to the provisions of this subpart, or;

(3) Any combination of the criteria of [paragraphs \(h\)\(1\) and \(h\)\(2\)](#) of this section.

(i) Where emissions from any EAF(s) or AOD vessel(s) are combined with emissions from facilities not subject to the provisions of this subpart, determinations of compliance with [§ 60.272a\(a\)\(3\)](#) will only be based upon emissions originating from the affected facility(ies).

(j) Unless the presence of inclement weather makes concurrent testing infeasible, the owner or operator shall conduct concurrently the performance tests required under [§ 60.8](#) to demonstrate compliance with [§ 60.272a\(a\) \(1\), \(2\), and \(3\) of this subpart](#).

[[49 FR 43845](#), Oct. 31, 1984, as amended at [54 FR 6673](#), Feb. 14, 1989; [54 FR 21344](#), May 17, 1989; [65 FR 61758](#), Oct. 17, 2000]

§ 60.276a Recordkeeping and reporting requirements.

(a) Records of the measurements required in [§ 60.274a](#) must be retained for at least 2 years following the date of the measurement.

(b) Each owner or operator shall submit a written report of exceedances of the control device opacity to the Administrator semi-annually. For the purposes of these reports, exceedances are defined as all 6-minute periods during which the average opacity is 3 percent or greater.

(c) Operation at a furnace static pressure that exceeds the value established under [§ 60.274a\(g\)](#) and either operation of control system fan motor amperes at values exceeding ± 15 percent of the value established under [§ 60.274a\(c\)](#) or operation at flow rates lower than those established under [§ 60.274a\(c\)](#) may be considered by the Administrator to be unacceptable operation and maintenance of the affected facility. Operation at such values shall be reported to the Administrator semiannually.

(d) The requirements of this section remain in force until and unless EPA, in delegating enforcement authority to a State under section 111(c) of the Act, approves reporting requirements or an alternative means of compliance surveillance adopted by such State. In that event, affected sources within the State will be relieved of the obligation to comply with this section, provided that they comply with the requirements established by the State.

(e) When the owner or operator of an EAF or AOD is required to demonstrate compliance with the standard under [§ 60.275 \(b\)\(2\)](#) or a combination of (b)(1) and (b)(2) the owner or operator shall obtain approval from the Administrator of the procedure(s) that will be used to determine compliance. Notification of the procedure(s) to be used must be postmarked at least 30 days prior to the performance test.

(f) For the purpose of this subpart, the owner or operator shall conduct the demonstration of compliance with [§ 60.272a\(a\) of this subpart](#) and furnish the Administrator a written report of the results of the test. This report shall include the following information:

(1) Facility name and address;

- (2) Plant representative;
- (3) Make and model of process, control device, and continuous monitoring equipment;
- (4) Flow diagram of process and emission capture equipment including other equipment or process(es) ducted to the same control device;
- (5) Rated (design) capacity of process equipment;
- (6) Those data required under [§ 60.274a\(h\) of this subpart](#);
 - (i) List of charge and tap weights and materials;
 - (ii) Heat times and process log;
 - (iii) Control device operation log; and
 - (iv) Continuous opacity monitor or Method 9 data.
- (7) Test dates and test times;
- (8) Test company;
- (9) Test company representative;
- (10) Test observers from outside agency;
- (11) Description of test methodology used, including any deviation from standard reference methods;
- (12) Schematic of sampling location;
- (13) Number of sampling points;
- (14) Description of sampling equipment;
- (15) Listing of sampling equipment calibrations and procedures;
- (16) Field and laboratory data sheets;
- (17) Description of sample recovery procedures;
- (18) Sampling equipment leak check results;
- (19) Description of quality assurance procedures;

(20) Description of analytical procedures;

(21) Notation of sample blank corrections; and

(22) Sample emission calculations.

(g) The owner or operator shall maintain records of all shop opacity observations made in accordance with [§ 60.273a\(d\)](#). All shop opacity observations in excess of the emission limit specified in [§ 60.272a\(a\)\(3\) of this subpart](#) shall indicate a period of excess emission, and shall be reported to the administrator semi-annually, according to [§ 60.7\(c\)](#).

(h) The owner or operator shall maintain the following records for each bag leak detection system required under [§ 60.273a\(e\)](#):

(1) Records of the bag leak detection system output;

(2) Records of bag leak detection system adjustments, including the date and time of the adjustment, the initial bag leak detection system settings, and the final bag leak detection system settings; and

(3) An identification of the date and time of all bag leak detection system alarms, the time that procedures to determine the cause of the alarm were initiated, if procedures were initiated within 1 hour of the alarm, the cause of the alarm, an explanation of the actions taken, the date and time the cause of the alarm was alleviated, and if the alarm was alleviated within 3 hours of the alarm.

[[49 FR 43845](#), Oct. 31, 1984, as amended at [54 FR 6673](#), Feb. 14, 1989; [64 FR 10111](#), Mar. 2, 1999; [65 FR 61758](#), Oct. 17, 2000; [70 FR 8533](#), Feb. 22, 2005]

Appendix C

40 C.F.R. Part 60 Subpart TT

Standards of Performance for Metal Coil Surface Coating

§ 60.460 Applicability and designation of affected facility.

(a) The provisions of this subpart apply to the following affected facilities in a metal coil surface coating operation: each prime coat operation, each finish coat operation, and each prime and finish coat operation combined when the finish coat is applied wet on wet over the prime coat and both coatings are cured simultaneously.

(b) This subpart applies to any facility identified in [paragraph \(a\)](#) of this section that commences construction, modification, or reconstruction after January 5, 1981.

§ 60.461 Definitions.

(a) All terms used in this subpart not defined below are given the same meaning as in the Act or in [subpart A of this part](#).

Coating means any organic material that is applied to the surface of metal coil.

Coating application station means that portion of the metal coil surface coating operation where the coating is applied to the surface of the metal coil. Included as part of the coating application station is the flashoff area between the coating application station and the curing oven.

Curing oven means the device that uses heat or radiation to dry or cure the coating applied to the metal coil.

Finish coat operation means the coating application station, curing oven, and quench station used to apply and dry or cure the final coating(s) on the surface of the metal coil. Where only a single coating is applied to the metal coil, that coating is considered a finish coat.

Metal coil surface coating operation means the application system used to apply an organic coating to the surface of any continuous metal strip with thickness of 0.15 millimeter (mm) (0.006 in.) or more that is packaged in a roll or coil.

Prime coat operation means the coating application station, curing oven, and quench station used to apply and dry or cure the initial coating(s) on the surface of the metal coil.

Quench station means that portion of the metal coil surface coating operation where the coated metal coil is cooled, usually by a water spray, after baking or curing.

VOC content means the quantity, in kilograms per liter of coating solids, of volatile organic compounds (VOC's) in a coating.

(b) All symbols used in this subpart not defined below are given the same meaning as in the Act and in [subpart A of this part](#).

C_a = the VOC concentration in each gas stream leaving the control device and entering the atmosphere (parts per million by volume, as carbon).

C_b = the VOC concentration in each gas stream entering the control device (parts per million by volume, as carbon).

C_f = the VOC concentration in each gas stream emitted directly to the atmosphere (parts per million by volume, as carbon).

D_c = density of each coating, as received (kilograms per liter).

D_d = density of each VOC-solvent added to coatings (kilograms per liter).

D_r = density of VOC-solvent recovered by an emission control device (kilograms per liter).

E = VOC destruction efficiency of the control device (fraction).

F = the proportion of total VOC's emitted by an affected facility that enters the control device (fraction).

G = volume-weighted average mass of VOC's in coatings consumed in a calendar month per unit volume of coating solids applied (kilograms per liter).

L_c = the volume of each coating consumed, as received (liters).

L_d = the volume of each VOC-solvent added to coatings (liters).

L_r = the volume of VOC-solvent recovered by an emission control device (liters).

L_s = the volume of coating solids consumed (liters).

M_d = the mass of VOC-solvent added to coatings (kilograms).

M_o = the mass of VOC's in coatings consumed, as received (kilograms).

M_r = the mass of VOC's recovered by an emission control device (kilograms).

N = the volume-weighted average mass of VOC emissions to the atmosphere per unit volume of coating solids applied (kilograms per liter).

Q_a = the volumetric flow rate of each gas stream leaving the control device and entering the atmosphere (dry standard cubic meters per hour).

Q_b = the volumetric flow rate of each gas stream entering the control device (dry standard cubic meters per hour).

Q_f = the volumetric flow rate of each gas stream emitted directly to the atmosphere (dry standard cubic meters per hour).

R = the overall VOC emission reduction achieved for an affected facility (fraction).

S = the calculated monthly allowable emission limit (kilograms of VOC per liter of coating solids applied).

V_s = the proportion of solids in each coating, as received (fraction by volume).

W_o = the proportion of VOC's in each coating, as received (fraction by weight).

§ 60.462 Standards for volatile organic compounds.

(a) On and after the date on which [§ 60.8](#) requires a performance test to be completed, each owner or operator subject to this subpart shall not cause to be discharged into the atmosphere more than:

(1) 0.28 kilogram VOC per liter (kg VOC/l) of coating solids applied for each calendar month for each affected facility that does not use an emission control device(s); or

(2) 0.14 kg VOC/l of coating solids applied for each calendar month for each affected facility that continuously uses an emission control device(s) operated at the most recently demonstrated overall efficiency; or

(3) 10 percent of the VOC's applied for each calendar month (90 percent emission reduction) for each affected facility that continuously uses an emission control device(s) operated at the most recently demonstrated overall efficiency; or

(4) A value between 0.14 (or a 90-percent emission reduction) and 0.28 kg VOC/l of coating solids applied for each calendar month for each affected facility that intermittently uses an emission control device operated at the most recently demonstrated overall efficiency.

§ 60.463 Performance test and compliance provisions.

(a) [Section 60.8\(d\)](#) and [\(f\)](#) do not apply to the performance test.

(b) The owner or operator of an affected facility shall conduct an initial performance test as required under [§ 60.8\(a\)](#) and thereafter a performance test for each calendar month for each affected facility according to the procedures in this section.

(c) The owner or operator shall use the following procedures for determining monthly volume-weighted average emissions of VOC's in kg/l of coating solids applied.

(1) An owner or operator shall use the following procedures for each affected facility that does not use a capture system and control device to comply with the emission limit specified under § 60.462(a)(1). The owner or operator shall determine the composition of the coatings by formulation data supplied by the manufacturer of the coating or by an analysis of each coating, as received, using Method 24. The Administrator may require the owner or operator who uses formulation data supplied by the manufacturer of the coatings to determine the VOC content of coatings using Method 24 or an equivalent or alternative method. The owner or operator shall determine the volume of coating and the mass of VOC-solvent added to coatings from company records on a monthly basis. If a common coating distribution system serves more than one affected facility or serves both affected and existing facilities, the owner or operator shall estimate the volume of coating used at each affected facility by using the average dry weight of coating and the surface area coated by each affected and existing facility or by other procedures acceptable to the Administrator.

(i) Calculate the volume-weighted average of the total mass of VOC's consumed per unit volume of coating solids applied during each calendar month for each affected facility, except as provided under paragraph (c)(1)(iv) of this section. The weighted average of the total mass of VOC's used per unit volume of coating solids applied each calendar month is determined by the following procedures.

(A) Calculate the mass of VOC's used ($M_o + M_d$) during each calendar month for each affected facility by the following equation:

$$M_o + M_d = \sum_{i=1}^n L_{ci} D_{ci} W_{oi} + \sum_{j=1}^m L_{dj} D_{dj} \quad \text{Equation 1}$$

($\sum L_{dj} D_{dj}$ will be 0 if no VOC solvent is added to the coatings, as received)

where

n is the number of different coatings used during the calendar month, and

m is the number of different VOC solvents added to coatings used during the calendar month.

(B) Calculate the total volume of coating solids used (L_s) in each calendar month for each affected facility by the following equation:

$$L_s = \sum_{i=1}^n V_{si} L_{ci} \quad \text{Equation 2}$$

Where:

n is the number of different coatings used during the calendar month.

(C) Calculate the volume-weighted average mass of VOC's used per unit volume of coating solids applied (G) during the calendar month for each affected facility by the following equation:

$$G = \frac{M_o + M_d}{L_s} \quad \text{Equation 3}$$

(ii) Calculate the volume-weighted average of VOC emissions to the atmosphere (N) during the calendar month for each affected facility by the following equation:

$$N = G \quad \text{Equation 4}$$

(iii) Where the volume-weighted average mass of VOC's discharged to the atmosphere per unit volume of coating solids applied (N) is equal to or less than 0.28 kg/l, the affected facility is in compliance.

(iv) If each individual coating used by an affected facility has a VOC content, as received, that is equal to or less than 0.28 kg/l of coating solids, the affected facility is in compliance provided no VOC's are added to the coatings during distribution or application.

(2) An owner or operator shall use the following procedures for each affected facility that continuously uses a capture system and a control device that destroys VOC's (e.g., incinerator) to comply with the emission limit specified under [§ 60.462\(a\) \(2\)](#) or [\(3\)](#).

(i) Determine the overall reduction efficiency (R) for the capture system and control device.

For the initial performance test, the overall reduction efficiency (R) shall be determined as prescribed in [paragraphs \(c\)\(2\)\(i\) \(A\)](#), [\(B\)](#), and [\(C\)](#) of this section. In subsequent months, the owner or operator may use the most recently determined overall reduction efficiency (R) for the performance test, providing control device and capture system operating conditions have not changed. The procedure in [paragraphs \(c\)\(2\)\(i\) \(A\)](#), [\(B\)](#), and [\(C\)](#) of this section, shall be repeated when directed by the Administrator or when the owner or operator elects to operate the control device or capture system at conditions different from the initial performance test.

(A) Determine the fraction (F) of total VOC's emitted by an affected facility that enters the control device using the following equation:

$$F = \frac{\sum_{i=1}^l C_{bi} Q_{bi}}{\sum_{i=1}^l C_{bi} Q_{bi} + \sum_{i=1}^p C_{ni} Q_{ni}}$$

Equation 5

Where:

l is the number of gas streams entering the control device, and

p is the number of gas streams emitted directly to the atmosphere.

(B) Determine the destruction efficiency of the control device (E) using values of the volumetric flow rate of each of the gas streams and the VOC content (as carbon) of each of the gas streams in and out of the device by the following equation:

$$E = \frac{\sum_{i=1}^n Q_{bi} C_{bi} - \sum_{j=1}^m Q_{aj} C_{aj}}{\sum_{i=1}^n Q_{bi} C_{bi}}$$

Equation 6

Where:

n is the number of gas streams entering the control device, and

m is the number of gas streams leaving the control device and entering the atmosphere.

The owner or operator of the affected facility shall construct the VOC emission reduction system so that all volumetric flow rates and total VOC emissions can be accurately determined by the applicable test methods and procedures specified in [§ 60.466](#). The owner or operator of the affected facility shall construct a temporary enclosure around the coating applicator and flashoff area during the performance test for the purpose of evaluating the capture efficiency of the system. The enclosure must be maintained at a negative pressure to ensure that all VOC emissions are measurable. If a permanent enclosure exists in the affected facility prior to the performance test and the Administrator is satisfied that the enclosure is adequately containing VOC emissions, no additional enclosure is required for the performance test.

(C) Determine overall reduction efficiency (R) using the following equation:

$$R = EF \quad \text{Equation 7}$$

If the overall reduction efficiency (R) is equal to or greater than 0.90, the affected facility is in compliance and no further computations are necessary. If the overall reduction efficiency (R) is less than 0.90, the average total VOC emissions to the atmosphere per unit volume of coating solids applied (N) shall be computed as follows.

(ii) Calculate the volume-weighted average of the total mass of VOC's per unit volume of coating solids applied (G) during each calendar month for each affected facility using equations in [paragraphs \(c\)\(1\)\(i\) \(A\), \(B\), and \(C\)](#) of this section.

(iii) Calculate the volume-weighted average of VOC emissions to the atmosphere (N) during each calendar month by the following equation:

$$N = G(1 - R) \quad \text{Equation 8}$$

(iv) If the volume-weighted average mass of VOC's emitted to the atmosphere for each calendar month (N) is less than or equal to 0.14 kg/l of coating solids applied, the affected facility is in compliance. Each monthly calculation is a performance test.

(3) An owner or operator shall use the following procedure for each affected facility that uses a control device that recovers the VOC's (e.g., carbon adsorber) to comply with the applicable emission limit specified under [§ 60.462\(a\) \(2\) or \(3\)](#).

(i) Calculate the total mass of VOC's consumed ($M_o + M_d$) during each calendar month for each affected facility using equation (1).

(ii) Calculate the total mass of VOC's recovered (M_r) during each calendar month using the following equation:

$$M_r = L_r D_r \quad \text{Equation 9}$$

(iii) Calculate the overall reduction efficiency of the control device (R) for each calendar month for each affected facility using the following equation:

$$R = \frac{M_r}{M_o + M_d} \quad \text{Equation 10}$$

If the overall reduction efficiency (R) is equal to or greater than 0.90, the affected facility is in compliance and no further computations are necessary. If the overall reduction efficiency (R) is less than 0.90, the average total VOC emissions to the atmosphere per unit volume of coating solids applied (N) must be computed as follows.

(iv) Calculate the total volume of coating solids consumed (L_s) and the volume-weighted average of the total mass of VOC's per unit volume of coating solids applied (G) during each calendar month for each affected facility using equations in [paragraphs \(c\)\(1\)\(i\) \(B\)](#) and [\(C\)](#) of this section.

(v) Calculate the volume-weighted average mass of VOC's emitted to the atmosphere (N) for each calendar month for each affected facility using equation (8).

(vi) If the weighted average mass of VOC's emitted to the atmosphere for each calendar month (N) is less than or equal to 0.14 kg/l of coating solids applied, the affected facility is in compliance. Each monthly calculation is a performance test.

(4) An owner or operator shall use the following procedures for each affected facility that intermittently uses a capture system and a control device to comply with the emission limit specified in [§ 60.462\(a\)\(4\)](#).

(i) Calculate the total volume of coating solids applied without the control device in operation (L_{sn}) during each calendar month for each affected facility using the following equation:

$$L_{sn} = \sum_{i=1}^n V_{si} L_{ci} \quad \text{Equation 11}$$

Where:

n is the number of coatings used during the calendar month without the control device in operation.

(ii) Calculate the total volume of coating solids applied with the control device in operation (L_{sc}) during each calendar month for each affected facility using the following equation:

$$L_{sc} = \sum_{i=1}^n V_{si} L_{ci} \quad \text{Equation 12}$$

Where:

n is the number of coatings used during the calendar month with the control device in operation.

(iii) Calculate the mass of VOC's used without the control device in operation ($M_{on} + M_{dn}$) during each calendar month for each affected facility using the following equation:

$$M_{on} + M_{dn} + \sum_{i=1}^n L_{ci} D_{ci} W_{oi} + \sum_{j=1}^m L_{dj} D_{dj} \quad \text{Equation 13}$$

Where:

n is the number of different coatings used without the control device in operation during the calendar month, and

m is the number of different VOC-solvents added to coatings used without the control device in operation during the calendar month.

(iv) Calculate the volume-weighted average of the total mass of VOC's consumed per unit volume of coating solids applied without the control device in operation (G_n) during each calendar month for each affected facility using the following equation:

$$G_n = \frac{M_{on} + M_{dn}}{L_{sn}} \quad \text{Equation 14}$$

(v) Calculate the mass of VOC's used with the control device in operation ($M_{oc} + M_{dc}$) during each calendar month for each affected facility using the following equation:

$$M_{oc} + M_{dc} = \sum_{i=1}^n L_{ci} D_{ci} W_{oi} + \sum_{j=1}^m L_{dj} D_{dj} \quad \text{Equation 15}$$

Where:

n is the number of different coatings used with the control device in operation during the calendar month, and

m is the number of different VOC-solvents added to coatings used with the control device in operation during the calendar month.

(vi) Calculate the volume-weighted average of the total mass of VOC's used per unit volume of coating solids applied with the control device in operation (G_c) during each calendar month for each affected facility using the following equation:

$$G = \frac{M_{oc} + M_{dc}}{L_{sn}} \quad \text{Equation 16}$$

(vii) Determine the overall reduction efficiency (R) for the capture system and control device using the procedures in paragraphs (c)(2)(i) (A), (B), and (C) or [paragraphs \(c\)\(3\) \(i\), \(ii\), and \(iii\)](#) of this section, whichever is applicable.

(viii) Calculate the volume-weighted average of VOC emissions to the atmosphere (N) during each calendar month for each affected facility using the following equation:

$$N = \frac{G_n L_{sn} + G_c L_{sc} (1 - R)}{L_{sn} + L_{sc}} \quad \text{Equation 17}$$

Equation 17

(ix) Calculate the emission limit(s) for each calendar month for each affected facility using the following equation:

$$S = \frac{0.28 L_{sn} + 0.1 G_c L_{sc}}{L_{ns} + L_{sc}}$$

or

$$\frac{0.28 L_{sn} + 0.14 L_{sc}}{L_{sn} + L_{sc}} \quad \text{Equation 18}$$

whichever is greater.

(x) If the volume-weighted average mass of VOC's emitted to the atmosphere for each calendar month (N) is less than or equal to the calculated emission limit (S) for the calendar month, the affected facility is in compliance. Each monthly calculation is a performance test.

[[47 FR 49612](#), Nov. 1, 1982; [48 FR 1056](#), Jan. 10, 1983, as amended at [65 FR 61761](#), Oct. 17, 2000]

§ 60.464 Monitoring of emissions and operations.

(a) Where compliance with the numerical limit specified in [§ 60.462\(a\) \(1\) or \(2\)](#) is achieved through the use of low VOC-content coatings without the use of emission control devices or through the use of higher VOC-content coatings in conjunction with emission control devices, the owner or operator shall compute and record the average VOC content of coatings applied during each calendar month for each affected facility, according to the equations provided in [§ 60.463](#).

(b) Where compliance with the limit specified in [§ 60.462\(a\)\(4\)](#) is achieved through the intermittent use of emission control devices, the owner or operator shall compute and record for each affected facility the average VOC content of coatings applied during each calendar month according to the equations provided in [§ 60.463](#).

(c) If thermal incineration is used, each owner or operator subject to the provisions of this subpart shall install, calibrate, operate, and maintain a device that continuously records the combustion temperature of any effluent gases incinerated to achieve compliance with [§ 60.462\(a\)\(2\)](#), [\(3\)](#), or [\(4\)](#). This device shall have an accuracy of ± 2.5 °C. or ± 0.75 percent of the temperature being measured expressed in degrees Celsius, whichever is greater. Each owner or operator shall also record all periods (during actual coating operations) in excess of 3 hours during which the average temperature in any thermal incinerator used to control emissions from an affected facility remains more than 28 °C (50 °F) below the temperature at which compliance with [§ 60.462\(a\)\(2\)](#), [\(3\)](#), or [\(4\)](#) was demonstrated during the most recent measurement of incinerator efficiency required by [§ 60.8](#). The records required by [§ 60.7](#) shall identify each such occurrence and its duration. If catalytic incineration is used, the owner or operator shall install, calibrate, operate, and maintain a device to monitor and record continuously the gas temperature both upstream and downstream of the incinerator catalyst bed. This device shall have an accuracy of ± 2.5 °C. or ± 0.75 percent of the temperature being measured expressed in degrees Celsius, whichever is greater. During coating operations, the owner or operator shall record all periods in excess of 3 hours where the average difference between the temperature upstream and downstream of the incinerator catalyst bed remains below 80 percent of the temperature difference at which compliance was demonstrated during the most recent measurement of incinerator efficiency or when the inlet temperature falls more than 28 °C (50 °F) below the temperature at which compliance with [§ 60.462\(a\)\(2\)](#), [\(3\)](#), or [\(4\)](#) was demonstrated during the most recent measurement of incinerator efficiency required by [§ 60.8](#). The records required by [§ 60.7](#) shall identify each such occurrence and its duration.

[[47 FR 49612](#), Nov. 1, 1982; [48 FR 1056](#), Jan. 10, 1983, as amended at [65 FR 61761](#), Oct. 17, 2000]

§ 60.465 Reporting and recordkeeping requirements.

(a) Where compliance with the numerical limit specified in [§ 60.462\(a\) \(1\)](#), [\(2\)](#), or [\(4\)](#) is achieved through the use of low VOC-content coatings without emission control devices or through the use of higher VOC-content coatings in conjunction with emission control devices, each owner or operator subject to the provisions of this subpart shall include in the initial compliance report required by [§ 60.8](#) the weighted average of the VOC content of coatings used during a period of one calendar month for each affected facility. Where compliance with [§ 60.462\(a\)\(4\)](#) is achieved through the intermittent use of a control device, reports shall include separate values of the weighted average VOC content of coatings used with and without the control device in operation.

(b) Where compliance with [§ 60.462\(a\)\(2\)](#), [\(3\)](#), or [\(4\)](#) is achieved through the use of an emission control device that destroys VOC's, each owner or operator subject to the provisions

of this subpart shall include the following data in the initial compliance report required by [§ 60.8](#):

(1) The overall VOC destruction rate used to attain compliance with [§ 60.462\(a\)\(2\)](#), [\(3\)](#), or [\(4\)](#) and the calculated emission limit used to attain compliance with [§ 60.462\(a\)\(4\)](#); and

(2) The combustion temperature of the thermal incinerator or the gas temperature, both upstream and downstream of the incinerator catalyst bed, used to attain compliance with [§ 60.462\(a\)\(2\)](#), [\(3\)](#), or [\(4\)](#).

(c) Following the initial performance test, the owner or operator of an affected facility shall identify, record, and submit a written report to the Administrator every calendar quarter of each instance in which the volume-weighted average of the local mass of VOC's emitted to the atmosphere per volume of applied coating solids (N) is greater than the limit specified under [§ 60.462](#). If no such instances have occurred during a particular quarter, a report stating this shall be submitted to the Administrator semiannually.

(d) The owner or operator of each affected facility shall also submit reports at the frequency specified in [§ 60.7\(c\)](#) when the incinerator temperature drops as defined under [§ 60.464\(c\)](#). If no such periods occur, the owner or operator shall state this in the report.

(e) Each owner or operator subject to the provisions of this subpart shall maintain at the source, for a period of at least 2 years, records of all data and calculations used to determine monthly VOC emissions from each affected facility and to determine the monthly emission limit, where applicable. Where compliance is achieved through the use of thermal incineration, each owner or operator shall maintain, at the source, daily records of the incinerator combustion temperature. If catalytic incineration is used, the owner or operator shall maintain at the source daily records of the gas temperature, both upstream and downstream of the incinerator catalyst bed.

[[47 FR 49612](#), Nov. 1, 1982, as amended at [55 FR 51383](#), Dec. 13, 1990; [56 FR 20497](#), May 3, 1991; [65 FR 61761](#), Oct. 17, 2000]

§ 60.466 Test methods and procedures.

(a) The reference methods in appendix A to this part, except as provided under [§ 60.8\(b\)](#), shall be used to determine compliance with [§ 60.462](#) as follows:

(1) Method 24, or data provided by the formulator of the coating, shall be used for determining the VOC content of each coating as applied to the surface of the metal coil. In the event of a dispute, Method 24 shall be the reference method. When VOC content of waterborne coatings, determined by Method 24, is used to determine compliance of affected facilities, the results of the Method 24 analysis shall be adjusted as described in [Section 12.6](#) of Method 24;

(2) Method 25, both for measuring the VOC concentration in each gas stream entering and leaving the control device on each stack equipped with an emission control device and for measuring the VOC concentration in each gas stream emitted directly to the atmosphere;

(3) Method 1 for sample and velocity traverses;

(4) Method 2 for velocity and volumetric flow rate;

(5) Method 3 for gas analysis; and

(6) Method 4 for stack gas moisture.

(b) For Method 24, the coating sample must be at least a 1-liter sample taken at a point where the sample will be representative of the coating as applied to the surface of the metal coil.

(c) For Method 25, the sampling time for each of three runs is to be at least 60 minutes, and the minimum sampling volume is to be at least 0.003 dscm (0.11 dscf); however, shorter sampling times or smaller volumes, when necessitated by process variables or other factors, may be approved by the Administrator.

(d) The Administrator will approve testing of representative stacks on a case-by-case basis if the owner or operator can demonstrate to the satisfaction of the Administrator that testing of representative stacks yields results comparable to those that would be obtained by testing all stacks.

[[47 FR 49612](#), Nov. 1, 1982, as amended at [51 FR 22938](#), June 24, 1986; [65 FR 61761](#), Oct. 17, 2000]

Appendix D

40 C.F.R. Part 60 Subpart III

Standards of Performance for Stationary Compression Ignition Internal Combustion Engines

Subpart III - Standards of Performance for Stationary Compression Ignition Internal Combustion Engines

Source: [71 FR 39172](#), July 11, 2006, unless otherwise noted.

What This Subpart Covers

§ 60.4200 Am I subject to this subpart?

(a) The provisions of this subpart are applicable to manufacturers, owners, and operators of stationary compression ignition (CI) internal combustion engines (ICE) and other persons as specified in [paragraphs \(a\)\(1\)](#) through [\(4\)](#) of this section. For the purposes of this subpart, the date that construction commences is the date the engine is ordered by the owner or operator.

(1) Manufacturers of stationary CI ICE with a displacement of less than 30 liters per cylinder where the model year is:

(i) 2007 or later, for engines that are not fire pump engines;

(ii) The model year listed in Table 3 to this subpart or later model year, for fire pump engines.

(2) Owners and operators of stationary CI ICE that commence construction after July 11, 2005, where the stationary CI ICE are:

(i) Manufactured after April 1, 2006, and are not fire pump engines, or

(ii) Manufactured as a certified National Fire Protection Association (NFPA) fire pump engine after July 1, 2006.

(3) Owners and operators of any stationary CI ICE that are modified or reconstructed after July 11, 2005 and any person that modifies or reconstructs any stationary CI ICE after July 11, 2005.

(4) The provisions of [§ 60.4208 of this subpart](#) are applicable to all owners and operators of stationary CI ICE that commence construction after July 11, 2005.

(b) The provisions of this subpart are not applicable to stationary CI ICE being tested at a stationary CI ICE test cell/stand.

(c) If you are an owner or operator of an area source subject to this subpart, you are exempt from the obligation to obtain a permit under [40 CFR part 70](#) or [40 CFR part 71](#), provided you are not required to obtain a permit under [40 CFR 70.3\(a\)](#) or [40 CFR 71.3\(a\)](#) for a reason other than your status as an area source under this subpart. Notwithstanding the previous sentence, you must continue to comply with the provisions of this subpart applicable to area sources.

(d) Stationary CI ICE may be eligible for exemption from the requirements of this subpart as described in [40 CFR part 1068, subpart C](#), except that owners and operators, as well as manufacturers, may be eligible to request an exemption for national security.

(e) Owners and operators of facilities with CI ICE that are acting as temporary replacement units and that are located at a stationary source for less than 1 year and that have been properly certified as meeting the standards that would be applicable to such engine under the appropriate nonroad engine provisions, are not required to meet any other provisions under this subpart with regard to such engines.

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37967](#), June 28, 2011; [86 FR 34357](#), June 29, 2021]

Emission Standards for Manufacturers

§ 60.4201 What emission standards must I meet for non-emergency engines if I am a stationary CI internal combustion engine manufacturer?

(a) Stationary CI internal combustion engine manufacturers must certify their 2007 model year and later non-emergency stationary CI ICE with a maximum engine power less than or equal to 2,237 kilowatt (KW) (3,000 horsepower (HP)) and a displacement of less than 10 liters per cylinder to the certification emission standards for new nonroad CI engines in [40 CFR 1039.101](#), [1039.102](#), [1039.104](#), [1039.105](#), [1039.107](#), and [1039.115](#) and [40 CFR part 1039, appendix I](#), as applicable, for all pollutants, for the same model year and maximum engine power.

(b) Stationary CI internal combustion engine manufacturers must certify their 2007 through 2010 model year non-emergency stationary CI ICE with a maximum engine power greater than 2,237 KW (3,000 HP) and a displacement of less than 10 liters per cylinder to the emission standards in table 1 to this subpart, for all pollutants, for the same maximum engine power.

(c) Stationary CI internal combustion engine manufacturers must certify their 2011 model year and later non-emergency stationary CI ICE with a maximum engine power greater than 2,237 KW (3,000 HP) and a displacement of less than 10 liters per cylinder to the certification emission standards for new nonroad CI engines in [40 CFR 1039.101](#), [40 CFR 1039.102](#), [40 CFR 1039.104](#), [40 CFR 1039.105](#), [40 CFR 1039.107](#), and [40 CFR 1039.115](#), as applicable, for all pollutants, for the same maximum engine power.

(d) Stationary CI internal combustion engine manufacturers must certify the following non-emergency stationary CI ICE to the appropriate Tier 2 emission standards for new marine CI engines as described in [40 CFR part 1042, appendix I](#), for all pollutants, for the same displacement and rated power:

(1) Their 2007 model year through 2012 non-emergency stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder;

(2) Their 2013 model year non-emergency stationary CI ICE with a maximum engine power greater than or equal to 3,700 KW (4,958 HP) and a displacement of greater than or equal to 10 liters per cylinder and less than 15 liters per cylinder; and

(3) Their 2013 model year non-emergency stationary CI ICE with a displacement of greater than or equal to 15 liters per cylinder and less than 30 liters per cylinder.

(e) Stationary CI internal combustion engine manufacturers must certify the following non-emergency stationary CI ICE to the certification emission standards and other requirements for new marine CI engines in [40 CFR 1042.101](#), [40 CFR 1042.107](#), [40 CFR 1042.110](#), [40 CFR 1042.115](#), [40 CFR 1042.120](#), and [40 CFR 1042.145](#), as applicable, for all pollutants, for the same displacement and maximum engine power:

(1) Their 2013 model year non-emergency stationary CI ICE with a maximum engine power less than 3,700 KW (4,958 HP) and a displacement of greater than or equal to 10 liters per cylinder and less than 15 liters per cylinder; and

(2) Their 2014 model year and later non-emergency stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder.

(f) Notwithstanding the requirements in [paragraphs \(a\)](#) through [\(c\)](#) of this section, stationary non-emergency CI ICE identified in [paragraphs \(a\)](#) and [\(c\)](#) of this section may be certified to the provisions of [40 CFR part 1042](#) for commercial engines that are applicable for the engine's model year, displacement, power density, and maximum engine power if the engines will be used solely in either or both of the following locations:

(1) Remote areas of Alaska; and

(2) Marine offshore installations.

(g) Notwithstanding the requirements in [paragraphs \(a\)](#) through [\(f\)](#) of this section, stationary CI internal combustion engine manufacturers are not required to certify reconstructed engines; however manufacturers may elect to do so. The reconstructed engine must be certified to the emission standards specified in [paragraphs \(a\)](#) through [\(e\)](#) of this section that are applicable to the model year, maximum engine power, and displacement of the reconstructed stationary CI ICE.

(h) Stationary CI ICE certified to the standards in [40 CFR part 1039](#) and equipped with auxiliary emission control devices (AECs) as specified in [40 CFR 1039.665](#) must meet the Tier 1 certification emission standards for new nonroad CI engines in [40 CFR part 1039, appendix I](#), while the AEC is activated during a qualified emergency situation. A qualified emergency situation is defined in [40 CFR 1039.665](#). When the qualified emergency situation

has ended and the AECD is deactivated, the engine must resume meeting the otherwise applicable emission standard specified in this section.

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37967](#), June 28, 2011; [81 FR 44219](#), July 7, 2016; [86 FR 34357](#), June 29, 2021]

§ 60.4202 What emission standards must I meet for emergency engines if I am a stationary CI internal combustion engine manufacturer?

(a) Stationary CI internal combustion engine manufacturers must certify their 2007 model year and later emergency stationary CI ICE with a maximum engine power less than or equal to 2,237 KW (3,000 HP) and a displacement of less than 10 liters per cylinder that are not fire pump engines to the emission standards specified in [paragraphs \(a\)\(1\)](#) through [\(2\)](#) of this section.

(1) For engines with a maximum engine power less than 37 KW (50 HP):

(i) The Tier 2 emission standards for new nonroad CI engines for the appropriate rated power as described in [40 CFR part 1039, appendix I](#), for all pollutants and the smoke standards as specified in [40 CFR 1039.105](#) for model year 2007 engines; and

(ii) The certification emission standards for new nonroad CI engines in [40 CFR 1039.104](#), [40 CFR 1039.105](#), [40 CFR 1039.107](#), [40 CFR 1039.115](#), and table 2 to this subpart, for 2008 model year and later engines.

(2) For engines with a rated power greater than or equal to 37 KW (50 HP), the Tier 2 or Tier 3 emission standards for new nonroad CI engines for the same rated power as described in [40 CFR part 1039, appendix I](#), for all pollutants and the smoke standards as specified in [40 CFR 1039.105](#) beginning in model year 2007.

(b) Stationary CI internal combustion engine manufacturers must certify their 2007 model year and later emergency stationary CI ICE with a maximum engine power greater than 2,237 KW (3,000 HP) and a displacement of less than 10 liters per cylinder that are not fire pump engines to the emission standards specified in [paragraphs \(b\)\(1\)](#) through [\(2\)](#) of this section.

(1) For 2007 through 2010 model years, the emission standards in table 1 to this subpart, for all pollutants, for the same maximum engine power.

(2) For 2011 model year and later, the Tier 2 emission standards as described in [40 CFR part 1039, appendix I](#), for all pollutants and the smoke standards as specified in [40 CFR 1039.105](#).

(c) [Reserved]

(d) Beginning with the model years in table 3 to this subpart, stationary CI internal combustion engine manufacturers must certify their fire pump stationary CI ICE to the emission standards in table 4 to this subpart, for all pollutants, for the same model year and NFPA nameplate power.

(e) Stationary CI internal combustion engine manufacturers must certify the following emergency stationary CI ICE that are not fire pump engines to the appropriate Tier 2 emission standards for new marine CI engines as described in [40 CFR part 1042, appendix I](#), for all pollutants, for the same displacement and rated power:

(1) Their 2007 model year through 2012 emergency stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder;

(2) Their 2013 model year and later emergency stationary CI ICE with a maximum engine power greater than or equal to 3,700 KW (4,958 HP) and a displacement of greater than or equal to 10 liters per cylinder and less than 15 liters per cylinder;

(3) Their 2013 model year emergency stationary CI ICE with a displacement of greater than or equal to 15 liters per cylinder and less than 30 liters per cylinder; and

(4) Their 2014 model year and later emergency stationary CI ICE with a maximum engine power greater than or equal to 2,000 KW (2,682 HP) and a displacement of greater than or equal to 15 liters per cylinder and less than 30 liters per cylinder.

(f) Stationary CI internal combustion engine manufacturers must certify the following emergency stationary CI ICE to the certification emission standards and other requirements applicable to Tier 3 new marine CI engines in [40 CFR 1042.101](#), [40 CFR 1042.107](#), [40 CFR 1042.115](#), [40 CFR 1042.120](#), and [40 CFR 1042.145](#), for all pollutants, for the same displacement and maximum engine power:

(1) Their 2013 model year and later emergency stationary CI ICE with a maximum engine power less than 3,700 KW (4,958 HP) and a displacement of greater than or equal to 10 liters per cylinder and less than 15 liters per cylinder; and

(2) Their 2014 model year and later emergency stationary CI ICE with a maximum engine power less than 2,000 KW (2,682 HP) and a displacement of greater than or equal to 15 liters per cylinder and less than 30 liters per cylinder.

(g) Notwithstanding the requirements in [paragraphs \(a\)](#) through [\(d\)](#) of this section, stationary emergency CI ICE identified in [paragraphs \(a\)](#) and [\(c\)](#) of this section may be certified to the provisions of [40 CFR part 1042](#) for commercial engines that are applicable for the engine's model year, displacement, power density, and maximum engine power if the engines will be used solely in either or both of the locations identified in [paragraphs \(g\)\(1\)](#) and [\(2\)](#) of this section. Engines that would be subject to the Tier 4 standards in [40 CFR part 1042](#) that are used solely in either or both of the locations identified in [paragraphs \(g\)\(1\)](#) and [\(2\)](#) of this

section may instead continue to be certified to the appropriate Tier 3 standards in [40 CFR part 1042](#).

(1) Remote areas of Alaska; and

(2) Marine offshore installations.

(h) Notwithstanding the requirements in [paragraphs \(a\)](#) through [\(f\)](#) of this section, stationary CI internal combustion engine manufacturers are not required to certify reconstructed engines; however manufacturers may elect to do so. The reconstructed engine must be certified to the emission standards specified in [paragraphs \(a\)](#) through [\(f\)](#) of this section that are applicable to the model year, maximum engine power and displacement of the reconstructed emergency stationary CI ICE.

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37968](#), June 28, 2011; [81 FR 44219](#), July 7, 2016; [86 FR 34358](#), June 29, 2021]

§ 60.4203 How long must my engines meet the emission standards if I am a manufacturer of stationary CI internal combustion engines?

Engines manufactured by stationary CI internal combustion engine manufacturers must meet the emission standards as required in [§§ 60.4201](#) and [60.4202](#) during the certified emissions life of the engines.

[[76 FR 37968](#), June 28, 2011]

Emission Standards for Owners and Operators

§ 60.4204 What emission standards must I meet for non-emergency engines if I am an owner or operator of a stationary CI internal combustion engine?

(a) Owners and operators of pre-2007 model year non-emergency stationary CI ICE with a displacement of less than 10 liters per cylinder must comply with the emission standards in table 1 to this subpart. Owners and operators of pre-2007 model year non-emergency stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder must comply with the Tier 1 emission standards in [40 CFR part 1042, appendix I](#).

(b) Owners and operators of 2007 model year and later non-emergency stationary CI ICE with a displacement of less than 30 liters per cylinder must comply with the emission standards for

new CI engines in [§ 60.4201](#) for their 2007 model year and later stationary CI ICE, as applicable.

(c) Owners and operators of non-emergency stationary CI engines with a displacement of greater than or equal to 30 liters per cylinder must meet the following requirements:

(1) For engines installed prior to January 1, 2012, limit the emissions of NO_x in the stationary CI internal combustion engine exhaust to the following:

(i) 17.0 grams per kilowatt-hour (g/KW-hr) (12.7 grams per horsepower-hr (g/HP-hr)) when maximum engine speed is less than 130 revolutions per minute (rpm);

(ii) $45 \cdot n^{-0.2}$ g/KW-hr ($34 \cdot n^{-0.2}$ g/HP-hr) when maximum engine speed is 130 or more but less than 2,000 rpm, where n is maximum engine speed; and

(iii) 9.8 g/KW-hr (7.3 g/HP-hr) when maximum engine speed is 2,000 rpm or more.

(2) For engines installed on or after January 1, 2012 and before January 1, 2016, limit the emissions of NO_x in the stationary CI internal combustion engine exhaust to the following:

(i) 14.4 g/KW-hr (10.7 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii) $44 \cdot n^{-0.23}$ g/KW-hr ($33 \cdot n^{-0.23}$ g/HP-hr) when maximum engine speed is greater than or equal to 130 but less than 2,000 rpm and where n is maximum engine speed; and

(iii) 7.7 g/KW-hr (5.7 g/HP-hr) when maximum engine speed is greater than or equal to 2,000 rpm.

(3) For engines installed on or after January 1, 2016, limit the emissions of NO_x in the stationary CI internal combustion engine exhaust to the following:

(i) 3.4 g/KW-hr (2.5 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii) $9.0 \cdot n^{-0.20}$ g/KW-hr ($6.7 \cdot n^{-0.20}$ g/HP-hr) where n (maximum engine speed) is 130 or more but less than 2,000 rpm; and

(iii) 2.0 g/KW-hr (1.5 g/HP-hr) where maximum engine speed is greater than or equal to 2,000 rpm.

(4) Reduce particulate matter (PM) emissions by 60 percent or more, or limit the emissions of PM in the stationary CI internal combustion engine exhaust to 0.15 g/KW-hr (0.11 g/HP-hr).

(d) Owners and operators of non-emergency stationary CI ICE with a displacement of less than 30 liters per cylinder who conduct performance tests in-use must meet the not-to-exceed (NTE) standards as indicated in [§ 60.4212](#).

(e) Owners and operators of any modified or reconstructed non-emergency stationary CI ICE subject to this subpart must meet the emission standards applicable to the model year, maximum engine power, and displacement of the modified or reconstructed non-emergency stationary CI ICE that are specified in [paragraphs \(a\)](#) through [\(d\)](#) of this section.

(f) Owners and operators of stationary CI ICE certified to the standards in [40 CFR part 1039](#) and equipped with AECs as specified in [40 CFR 1039.665](#) must meet the Tier 1 certification emission standards for new nonroad CI engines in [40 CFR part 1039, appendix I](#), while the AEC is activated during a qualified emergency situation. A qualified emergency situation is defined in [40 CFR 1039.665](#). When the qualified emergency situation has ended and the AEC is deactivated, the engine must resume meeting the otherwise applicable emission standard specified in this section.

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37968](#), June 28, 2011; [81 FR 44219](#), July 7, 2016; [86 FR 34358](#), June 29, 2021]

§ 60.4205 What emission standards must I meet for emergency engines if I am an owner or operator of a stationary CI internal combustion engine?

(a) Owners and operators of pre-2007 model year emergency stationary CI ICE with a displacement of less than 10 liters per cylinder that are not fire pump engines must comply with the emission standards in Table 1 to this subpart. Owners and operators of pre-2007 model year emergency stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder that are not fire pump engines must comply with the Tier 1 emission standards in [40 CFR part 1042, appendix I](#).

(b) Owners and operators of 2007 model year and later emergency stationary CI ICE with a displacement of less than 30 liters per cylinder that are not fire pump engines must comply with the emission standards for new nonroad CI engines in [§ 60.4202](#), for all pollutants, for the same model year and maximum engine power for their 2007 model year and later emergency stationary CI ICE.

(c) Owners and operators of fire pump engines with a displacement of less than 30 liters per cylinder must comply with the emission standards in table 4 to this subpart, for all pollutants.

(d) Owners and operators of emergency stationary CI engines with a displacement of greater than or equal to 30 liters per cylinder must meet the requirements in this section.

(1) For engines installed prior to January 1, 2012, limit the emissions of NO_x in the stationary CI internal combustion engine exhaust to the following:

(i) 17.0 g/KW-hr (12.7 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii) $45 \cdot n^{-0.2}$ g/KW-hr ($34 \cdot n^{-0.2}$ g/HP-hr) when maximum engine speed is 130 or more but less than 2,000 rpm, where n is maximum engine speed; and

(iii) 9.8 g/kW-hr (7.3 g/HP-hr) when maximum engine speed is 2,000 rpm or more.

(2) For engines installed on or after January 1, 2012, limit the emissions of NO_x in the stationary CI internal combustion engine exhaust to the following:

(i) 14.4 g/KW-hr (10.7 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii) $44 \cdot n^{-0.23}$ g/KW-hr ($33 \cdot n^{-0.23}$ g/HP-hr) when maximum engine speed is greater than or equal to 130 but less than 2,000 rpm and where n is maximum engine speed; and

(iii) 7.7 g/KW-hr (5.7 g/HP-hr) when maximum engine speed is greater than or equal to 2,000 rpm.

(3) Limit the emissions of PM in the stationary CI internal combustion engine exhaust to 0.40 g/KW-hr (0.30 g/HP-hr).

(e) Owners and operators of emergency stationary CI ICE with a displacement of less than 30 liters per cylinder who conduct performance tests in-use must meet the NTE standards as indicated in [§ 60.4212](#).

(f) Owners and operators of any modified or reconstructed emergency stationary CI ICE subject to this subpart must meet the emission standards applicable to the model year, maximum engine power, and displacement of the modified or reconstructed CI ICE that are specified in [paragraphs \(a\)](#) through [\(e\)](#) of this section.

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37969](#), June 28, 2011; [86 FR 34358](#), June 29, 2021]

§ 60.4206 How long must I meet the emission standards if I am an owner or operator of a stationary CI internal combustion engine?

Owners and operators of stationary CI ICE must operate and maintain stationary CI ICE that achieve the emission standards as required in [§§ 60.4204](#) and [60.4205](#) over the entire life of the engine.

[[76 FR 37969](#), June 28, 2011]

Fuel Requirements for Owners and Operators

§ 60.4207 What fuel requirements must I meet if I am an owner or operator of a stationary CI internal combustion engine subject to this subpart?

(a) [Reserved]

(b) Beginning October 1, 2010, owners and operators of stationary CI ICE subject to this subpart with a displacement of less than 30 liters per cylinder that use diesel fuel must use diesel fuel that meets the requirements of [40 CFR 1090.305](#) for nonroad diesel fuel, except that any existing diesel fuel purchased (or otherwise obtained) prior to October 1, 2010, may be used until depleted.

(c) [Reserved]

(d) Beginning June 1, 2012, owners and operators of stationary CI ICE subject to this subpart with a displacement of greater than or equal to 30 liters per cylinder must use diesel fuel that meets a maximum per-gallon sulfur content of 1,000 parts per million (ppm).

(e) Stationary CI ICE that have a national security exemption under [§ 60.4200\(d\)](#) are also exempt from the fuel requirements in this section.

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37969](#), June 28, 2011; [78 FR 6695](#), Jan. 30, 2013; [85 FR 78463](#), Dec. 4, 2020]

Other Requirements for Owners and Operators

§ 60.4208 What is the deadline for importing or installing stationary CI ICE produced in previous model years?

(a) After December 31, 2008, owners and operators may not install stationary CI ICE (excluding fire pump engines) that do not meet the applicable requirements for 2007 model year engines.

(b) After December 31, 2009, owners and operators may not install stationary CI ICE with a maximum engine power of less than 19 KW (25 HP) (excluding fire pump engines) that do not meet the applicable requirements for 2008 model year engines.

(c) After December 31, 2014, owners and operators may not install non-emergency stationary CI ICE with a maximum engine power of greater than or equal to 19 KW (25 HP) and less than 56 KW (75 HP) that do not meet the applicable requirements for 2013 model year non-emergency engines.

(d) After December 31, 2013, owners and operators may not install non-emergency stationary CI ICE with a maximum engine power of greater than or equal to 56 KW (75 HP) and less than

130 KW (175 HP) that do not meet the applicable requirements for 2012 model year non-emergency engines.

(e) After December 31, 2012, owners and operators may not install non-emergency stationary CI ICE with a maximum engine power of greater than or equal to 130 KW (175 HP), including those above 560 KW (750 HP), that do not meet the applicable requirements for 2011 model year non-emergency engines.

(f) After December 31, 2016, owners and operators may not install non-emergency stationary CI ICE with a maximum engine power of greater than or equal to 560 KW (750 HP) that do not meet the applicable requirements for 2015 model year non-emergency engines.

(g) After December 31, 2018, owners and operators may not install non-emergency stationary CI ICE with a maximum engine power greater than or equal to 600 KW (804 HP) and less than 2,000 KW (2,680 HP) and a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder that do not meet the applicable requirements for 2017 model year non-emergency engines.

(h) In addition to the requirements specified in [§§ 60.4201](#), [60.4202](#), [60.4204](#), and [60.4205](#), it is prohibited to import stationary CI ICE with a displacement of less than 30 liters per cylinder that do not meet the applicable requirements specified in [paragraphs \(a\)](#) through [\(g\)](#) of this section after the dates specified in [paragraphs \(a\)](#) through [\(g\)](#) of this section.

(i) The requirements of this section do not apply to owners or operators of stationary CI ICE that have been modified, reconstructed, and do not apply to engines that were removed from one existing location and reinstalled at a new location.

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37969](#), June 28, 2011]

§ 60.4209 What are the monitoring requirements if I am an owner or operator of a stationary CI internal combustion engine?

If you are an owner or operator, you must meet the monitoring requirements of this section. In addition, you must also meet the monitoring requirements specified in [§ 60.4211](#).

(a) If you are an owner or operator of an emergency stationary CI internal combustion engine that does not meet the standards applicable to non-emergency engines, you must install a non-resettable hour meter prior to startup of the engine.

(b) If you are an owner or operator of a stationary CI internal combustion engine equipped with a diesel particulate filter to comply with the emission standards in [§ 60.4204](#), the diesel particulate filter must be installed with a backpressure monitor that notifies the owner or operator when the high backpressure limit of the engine is approached.

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37969](#), June 28, 2011]

Compliance Requirements

§ 60.4210 What are my compliance requirements if I am a stationary CI internal combustion engine manufacturer?

(a) Stationary CI internal combustion engine manufacturers must certify their stationary CI ICE with a displacement of less than 10 liters per cylinder to the emission standards specified in [§§ 60.4201\(a\)](#) through [\(c\)](#) and [60.4202\(a\)](#), [\(b\)](#), and [\(d\)](#) using the certification procedures required in [40 CFR part 1039, subpart C](#), and must test their engines as specified in [40 CFR part 1039](#). For the purposes of this subpart, engines certified to the standards in Table 1 to this subpart shall be subject to the same certification procedures required for engines certified to the Tier 1 standards in [40 CFR part 1039, appendix I](#). For the purposes of this subpart, engines certified to the standards in Table 4 to this subpart shall be subject to the same certification procedures required for engines certified to the Tier 1 standards in [40 CFR part 1039, appendix I](#), except that engines with NFPA nameplate power of less than 37 KW (50 HP) certified to model year 2011 or later standards shall be subject to the same requirements as engines certified to the standards in [40 CFR part 1039](#).

(b) Stationary CI internal combustion engine manufacturers must certify their stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder to the emission standards specified in [§§ 60.4201\(d\)](#) and [\(e\)](#) and [60.4202\(e\)](#) and [\(f\)](#) using the certification procedures required in [40 CFR part 1042, subpart C](#), and must test their engines as specified in [40 CFR part 1042](#).

(c) Stationary CI internal combustion engine manufacturers must meet the requirements of [40 CFR 1039.120](#), [1039.125](#), [1039.130](#), and [1039.135](#) and [40 CFR part 1068](#) for engines that are certified to the emission standards in [40 CFR part 1039](#). Stationary CI internal combustion engine manufacturers must meet the corresponding provisions of [40 CFR part 1042](#) for engines that would be covered by that part if they were nonroad (including marine) engines. Labels on such engines must refer to stationary engines, rather than or in addition to nonroad or marine engines, as appropriate. Stationary CI internal combustion engine manufacturers must label their engines according to [paragraphs \(c\)\(1\)](#) through [\(3\)](#) of this section.

(1) Stationary CI internal combustion engines manufactured from January 1, 2006 to March 31, 2006 (January 1, 2006 to June 30, 2006 for fire pump engines), other than those that are part of certified engine families under the nonroad CI engine regulations, must be labeled according to [40 CFR 1039.20](#).

(2) Stationary CI internal combustion engines manufactured from April 1, 2006 to December 31, 2006 (or, for fire pump engines, July 1, 2006 to December 31 of the year preceding the year listed in table 3 to this subpart) must be labeled according to [paragraphs \(c\)\(2\)\(i\)](#) through [\(iii\)](#) of this section:

(i) Stationary CI internal combustion engines that are part of certified engine families under the nonroad regulations must meet the labeling requirements for nonroad CI engines, but do not have to meet the labeling requirements in [40 CFR 1039.20](#).

(ii) Stationary CI internal combustion engines that meet Tier 1 requirements (or requirements for fire pumps) under this subpart, but do not meet the requirements applicable to nonroad CI engines must be labeled according to [40 CFR 1039.20](#). The engine manufacturer may add language to the label clarifying that the engine meets Tier 1 requirements (or requirements for fire pumps) of this subpart.

(iii) Stationary CI internal combustion engines manufactured after April 1, 2006 that do not meet Tier 1 requirements of this subpart, or fire pumps engines manufactured after July 1, 2006 that do not meet the requirements for fire pumps under this subpart, may not be used in the U.S. If any such engines are manufactured in the U.S. after April 1, 2006 (July 1, 2006 for fire pump engines), they must be exported or must be brought into compliance with the appropriate standards prior to initial operation. The export provisions of [40 CFR 1068.230](#) would apply to engines for export and the manufacturers must label such engines according to [40 CFR 1068.230](#).

(3) Stationary CI internal combustion engines manufactured after January 1, 2007 (for fire pump engines, after January 1 of the year listed in table 3 to this subpart, as applicable) must be labeled according to [paragraphs \(c\)\(3\)\(i\)](#) through [\(iii\)](#) of this section.

(i) Stationary CI internal combustion engines that meet the requirements of this subpart and the corresponding requirements for nonroad (including marine) engines of the same model year and HP must be labeled according to the provisions in [40 CFR part 1039](#) or [1042](#), as appropriate.

(ii) Stationary CI internal combustion engines that meet the requirements of this subpart, but are not certified to the standards applicable to nonroad (including marine) engines of the same model year and HP must be labeled according to the provisions in [40 CFR part 1039](#) or [1042](#), as appropriate, but the words “stationary” must be included instead of “nonroad” or “marine” on the label. In addition, such engines must be labeled according to [40 CFR 1039.20](#).

(iii) Stationary CI internal combustion engines that do not meet the requirements of this subpart must be labeled according to [40 CFR 1068.230](#) and must be exported under the provisions of [40 CFR 1068.230](#).

(d) An engine manufacturer certifying an engine family or families to standards under this subpart that are identical to standards applicable under [40 CFR part 1039](#) or [1042](#) for that model year may certify any such family that contains both nonroad (including marine) and stationary engines as a single engine family and/or may include any such family containing stationary engines in the averaging, banking, and trading provisions applicable for such engines under those parts.

(e) Manufacturers of engine families discussed in [paragraph \(d\)](#) of this section may meet the labeling requirements referred to in [paragraph \(c\)](#) of this section for stationary CI ICE by either adding a separate label containing the information required in [paragraph \(c\)](#) of this section or by adding the words “and stationary” after the word “nonroad” or “marine,” as appropriate, to the label.

(f) Starting with the model years shown in table 5 to this subpart, stationary CI internal combustion engine manufacturers must add a permanent label stating that the engine is for stationary emergency use only to each new emergency stationary CI internal combustion engine greater than or equal to 19 KW (25 HP) that meets all the emission standards for emergency engines in [§ 60.4202](#) but does not meet all the emission standards for non-emergency engines in [§ 60.4201](#). The label must be added according to the labeling requirements specified in [40 CFR 1039.135\(b\)](#). Engine manufacturers must specify in the owner's manual that operation of emergency engines is limited to emergency operations and required maintenance and testing.

(g) Manufacturers of fire pump engines may use the test cycle in table 6 to this subpart for testing fire pump engines and may test at the NFPA certified nameplate HP, provided that the engine is labeled as “Fire Pump Applications Only”.

(h) Engine manufacturers, including importers, may introduce into commerce uncertified engines or engines certified to earlier standards that were manufactured before the new or changed standards took effect until inventories are depleted, as long as such engines are part of normal inventory. For example, if the engine manufacturers' normal industry practice is to keep on hand a one-month supply of engines based on its projected sales, and a new tier of standards starts to apply for the 2009 model year, the engine manufacturer may manufacture engines based on the normal inventory requirements late in the 2008 model year, and sell those engines for installation. The engine manufacturer may not circumvent the provisions of [§ 60.4201](#) or [§ 60.4202](#) by stockpiling engines that are built before new or changed standards take effect. Stockpiling of such engines beyond normal industry practice is a violation of this subpart.

(i) The replacement engine provisions of [40 CFR 1068.240](#) are applicable to stationary CI engines replacing existing equipment that is less than 15 years old.

(j) Stationary CI ICE manufacturers may equip their stationary CI internal combustion engines certified to the emission standards in [40 CFR part 1039](#) with AECDs for qualified emergency situations according to the requirements of [40 CFR 1039.665](#). Manufacturers of stationary CI ICE equipped with AECDs as allowed by [40 CFR 1039.665](#) must meet all the requirements in [40 CFR 1039.665](#) that apply to manufacturers. Manufacturers must document that the engine complies with the Tier 1 standard in [40 CFR part 1039, appendix I](#), when the AECD is activated. Manufacturers must provide any relevant testing, engineering analysis, or other information in sufficient detail to support such statement when applying for certification (including amending an existing certificate) of an engine equipped with an AECD as allowed by [40 CFR 1039.665](#).

(k) Manufacturers of any size may certify their emergency stationary CI internal combustion engines under this section using assigned deterioration factors established by EPA, consistent with [40 CFR 1039.240](#) and [1042.240](#).

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37969](#), June 28, 2011; [81 FR 44219](#), July 7, 2016; [86 FR 34358](#), June 29, 2021]

§ 60.4211 What are my compliance requirements if I am an owner or operator of a stationary CI internal combustion engine?

(a) If you are an owner or operator and must comply with the emission standards specified in this subpart, you must do all of the following, except as permitted under [paragraph \(g\)](#) of this section:

- (1) Operate and maintain the stationary CI internal combustion engine and control device according to the manufacturer's emission-related written instructions;
- (2) Change only those emission-related settings that are permitted by the manufacturer; and
- (3) Meet the requirements of [40 CFR part 1068](#), as they apply to you.

(b) If you are an owner or operator of a pre-2007 model year stationary CI internal combustion engine and must comply with the emission standards specified in [§ 60.4204\(a\)](#) or [§ 60.4205\(a\)](#), or if you are an owner or operator of a CI fire pump engine that is manufactured prior to the model years in table 3 to this subpart and must comply with the emission standards specified in [§ 60.4205\(c\)](#), you must demonstrate compliance according to one of the methods specified in [paragraphs \(b\)\(1\)](#) through [\(5\)](#) of this section.

- (1) Purchasing an engine certified to emission standards for the same model year and maximum engine power as described in [40 CFR parts 1039](#) and [1042](#), as applicable. The engine must be installed and configured according to the manufacturer's specifications.
- (2) Keeping records of performance test results for each pollutant for a test conducted on a similar engine. The test must have been conducted using the same methods specified in this subpart and these methods must have been followed correctly.
- (3) Keeping records of engine manufacturer data indicating compliance with the standards.
- (4) Keeping records of control device vendor data indicating compliance with the standards.
- (5) Conducting an initial performance test to demonstrate compliance with the emission standards according to the requirements specified in [§ 60.4212](#), as applicable.

(c) If you are an owner or operator of a 2007 model year and later stationary CI internal combustion engine and must comply with the emission standards specified in [§ 60.4204\(b\)](#) or [§ 60.4205\(b\)](#), or if you are an owner or operator of a CI fire pump engine that is manufactured during or after the model year that applies to your fire pump engine power rating in table 3 to this subpart and must comply with the emission standards specified in [§ 60.4205\(c\)](#), you must comply by purchasing an engine certified to the emission standards in [§ 60.4204\(b\)](#), or [§ 60.4205\(b\)](#) or [\(c\)](#), as applicable, for the same model year and maximum (or in the case of fire pumps, NFPA nameplate) engine power. The engine must be installed and configured according to the manufacturer's emission-related specifications, except as permitted in [paragraph \(g\)](#) of this section.

(d) If you are an owner or operator and must comply with the emission standards specified in [§ 60.4204\(c\)](#) or [§ 60.4205\(d\)](#), you must demonstrate compliance according to the requirements specified in [paragraphs \(d\)\(1\)](#) through [\(3\)](#) of this section.

(1) Conducting an initial performance test to demonstrate initial compliance with the emission standards as specified in [§ 60.4213](#).

(2) Establishing operating parameters to be monitored continuously to ensure the stationary internal combustion engine continues to meet the emission standards. The owner or operator must petition the Administrator for approval of operating parameters to be monitored continuously. The petition must include the information described in [paragraphs \(d\)\(2\)\(i\)](#) through [\(v\)](#) of this section.

(i) Identification of the specific parameters you propose to monitor continuously;

(ii) A discussion of the relationship between these parameters and NO_x and PM emissions, identifying how the emissions of these pollutants change with changes in these parameters, and how limitations on these parameters will serve to limit NO_x and PM emissions;

(iii) A discussion of how you will establish the upper and/or lower values for these parameters which will establish the limits on these parameters in the operating limitations;

(iv) A discussion identifying the methods and the instruments you will use to monitor these parameters, as well as the relative accuracy and precision of these methods and instruments; and

(v) A discussion identifying the frequency and methods for recalibrating the instruments you will use for monitoring these parameters.

(3) For non-emergency engines with a displacement of greater than or equal to 30 liters per cylinder, conducting annual performance tests to demonstrate continuous compliance with the emission standards as specified in [§ 60.4213](#).

(e) If you are an owner or operator of a modified or reconstructed stationary CI internal combustion engine and must comply with the emission standards specified in [§ 60.4204\(e\)](#) or [§](#)

[60.4205\(f\)](#), you must demonstrate compliance according to one of the methods specified in [paragraphs \(e\)\(1\)](#) or [\(2\)](#) of this section.

(1) Purchasing, or otherwise owning or operating, an engine certified to the emission standards in [§ 60.4204\(e\)](#) or [§ 60.4205\(f\)](#), as applicable.

(2) Conducting a performance test to demonstrate initial compliance with the emission standards according to the requirements specified in [§ 60.4212](#) or [§ 60.4213](#), as appropriate. The test must be conducted within 60 days after the engine commences operation after the modification or reconstruction.

(f) If you own or operate an emergency stationary ICE, you must operate the emergency stationary ICE according to the requirements in [paragraphs \(f\)\(1\)](#) through [\(3\)](#) of this section. In order for the engine to be considered an emergency stationary ICE under this subpart, any operation other than emergency operation, maintenance and testing, emergency demand response, and operation in non-emergency situations for 50 hours per year, as described in [paragraphs \(f\)\(1\)](#) through [\(3\)](#) of this section, is prohibited. If you do not operate the engine according to the requirements in [paragraphs \(f\)\(1\)](#) through [\(3\)](#) of this section, the engine will not be considered an emergency engine under this subpart and must meet all requirements for non-emergency engines.

(1) There is no time limit on the use of emergency stationary ICE in emergency situations.

(2) You may operate your emergency stationary ICE for any combination of the purposes specified in [paragraphs \(f\)\(2\)\(i\)](#) through [\(iii\)](#) of this section for a maximum of 100 hours per calendar year. Any operation for non-emergency situations as allowed by [paragraph \(f\)\(3\)](#) of this section counts as part of the 100 hours per calendar year allowed by this [paragraph \(f\)\(2\)](#).

(i) Emergency stationary ICE may be operated for maintenance checks and readiness testing, provided that the tests are recommended by federal, state or local government, the manufacturer, the vendor, the regional transmission organization or equivalent balancing authority and transmission operator, or the insurance company associated with the engine. The owner or operator may petition the Administrator for approval of additional hours to be used for maintenance checks and readiness testing, but a petition is not required if the owner or operator maintains records indicating that federal, state, or local standards require maintenance and testing of emergency ICE beyond 100 hours per calendar year.

(ii) Emergency stationary ICE may be operated for emergency demand response for periods in which the Reliability Coordinator under the North American Electric Reliability Corporation (NERC) Reliability Standard EOP-002-3, Capacity and Energy Emergencies (incorporated by reference, see [§ 60.17](#)), or other authorized entity as determined by the Reliability Coordinator, has declared an Energy Emergency Alert Level 2 as defined in the NERC Reliability Standard EOP-002-3.

(iii) Emergency stationary ICE may be operated for periods where there is a deviation of voltage or frequency of 5 percent or greater below standard voltage or frequency.

(3) Emergency stationary ICE may be operated for up to 50 hours per calendar year in non-emergency situations. The 50 hours of operation in non-emergency situations are counted as part of the 100 hours per calendar year for maintenance and testing and emergency demand response provided in [paragraph \(f\)\(2\)](#) of this section. Except as provided in [paragraph \(f\)\(3\)\(i\)](#) of this section, the 50 hours per calendar year for non-emergency situations cannot be used for peak shaving or non-emergency demand response, or to generate income for a facility to an electric grid or otherwise supply power as part of a financial arrangement with another entity.

(i) The 50 hours per year for non-emergency situations can be used to supply power as part of a financial arrangement with another entity if all of the following conditions are met:

(A) The engine is dispatched by the local balancing authority or local transmission and distribution system operator;

(B) The dispatch is intended to mitigate local transmission and/or distribution limitations so as to avert potential voltage collapse or line overloads that could lead to the interruption of power supply in a local area or region.

(C) The dispatch follows reliability, emergency operation or similar protocols that follow specific NERC, regional, state, public utility commission or local standards or guidelines.

(D) The power is provided only to the facility itself or to support the local transmission and distribution system.

(E) The owner or operator identifies and records the entity that dispatches the engine and the specific NERC, regional, state, public utility commission or local standards or guidelines that are being followed for dispatching the engine. The local balancing authority or local transmission and distribution system operator may keep these records on behalf of the engine owner or operator.

(ii) [Reserved]

(g) If you do not install, configure, operate, and maintain your engine and control device according to the manufacturer's emission-related written instructions, or you change emission-related settings in a way that is not permitted by the manufacturer, you must demonstrate compliance as follows:

(1) If you are an owner or operator of a stationary CI internal combustion engine with maximum engine power less than 100 HP, you must keep a maintenance plan and records of conducted maintenance to demonstrate compliance and must, to the extent practicable, maintain and operate the engine in a manner consistent with good air pollution control practice for minimizing emissions. In addition, if you do not install and configure the engine and control device according to the manufacturer's emission-related written instructions, or you change the emission-related settings in a way that is not permitted by the manufacturer,

you must conduct an initial performance test to demonstrate compliance with the applicable emission standards within 1 year of such action.

(2) If you are an owner or operator of a stationary CI internal combustion engine greater than or equal to 100 HP and less than or equal to 500 HP, you must keep a maintenance plan and records of conducted maintenance and must, to the extent practicable, maintain and operate the engine in a manner consistent with good air pollution control practice for minimizing emissions. In addition, you must conduct an initial performance test to demonstrate compliance with the applicable emission standards within 1 year of startup, or within 1 year after an engine and control device is no longer installed, configured, operated, and maintained in accordance with the manufacturer's emission-related written instructions, or within 1 year after you change emission-related settings in a way that is not permitted by the manufacturer.

(3) If you are an owner or operator of a stationary CI internal combustion engine greater than 500 HP, you must keep a maintenance plan and records of conducted maintenance and must, to the extent practicable, maintain and operate the engine in a manner consistent with good air pollution control practice for minimizing emissions. In addition, you must conduct an initial performance test to demonstrate compliance with the applicable emission standards within 1 year of startup, or within 1 year after an engine and control device is no longer installed, configured, operated, and maintained in accordance with the manufacturer's emission-related written instructions, or within 1 year after you change emission-related settings in a way that is not permitted by the manufacturer. You must conduct subsequent performance testing every 8,760 hours of engine operation or 3 years, whichever comes first, thereafter to demonstrate compliance with the applicable emission standards.

(h) The requirements for operators and prohibited acts specified in [40 CFR 1039.665](#) apply to owners or operators of stationary CI ICE equipped with AECs for qualified emergency situations as allowed by [40 CFR 1039.665](#).

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37970](#), June 28, 2011; [78 FR 6695](#), Jan. 30, 2013; [81 FR 44219](#), July 7, 2016; [86 FR 34359](#), June 29, 2021]

Testing Requirements for Owners and Operators

§ 60.4212 What test methods and other procedures must I use if I am an owner or operator of a stationary CI internal combustion engine with a displacement of less than 30 liters per cylinder?

Owners and operators of stationary CI ICE with a displacement of less than 30 liters per cylinder who conduct performance tests pursuant to this subpart must do so according to [paragraphs \(a\)](#) through [\(e\)](#) of this section.

(a) The performance test must be conducted according to the in-use testing procedures in [40 CFR part 1039, subpart F](#), for stationary CI ICE with a displacement of less than 10 liters per cylinder, and according to [40 CFR part 1042, subpart F](#), for stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder. Alternatively, stationary CI ICE that are complying with Tier 2 or Tier 3 emission standards as described in [40 CFR part 1039, appendix I](#), or with Tier 2 emission standards as described in [40 CFR part 1042, appendix I](#), may follow the testing procedures specified in [§ 60.4213](#), as appropriate.

(b) Exhaust emissions from stationary CI ICE that are complying with the emission standards for new CI engines in [40 CFR part 1039](#) must not exceed the not-to-exceed (NTE) standards for the same model year and maximum engine power as required in [40 CFR 1039.101\(e\)](#) and [40 CFR 1039.102\(g\)\(1\)](#), except as specified in [40 CFR 1039.104\(d\)](#). This requirement starts when NTE requirements take effect for nonroad diesel engines under [40 CFR part 1039](#).

(c) Exhaust emissions from stationary CI ICE subject to Tier 2 or Tier 3 emission standards as described in [40 CFR part 1039, appendix I](#), or Tier 2 emission standards as described in [40 CFR part 1042, appendix I](#), must not exceed the NTE numerical requirements, rounded to the same number of decimal places as the applicable standard, determined from the following equation:

$$\text{NTE requirement for each pollutant} = (1.25) \times (\text{STD}) \text{ (Eq. 1)}$$

Where:

STD = The standard specified for that pollutant in [40 CFR part 1039](#) or [1042](#), as applicable.

(d) Exhaust emissions from stationary CI ICE that are complying with the emission standards for pre-2007 model year engines in [§ 60.4204\(a\)](#), [§ 60.4205\(a\)](#), or [§ 60.4205\(c\)](#) must not exceed the NTE numerical requirements, rounded to the same number of decimal places as the applicable standard in [§ 60.4204\(a\)](#), [§ 60.4205\(a\)](#), or [§ 60.4205\(c\)](#), determined from the equation in [paragraph \(c\)](#) of this section.

Where:

STD = The standard specified for that pollutant in [§ 60.4204\(a\)](#), [§ 60.4205\(a\)](#), or [§ 60.4205\(c\)](#).

Alternatively, stationary CI ICE that are complying with the emission standards for pre-2007 model year engines in [§ 60.4204\(a\)](#), [§ 60.4205\(a\)](#), or [§ 60.4205\(c\)](#) may follow the testing procedures specified in [§ 60.4213](#), as appropriate.

(e) Exhaust emissions from stationary CI ICE that are complying with the emission standards for new CI engines in [40 CFR part 1042](#) must not exceed the NTE standards for the same model year and maximum engine power as required in [40 CFR 1042.101\(c\)](#).

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37971](#), June 28, 2011; [86 FR 34359](#), June 29, 2021]

§ 60.4213 What test methods and other procedures must I use if I am an owner or operator of a stationary CI internal combustion engine with a displacement of greater than or equal to 30 liters per cylinder?

Owners and operators of stationary CI ICE with a displacement of greater than or equal to 30 liters per cylinder must conduct performance tests according to [paragraphs \(a\)](#) through [\(f\)](#) of this section.

(a) Each performance test must be conducted according to the requirements in [§ 60.8](#) and under the specific conditions that this subpart specifies in table 7. The test must be conducted within 10 percent of 100 percent peak (or the highest achievable) load.

(b) You may not conduct performance tests during periods of startup, shutdown, or malfunction, as specified in [§ 60.8\(c\)](#).

(c) You must conduct three separate test runs for each performance test required in this section, as specified in [§ 60.8\(f\)](#). Each test run must last at least 1 hour.

(d) To determine compliance with the percent reduction requirement, you must follow the requirements as specified in [paragraphs \(d\)\(1\)](#) through [\(3\)](#) of this section.

(1) You must use Equation 2 of this section to determine compliance with the percent reduction requirement:

$$\frac{C_i - C_o}{C_i} \times 100 = R \quad (\text{Eq. 2})$$

Where:

C_i = concentration of NO_x or PM at the control device inlet,

C_o = concentration of NO_x or PM at the control device outlet, and

R = percent reduction of NO_x or PM emissions.

(2) You must normalize the NO_x or PM concentrations at the inlet and outlet of the control device to a dry basis and to 15 percent oxygen (O_2) using Equation 3 of this section, or an

equivalent percent carbon dioxide (CO₂) using the procedures described in [paragraph \(d\)\(3\)](#) of this section.

$$C_{\text{adj}} = C_{\text{d}} \frac{5.9}{20.9 - \% \text{ O}_2} \quad (\text{Eq. 3})$$

Where:

C_{adj} = Calculated NO_x or PM concentration adjusted to 15 percent O₂.

C_{d} = Measured concentration of NO_x or PM, uncorrected.

5.9 = 20.9 percent O₂–15 percent O₂, the defined O₂ correction value, percent.

%O₂ = Measured O₂ concentration, dry basis, percent.

(3) If pollutant concentrations are to be corrected to 15 percent O₂ and CO₂ concentration is measured in lieu of O₂ concentration measurement, a CO₂ correction factor is needed. Calculate the CO₂ correction factor as described in [paragraphs \(d\)\(3\)\(i\)](#) through [\(iii\)](#) of this section.

(i) Calculate the fuel-specific F_o value for the fuel burned during the test using values obtained from Method 19, [Section 5.2](#), and the following equation:

$$F_o = \frac{0.209 F_d}{F_c} \quad (\text{Eq. 4})$$

Where:

F_o = Fuel factor based on the ratio of O₂ volume to the ultimate CO₂ volume produced by the fuel at zero percent excess air.

0.209 = Fraction of air that is O₂, percent/100.

F_d = Ratio of the volume of dry effluent gas to the gross calorific value of the fuel from Method 19, dsm³/J (dscf/10⁶ Btu).

F_c = Ratio of the volume of CO₂ produced to the gross calorific value of the fuel from Method 19, dsm³/J (dscf/10⁶ Btu).

(ii) Calculate the CO₂ correction factor for correcting measurement data to 15 percent O₂, as follows:

$$X_{\text{CO}_2} = \frac{5.9}{F_o} \quad (\text{Eq. 5})$$

Where:

X_{CO_2} = CO₂ correction factor, percent.

5.9 = 20.9 percent O₂–15 percent O₂, the defined O₂ correction value, percent.

(iii) Calculate the NO_x and PM gas concentrations adjusted to 15 percent O₂ using CO₂ as follows:

$$C_{\text{adj}} = C_d \frac{X_{\text{CO}_2}}{\% \text{CO}_2} \quad (\text{Eq. 6})$$

Where:

C_{adj} = Calculated NO_x or PM concentration adjusted to 15 percent O₂.

C_d = Measured concentration of NO_x or PM, uncorrected.

%CO₂ = Measured CO₂ concentration, dry basis, percent.

(e) To determine compliance with the NO_x mass per unit output emission limitation, convert the concentration of NO_x in the engine exhaust using Equation 7 of this section:

$$\text{ER} = \frac{C_d \times 1.912 \times 10^{-3} \times Q \times T}{\text{KW-hour}} \quad (\text{Eq. 7})$$

Where:

ER = Emission rate in grams per KW-hour.

C_d = Measured NO_x concentration in ppm.

1.912×10^{-3} = Conversion constant for ppm NO_x to grams per standard cubic meter at 25 degrees Celsius.

Q = Stack gas volumetric flow rate, in standard cubic meter per hour.

T = Time of test run, in hours.

KW-hour = Brake work of the engine, in KW-hour.

(f) To determine compliance with the PM mass per unit output emission limitation, convert the concentration of PM in the engine exhaust using Equation 8 of this section:

$$ER = \frac{C_{adj} \times Q \times T}{KW\text{-hour}} \quad (\text{Eq. 8})$$

Where:

ER = Emission rate in grams per KW-hour.

C_{adj} = Calculated PM concentration in grams per standard cubic meter.

Q = Stack gas volumetric flow rate, in standard cubic meter per hour.

T = Time of test run, in hours.

KW-hour = Energy output of the engine, in KW.

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37971](#), June 28, 2011]

Notification, Reports, and Records for Owners and Operators

§ 60.4214 What are my notification, reporting, and recordkeeping requirements if I am an owner or operator of a stationary CI internal combustion engine?

(a) Owners and operators of non-emergency stationary CI ICE that are greater than 2,237 KW (3,000 HP), or have a displacement of greater than or equal to 10 liters per cylinder, or are pre-2007 model year engines that are greater than 130 KW (175 HP) and not certified, must meet the requirements of [paragraphs \(a\)\(1\)](#) and [\(2\)](#) of this section.

(1) Submit an initial notification as required in [§ 60.7\(a\)\(1\)](#). The notification must include the information in [paragraphs \(a\)\(1\)\(i\)](#) through [\(v\)](#) of this section.

(i) Name and address of the owner or operator;

(ii) The address of the affected source;

(iii) Engine information including make, model, engine family, serial number, model year, maximum engine power, and engine displacement;

(iv) Emission control equipment; and

(v) Fuel used.

(2) Keep records of the information in [paragraphs \(a\)\(2\)\(i\)](#) through [\(iv\)](#) of this section.

(i) All notifications submitted to comply with this subpart and all documentation supporting any notification.

(ii) Maintenance conducted on the engine.

(iii) If the stationary CI internal combustion is a certified engine, documentation from the manufacturer that the engine is certified to meet the emission standards.

(iv) If the stationary CI internal combustion is not a certified engine, documentation that the engine meets the emission standards.

(b) If the stationary CI internal combustion engine is an emergency stationary internal combustion engine, the owner or operator is not required to submit an initial notification. Starting with the model years in table 5 to this subpart, if the emergency engine does not meet the standards applicable to non-emergency engines in the applicable model year, the owner or operator must keep records of the operation of the engine in emergency and non-emergency service that are recorded through the non-resettable hour meter. The owner must record the time of operation of the engine and the reason the engine was in operation during that time.

(c) If the stationary CI internal combustion engine is equipped with a diesel particulate filter, the owner or operator must keep records of any corrective action taken after the backpressure monitor has notified the owner or operator that the high backpressure limit of the engine is approached.

(d) If you own or operate an emergency stationary CI ICE with a maximum engine power more than 100 HP that operates or is contractually obligated to be available for more than 15 hours per calendar year for the purposes specified in [§ 60.4211\(f\)\(2\)\(ii\)](#) and [\(iii\)](#) or that operates for the purposes specified in [§ 60.4211\(f\)\(3\)\(i\)](#), you must submit an annual report according to the requirements in [paragraphs \(d\)\(1\)](#) through [\(3\)](#) of this section.

(1) The report must contain the following information:

(i) Company name and address where the engine is located.

(ii) Date of the report and beginning and ending dates of the reporting period.

(iii) Engine site rating and model year.

(iv) Latitude and longitude of the engine in decimal degrees reported to the fifth decimal place.

(v) Hours operated for the purposes specified in [§ 60.4211\(f\)\(2\)\(ii\)](#) and [\(iii\)](#), including the date, start time, and end time for engine operation for the purposes specified in [§ 60.4211\(f\)\(2\)\(ii\)](#) and [\(iii\)](#).

(vi) Number of hours the engine is contractually obligated to be available for the purposes specified in [§ 60.4211\(f\)\(2\)\(ii\)](#) and [\(iii\)](#).

(vii) Hours spent for operation for the purposes specified in [§ 60.4211\(f\)\(3\)\(i\)](#), including the date, start time, and end time for engine operation for the purposes specified in [§ 60.4211\(f\)\(3\)\(i\)](#). The report must also identify the entity that dispatched the engine and the situation that necessitated the dispatch of the engine.

(2) The first annual report must cover the calendar year 2015 and must be submitted no later than March 31, 2016. Subsequent annual reports for each calendar year must be submitted no later than March 31 of the following calendar year.

(3) The annual report must be submitted electronically using the subpart specific reporting form in the Compliance and Emissions Data Reporting Interface (CEDRI) that is accessed through EPA's Central Data Exchange (CDX) (www.epa.gov/cdx). However, if the reporting form specific to this subpart is not available in CEDRI at the time that the report is due, the written report must be submitted to the Administrator at the appropriate address listed in [§ 60.4](#).

(e) Owners or operators of stationary CI ICE equipped with AECs pursuant to the requirements of [40 CFR 1039.665](#) must report the use of AECs as required by [40 CFR 1039.665\(e\)](#).

[[71 FR 39172](#), July 11, 2006, as amended at [78 FR 6696](#), Jan. 30, 2013; [81 FR 44219](#), July 7, 2016]

Special Requirements

§ 60.4215 What requirements must I meet for engines used in Guam, American Samoa, or the Commonwealth of the Northern Mariana Islands?

(a) Stationary CI ICE with a displacement of less than 30 liters per cylinder that are used in Guam, American Samoa, or the Commonwealth of the Northern Mariana Islands are required to meet the applicable emission standards in [§§ 60.4202](#) and [60.4205](#).

(b) Stationary CI ICE that are used in Guam, American Samoa, or the Commonwealth of the Northern Mariana Islands are not required to meet the fuel requirements in [§ 60.4207](#).

(c) Stationary CI ICE with a displacement of greater than or equal to 30 liters per cylinder that are used in Guam, American Samoa, or the Commonwealth of the Northern Mariana Islands are required to meet the following emission standards:

(1) For engines installed prior to January 1, 2012, limit the emissions of NO_x in the stationary CI internal combustion engine exhaust to the following:

(i) 17.0 g/KW-hr (12.7 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii) $45 \cdot n^{-0.2}$ g/KW-hr ($34 \cdot n^{-0.2}$ g/HP-hr) when maximum engine speed is 130 or more but less than 2,000 rpm, where n is maximum engine speed; and

(iii) 9.8 g/KW-hr (7.3 g/HP-hr) when maximum engine speed is 2,000 rpm or more.

(2) For engines installed on or after January 1, 2012, limit the emissions of NO_x in the stationary CI internal combustion engine exhaust to the following:

(i) 14.4 g/KW-hr (10.7 g/HP-hr) when maximum engine speed is less than 130 rpm;

(ii) $44 \cdot n^{-0.23}$ g/KW-hr ($33 \cdot n^{-0.23}$ g/HP-hr) when maximum engine speed is greater than or equal to 130 but less than 2,000 rpm and where n is maximum engine speed; and

(iii) 7.7 g/KW-hr (5.7 g/HP-hr) when maximum engine speed is greater than or equal to 2,000 rpm.

(3) Limit the emissions of PM in the stationary CI internal combustion engine exhaust to 0.40 g/KW-hr (0.30 g/HP-hr).

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37971](#), June 28, 2011]

§ 60.4216 What requirements must I meet for engines used in Alaska?

(a) Prior to December 1, 2010, owners and operators of stationary CI ICE with a displacement of less than 30 liters per cylinder located in areas of Alaska not accessible by the FAHS should refer to [40 CFR part 69](#) to determine the diesel fuel requirements applicable to such engines.

(b) Except as indicated in [paragraph \(c\)](#) of this section, manufacturers, owners and operators of stationary CI ICE with a displacement of less than 10 liters per cylinder located in remote areas of Alaska may meet the requirements of this subpart by manufacturing and installing engines meeting the Tier 2 or Tier 3 emission standards described in [40 CFR part 1042](#) for the same model year, displacement, and maximum engine power, as appropriate, rather than the otherwise applicable requirements of [40 CFR part 1039](#), as indicated in [§§ 60.4201\(f\)](#) and [60.4202\(g\)](#).

(c) Manufacturers, owners, and operators of stationary CI ICE that are located in remote areas of Alaska may choose to meet the applicable emission standards for emergency engines in §§ [60.4202](#) and [60.4205](#), and not those for non-emergency engines in §§ [60.4201](#) and [60.4204](#), except that for 2014 model year and later nonemergency CI ICE, the owner or operator of any such engine must have that engine certified as meeting at least the Tier 3 PM standards identified in appendix I of [40 CFR part 1039](#) or in [40 CFR 1042.101](#).

(d) The provisions of [§ 60.4207](#) do not apply to owners and operators of pre-2014 model year stationary CI ICE subject to this subpart that are located in remote areas of Alaska.

(e) The provisions of [§ 60.4208\(a\)](#) do not apply to owners and operators of stationary CI ICE subject to this subpart that are located in areas of Alaska not accessible by the FAHS until after December 31, 2009.

(f) The provisions of this section and [§ 60.4207](#) do not prevent owners and operators of stationary CI ICE subject to this subpart that are located in remote areas of Alaska from using fuels mixed with used lubricating oil, in volumes of up to 1.75 percent of the total fuel. The sulfur content of the used lubricating oil must be less than 200 parts per million. The used lubricating oil must meet the on-specification levels and properties for used oil in [40 CFR 279.11](#).

[[76 FR 37971](#), June 28, 2011, as amended at [81 FR 44219](#), July 7, 2016; [86 FR 34359](#), June 29, 2021]

§ 60.4217 What emission standards must I meet if I am an owner or operator of a stationary internal combustion engine using special fuels?

Owners and operators of stationary CI ICE that do not use diesel fuel may petition the Administrator for approval of alternative emission standards, if they can demonstrate that they use a fuel that is not the fuel on which the manufacturer of the engine certified the engine and that the engine cannot meet the applicable standards required in [§ 60.4204](#) or [§ 60.4205](#) using such fuels and that use of such fuel is appropriate and reasonably necessary, considering cost, energy, technical feasibility, human health and environmental, and other factors, for the operation of the engine.

[[76 FR 37972](#), June 28, 2011]

General Provisions

§ 60.4218 What parts of the General Provisions apply to me?

Table 8 to this subpart shows which parts of the General Provisions in [§§ 60.1](#) through [60.19](#) apply to you.

Definitions

§ 60.4219 What definitions apply to this subpart?

As used in this subpart, all terms not defined herein shall have the meaning given them in the CAA and in [subpart A of this part](#).

Alaska Railbelt Grid means the service areas of the six regulated public utilities that extend from Fairbanks to Anchorage and the Kenai Peninsula. These utilities are Golden Valley Electric Association; Chugach Electric Association; Matanuska Electric Association; Homer Electric Association; Anchorage Municipal Light & Power; and the City of Seward Electric System.

Certified emissions life means the period during which the engine is designed to properly function in terms of reliability and fuel consumption, without being remanufactured, specified as a number of hours of operation or calendar years, whichever comes first. The values for certified emissions life for stationary CI ICE with a displacement of less than 10 liters per cylinder are given in [40 CFR 1039.101\(g\)](#). The values for certified emissions life for stationary CI ICE with a displacement of greater than or equal to 10 liters per cylinder and less than 30 liters per cylinder are given in [40 CFR 1042.101\(e\)](#).

Combustion turbine means all equipment, including but not limited to the turbine, the fuel, air, lubrication and exhaust gas systems, control systems (except emissions control equipment), and any ancillary components and sub-components comprising any simple cycle combustion turbine, any regenerative/recuperative cycle combustion turbine, the combustion turbine portion of any cogeneration cycle combustion system, or the combustion turbine portion of any combined cycle steam/electric generating system.

Compression ignition means relating to a type of stationary internal combustion engine that is not a spark ignition engine.

Date of manufacture means one of the following things:

(1) For freshly manufactured engines and modified engines, date of manufacture means the date the engine is originally produced.

(2) For reconstructed engines, date of manufacture means the date the engine was originally produced, except as specified in paragraph (3) of this definition.

(3) Reconstructed engines are assigned a new date of manufacture if the fixed capital cost of the new and refurbished components exceeds 75 percent of the fixed capital cost of a comparable entirely new facility. An engine that is produced from a previously used engine block does not retain the date of manufacture of the engine in which the engine block was previously used if the engine is produced using all new components except for the engine block. In these cases, the date of manufacture is the date of reconstruction or the date the new engine is produced.

Diesel fuel means any liquid obtained from the distillation of petroleum with a boiling point of approximately 150 to 360 degrees Celsius. One commonly used form is number 2 distillate oil.

Diesel particulate filter means an emission control technology that reduces PM emissions by trapping the particles in a flow filter substrate and periodically removes the collected particles by either physical action or by oxidizing (burning off) the particles in a process called regeneration.

Emergency stationary internal combustion engine means any stationary reciprocating internal combustion engine that meets all of the criteria in paragraphs (1) through (3) of this definition. All emergency stationary ICE must comply with the requirements specified in [§ 60.4211\(f\)](#) in order to be considered emergency stationary ICE. If the engine does not comply with the requirements specified in [§ 60.4211\(f\)](#), then it is not considered to be an emergency stationary ICE under this subpart.

(1) The stationary ICE is operated to provide electrical power or mechanical work during an emergency situation. Examples include stationary ICE used to produce power for critical networks or equipment (including power supplied to portions of a facility) when electric power from the local utility (or the normal power source, if the facility runs on its own power production) is interrupted, or stationary ICE used to pump water in the case of fire or flood, etc.

(2) The stationary ICE is operated under limited circumstances for situations not included in paragraph (1) of this definition, as specified in [§ 60.4211\(f\)](#).

(3) The stationary ICE operates as part of a financial arrangement with another entity in situations not included in paragraph (1) of this definition only as allowed in [§ 60.4211\(f\)\(2\)\(ii\)](#) or [\(iii\)](#) and [§ 60.4211\(f\)\(3\)\(i\)](#).

Engine manufacturer means the manufacturer of the engine. See the definition of “manufacturer” in this section.

Fire pump engine means an emergency stationary internal combustion engine certified to NFPA requirements that is used to provide power to pump water for fire suppression or protection.

Freshly manufactured engine means an engine that has not been placed into service. An engine becomes freshly manufactured when it is originally produced.

Installed means the engine is placed and secured at the location where it is intended to be operated.

Manufacturer has the meaning given in section 216(1) of the Act. In general, this term includes any person who manufactures a stationary engine for sale in the United States or otherwise introduces a new stationary engine into commerce in the United States. This includes importers who import stationary engines for sale or resale.

Maximum engine power means maximum engine power as defined in [40 CFR 1039.801](#).

Model year means the calendar year in which an engine is manufactured (see “date of manufacture”), except as follows:

(1) Model year means the annual new model production period of the engine manufacturer in which an engine is manufactured (see “date of manufacture”), if the annual new model production period is different than the calendar year and includes January 1 of the calendar year for which the model year is named. It may not begin before January 2 of the previous calendar year and it must end by December 31 of the named calendar year.

(2) For an engine that is converted to a stationary engine after being placed into service as a nonroad or other non-stationary engine, model year means the calendar year or new model production period in which the engine was manufactured (see “date of manufacture”).

Other internal combustion engine means any internal combustion engine, except combustion turbines, which is not a reciprocating internal combustion engine or rotary internal combustion engine.

Reciprocating internal combustion engine means any internal combustion engine which uses reciprocating motion to convert heat energy into mechanical work.

Remote areas of Alaska means areas of Alaska that meet either paragraph (1) or (2) of this definition.

(1) Areas of Alaska that are not accessible by the Federal Aid Highway System (FAHS).

(2) Areas of Alaska that meet all of the following criteria:

(i) The only connection to the FAHS is through the Alaska Marine Highway System, or the stationary CI ICE operation is within an isolated grid in Alaska that is not connected to the statewide electrical grid referred to as the Alaska Railbelt Grid.

(ii) At least 10 percent of the power generated by the stationary CI ICE on an annual basis is used for residential purposes.

(iii) The generating capacity of the source is less than 12 megawatts, or the stationary CI ICE is used exclusively for backup power for renewable energy.

Rotary internal combustion engine means any internal combustion engine which uses rotary motion to convert heat energy into mechanical work.

Spark ignition means relating to a gasoline, natural gas, or liquefied petroleum gas fueled engine or any other type of engine with a spark plug (or other sparking device) and with operating characteristics significantly similar to the theoretical Otto combustion cycle. Spark ignition engines usually use a throttle to regulate intake air flow to control power during normal operation. Dual-fuel engines in which a liquid fuel (typically diesel fuel) is used for CI and gaseous fuel (typically natural gas) is used as the primary fuel at an annual average ratio of less

than 2 parts diesel fuel to 100 parts total fuel on an energy equivalent basis are spark ignition engines.

Stationary internal combustion engine means any internal combustion engine, except combustion turbines, that converts heat energy into mechanical work and is not mobile. Stationary ICE differ from mobile ICE in that a stationary internal combustion engine is not a nonroad engine as defined at [40 CFR 1068.30](#) (excluding paragraph (2)(ii) of that definition), and is not used to propel a motor vehicle, aircraft, or a vehicle used solely for competition. Stationary ICE include reciprocating ICE, rotary ICE, and other ICE, except combustion turbines.

Subpart means [40 CFR part 60, subpart III](#).

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37972](#), June 28, 2011; [78 FR 6696](#), Jan. 30, 2013; [81 FR 44219](#), July 7, 2016; [86 FR 34360](#), June 29, 2021]

Table 1 to Subpart III of Part 60 - Emission Standards for Stationary Pre-2007 Model Year Engines With a Displacement of <10 Liters per Cylinder and 2007-2010 Model Year Engines >2,237 KW (3,000 HP) and With a Displacement of <10 Liters per Cylinder

[As stated in [§§ 60.4201\(b\)](#), [60.4202\(b\)](#), [60.4204\(a\)](#), and [60.4205\(a\)](#), you must comply with the following emission standards]

Maximum engine power	Emission standards for stationary pre-2007 model year engines with a displacement of <10 liters per cylinder and 2007-2010 model year engines >2,237 KW (3,000 HP) and with a displacement of <10 liters per cylinder in g/KW-hr (g/HP-hr)				
	NMHC + NO _x	HC	NO _x	CO	PM
KW<8 (HP<11)	10.5 (7.8)			8.0 (6.0)	1.0 (0.75)
8≤KW<19 (11≤HP<25)	9.5 (7.1)			6.6 (4.9)	0.80 (0.60)
19≤KW<37 (25≤HP<50)	9.5 (7.1)			5.5 (4.1)	0.80 (0.60)
37≤KW<56			9.2 (6.9)		

Maximum engine power	Emission standards for stationary pre-2007 model year engines with a displacement of <10 liters per cylinder and 2007-2010 model year engines >2,237 KW (3,000 HP) and with a displacement of <10 liters per cylinder in g/KW-hr (g/HP-hr)				
	NMHC + NO _x	HC	NO _x	CO	PM
(50≤HP<75)					
56≤KW<75 (75≤HP<100)			9.2 (6.9)		
75≤KW<130 (100≤HP<175)			9.2 (6.9)		
130≤KW<225 (175≤HP<300)		1.3 (1.0)	9.2 (6.9)	11.4 (8.5)	0.54 (0.40)
225≤KW<450 (300≤HP<600)		1.3 (1.0)	9.2 (6.9)	11.4 (8.5)	0.54 (0.40)
450≤KW≤560 (600≤HP≤750)		1.3 (1.0)	9.2 (6.9)	11.4 (8.5)	0.54 (0.40)
KW>560 (HP>750)		1.3 (1.0)	9.2 (6.9)	11.4 (8.5)	0.54 (0.40)

Table 2 to Subpart IIII of Part 60 - Emission Standards for 2008 Model Year and Later Emergency Stationary CI ICE <37 KW (50 HP) With a Displacement of <10 Liters per Cylinder

[As stated in [§ 60.4202\(a\)\(1\)](#), you must comply with the following emission standards]

Engine power	Emission standards for 2008 model year and later emergency stationary CI ICE <37 KW (50 HP) with a displacement of <10 liters per cylinder in g/KW-hr (g/HP-hr)			
	Model year(s)	NO _x + NMHC	CO	PM

Engine power	Emission standards for 2008 model year and later emergency stationary CI ICE <37 KW (50 HP) with a displacement of <10 liters per cylinder in g/KW-hr (g/HP-hr)			
	Model year(s)	NO _x + NMHC	CO	PM
KW<8 (HP<11)	2008 +	7.5 (5.6)	8.0 (6.0)	0.40 (0.30)
8≤KW<19 (11≤HP<25)	2008 +	7.5 (5.6)	6.6 (4.9)	0.40 (0.30)
19≤KW<37 (25≤HP<50)	2008 +	7.5 (5.6)	5.5 (4.1)	0.30 (0.22)

Table 3 to Subpart IIII of Part 60 - Certification Requirements for Stationary Fire Pump Engines

As stated in [§ 60.4202\(d\)](#), you must certify new stationary fire pump engines beginning with the following model years:

Engine power	Starting model year engine manufacturers must certify new stationary fire pump engines according to § 60.4202(d) ¹
KW<75 (HP<100)	2011
75≤KW<130 (100≤HP<175)	2010
130≤KW≤560 (175≤HP≤750)	2009
KW>560 (HP>750)	2008

¹Manufacturers of fire pump stationary CI ICE with a maximum engine power greater than or equal to 37 kW (50 HP) and less than 450 KW (600 HP) and a rated speed of greater than 2,650 revolutions per minute (rpm) are not required to certify such engines until three model years following the model year indicated in this Table 3 for engines in the applicable engine power category.

[[71 FR 39172](#), July 11, 2006, as amended at [76 FR 37972](#), June 28, 2011]

Table 4 to Subpart IIII of Part 60 - Emission Standards for Stationary Fire Pump Engines

[As stated in [§§ 60.4202\(d\)](#) and [60.4205\(c\)](#), you must comply with the following emission standards for stationary fire pump engines]

Maximum engine power	Model year(s)	NMHC + NO _x	CO	PM
KW<8 (HP<11)	2010 and earlier	10.5 (7.8)	8.0 (6.0)	1.0 (0.75)
	2011 +	7.5 (5.6)		0.40 (0.30)
8≤KW<19 (11≤HP<25)	2010 and earlier	9.5 (7.1)	6.6 (4.9)	0.80 (0.60)
	2011 +	7.5 (5.6)		0.40 (0.30)
19≤KW<37 (25≤HP<50)	2010 and earlier	9.5 (7.1)	5.5 (4.1)	0.80 (0.60)
	2011 +	7.5 (5.6)		0.30 (0.22)
37≤KW<56 (50≤HP<75)	2010 and earlier	10.5 (7.8)	5.0 (3.7)	0.80 (0.60)
	2011 + ¹	4.7 (3.5)		0.40 (0.30)
56≤KW<75 (75≤HP<100)	2010 and earlier	10.5 (7.8)	5.0 (3.7)	0.80 (0.60)
	2011 + ¹	4.7 (3.5)		0.40 (0.30)
75≤KW<130 (100≤HP<175)	2009 and earlier	10.5 (7.8)	5.0 (3.7)	0.80 (0.60)
	2010 + ²	4.0 (3.0)		0.30 (0.22)
130≤KW<225 (175≤HP<300)	2008 and earlier	10.5 (7.8)	3.5 (2.6)	0.54 (0.40)
	2009 + ³	4.0 (3.0)		0.20 (0.15)

Maximum engine power	Model year(s)	NMHC + NO _x	CO	PM
225≤KW<450 (300≤HP<600)	2008 and earlier	10.5 (7.8)	3.5 (2.6)	0.54 (0.40)
	2009 + ³	4.0 (3.0)		0.20 (0.15)
450≤KW≤560 (600≤HP≤750)	2008 and earlier	10.5 (7.8)	3.5 (2.6)	0.54 (0.40)
	2009 +	4.0 (3.0)		0.20 (0.15)
KW>560 (HP>750)	2007 and earlier	10.5 (7.8)	3.5 (2.6)	0.54 (0.40)
	2008 +	6.4 (4.8)		0.20 (0.15)

¹ For model years 2011-2013, manufacturers, owners and operators of fire pump stationary CI ICE in this engine power category with a rated speed of greater than 2,650 revolutions per minute (rpm) may comply with the emission limitations for 2010 model year engines.

² For model years 2010-2012, manufacturers, owners and operators of fire pump stationary CI ICE in this engine power category with a rated speed of greater than 2,650 rpm may comply with the emission limitations for 2009 model year engines.

³ In model years 2009-2011, manufacturers of fire pump stationary CI ICE in this engine power category with a rated speed of greater than 2,650 rpm may comply with the emission limitations for 2008 model year engines.

Table 5 to Subpart IIII of Part 60 - Labeling and Recordkeeping Requirements for New Stationary Emergency Engines

[You must comply with the labeling requirements in [§ 60.4210\(f\)](#) and the recordkeeping requirements in [§ 60.4214\(b\)](#) for new emergency stationary CI ICE beginning in the following model years:]

Engine power	Starting model year
19≤KW<56 (25≤HP<75)	2013
56≤KW<130 (75≤HP<175)	2012
KW≥130 (HP≥175)	2011

Table 6 to Subpart III of Part 60 - Optional 3-Mode Test Cycle for Stationary Fire Pump Engines

[As stated in [§ 60.4210\(g\)](#), manufacturers of fire pump engines may use the following test cycle for testing fire pump engines:]

Mode No.	Engine speed ¹	Torque (percent) ²	Weighting factors
1	Rated	100	0.30
2	Rated	75	0.50
3	Rated	50	0.20

¹ Engine speed: ± 2 percent of point.

² Torque: NFPA certified nameplate HP for 100 percent point. All points should be ± 2 percent of engine percent load value.

Table 7 to Subpart III of Part 60 - Requirements for Performance Tests for Stationary CI ICE With a Displacement of ≥ 30 Liters per Cylinder

As stated in [§ 60.4213](#), you must comply with the following requirements for performance tests for stationary CI ICE with a displacement of ≥ 30 liters per cylinder:

Each	Complying with the requirement to	You must	Using	According to the following requirements
1. Stationary CI internal combustion engine with a displacement of ≥ 30 liters per cylinder	a. Reduce NO _x emissions by 90 percent or more;	i. Select the sampling port location and number/location of traverse points at the inlet and outlet of the control device;		(a) For NO _x , O ₂ , and moisture measurement, ducts ≤ 6 inches in diameter may be sampled at a single point located at the duct centroid and ducts > 6 and ≤ 12 inches in

Each	Complying with the requirement to	You must	Using	According to the following requirements
				diameter may be sampled at 3 traverse points located at 16.7, 50.0, and 83.3% of the measurement line ('3-point long line'). If the duct is >12 inches in diameter <i>and</i> the sampling port location meets the two and half-diameter criterion of Section 11.1.1 of Method 1 of 40 CFR part 60, appendix A-1 , the duct may be sampled at '3-point long line'; otherwise, conduct the stratification testing and select sampling points according to Section 8.1.2 of Method 7E of 40 CFR part 60, appendix A-4 .
	ii. Measure O ₂ at the inlet and outlet of the control device;		(1) Method 3, 3A, or 3B of 40 CFR part 60, appendix A-2	(b) Measurements to determine O ₂ concentration must be made at the same time as the measurements for NO _x concentration.
	iii. If necessary, measure moisture content at the inlet and outlet of the		(2) Method 4 of 40 CFR part 60, appendix A-3 , Method 320	(c) Measurements to determine moisture content must be made at the same time as the

Each	Complying with the requirement to	You must	Using	According to the following requirements
		control device; and	of 40 CFR part 63, appendix A , or ASTM D 6348-03 (incorporated by reference, see § 60.17)	measurements for NO _x concentration.
		iv. Measure NO _x at the inlet and outlet of the control device.	(3) Method 7E of 40 CFR part 60, appendix A-4 , Method 320 of 40 CFR part 63, appendix A , or ASTM D 6348-03 (incorporated by reference, see § 60.17)	(d) NO _x concentration must be at 15 percent O ₂ , dry basis. Results of this test consist of the average of the three 1-hour or longer runs.
	b. Limit the concentration of NO _x in the stationary CI internal combustion engine exhaust.	i. Select the sampling port location and number/location of traverse points at the exhaust of the stationary internal combustion engine;		(a) For NO _x , O ₂ , and moisture measurement, ducts ≤6 inches in diameter may be sampled at a single point located at the duct centroid and ducts >6 and ≤12 inches in diameter may be sampled at 3 traverse points located at 16.7, 50.0, and 83.3% of the measurement line ('3-point long line'). If the duct is >12 inches in diameter <i>and</i> the

Each	Complying with the requirement to	You must	Using	According to the following requirements
				<p>sampling port location meets the two and half-diameter criterion of Section 11.1.1 of Method 1 of 40 CFR part 60, appendix A-1, the duct may be sampled at '3-point long line'; otherwise, conduct the stratification testing and select sampling points according to Section 8.1.2 of Method 7E of 40 CFR part 60, appendix A-4.</p>
	<p>ii. Determine the O₂ concentration of the stationary internal combustion engine exhaust at the sampling port location;</p>		<p>(1) Method 3, 3A, or 3B of 40 CFR part 60, appendix A-2</p>	<p>(b) Measurements to determine O₂ concentration must be made at the same time as the measurement for NO_x concentration.</p>
	<p>iii. If necessary, measure moisture content of the stationary internal combustion engine exhaust at the sampling port location; and</p>		<p>(2) Method 4 of 40 CFR part 60, appendix A-3, Method 320 of 40 CFR part 63, appendix A, or ASTM D 6348-03 (incorporated by reference, see §</p>	<p>(c) Measurements to determine moisture content must be made at the same time as the measurement for NO_x concentration.</p>

Each	Complying with the requirement to	You must	Using	According to the following requirements
			60.17)	
		iv. Measure NO _x at the exhaust of the stationary internal combustion engine; if using a control device, the sampling site must be located at the outlet of the control device.	(3) Method 7E of 40 CFR part 60, appendix A-4 , Method 320 of 40 CFR part 63, appendix A , or ASTM D 6348-03 (incorporated by reference, see § 60.17)	(d) NO _x concentration must be at 15 percent O ₂ , dry basis. Results of this test consist of the average of the three 1-hour or longer runs.
	c. Reduce PM emissions by 60 percent or more	i. Select the sampling port location and the number of traverse points;	(1) Method 1 or 1A of 40 CFR part 60, appendix A-1	(a) Sampling sites must be located at the inlet and outlet of the control device.
		ii. Measure O ₂ at the inlet and outlet of the control device;	(2) Method 3, 3A, or 3B of 40 CFR part 60, appendix A-2	(b) Measurements to determine O ₂ concentration must be made at the same time as the measurements for PM concentration.
		iii. If necessary, measure moisture content at the inlet and outlet of the control device; and	(3) Method 4 of 40 CFR part 60, appendix A-3	(c) Measurements to determine and moisture content must be made at the same time as the measurements for PM concentration.
		iv. Measure PM at the inlet and outlet	(4) Method 5 of 40 CFR part	(d) PM concentration must be at 15 percent

Each	Complying with the requirement to	You must	Using	According to the following requirements
		of the control device.	60, appendix A-3	O ₂ , dry basis. Results of this test consist of the average of the three 1-hour or longer runs.
	d. Limit the concentration of PM in the stationary CI internal combustion engine exhaust	<p>i. Select the sampling port location and the number of traverse points;</p> <p>ii. Determine the O₂ concentration of the stationary internal combustion engine exhaust at the sampling port location;</p> <p>iii. If necessary, measure moisture content of the stationary internal combustion engine exhaust at the sampling port location; and</p> <p>iv. Measure PM at the exhaust of the stationary internal combustion engine.</p>	<p>(1) Method 1 or 1A of 40 CFR part 60, appendix A-1</p> <p>(2) Method 3, 3A, or 3B of 40 CFR part 60, appendix A-2</p> <p>(3) Method 4 of 40 CFR part 60, appendix A-3</p> <p>(4) Method 5 of 40 CFR part 60, appendix A-3</p>	<p>(a) If using a control device, the sampling site must be located at the outlet of the control device.</p> <p>(b) Measurements to determine O₂ concentration must be made at the same time as the measurements for PM concentration.</p> <p>(c) Measurements to determine moisture content must be made at the same time as the measurements for PM concentration.</p> <p>(d) PM concentration must be at 15 percent O₂, dry basis. Results of this test consist of the average of the three</p>

Each	Complying with the requirement to	You must	Using	According to the following requirements
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1-hour or longer runs.

[[79 FR 11251](#), Feb. 27, 2014]

Table 8 to Subpart III of Part 60 - Applicability of General Provisions to Subpart III

[As stated in [§ 60.4218](#), you must comply with the following applicable General Provisions:]

General Provisions citation	Subject of citation	Applies to subpart	Explanation
§ 60.1	General applicability of the General Provisions	Yes	
§ 60.2	Definitions	Yes	Additional terms defined in § 60.4219 .
§ 60.3	Units and abbreviations	Yes	
§ 60.4	Address	Yes	
§ 60.5	Determination of construction or modification	Yes	
§ 60.6	Review of plans	Yes	
§ 60.7	Notification and Recordkeeping	Yes	Except that § 60.7 only applies as specified in § 60.4214(a) .
§ 60.8	Performance tests	Yes	Except that § 60.8 only applies to stationary CI ICE with a displacement of (\geq 30 liters per cylinder and engines that are not certified.

General Provisions citation	Subject of citation	Applies to subpart	Explanation
§ 60.9	Availability of information	Yes	
§ 60.10	State Authority	Yes	
§ 60.11	Compliance with standards and maintenance requirements	No	Requirements are specified in subpart III.
§ 60.12	Circumvention	Yes	
§ 60.13	Monitoring requirements	Yes	Except that § 60.13 only applies to stationary CI ICE with a displacement of (\geq 30 liters per cylinder).
§ 60.14	Modification	Yes	
§ 60.15	Reconstruction	Yes	
§ 60.16	Priority list	Yes	
§ 60.17	Incorporations by reference	Yes	
§ 60.18	General control device requirements	No	
§ 60.19	General notification and reporting requirements	Yes	

Appendix E

40 C.F.R. Part 63 Subpart ZZZZ

***National Emission Standards for Hazardous Air Pollutants for Stationary Reciprocating
Internal Combustion Engine***

Subpart ZZZZ - National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines

Source: [69 FR 33506](#), June 15, 2004, unless otherwise noted.

What This Subpart Covers

§ 63.6580 What is the purpose of subpart ZZZZ?

Subpart ZZZZ establishes national emission limitations and operating limitations for hazardous air pollutants (HAP) emitted from stationary reciprocating internal combustion engines (RICE) located at major and area sources of HAP emissions. This subpart also establishes requirements to demonstrate initial and continuous compliance with the emission limitations and operating limitations.

[[73 FR 3603](#), Jan. 18, 2008]

§ 63.6585 Am I subject to this subpart?

You are subject to this subpart if you own or operate a stationary RICE at a major or area source of HAP emissions, except if the stationary RICE is being tested at a stationary RICE test cell/stand.

- (a) A stationary RICE is any internal combustion engine which uses reciprocating motion to convert heat energy into mechanical work and which is not mobile. Stationary RICE differ from mobile RICE in that a stationary RICE is not a non-road engine as defined at [40 CFR 1068.30](#), and is not used to propel a motor vehicle or a vehicle used solely for competition.
- (b) A major source of HAP emissions is a plant site that emits or has the potential to emit any single HAP at a rate of 10 tons (9.07 megagrams) or more per year or any combination of HAP at a rate of 25 tons (22.68 megagrams) or more per year, except that for oil and gas production facilities, a major source of HAP emissions is determined for each surface site.
- (c) An area source of HAP emissions is a source that is not a major source.
- (d) If you are an owner or operator of an area source subject to this subpart, your status as an entity subject to a standard or other requirements under this subpart does not subject you to the obligation to obtain a permit under [40 CFR part 70](#) or [71](#), provided you are not required to obtain a permit under [40 CFR 70.3\(a\)](#) or [40 CFR 71.3\(a\)](#) for a reason other than your status as an area source under this subpart. Notwithstanding the previous sentence, you must continue to comply with the provisions of this subpart as applicable.
- (e) If you are an owner or operator of a stationary RICE used for national security purposes, you may be eligible to request an exemption from the requirements of this subpart as described in [40 CFR part 1068, subpart C](#).

(f) The emergency stationary RICE listed in [paragraphs \(f\)\(1\) through \(3\)](#) of this section are not subject to this subpart. The stationary RICE must meet the definition of an emergency stationary RICE in [§ 63.6675](#), which includes operating according to the provisions specified in [§ 63.6640\(f\)](#).

(1) Existing residential emergency stationary RICE located at an area source of HAP emissions that do not operate or are not contractually obligated to be available for more than 15 hours per calendar year for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#) and that do not operate for the purpose specified in [§ 63.6640\(f\)\(4\)\(ii\)](#).

(2) Existing commercial emergency stationary RICE located at an area source of HAP emissions that do not operate or are not contractually obligated to be available for more than 15 hours per calendar year for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#) and that do not operate for the purpose specified in [§ 63.6640\(f\)\(4\)\(ii\)](#).

(3) Existing institutional emergency stationary RICE located at an area source of HAP emissions that do not operate or are not contractually obligated to be available for more than 15 hours per calendar year for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#) and that do not operate for the purpose specified in [§ 63.6640\(f\)\(4\)\(ii\)](#).

[[69 FR 33506](#), June 15, 2004, as amended at [73 FR 3603](#), Jan. 18, 2008; [78 FR 6700](#), Jan. 30, 2013]

§ 63.6590 What parts of my plant does this subpart cover?

This subpart applies to each affected source.

(a) **Affected source.** An affected source is any existing, new, or reconstructed stationary RICE located at a major or area source of HAP emissions, excluding stationary RICE being tested at a stationary RICE test cell/stand.

(1) **Existing stationary RICE.**

(i) For stationary RICE with a site rating of more than 500 brake horsepower (HP) located at a major source of HAP emissions, a stationary RICE is existing if you commenced construction or reconstruction of the stationary RICE before December 19, 2002.

(ii) For stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions, a stationary RICE is existing if you commenced construction or reconstruction of the stationary RICE before June 12, 2006.

(iii) For stationary RICE located at an area source of HAP emissions, a stationary RICE is existing if you commenced construction or reconstruction of the stationary RICE before June 12, 2006.

(iv) A change in ownership of an existing stationary RICE does not make that stationary RICE a new or reconstructed stationary RICE.

(2) *New stationary RICE.*

(i) A stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions is new if you commenced construction of the stationary RICE on or after December 19, 2002.

(ii) A stationary RICE with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions is new if you commenced construction of the stationary RICE on or after June 12, 2006.

(iii) A stationary RICE located at an area source of HAP emissions is new if you commenced construction of the stationary RICE on or after June 12, 2006.

(3) *Reconstructed stationary RICE.*

(i) A stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions is reconstructed if you meet the definition of reconstruction in [§ 63.2](#) and reconstruction is commenced on or after December 19, 2002.

(ii) A stationary RICE with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions is reconstructed if you meet the definition of reconstruction in [§ 63.2](#) and reconstruction is commenced on or after June 12, 2006.

(iii) A stationary RICE located at an area source of HAP emissions is reconstructed if you meet the definition of reconstruction in [§ 63.2](#) and reconstruction is commenced on or after June 12, 2006.

(b) *Stationary RICE subject to limited requirements.*

(1) An affected source which meets either of the criteria in [paragraphs \(b\)\(1\)\(i\)](#) through [\(ii\)](#) of this section does not have to meet the requirements of this subpart and of [subpart A of this part](#) except for the initial notification requirements of [§ 63.6645\(f\)](#).

(i) The stationary RICE is a new or reconstructed emergency stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions that does not operate or is not contractually obligated to be available for more than 15 hours per calendar year for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#).

(ii) The stationary RICE is a new or reconstructed limited use stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions.

(2) A new or reconstructed stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions which combusts landfill or digester gas

equivalent to 10 percent or more of the gross heat input on an annual basis must meet the initial notification requirements of [§ 63.6645\(f\)](#) and the requirements of [§§ 63.6625\(c\)](#), [63.6650\(g\)](#), and [63.6655\(c\)](#). These stationary RICE do not have to meet the emission limitations and operating limitations of this subpart.

(3) The following stationary RICE do not have to meet the requirements of this subpart and of [subpart A of this part](#), including initial notification requirements:

- (i) Existing spark ignition 2 stroke lean burn (2SLB) stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions;
- (ii) Existing spark ignition 4 stroke lean burn (4SLB) stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions;
- (iii) Existing emergency stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions that does not operate or is not contractually obligated to be available for more than 15 hours per calendar year for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#).
- (iv) Existing limited use stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions;
- (v) Existing stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis;

(c) ***Stationary RICE subject to Regulations under 40 CFR Part 60.*** An affected source that meets any of the criteria in [paragraphs \(c\)\(1\)](#) through [\(7\)](#) of this section must meet the requirements of this part by meeting the requirements of [40 CFR part 60 subpart III](#), for compression ignition engines or [40 CFR part 60 subpart JJJJ](#), for spark ignition engines. No further requirements apply for such engines under this part.

- (1) A new or reconstructed stationary RICE located at an area source;
- (2) A new or reconstructed 2SLB stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions;
- (3) A new or reconstructed 4SLB stationary RICE with a site rating of less than 250 brake HP located at a major source of HAP emissions;
- (4) A new or reconstructed spark ignition 4 stroke rich burn (4SRB) stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions;
- (5) A new or reconstructed stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions which combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis;

(6) A new or reconstructed emergency or limited use stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions;

(7) A new or reconstructed compression ignition (CI) stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions.

[[69 FR 33506](#), June 15, 2004, as amended at [73 FR 3604](#), Jan. 18, 2008; [75 FR 9674](#), Mar. 3, 2010; [75 FR 37733](#), June 30, 2010; [75 FR 51588](#), Aug. 20, 2010; [78 FR 6700](#), Jan. 30, 2013]

§ 63.6595 When do I have to comply with this subpart?

(a) *Affected sources.*

(1) If you have an existing stationary RICE, excluding existing non-emergency CI stationary RICE, with a site rating of more than 500 brake HP located at a major source of HAP emissions, you must comply with the applicable emission limitations, operating limitations and other requirements no later than June 15, 2007. If you have an existing non-emergency CI stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, an existing stationary CI RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions, or an existing stationary CI RICE located at an area source of HAP emissions, you must comply with the applicable emission limitations, operating limitations, and other requirements no later than May 3, 2013. If you have an existing stationary SI RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions, or an existing stationary SI RICE located at an area source of HAP emissions, you must comply with the applicable emission limitations, operating limitations, and other requirements no later than October 19, 2013.

(2) If you start up your new or reconstructed stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions before August 16, 2004, you must comply with the applicable emission limitations and operating limitations in this subpart no later than August 16, 2004.

(3) If you start up your new or reconstructed stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions after August 16, 2004, you must comply with the applicable emission limitations and operating limitations in this subpart upon startup of your affected source.

(4) If you start up your new or reconstructed stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions before January 18, 2008, you must comply with the applicable emission limitations and operating limitations in this subpart no later than January 18, 2008.

(5) If you start up your new or reconstructed stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions after January 18, 2008, you must comply with the applicable emission limitations and operating limitations in this subpart upon startup of your affected source.

(6) If you start up your new or reconstructed stationary RICE located at an area source of HAP emissions before January 18, 2008, you must comply with the applicable emission limitations and operating limitations in this subpart no later than January 18, 2008.

(7) If you start up your new or reconstructed stationary RICE located at an area source of HAP emissions after January 18, 2008, you must comply with the applicable emission limitations and operating limitations in this subpart upon startup of your affected source.

(b) *Area sources that become major sources.* If you have an area source that increases its emissions or its potential to emit such that it becomes a major source of HAP, the compliance dates in [paragraphs \(b\)\(1\)](#) and [\(2\)](#) of this section apply to you.

(1) Any stationary RICE for which construction or reconstruction is commenced after the date when your area source becomes a major source of HAP must be in compliance with this subpart upon startup of your affected source.

(2) Any stationary RICE for which construction or reconstruction is commenced before your area source becomes a major source of HAP must be in compliance with the provisions of this subpart that are applicable to RICE located at major sources within 3 years after your area source becomes a major source of HAP.

(c) If you own or operate an affected source, you must meet the applicable notification requirements in [§ 63.6645](#) and in [40 CFR part 63, subpart A](#).

[[69 FR 33506](#), June 15, 2004, as amended at [73 FR 3604](#), Jan. 18, 2008; [75 FR 9675](#), Mar. 3, 2010; [75 FR 51589](#), Aug. 20, 2010; [78 FR 6701](#), Jan. 30, 2013]

Emission and Operating Limitations

§ 63.6600 What emission limitations and operating limitations must I meet if I own or operate a stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions?

Compliance with the numerical emission limitations established in this subpart is based on the results of testing the average of three 1-hour runs using the testing requirements and procedures in [§ 63.6620](#) and Table 4 to this subpart.

(a) If you own or operate an existing, new, or reconstructed spark ignition 4SRB stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you must comply with the emission limitations in Table 1a to this subpart and the operating limitations in Table 1b to this subpart which apply to you.

(b) If you own or operate a new or reconstructed 2SLB stationary RICE with a site rating of more than 500 brake HP located at major source of HAP emissions, a new or reconstructed 4SLB stationary RICE with a site rating of more than 500 brake HP located at major source of HAP emissions, or a new or reconstructed CI stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you must comply with the emission limitations in Table 2a to this subpart and the operating limitations in Table 2b to this subpart which apply to you.

(c) If you own or operate any of the following stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you do not need to comply with the emission limitations in Tables 1a, 2a, 2c, and 2d to this subpart or operating limitations in Tables 1b and 2b to this subpart: an existing 2SLB stationary RICE; an existing 4SLB stationary RICE; a stationary RICE that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis; an emergency stationary RICE; or a limited use stationary RICE.

(d) If you own or operate an existing non-emergency stationary CI RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you must comply with the emission limitations in Table 2c to this subpart and the operating limitations in Table 2b to this subpart which apply to you.

[[73 FR 3605](#), Jan. 18, 2008, as amended at [75 FR 9675](#), Mar. 3, 2010]

§ 63.6601 What emission limitations must I meet if I own or operate a new or reconstructed 4SLB stationary RICE with a site rating of greater than or equal to 250 brake HP and less than or equal to 500 brake HP located at a major source of HAP emissions?

Compliance with the numerical emission limitations established in this subpart is based on the results of testing the average of three 1-hour runs using the testing requirements and procedures in [§ 63.6620](#) and Table 4 to this subpart. If you own or operate a new or reconstructed 4SLB stationary RICE with a site rating of greater than or equal to 250 and less than or equal to 500 brake HP located at major source of HAP emissions manufactured on or after January 1, 2008, you must comply with the emission limitations in Table 2a to this subpart and the operating limitations in Table 2b to this subpart which apply to you.

[[73 FR 3605](#), Jan. 18, 2008, as amended at [75 FR 9675](#), Mar. 3, 2010; [75 FR 51589](#), Aug. 20, 2010]

§ 63.6602 What emission limitations and other requirements must I meet if I own or operate an existing stationary RICE

with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions?

If you own or operate an existing stationary RICE with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions, you must comply with the emission limitations and other requirements in Table 2c to this subpart which apply to you. Compliance with the numerical emission limitations established in this subpart is based on the results of testing the average of three 1-hour runs using the testing requirements and procedures in [§ 63.6620](#) and Table 4 to this subpart.

[[78 FR 6701](#), Jan. 30, 2013]

§ 63.6603 What emission limitations, operating limitations, and other requirements must I meet if I own or operate an existing stationary RICE located at an area source of HAP emissions?

Compliance with the numerical emission limitations established in this subpart is based on the results of testing the average of three 1-hour runs using the testing requirements and procedures in [§ 63.6620](#) and Table 4 to this subpart.

- (a) If you own or operate an existing stationary RICE located at an area source of HAP emissions, you must comply with the requirements in Table 2d to this subpart and the operating limitations in Table 2b to this subpart that apply to you.
- (b) If you own or operate an existing stationary non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP that meets either [paragraph \(b\)\(1\)](#) or [\(2\)](#) of this section, you do not have to meet the numerical CO emission limitations specified in Table 2d of this subpart. Existing stationary non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP that meet either [paragraph \(b\)\(1\)](#) or [\(2\)](#) of this section must meet the management practices that are shown for stationary non-emergency CI RICE with a site rating of less than or equal to 300 HP in Table 2d of this subpart.
 - (1) The area source is located in an area of Alaska that is not accessible by the Federal Aid Highway System (FAHS).
 - (2) The stationary RICE is located at an area source that meets [paragraphs \(b\)\(2\)\(i\)](#), [\(ii\)](#), and [\(iii\)](#) of this section.
 - (i) The only connection to the FAHS is through the Alaska Marine Highway System (AMHS), or the stationary RICE operation is within an isolated grid in Alaska that is not connected to the statewide electrical grid referred to as the Alaska Railbelt Grid.

(ii) At least 10 percent of the power generated by the stationary RICE on an annual basis is used for residential purposes.

(iii) The generating capacity of the area source is less than 12 megawatts, or the stationary RICE is used exclusively for backup power for renewable energy.

(c) If you own or operate an existing stationary non-emergency CI RICE with a site rating of more than 300 HP located on an offshore vessel that is an area source of HAP and is a nonroad vehicle that is an Outer Continental Shelf (OCS) source as defined in [40 CFR 55.2](#), you do not have to meet the numerical CO emission limitations specified in Table 2d of this subpart. You must meet all of the following management practices:

(1) Change oil every 1,000 hours of operation or annually, whichever comes first. Sources have the option to utilize an oil analysis program as described in [§ 63.6625\(i\)](#) in order to extend the specified oil change requirement.

(2) Inspect and clean air filters every 750 hours of operation or annually, whichever comes first, and replace as necessary.

(3) Inspect fuel filters and belts, if installed, every 750 hours of operation or annually, whichever comes first, and replace as necessary.

(4) Inspect all flexible hoses every 1,000 hours of operation or annually, whichever comes first, and replace as necessary.

(d) If you own or operate an existing non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP emissions that is certified to the Tier 1 or Tier 2 emission standards in Table 1 of [40 CFR 89.112](#) and that is subject to an enforceable state or local standard that requires the engine to be replaced no later than June 1, 2018, you may until January 1, 2015, or 12 years after the installation date of the engine (whichever is later), but not later than June 1, 2018, choose to comply with the management practices that are shown for stationary non-emergency CI RICE with a site rating of less than or equal to 300 HP in Table 2d of this subpart instead of the applicable emission limitations in Table 2d, operating limitations in Table 2b, and crankcase ventilation system requirements in [§ 63.6625\(g\)](#). You must comply with the emission limitations in Table 2d and operating limitations in Table 2b that apply for non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP emissions by January 1, 2015, or 12 years after the installation date of the engine (whichever is later), but not later than June 1, 2018. You must also comply with the crankcase ventilation system requirements in [§ 63.6625\(g\)](#) by January 1, 2015, or 12 years after the installation date of the engine (whichever is later), but not later than June 1, 2018.

(e) If you own or operate an existing non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP emissions that is certified to the Tier 3 (Tier 2 for engines above 560 kilowatt (kW)) emission standards in Table 1 of [40 CFR 89.112](#), you may comply with the requirements under this part by meeting the requirements for Tier 3 engines (Tier 2 for engines above 560 kW) in [40 CFR part 60 subpart IIII](#) instead of the emission

limitations and other requirements that would otherwise apply under this part for existing non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP emissions.

(f) An existing non-emergency SI 4SLB and 4SRB stationary RICE with a site rating of more than 500 HP located at area sources of HAP must meet the definition of remote stationary RICE in [§ 63.6675](#) on the initial compliance date for the engine, October 19, 2013, in order to be considered a remote stationary RICE under this subpart. Owners and operators of existing non-emergency SI 4SLB and 4SRB stationary RICE with a site rating of more than 500 HP located at area sources of HAP that meet the definition of remote stationary RICE in [§ 63.6675 of this subpart](#) as of October 19, 2013 must evaluate the status of their stationary RICE every 12 months. Owners and operators must keep records of the initial and annual evaluation of the status of the engine. If the evaluation indicates that the stationary RICE no longer meets the definition of remote stationary RICE in [§ 63.6675 of this subpart](#), the owner or operator must comply with all of the requirements for existing non-emergency SI 4SLB and 4SRB stationary RICE with a site rating of more than 500 HP located at area sources of HAP that are not remote stationary RICE within 1 year of the evaluation.

[[75 FR 9675](#), Mar. 3, 2010, as amended at [75 FR 51589](#), Aug. 20, 2010; [76 FR 12866](#), Mar. 9, 2011; [78 FR 6701](#), Jan. 30, 2013]

§ 63.6604 What fuel requirements must I meet if I own or operate a stationary CI RICE?

(a) If you own or operate an existing non-emergency, non-black start CI stationary RICE with a site rating of more than 300 brake HP with a displacement of less than 30 liters per cylinder that uses diesel fuel, you must use diesel fuel that meets the requirements in [40 CFR 1090.305](#) for nonroad diesel fuel.

(b) Beginning January 1, 2015, if you own or operate an existing emergency CI stationary RICE with a site rating of more than 100 brake HP and a displacement of less than 30 liters per cylinder that uses diesel fuel and operates or is contractually obligated to be available for more than 15 hours per calendar year for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#) or that operates for the purpose specified in [§ 63.6640\(f\)\(4\)\(ii\)](#), you must use diesel fuel that meets the requirements in [40 CFR 1090.305](#) for nonroad diesel fuel, except that any existing diesel fuel purchased (or otherwise obtained) prior to January 1, 2015, may be used until depleted.

(c) Beginning January 1, 2015, if you own or operate a new emergency CI stationary RICE with a site rating of more than 500 brake HP and a displacement of less than 30 liters per cylinder located at a major source of HAP that uses diesel fuel and operates or is contractually obligated to be available for more than 15 hours per calendar year for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#), you must use diesel fuel that meets the requirements in [40 CFR 1090.305](#) for nonroad diesel fuel, except that any existing diesel fuel purchased (or otherwise obtained) prior to January 1, 2015, may be used until depleted.

(d) Existing CI stationary RICE located in Guam, American Samoa, the Commonwealth of the Northern Mariana Islands, at area sources in areas of Alaska that meet either [§ 63.6603\(b\)\(1\)](#) or [§ 63.6603\(b\)\(2\)](#), or are on offshore vessels that meet [§ 63.6603\(c\)](#) are exempt from the requirements of this section.

[[78 FR 6702](#), Jan. 30, 2013, as amended at [85 FR 78463](#), Dec. 4, 2020]

General Compliance Requirements

§ 63.6605 What are my general requirements for complying with this subpart?

(a) You must be in compliance with the emission limitations, operating limitations, and other requirements in this subpart that apply to you at all times.

(b) At all times you must operate and maintain any affected source, including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions. The general duty to minimize emissions does not require you to make any further efforts to reduce emissions if levels required by this standard have been achieved. Determination of whether such operation and maintenance procedures are being used will be based on information available to the Administrator which may include, but is not limited to, monitoring results, review of operation and maintenance procedures, review of operation and maintenance records, and inspection of the source.

[[75 FR 9675](#), Mar. 3, 2010, as amended at [78 FR 6702](#), Jan. 30, 2013]

Testing and Initial Compliance Requirements

§ 63.6610 By what date must I conduct the initial performance tests or other initial compliance demonstrations if I own or operate a stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions?

If you own or operate a stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions you are subject to the requirements of this section.

(a) You must conduct the initial performance test or other initial compliance demonstrations in Table 4 to this subpart that apply to you within 180 days after the compliance date that is specified for your stationary RICE in [§ 63.6595](#) and according to the provisions in [§ 63.7\(a\)\(2\)](#).

(b) If you commenced construction or reconstruction between December 19, 2002 and June 15, 2004 and own or operate stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you must demonstrate initial compliance with either the proposed emission limitations or the promulgated emission limitations no later than February 10, 2005 or no later than 180 days after startup of the source, whichever is later, according to [§ 63.7\(a\)\(2\)\(ix\)](#).

(c) If you commenced construction or reconstruction between December 19, 2002 and June 15, 2004 and own or operate stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, and you chose to comply with the proposed emission limitations when demonstrating initial compliance, you must conduct a second performance test to demonstrate compliance with the promulgated emission limitations by December 13, 2007 or after startup of the source, whichever is later, according to [§ 63.7\(a\)\(2\)\(ix\)](#).

(d) An owner or operator is not required to conduct an initial performance test on units for which a performance test has been previously conducted, but the test must meet all of the conditions described in [paragraphs \(d\)\(1\) through \(5\)](#) of this section.

(1) The test must have been conducted using the same methods specified in this subpart, and these methods must have been followed correctly.

(2) The test must not be older than 2 years.

(3) The test must be reviewed and accepted by the Administrator.

(4) Either no process or equipment changes must have been made since the test was performed, or the owner or operator must be able to demonstrate that the results of the performance test, with or without adjustments, reliably demonstrate compliance despite process or equipment changes.

(5) The test must be conducted at any load condition within plus or minus 10 percent of 100 percent load.

[[69 FR 33506](#), June 15, 2004, as amended at [73 FR 3605](#), Jan. 18, 2008]

§ 63.6611 By what date must I conduct the initial performance tests or other initial compliance demonstrations if I own or operate a new or reconstructed 4SLB SI stationary RICE with a site rating of greater than or equal to 250 and less than or equal to 500 brake HP located at a major source of HAP emissions?

If you own or operate a new or reconstructed 4SLB stationary RICE with a site rating of greater than or equal to 250 and less than or equal to 500 brake HP located at a major source of HAP emissions, you must conduct an initial performance test within 240 days after the compliance date that is specified for your stationary RICE in [§ 63.6595](#) and according to the provisions specified in Table 4 to this subpart, as appropriate.

[[73 FR 3605](#), Jan. 18, 2008, as amended at [75 FR 51589](#), Aug. 20, 2010]

§ 63.6612 By what date must I conduct the initial performance tests or other initial compliance demonstrations if I own or operate an existing stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions or an existing stationary RICE located at an area source of HAP emissions?

If you own or operate an existing stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions or an existing stationary RICE located at an area source of HAP emissions you are subject to the requirements of this section.

(a) You must conduct any initial performance test or other initial compliance demonstration according to Tables 4 and 5 to this subpart that apply to you within 180 days after the compliance date that is specified for your stationary RICE in [§ 63.6595](#) and according to the provisions in [§ 63.7\(a\)\(2\)](#).

(b) An owner or operator is not required to conduct an initial performance test on a unit for which a performance test has been previously conducted, but the test must meet all of the conditions described in [paragraphs \(b\)\(1\) through \(4\)](#) of this section.

(1) The test must have been conducted using the same methods specified in this subpart, and these methods must have been followed correctly.

(2) The test must not be older than 2 years.

(3) The test must be reviewed and accepted by the Administrator.

(4) Either no process or equipment changes must have been made since the test was performed, or the owner or operator must be able to demonstrate that the results of the performance test, with or without adjustments, reliably demonstrate compliance despite process or equipment changes.

[[75 FR 9676](#), Mar. 3, 2010, as amended at [75 FR 51589](#), Aug. 20, 2010]

§ 63.6615 When must I conduct subsequent performance tests?

If you must comply with the emission limitations and operating limitations, you must conduct subsequent performance tests as specified in Table 3 of this subpart.

§ 63.6620 What performance tests and other procedures must I use?

(a) You must conduct each performance test in Tables 3 and 4 of this subpart that applies to you.

(b) Each performance test must be conducted according to the requirements that this subpart specifies in Table 4 to this subpart. If you own or operate a non-operational stationary RICE that is subject to performance testing, you do not need to start up the engine solely to conduct the performance test. Owners and operators of a non-operational engine can conduct the performance test when the engine is started up again. The test must be conducted at any load condition within plus or minus 10 percent of 100 percent load for the stationary RICE listed in [paragraphs \(b\)\(1\) through \(4\)](#) of this section.

(1) Non-emergency 4SRB stationary RICE with a site rating of greater than 500 brake HP located at a major source of HAP emissions.

(2) New non-emergency 4SLB stationary RICE with a site rating of greater than or equal to 250 brake HP located at a major source of HAP emissions.

(3) New non-emergency 2SLB stationary RICE with a site rating of greater than 500 brake HP located at a major source of HAP emissions.

(4) New non-emergency CI stationary RICE with a site rating of greater than 500 brake HP located at a major source of HAP emissions.

(c) [Reserved]

(d) You must conduct three separate test runs for each performance test required in this section, as specified in [§ 63.7\(e\)\(3\)](#). Each test run must last at least 1 hour, unless otherwise specified in this subpart.

(e)

(1) You must use Equation 1 of this section to determine compliance with the percent reduction requirement:

$$\frac{C_i - C_o}{C_i} \times 100 = R \quad (\text{Eq. 1})$$

Where:

C_i = concentration of carbon monoxide (CO), total hydrocarbons (THC), or formaldehyde at the control device inlet,

C_o = concentration of CO, THC, or formaldehyde at the control device outlet, and

R = percent reduction of CO, THC, or formaldehyde emissions.

(2) You must normalize the CO, THC, or formaldehyde concentrations at the inlet and outlet of the control device to a dry basis and to 15 percent oxygen, or an equivalent percent carbon dioxide (CO₂). If pollutant concentrations are to be corrected to 15 percent oxygen and CO₂ concentration is measured in lieu of oxygen concentration measurement, a CO₂ correction factor is needed. Calculate the CO₂ correction factor as described in [paragraphs \(e\)\(2\)\(i\)](#) through [\(iii\)](#) of this section.

(i) Calculate the fuel-specific F_o value for the fuel burned during the test using values obtained from Method 19, [Section 5.2](#), and the following equation:

$$F_o = \frac{0.209 F_d}{F_c} \quad (\text{Eq. 2})$$

Where:

F_o = Fuel factor based on the ratio of oxygen volume to the ultimate CO₂ volume produced by the fuel at zero percent excess air.

0.209 = Fraction of air that is oxygen, percent/100.

F_d = Ratio of the volume of dry effluent gas to the gross calorific value of the fuel from Method 19, dsm³/J (dscf/10⁶ Btu).

F_c = Ratio of the volume of CO₂ produced to the gross calorific value of the fuel from Method 19, dsm³/J (dscf/10⁶ Btu)

(ii) Calculate the CO₂ correction factor for correcting measurement data to 15 percent O₂, as follows:

$$X_{CO_2} = \frac{5.9}{F_O} \quad (\text{Eq. 3})$$

Where:

X_{CO_2} = CO₂ correction factor, percent.

5.9 = 20.9 percent O₂ - 15 percent O₂, the defined O₂ correction value, percent.

(iii) Calculate the CO, THC, and formaldehyde gas concentrations adjusted to 15 percent O₂ using CO₂ as follows:

$$C_{adj} = C_d \frac{X_{CO_2}}{\%CO_2} \quad (\text{Eq. 4})$$

Where:

C_{adj} = Calculated concentration of CO, THC, or formaldehyde adjusted to 15 percent O₂.

C_d = Measured concentration of CO, THC, or formaldehyde, uncorrected.

X_{CO_2} = CO₂ correction factor, percent.

$\%CO_2$ = Measured CO₂ concentration measured, dry basis, percent.

(f) If you comply with the emission limitation to reduce CO and you are not using an oxidation catalyst, if you comply with the emission limitation to reduce formaldehyde and you are not using NSCR, or if you comply with the emission limitation to limit the concentration of formaldehyde in the stationary RICE exhaust and you are not using an oxidation catalyst or NSCR, you must petition the Administrator for operating limitations to be established during the initial performance test and continuously monitored thereafter; or for approval of no operating limitations. You must not conduct the initial performance test until after the petition has been approved by the Administrator.

(g) If you petition the Administrator for approval of operating limitations, your petition must include the information described in [paragraphs \(g\)\(1\)](#) through [\(5\)](#) of this section.

(1) Identification of the specific parameters you propose to use as operating limitations;

(2) A discussion of the relationship between these parameters and HAP emissions, identifying how HAP emissions change with changes in these parameters, and how limitations on these parameters will serve to limit HAP emissions;

- (3) A discussion of how you will establish the upper and/or lower values for these parameters which will establish the limits on these parameters in the operating limitations;
- (4) A discussion identifying the methods you will use to measure and the instruments you will use to monitor these parameters, as well as the relative accuracy and precision of these methods and instruments; and
- (5) A discussion identifying the frequency and methods for recalibrating the instruments you will use for monitoring these parameters.
- (h) If you petition the Administrator for approval of no operating limitations, your petition must include the information described in [paragraphs \(h\)\(1\)](#) through [\(7\)](#) of this section.
- (1) Identification of the parameters associated with operation of the stationary RICE and any emission control device which could change intentionally (*e.g.*, operator adjustment, automatic controller adjustment, etc.) or unintentionally (*e.g.*, wear and tear, error, etc.) on a routine basis or over time;
- (2) A discussion of the relationship, if any, between changes in the parameters and changes in HAP emissions;
- (3) For the parameters which could change in such a way as to increase HAP emissions, a discussion of whether establishing limitations on the parameters would serve to limit HAP emissions;
- (4) For the parameters which could change in such a way as to increase HAP emissions, a discussion of how you could establish upper and/or lower values for the parameters which would establish limits on the parameters in operating limitations;
- (5) For the parameters, a discussion identifying the methods you could use to measure them and the instruments you could use to monitor them, as well as the relative accuracy and precision of the methods and instruments;
- (6) For the parameters, a discussion identifying the frequency and methods for recalibrating the instruments you could use to monitor them; and
- (7) A discussion of why, from your point of view, it is infeasible or unreasonable to adopt the parameters as operating limitations.
- (i) The engine percent load during a performance test must be determined by documenting the calculations, assumptions, and measurement devices used to measure or estimate the percent load in a specific application. A written report of the average percent load determination must be included in the notification of compliance status. The following information must be included in the written report: the engine model number, the engine manufacturer, the year of purchase, the manufacturer's site-rated brake horsepower, the ambient temperature, pressure, and humidity during the performance test, and all assumptions that were made to estimate or

calculate percent load during the performance test must be clearly explained. If measurement devices such as flow meters, kilowatt meters, beta analyzers, stain gauges, etc. are used, the model number of the measurement device, and an estimate of its accurate in percentage of true value must be provided.

[[69 FR 33506](#), June 15, 2004, as amended at [75 FR 9676](#), Mar. 3, 2010; [78 FR 6702](#), Jan. 30, 2013]

§ 63.6625 What are my monitoring, installation, collection, operation, and maintenance requirements?

(a) If you elect to install a CEMS as specified in Table 5 of this subpart, you must install, operate, and maintain a CEMS to monitor CO and either O₂ or CO₂ according to the requirements in [paragraphs \(a\)\(1\) through \(4\)](#) of this section. If you are meeting a requirement to reduce CO emissions, the CEMS must be installed at both the inlet and outlet of the control device. If you are meeting a requirement to limit the concentration of CO, the CEMS must be installed at the outlet of the control device.

(1) Each CEMS must be installed, operated, and maintained according to the applicable performance specifications of [40 CFR part 60, appendix B](#).

(2) You must conduct an initial performance evaluation and an annual relative accuracy test audit (RATA) of each CEMS according to the requirements in [§ 63.8](#) and according to the applicable performance specifications of [40 CFR part 60, appendix B](#) as well as daily and periodic data quality checks in accordance with [40 CFR part 60, appendix F](#), procedure 1.

(3) As specified in [§ 63.8\(c\)\(4\)\(ii\)](#), each CEMS must complete a minimum of one cycle of operation (sampling, analyzing, and data recording) for each successive 15-minute period. You must have at least two data points, with each representing a different 15-minute period, to have a valid hour of data.

(4) The CEMS data must be reduced as specified in [§ 63.8\(g\)\(2\)](#) and recorded in parts per million or parts per billion (as appropriate for the applicable limitation) at 15 percent oxygen or the equivalent CO₂ concentration.

(b) If you are required to install a continuous parameter monitoring system (CPMS) as specified in Table 5 of this subpart, you must install, operate, and maintain each CPMS according to the requirements in [paragraphs \(b\)\(1\) through \(6\)](#) of this section. For an affected source that is complying with the emission limitations and operating limitations on March 9, 2011, the requirements in [paragraph \(b\)](#) of this section are applicable September 6, 2011.

(1) You must prepare a site-specific monitoring plan that addresses the monitoring system design, data collection, and the quality assurance and quality control elements outlined in [paragraphs \(b\)\(1\)\(i\) through \(v\)](#) of this section and in [§ 63.8\(d\)](#). As specified in [§ 63.8\(f\)\(4\)](#), you may request approval of monitoring system quality assurance and quality

control procedures alternative to those specified in [paragraphs \(b\)\(1\) through \(5\)](#) of this section in your site-specific monitoring plan.

(i) The performance criteria and design specifications for the monitoring system equipment, including the sample interface, detector signal analyzer, and data acquisition and calculations;

(ii) Sampling interface (*e.g.*, thermocouple) location such that the monitoring system will provide representative measurements;

(iii) Equipment performance evaluations, system accuracy audits, or other audit procedures;

(iv) Ongoing operation and maintenance procedures in accordance with provisions in [§ 63.8\(c\)\(1\)\(ii\)](#) and [\(c\)\(3\)](#); and

(v) Ongoing reporting and recordkeeping procedures in accordance with provisions in [§ 63.10\(c\)](#), [\(e\)\(1\)](#), and [\(e\)\(2\)\(i\)](#).

(2) You must install, operate, and maintain each CPMS in continuous operation according to the procedures in your site-specific monitoring plan.

(3) The CPMS must collect data at least once every 15 minutes (see also [§ 63.6635](#)).

(4) For a CPMS for measuring temperature range, the temperature sensor must have a minimum tolerance of 2.8 degrees Celsius (5 degrees Fahrenheit) or 1 percent of the measurement range, whichever is larger.

(5) You must conduct the CPMS equipment performance evaluation, system accuracy audits, or other audit procedures specified in your site-specific monitoring plan at least annually.

(6) You must conduct a performance evaluation of each CPMS in accordance with your site-specific monitoring plan.

(c) If you are operating a new or reconstructed stationary RICE which fires landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, you must monitor and record your fuel usage daily with separate fuel meters to measure the volumetric flow rate of each fuel. In addition, you must operate your stationary RICE in a manner which reasonably minimizes HAP emissions.

(d) If you are operating a new or reconstructed emergency 4SLB stationary RICE with a site rating of greater than or equal to 250 and less than or equal to 500 brake HP located at a major source of HAP emissions, you must install a non-resettable hour meter prior to the startup of the engine.

(e) If you own or operate any of the following stationary RICE, you must operate and maintain the stationary RICE and after-treatment control device (if any) according to the manufacturer's emission-related written instructions or develop your own maintenance plan which must provide to the extent practicable for the maintenance and operation of the engine in a manner consistent with good air pollution control practice for minimizing emissions:

(1) An existing stationary RICE with a site rating of less than 100 HP located at a major source of HAP emissions;

(2) An existing emergency or black start stationary RICE with a site rating of less than or equal to 500 HP located at a major source of HAP emissions;

(3) An existing emergency or black start stationary RICE located at an area source of HAP emissions;

(4) An existing non-emergency, non-black start stationary CI RICE with a site rating less than or equal to 300 HP located at an area source of HAP emissions;

(5) An existing non-emergency, non-black start 2SLB stationary RICE located at an area source of HAP emissions;

(6) An existing non-emergency, non-black start stationary RICE located at an area source of HAP emissions which combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis.

(7) An existing non-emergency, non-black start 4SLB stationary RICE with a site rating less than or equal to 500 HP located at an area source of HAP emissions;

(8) An existing non-emergency, non-black start 4SRB stationary RICE with a site rating less than or equal to 500 HP located at an area source of HAP emissions;

(9) An existing, non-emergency, non-black start 4SLB stationary RICE with a site rating greater than 500 HP located at an area source of HAP emissions that is operated 24 hours or less per calendar year; and

(10) An existing, non-emergency, non-black start 4SRB stationary RICE with a site rating greater than 500 HP located at an area source of HAP emissions that is operated 24 hours or less per calendar year.

(f) If you own or operate an existing emergency stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions or an existing emergency stationary RICE located at an area source of HAP emissions, you must install a non-resettable hour meter if one is not already installed.

(g) If you own or operate an existing non-emergency, non-black start CI engine greater than or equal to 300 HP that is not equipped with a closed crankcase ventilation system, you must

comply with either paragraph (g)(1) or [paragraph \(2\)](#) of this section. Owners and operators must follow the manufacturer's specified maintenance requirements for operating and maintaining the open or closed crankcase ventilation systems and replacing the crankcase filters, or can request the Administrator to approve different maintenance requirements that are as protective as manufacturer requirements. Existing CI engines located at area sources in areas of Alaska that meet either [§ 63.6603\(b\)\(1\)](#) or [§ 63.6603\(b\)\(2\)](#) do not have to meet the requirements of this [paragraph \(g\)](#). Existing CI engines located on offshore vessels that meet [§ 63.6603\(c\)](#) do not have to meet the requirements of this [paragraph \(g\)](#).

(1) Install a closed crankcase ventilation system that prevents crankcase emissions from being emitted to the atmosphere, or

(2) Install an open crankcase filtration emission control system that reduces emissions from the crankcase by filtering the exhaust stream to remove oil mist, particulates and metals.

(h) If you operate a new, reconstructed, or existing stationary engine, you must minimize the engine's time spent at idle during startup and minimize the engine's startup time to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes, after which time the emission standards applicable to all times other than startup in Tables 1a, 2a, 2c, and 2d to this subpart apply.

(i) If you own or operate a stationary CI engine that is subject to the work, operation or management practices in items 1 or 2 of Table 2c to this subpart or in items 1 or 4 of Table 2d to this subpart, you have the option of utilizing an oil analysis program in order to extend the specified oil change requirement in Tables 2c and 2d to this subpart. The oil analysis must be performed at the same frequency specified for changing the oil in Table 2c or 2d to this subpart. The analysis program must at a minimum analyze the following three parameters: Total Base Number, viscosity, and percent water content. The condemning limits for these parameters are as follows: Total Base Number is less than 30 percent of the Total Base Number of the oil when new; viscosity of the oil has changed by more than 20 percent from the viscosity of the oil when new; or percent water content (by volume) is greater than 0.5. If all of these condemning limits are not exceeded, the engine owner or operator is not required to change the oil. If any of the limits are exceeded, the engine owner or operator must change the oil within 2 business days of receiving the results of the analysis; if the engine is not in operation when the results of the analysis are received, the engine owner or operator must change the oil within 2 business days or before commencing operation, whichever is later. The owner or operator must keep records of the parameters that are analyzed as part of the program, the results of the analysis, and the oil changes for the engine. The analysis program must be part of the maintenance plan for the engine.

(j) If you own or operate a stationary SI engine that is subject to the work, operation or management practices in items 6, 7, or 8 of Table 2c to this subpart or in items 5, 6, 7, 9, or 11 of Table 2d to this subpart, you have the option of utilizing an oil analysis program in order to extend the specified oil change requirement in Tables 2c and 2d to this subpart. The oil analysis must be performed at the same frequency specified for changing the oil in Table 2c or 2d to this subpart. The analysis program must at a minimum analyze the following three

parameters: Total Acid Number, viscosity, and percent water content. The condemning limits for these parameters are as follows: Total Acid Number increases by more than 3.0 milligrams of potassium hydroxide (KOH) per gram from Total Acid Number of the oil when new; viscosity of the oil has changed by more than 20 percent from the viscosity of the oil when new; or percent water content (by volume) is greater than 0.5. If all of these condemning limits are not exceeded, the engine owner or operator is not required to change the oil. If any of the limits are exceeded, the engine owner or operator must change the oil within 2 business days of receiving the results of the analysis; if the engine is not in operation when the results of the analysis are received, the engine owner or operator must change the oil within 2 business days or before commencing operation, whichever is later. The owner or operator must keep records of the parameters that are analyzed as part of the program, the results of the analysis, and the oil changes for the engine. The analysis program must be part of the maintenance plan for the engine.

[[69 FR 33506](#), June 15, 2004, as amended at [73 FR 3606](#), Jan. 18, 2008; [75 FR 9676](#), Mar. 3, 2010; [75 FR 51589](#), Aug. 20, 2010; [76 FR 12866](#), Mar. 9, 2011; [78 FR 6703](#), Jan. 30, 2013]

§ 63.6630 How do I demonstrate initial compliance with the emission limitations, operating limitations, and other requirements?

- (a) You must demonstrate initial compliance with each emission limitation, operating limitation, and other requirement that applies to you according to Table 5 of this subpart.
- (b) During the initial performance test, you must establish each operating limitation in Tables 1b and 2b of this subpart that applies to you.
- (c) You must submit the Notification of Compliance Status containing the results of the initial compliance demonstration according to the requirements in [§ 63.6645](#).
- (d) Non-emergency 4SRB stationary RICE complying with the requirement to reduce formaldehyde emissions by 76 percent or more can demonstrate initial compliance with the formaldehyde emission limit by testing for THC instead of formaldehyde. The testing must be conducted according to the requirements in Table 4 of this subpart. The average reduction of emissions of THC determined from the performance test must be equal to or greater than 30 percent.
- (e) The initial compliance demonstration required for existing non-emergency 4SLB and 4SRB stationary RICE with a site rating of more than 500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per calendar year must be conducted according to the following requirements:
 - (1) The compliance demonstration must consist of at least three test runs.

(2) Each test run must be of at least 15 minute duration, except that each test conducted using the method in appendix A to this subpart must consist of at least one measurement cycle and include at least 2 minutes of test data phase measurement.

(3) If you are demonstrating compliance with the CO concentration or CO percent reduction requirement, you must measure CO emissions using one of the CO measurement methods specified in Table 4 of this subpart, or using appendix A to this subpart.

(4) If you are demonstrating compliance with the THC percent reduction requirement, you must measure THC emissions using Method 25A, reported as propane, of [40 CFR part 60, appendix A](#).

(5) You must measure O₂ using one of the O₂ measurement methods specified in Table 4 of this subpart. Measurements to determine O₂ concentration must be made at the same time as the measurements for CO or THC concentration.

(6) If you are demonstrating compliance with the CO or THC percent reduction requirement, you must measure CO or THC emissions and O₂ emissions simultaneously at the inlet and outlet of the control device.

[[69 FR 33506](#), June 15, 2004, as amended at [78 FR 6704](#), Jan. 30, 2013]

Continuous Compliance Requirements

§ 63.6635 How do I monitor and collect data to demonstrate continuous compliance?

(a) If you must comply with emission and operating limitations, you must monitor and collect data according to this section.

(b) Except for monitor malfunctions, associated repairs, required performance evaluations, and required quality assurance or control activities, you must monitor continuously at all times that the stationary RICE is operating. A monitoring malfunction is any sudden, infrequent, not reasonably preventable failure of the monitoring to provide valid data. Monitoring failures that are caused in part by poor maintenance or careless operation are not malfunctions.

(c) You may not use data recorded during monitoring malfunctions, associated repairs, and required quality assurance or control activities in data averages and calculations used to report emission or operating levels. You must, however, use all the valid data collected during all other periods.

[[69 FR 33506](#), June 15, 2004, as amended at [76 FR 12867](#), Mar. 9, 2011]

§ 63.6640 How do I demonstrate continuous compliance with the emission limitations, operating limitations, and other requirements?

(a) You must demonstrate continuous compliance with each emission limitation, operating limitation, and other requirements in Tables 1a and 1b, Tables 2a and 2b, Table 2c, and Table 2d to this subpart that apply to you according to methods specified in Table 6 to this subpart.

(b) You must report each instance in which you did not meet each emission limitation or operating limitation in Tables 1a and 1b, Tables 2a and 2b, Table 2c, and Table 2d to this subpart that apply to you. These instances are deviations from the emission and operating limitations in this subpart. These deviations must be reported according to the requirements in [§ 63.6650](#). If you change your catalyst, you must reestablish the values of the operating parameters measured during the initial performance test. When you reestablish the values of your operating parameters, you must also conduct a performance test to demonstrate that you are meeting the required emission limitation applicable to your stationary RICE.

(c) The annual compliance demonstration required for existing non-emergency 4SLB and 4SRB stationary RICE with a site rating of more than 500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per calendar year must be conducted according to the following requirements:

(1) The compliance demonstration must consist of at least one test run.

(2) Each test run must be of at least 15 minute duration, except that each test conducted using the method in appendix A to this subpart must consist of at least one measurement cycle and include at least 2 minutes of test data phase measurement.

(3) If you are demonstrating compliance with the CO concentration or CO percent reduction requirement, you must measure CO emissions using one of the CO measurement methods specified in Table 4 of this subpart, or using appendix A to this subpart.

(4) If you are demonstrating compliance with the THC percent reduction requirement, you must measure THC emissions using Method 25A, reported as propane, of [40 CFR part 60, appendix A](#).

(5) You must measure O₂ using one of the O₂ measurement methods specified in Table 4 of this subpart. Measurements to determine O₂ concentration must be made at the same time as the measurements for CO or THC concentration.

(6) If you are demonstrating compliance with the CO or THC percent reduction requirement, you must measure CO or THC emissions and O₂ emissions simultaneously at the inlet and outlet of the control device.

(7) If the results of the annual compliance demonstration show that the emissions exceed the levels specified in Table 6 of this subpart, the stationary RICE must be shut down as soon as safely possible, and appropriate corrective action must be taken (e.g., repairs, catalyst cleaning, catalyst replacement). The stationary RICE must be retested within 7 days of being restarted and the emissions must meet the levels specified in Table 6 of this subpart. If the retest shows that the emissions continue to exceed the specified levels, the stationary RICE must again be shut down as soon as safely possible, and the stationary RICE may not operate, except for purposes of startup and testing, until the owner/operator demonstrates through testing that the emissions do not exceed the levels specified in Table 6 of this subpart.

(d) For new, reconstructed, and rebuilt stationary RICE, deviations from the emission or operating limitations that occur during the first 200 hours of operation from engine startup (engine burn-in period) are not violations. Rebuilt stationary RICE means a stationary RICE that has been rebuilt as that term is defined in [40 CFR 94.11\(a\)](#).

(e) You must also report each instance in which you did not meet the requirements in Table 8 to this subpart that apply to you. If you own or operate a new or reconstructed stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions (except new or reconstructed 4SLB engines greater than or equal to 250 and less than or equal to 500 brake HP), a new or reconstructed stationary RICE located at an area source of HAP emissions, or any of the following RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you do not need to comply with the requirements in Table 8 to this subpart: An existing 2SLB stationary RICE, an existing 4SLB stationary RICE, an existing emergency stationary RICE, an existing limited use stationary RICE, or an existing stationary RICE which fires landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis. If you own or operate any of the following RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you do not need to comply with the requirements in Table 8 to this subpart, except for the initial notification requirements: a new or reconstructed stationary RICE that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, a new or reconstructed emergency stationary RICE, or a new or reconstructed limited use stationary RICE.

(f) If you own or operate an emergency stationary RICE, you must operate the emergency stationary RICE according to the requirements in [paragraphs \(f\)\(1\) through \(4\)](#) of this section. In order for the engine to be considered an emergency stationary RICE under this subpart, any operation other than emergency operation, maintenance and testing, emergency demand response, and operation in non-emergency situations for 50 hours per year, as described in [paragraphs \(f\)\(1\) through \(4\)](#) of this section, is prohibited. If you do not operate the engine according to the requirements in [paragraphs \(f\)\(1\) through \(4\)](#) of this section, the engine will not be considered an emergency engine under this subpart and must meet all requirements for non-emergency engines.

(1) There is no time limit on the use of emergency stationary RICE in emergency situations.

(2) You may operate your emergency stationary RICE for any combination of the purposes specified in [paragraphs \(f\)\(2\)\(i\) through \(iii\)](#) of this section for a maximum of 100 hours per calendar year. Any operation for non-emergency situations as allowed by [paragraphs \(f\)\(3\) and \(4\)](#) of this section counts as part of the 100 hours per calendar year allowed by this [paragraph \(f\)\(2\)](#).

(i) Emergency stationary RICE may be operated for maintenance checks and readiness testing, provided that the tests are recommended by federal, state or local government, the manufacturer, the vendor, the regional transmission organization or equivalent balancing authority and transmission operator, or the insurance company associated with the engine. The owner or operator may petition the Administrator for approval of additional hours to be used for maintenance checks and readiness testing, but a petition is not required if the owner or operator maintains records indicating that federal, state, or local standards require maintenance and testing of emergency RICE beyond 100 hours per calendar year.

(ii) Emergency stationary RICE may be operated for emergency demand response for periods in which the Reliability Coordinator under the North American Electric Reliability Corporation (NERC) Reliability Standard EOP-002-3, Capacity and Energy Emergencies (incorporated by reference, see [§ 63.14](#)), or other authorized entity as determined by the Reliability Coordinator, has declared an Energy Emergency Alert Level 2 as defined in the NERC Reliability Standard EOP-002-3.

(iii) Emergency stationary RICE may be operated for periods where there is a deviation of voltage or frequency of 5 percent or greater below standard voltage or frequency.

(3) Emergency stationary RICE located at major sources of HAP may be operated for up to 50 hours per calendar year in non-emergency situations. The 50 hours of operation in non-emergency situations are counted as part of the 100 hours per calendar year for maintenance and testing and emergency demand response provided in [paragraph \(f\)\(2\)](#) of this section. The 50 hours per year for non-emergency situations cannot be used for peak shaving or non-emergency demand response, or to generate income for a facility to supply power to an electric grid or otherwise supply power as part of a financial arrangement with another entity.

(4) Emergency stationary RICE located at area sources of HAP may be operated for up to 50 hours per calendar year in non-emergency situations. The 50 hours of operation in non-emergency situations are counted as part of the 100 hours per calendar year for maintenance and testing and emergency demand response provided in [paragraph \(f\)\(2\)](#) of this section. Except as provided in [paragraphs \(f\)\(4\)\(i\) and \(ii\)](#) of this section, the 50 hours per year for non-emergency situations cannot be used for peak shaving or non-emergency demand response, or to generate income for a facility to an electric grid or otherwise supply power as part of a financial arrangement with another entity.

(i) Prior to May 3, 2014, the 50 hours per year for non-emergency situations can be used for peak shaving or non-emergency demand response to generate income for a facility, or to otherwise supply power as part of a financial arrangement with another entity if the engine is operated as part of a peak shaving (load management program) with the local

distribution system operator and the power is provided only to the facility itself or to support the local distribution system.

(ii) The 50 hours per year for non-emergency situations can be used to supply power as part of a financial arrangement with another entity if all of the following conditions are met:

(A) The engine is dispatched by the local balancing authority or local transmission and distribution system operator.

(B) The dispatch is intended to mitigate local transmission and/or distribution limitations so as to avert potential voltage collapse or line overloads that could lead to the interruption of power supply in a local area or region.

(C) The dispatch follows reliability, emergency operation or similar protocols that follow specific NERC, regional, state, public utility commission or local standards or guidelines.

(D) The power is provided only to the facility itself or to support the local transmission and distribution system.

(E) The owner or operator identifies and records the entity that dispatches the engine and the specific NERC, regional, state, public utility commission or local standards or guidelines that are being followed for dispatching the engine. The local balancing authority or local transmission and distribution system operator may keep these records on behalf of the engine owner or operator.

[[69 FR 33506](#), June 15, 2004, as amended at [71 FR 20467](#), Apr. 20, 2006; [73 FR 3606](#), Jan. 18, 2008; [75 FR 9676](#), Mar. 3, 2010; [75 FR 51591](#), Aug. 20, 2010; [78 FR 6704](#), Jan. 30, 2013]

Notifications, Reports, and Records

§ 63.6645 What notifications must I submit and when?

(a) You must submit all of the notifications in [§§ 63.7\(b\)](#) and [\(c\)](#), [63.8\(e\)](#), [\(f\)\(4\)](#) and [\(f\)\(6\)](#), [63.9\(b\)](#) through [\(e\)](#), and [\(g\)](#) and [\(h\)](#) that apply to you by the dates specified if you own or operate any of the following;

(1) An existing stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions.

(2) An existing stationary RICE located at an area source of HAP emissions.

(3) A stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions.

(4) A new or reconstructed 4SLB stationary RICE with a site rating of greater than or equal to 250 HP located at a major source of HAP emissions.

(5) This requirement does not apply if you own or operate an existing stationary RICE less than 100 HP, an existing stationary emergency RICE, or an existing stationary RICE that is not subject to any numerical emission standards.

(b) As specified in [§ 63.9\(b\)\(2\)](#), if you start up your stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions before the effective date of this subpart, you must submit an Initial Notification not later than December 13, 2004, or no later than 120 days after the source becomes subject to this subpart, whichever is later.

(c) If you start up your new or reconstructed stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions on or after August 16, 2004, you must submit an Initial Notification not later than 120 days after you become subject to this subpart.

(d) As specified in [§ 63.9\(b\)\(2\)](#), if you start up your stationary RICE with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions before the effective date of this subpart and you are required to submit an initial notification, you must submit an Initial Notification not later than July 16, 2008, or no later than 120 days after the source becomes subject to this subpart, whichever is later.

(e) If you start up your new or reconstructed stationary RICE with a site rating of equal to or less than 500 brake HP located at a major source of HAP emissions on or after March 18, 2008 and you are required to submit an initial notification, you must submit an Initial Notification not later than 120 days after you become subject to this subpart.

(f) If you are required to submit an Initial Notification but are otherwise not affected by the requirements of this subpart, in accordance with [§ 63.6590\(b\)](#), your notification should include the information in [§ 63.9\(b\)\(2\)\(i\)](#) through [\(v\)](#), and a statement that your stationary RICE has no additional requirements and explain the basis of the exclusion (for example, that it operates exclusively as an emergency stationary RICE if it has a site rating of more than 500 brake HP located at a major source of HAP emissions).

(g) If you are required to conduct a performance test, you must submit a Notification of Intent to conduct a performance test at least 60 days before the performance test is scheduled to begin as required in [§ 63.7\(b\)\(1\)](#).

(h) If you are required to conduct a performance test or other initial compliance demonstration as specified in Tables 4 and 5 to this subpart, you must submit a Notification of Compliance Status according to [§ 63.9\(h\)\(2\)\(ii\)](#).

(1) For each initial compliance demonstration required in Table 5 to this subpart that does not include a performance test, you must submit the Notification of Compliance Status before the close of business on the 30th day following the completion of the initial compliance demonstration.

(2) For each initial compliance demonstration required in Table 5 to this subpart that includes a performance test conducted according to the requirements in Table 3 to this subpart, you must submit the Notification of Compliance Status, including the performance test results, before the close of business on the 60th day following the completion of the performance test according to [§ 63.10\(d\)\(2\)](#).

(i) If you own or operate an existing non-emergency CI RICE with a site rating of more than 300 HP located at an area source of HAP emissions that is certified to the Tier 1 or Tier 2 emission standards in Table 1 of [40 CFR 89.112](#) and subject to an enforceable state or local standard requiring engine replacement and you intend to meet management practices rather than emission limits, as specified in [§ 63.6603\(d\)](#), you must submit a notification by March 3, 2013, stating that you intend to use the provision in [§ 63.6603\(d\)](#) and identifying the state or local regulation that the engine is subject to.

[[73 FR 3606](#), Jan. 18, 2008, as amended at [75 FR 9677](#), Mar. 3, 2010; [75 FR 51591](#), Aug. 20, 2010; [78 FR 6705](#), Jan. 30, 2013; [85 FR 73912](#), Nov. 19, 2020]

§ 63.6650 What reports must I submit and when?

(a) You must submit each report in Table 7 of this subpart that applies to you.

(b) Unless the Administrator has approved a different schedule for submission of reports under [§ 63.10\(a\)](#), you must submit each report by the date in Table 7 of this subpart and according to the requirements in [paragraphs \(b\)\(1\) through \(b\)\(9\)](#) of this section.

(1) For semiannual Compliance reports, the first Compliance report must cover the period beginning on the compliance date that is specified for your affected source in [§ 63.6595](#) and ending on June 30 or December 31, whichever date is the first date following the end of the first calendar half after the compliance date that is specified for your source in [§ 63.6595](#).

(2) For semiannual Compliance reports, the first Compliance report must be postmarked or delivered no later than July 31 or January 31, whichever date follows the end of the first calendar half after the compliance date that is specified for your affected source in [§ 63.6595](#).

(3) For semiannual Compliance reports, each subsequent Compliance report must cover the semiannual reporting period from January 1 through June 30 or the semiannual reporting period from July 1 through December 31.

(4) For semiannual Compliance reports, each subsequent Compliance report must be postmarked or delivered no later than July 31 or January 31, whichever date is the first date following the end of the semiannual reporting period.

(5) For each stationary RICE that is subject to permitting regulations pursuant to [40 CFR part 70](#) or [71](#), and if the permitting authority has established dates for submitting semiannual reports pursuant to [40 CFR 70.6\(a\)\(3\)\(iii\)\(A\)](#) or [40 CFR 71.6 \(a\)\(3\)\(iii\)\(A\)](#), you may submit the first and subsequent Compliance reports according to the dates the permitting authority

has established instead of according to the dates in [paragraphs \(b\)\(1\)](#) through [\(b\)\(4\)](#) of this section.

(6) For annual Compliance reports, the first Compliance report must cover the period beginning on the compliance date that is specified for your affected source in [§ 63.6595](#) and ending on December 31.

(7) For annual Compliance reports, the first Compliance report must be postmarked or delivered no later than January 31 following the end of the first calendar year after the compliance date that is specified for your affected source in [§ 63.6595](#).

(8) For annual Compliance reports, each subsequent Compliance report must cover the annual reporting period from January 1 through December 31.

(9) For annual Compliance reports, each subsequent Compliance report must be postmarked or delivered no later than January 31.

(c) The Compliance report must contain the information in [paragraphs \(c\)\(1\)](#) through [\(6\)](#) of this section.

(1) Company name and address.

(2) Statement by a responsible official, with that official's name, title, and signature, certifying the accuracy of the content of the report.

(3) Date of report and beginning and ending dates of the reporting period.

(4) If you had a malfunction during the reporting period, the compliance report must include the number, duration, and a brief description for each type of malfunction which occurred during the reporting period and which caused or may have caused any applicable emission limitation to be exceeded. The report must also include a description of actions taken by an owner or operator during a malfunction of an affected source to minimize emissions in accordance with [§ 63.6605\(b\)](#), including actions taken to correct a malfunction.

(5) If there are no deviations from any emission or operating limitations that apply to you, a statement that there were no deviations from the emission or operating limitations during the reporting period.

(6) If there were no periods during which the continuous monitoring system (CMS), including CEMS and CPMS, was out-of-control, as specified in [§ 63.8\(c\)\(7\)](#), a statement that there were no periods during which the CMS was out-of-control during the reporting period.

(d) For each deviation from an emission or operating limitation that occurs for a stationary RICE where you are not using a CMS to comply with the emission or operating limitations in this subpart, the Compliance report must contain the information in [paragraphs \(c\)\(1\)](#) through [\(4\)](#) of this section and the information in [paragraphs \(d\)\(1\)](#) and [\(2\)](#) of this section.

(1) The total operating time of the stationary RICE at which the deviation occurred during the reporting period.

(2) Information on the number, duration, and cause of deviations (including unknown cause, if applicable), as applicable, and the corrective action taken.

(e) For each deviation from an emission or operating limitation occurring for a stationary RICE where you are using a CMS to comply with the emission and operating limitations in this subpart, you must include information in [paragraphs \(c\)\(1\) through \(4\)](#) and [\(e\)\(1\) through \(12\)](#) of this section.

(1) The date and time that each malfunction started and stopped.

(2) The date, time, and duration that each CMS was inoperative, except for zero (low-level) and high-level checks.

(3) The date, time, and duration that each CMS was out-of-control, including the information in [§ 63.8\(c\)\(8\)](#).

(4) The date and time that each deviation started and stopped, and whether each deviation occurred during a period of malfunction or during another period.

(5) A summary of the total duration of the deviation during the reporting period, and the total duration as a percent of the total source operating time during that reporting period.

(6) A breakdown of the total duration of the deviations during the reporting period into those that are due to control equipment problems, process problems, other known causes, and other unknown causes.

(7) A summary of the total duration of CMS downtime during the reporting period, and the total duration of CMS downtime as a percent of the total operating time of the stationary RICE at which the CMS downtime occurred during that reporting period.

(8) An identification of each parameter and pollutant (CO or formaldehyde) that was monitored at the stationary RICE.

(9) A brief description of the stationary RICE.

(10) A brief description of the CMS.

(11) The date of the latest CMS certification or audit.

(12) A description of any changes in CMS, processes, or controls since the last reporting period.

(f) Each affected source that has obtained a title V operating permit pursuant to [40 CFR part 70](#) or [71](#) must report all deviations as defined in this subpart in the semiannual monitoring report required by [40 CFR 70.6\(a\)\(3\)\(iii\)\(A\)](#) or [40 CFR 71.6\(a\)\(3\)\(iii\)\(A\)](#). If an affected source submits a Compliance report pursuant to Table 7 of this subpart along with, or as part of, the semiannual monitoring report required by [40 CFR 70.6\(a\)\(3\)\(iii\)\(A\)](#) or [40 CFR 71.6\(a\)\(3\)\(iii\)\(A\)](#), and the Compliance report includes all required information concerning deviations from any emission or operating limitation in this subpart, submission of the Compliance report shall be deemed to satisfy any obligation to report the same deviations in the semiannual monitoring report. However, submission of a Compliance report shall not otherwise affect any obligation the affected source may have to report deviations from permit requirements to the permit authority.

(g) If you are operating as a new or reconstructed stationary RICE which fires landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, you must submit an annual report according to Table 7 of this subpart by the date specified unless the Administrator has approved a different schedule, according to the information described in [paragraphs \(b\)\(1\)](#) through [\(b\)\(5\)](#) of this section. You must report the data specified in [\(g\)\(1\)](#) through [\(g\)\(3\)](#) of this section.

(1) Fuel flow rate of each fuel and the heating values that were used in your calculations. You must also demonstrate that the percentage of heat input provided by landfill gas or digester gas is equivalent to 10 percent or more of the total fuel consumption on an annual basis.

(2) The operating limits provided in your federally enforceable permit, and any deviations from these limits.

(3) Any problems or errors suspected with the meters.

(h) If you own or operate an emergency stationary RICE with a site rating of more than 100 brake HP that operates or is contractually obligated to be available for more than 15 hours per calendar year for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#) or that operates for the purpose specified in [§ 63.6640\(f\)\(4\)\(ii\)](#), you must submit an annual report according to the requirements in [paragraphs \(h\)\(1\)](#) through [\(3\)](#) of this section.

(1) The report must contain the following information:

(i) Company name and address where the engine is located.

(ii) Date of the report and beginning and ending dates of the reporting period.

(iii) Engine site rating and model year.

(iv) Latitude and longitude of the engine in decimal degrees reported to the fifth decimal place.

(v) Hours operated for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#), including the date, start time, and end time for engine operation for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#).

(vi) Number of hours the engine is contractually obligated to be available for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#).

(vii) Hours spent for operation for the purpose specified in [§ 63.6640\(f\)\(4\)\(ii\)](#), including the date, start time, and end time for engine operation for the purposes specified in [§ 63.6640\(f\)\(4\)\(ii\)](#). The report must also identify the entity that dispatched the engine and the situation that necessitated the dispatch of the engine.

(viii) If there were no deviations from the fuel requirements in [§ 63.6604](#) that apply to the engine (if any), a statement that there were no deviations from the fuel requirements during the reporting period.

(ix) If there were deviations from the fuel requirements in [§ 63.6604](#) that apply to the engine (if any), information on the number, duration, and cause of deviations, and the corrective action taken.

(2) The first annual report must cover the calendar year 2015 and must be submitted no later than March 31, 2016. Subsequent annual reports for each calendar year must be submitted no later than March 31 of the following calendar year.

(3) The annual report must be submitted electronically using the subpart specific reporting form in the Compliance and Emissions Data Reporting Interface (CEDRI) that is accessed through EPA's Central Data Exchange (CDX) (www.epa.gov/cdx). However, if the reporting form specific to this subpart is not available in CEDRI at the time that the report is due, the written report must be submitted to the Administrator at the appropriate address listed in [§ 63.13](#).

[[69 FR 33506](#), June 15, 2004, as amended at [75 FR 9677](#), Mar. 3, 2010; [78 FR 6705](#), Jan. 30, 2013]

§ 63.6655 What records must I keep?

(a) If you must comply with the emission and operating limitations, you must keep the records described in [paragraphs \(a\)\(1\) through \(a\)\(5\)](#), [\(b\)\(1\) through \(b\)\(3\)](#) and [\(c\)](#) of this section.

(1) A copy of each notification and report that you submitted to comply with this subpart, including all documentation supporting any Initial Notification or Notification of Compliance Status that you submitted, according to the requirement in [§ 63.10\(b\)\(2\)\(xiv\)](#).

(2) Records of the occurrence and duration of each malfunction of operation (*i.e.*, process equipment) or the air pollution control and monitoring equipment.

(3) Records of performance tests and performance evaluations as required in [§ 63.10\(b\)\(2\)\(viii\)](#).

(4) Records of all required maintenance performed on the air pollution control and monitoring equipment.

(5) Records of actions taken during periods of malfunction to minimize emissions in accordance with [§ 63.6605\(b\)](#), including corrective actions to restore malfunctioning process and air pollution control and monitoring equipment to its normal or usual manner of operation.

(b) For each CEMS or CPMS, you must keep the records listed in [paragraphs \(b\)\(1\)](#) through [\(3\)](#) of this section.

(1) Records described in [§ 63.10\(b\)\(2\)\(vi\)](#) through [\(xi\)](#).

(2) Previous (*i.e.*, superseded) versions of the performance evaluation plan as required in [§ 63.8\(d\)\(3\)](#).

(3) Requests for alternatives to the relative accuracy test for CEMS or CPMS as required in [§ 63.8\(f\)\(6\)\(i\)](#), if applicable.

(c) If you are operating a new or reconstructed stationary RICE which fires landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, you must keep the records of your daily fuel usage monitors.

(d) You must keep the records required in Table 6 of this subpart to show continuous compliance with each emission or operating limitation that applies to you.

(e) You must keep records of the maintenance conducted on the stationary RICE in order to demonstrate that you operated and maintained the stationary RICE and after-treatment control device (if any) according to your own maintenance plan if you own or operate any of the following stationary RICE;

(1) An existing stationary RICE with a site rating of less than 100 brake HP located at a major source of HAP emissions.

(2) An existing stationary emergency RICE.

(3) An existing stationary RICE located at an area source of HAP emissions subject to management practices as shown in Table 2d to this subpart.

(f) If you own or operate any of the stationary RICE in [paragraphs \(f\)\(1\)](#) through [\(2\)](#) of this section, you must keep records of the hours of operation of the engine that is recorded through the non-resettable hour meter. The owner or operator must document how many hours are spent for emergency operation, including what classified the operation as emergency and how

many hours are spent for non-emergency operation. If the engine is used for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) or [\(iii\)](#) or [§ 63.6640\(f\)\(4\)\(ii\)](#), the owner or operator must keep records of the notification of the emergency situation, and the date, start time, and end time of engine operation for these purposes.

(1) An existing emergency stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions that does not meet the standards applicable to non-emergency engines.

(2) An existing emergency stationary RICE located at an area source of HAP emissions that does not meet the standards applicable to non-emergency engines.

[[69 FR 33506](#), June 15, 2004, as amended at [75 FR 9678](#), Mar. 3, 2010; [75 FR 51592](#), Aug. 20, 2010; [78 FR 6706](#), Jan. 30, 2013]

§ 63.6660 In what form and how long must I keep my records?

(a) Your records must be in a form suitable and readily available for expeditious review according to [§ 63.10\(b\)\(1\)](#).

(b) As specified in [§ 63.10\(b\)\(1\)](#), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record.

(c) You must keep each record readily accessible in hard copy or electronic form for at least 5 years after the date of each occurrence, measurement, maintenance, corrective action, report, or record, according to [§ 63.10\(b\)\(1\)](#).

[[69 FR 33506](#), June 15, 2004, as amended at [75 FR 9678](#), Mar. 3, 2010]

Other Requirements and Information

§ 63.6665 What parts of the General Provisions apply to me?

Table 8 to this subpart shows which parts of the General Provisions in [§§ 63.1](#) through [63.15](#) apply to you. If you own or operate a new or reconstructed stationary RICE with a site rating of less than or equal to 500 brake HP located at a major source of HAP emissions (except new or reconstructed 4SLB engines greater than or equal to 250 and less than or equal to 500 brake HP), a new or reconstructed stationary RICE located at an area source of HAP emissions, or any of the following RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you do not need to comply with any of the requirements of the General Provisions specified in Table 8: An existing 2SLB stationary RICE, an existing 4SLB stationary RICE, an existing stationary RICE that combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, an existing emergency stationary RICE, or an existing limited use stationary RICE. If you own or operate any of the following RICE with a site rating

of more than 500 brake HP located at a major source of HAP emissions, you do not need to comply with the requirements in the General Provisions specified in Table 8 except for the initial notification requirements: A new stationary RICE that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, a new emergency stationary RICE, or a new limited use stationary RICE.

[[75 FR 9678](#), Mar. 3, 2010]

§ 63.6670 Who implements and enforces this subpart?

(a) This subpart is implemented and enforced by the U.S. EPA, or a delegated authority such as your State, local, or tribal agency. If the U.S. EPA Administrator has delegated authority to your State, local, or tribal agency, then that agency (as well as the U.S. EPA) has the authority to implement and enforce this subpart. You should contact your U.S. EPA Regional Office to find out whether this subpart is delegated to your State, local, or tribal agency.

(b) In delegating implementation and enforcement authority of this subpart to a State, local, or tribal agency under [40 CFR part 63, subpart E](#), the authorities contained in [paragraph \(c\)](#) of this section are retained by the Administrator of the U.S. EPA and are not transferred to the State, local, or tribal agency.

(c) The authorities that will not be delegated to State, local, or tribal agencies are:

(1) Approval of alternatives to the non-opacity emission limitations and operating limitations in [§ 63.6600](#) under [§ 63.6\(g\)](#).

(2) Approval of major alternatives to test methods under [§ 63.7\(e\)\(2\)\(ii\)](#) and [\(f\)](#) and as defined in [§ 63.90](#).

(3) Approval of major alternatives to monitoring under [§ 63.8\(f\)](#) and as defined in [§ 63.90](#).

(4) Approval of major alternatives to recordkeeping and reporting under [§ 63.10\(f\)](#) and as defined in [§ 63.90](#).

(5) Approval of a performance test which was conducted prior to the effective date of the rule, as specified in [§ 63.6610\(b\)](#).

§ 63.6675 What definitions apply to this subpart?

Terms used in this subpart are defined in the Clean Air Act (CAA); in [40 CFR 63.2](#), the General Provisions of this part; and in this section as follows:

Alaska Railbelt Grid means the service areas of the six regulated public utilities that extend from Fairbanks to Anchorage and the Kenai Peninsula. These utilities are Golden Valley Electric

Association; Chugach Electric Association; Matanuska Electric Association; Homer Electric Association; Anchorage Municipal Light & Power; and the City of Seward Electric System.

Area source means any stationary source of HAP that is not a major source as defined in part 63.

Associated equipment as used in this subpart and as referred to in section 112(n)(4) of the CAA, means equipment associated with an oil or natural gas exploration or production well, and includes all equipment from the well bore to the point of custody transfer, except glycol dehydration units, storage vessels with potential for flash emissions, combustion turbines, and stationary RICE.

Backup power for renewable energy means an engine that provides backup power to a facility that generates electricity from renewable energy resources, as that term is defined in Alaska Statute 42.45.045(1)(5) (incorporated by reference, see [§ 63.14](#)).

Black start engine means an engine whose only purpose is to start up a combustion turbine.

CAA means the Clean Air Act ([42 U.S.C. 7401](#) *et seq.*, as amended by Public Law 101-549, 104 Stat. 2399).

Commercial emergency stationary RICE means an emergency stationary RICE used in commercial establishments such as office buildings, hotels, stores, telecommunications facilities, restaurants, financial institutions such as banks, doctor's offices, and sports and performing arts facilities.

Compression ignition means relating to a type of stationary internal combustion engine that is not a spark ignition engine.

Custody transfer means the transfer of hydrocarbon liquids or natural gas: After processing and/or treatment in the producing operations, or from storage vessels or automatic transfer facilities or other such equipment, including product loading racks, to pipelines or any other forms of transportation. For the purposes of this subpart, the point at which such liquids or natural gas enters a natural gas processing plant is a point of custody transfer.

Deviation means any instance in which an affected source subject to this subpart, or an owner or operator of such a source:

- (1) Fails to meet any requirement or obligation established by this subpart, including but not limited to any emission limitation or operating limitation;
- (2) Fails to meet any term or condition that is adopted to implement an applicable requirement in this subpart and that is included in the operating permit for any affected source required to obtain such a permit; or
- (3) Fails to meet any emission limitation or operating limitation in this subpart during malfunction, regardless of whether or not such failure is permitted by this subpart.

(4) Fails to satisfy the general duty to minimize emissions established by [§ 63.6\(e\)\(1\)\(i\)](#).

Diesel engine means any stationary RICE in which a high boiling point liquid fuel injected into the combustion chamber ignites when the air charge has been compressed to a temperature sufficiently high for auto-ignition. This process is also known as compression ignition.

Diesel fuel means any liquid obtained from the distillation of petroleum with a boiling point of approximately 150 to 360 degrees Celsius. One commonly used form is fuel oil number 2. Diesel fuel also includes any non-distillate fuel with comparable physical and chemical properties (*e.g.* biodiesel) that is suitable for use in compression ignition engines.

Digester gas means any gaseous by-product of wastewater treatment typically formed through the anaerobic decomposition of organic waste materials and composed principally of methane and CO₂.

Dual-fuel engine means any stationary RICE in which a liquid fuel (typically diesel fuel) is used for compression ignition and gaseous fuel (typically natural gas) is used as the primary fuel.

Emergency stationary RICE means any stationary reciprocating internal combustion engine that meets all of the criteria in paragraphs (1) through (3) of this definition. All emergency stationary RICE must comply with the requirements specified in [§ 63.6640\(f\)](#) in order to be considered emergency stationary RICE. If the engine does not comply with the requirements specified in [§ 63.6640\(f\)](#), then it is not considered to be an emergency stationary RICE under this subpart.

(1) The stationary RICE is operated to provide electrical power or mechanical work during an emergency situation. Examples include stationary RICE used to produce power for critical networks or equipment (including power supplied to portions of a facility) when electric power from the local utility (or the normal power source, if the facility runs on its own power production) is interrupted, or stationary RICE used to pump water in the case of fire or flood, etc.

(2) The stationary RICE is operated under limited circumstances for situations not included in paragraph (1) of this definition, as specified in [§ 63.6640\(f\)](#).

(3) The stationary RICE operates as part of a financial arrangement with another entity in situations not included in paragraph (1) of this definition only as allowed in [§ 63.6640\(f\)\(2\)\(ii\)](#) or [\(iii\)](#) and [§ 63.6640\(f\)\(4\)\(i\)](#) or [\(ii\)](#).

Engine startup means the time from initial start until applied load and engine and associated equipment reaches steady state or normal operation. For stationary engine with catalytic controls, engine startup means the time from initial start until applied load and engine and associated equipment, including the catalyst, reaches steady state or normal operation.

Four-stroke engine means any type of engine which completes the power cycle in two crankshaft revolutions, with intake and compression strokes in the first revolution and power and exhaust strokes in the second revolution.

Gaseous fuel means a material used for combustion which is in the gaseous state at standard atmospheric temperature and pressure conditions.

Gasoline means any fuel sold in any State for use in motor vehicles and motor vehicle engines, or nonroad or stationary engines, and commonly or commercially known or sold as gasoline.

Glycol dehydration unit means a device in which a liquid glycol (including, but not limited to, ethylene glycol, diethylene glycol, or triethylene glycol) absorbent directly contacts a natural gas stream and absorbs water in a contact tower or absorption column (absorber). The glycol contacts and absorbs water vapor and other gas stream constituents from the natural gas and becomes “rich” glycol. This glycol is then regenerated in the glycol dehydration unit reboiler. The “lean” glycol is then recycled.

Hazardous air pollutants (HAP) means any air pollutants listed in or pursuant to section 112(b) of the CAA.

Institutional emergency stationary RICE means an emergency stationary RICE used in institutional establishments such as medical centers, nursing homes, research centers, institutions of higher education, correctional facilities, elementary and secondary schools, libraries, religious establishments, police stations, and fire stations.

ISO standard day conditions means 288 degrees Kelvin (15 degrees Celsius), 60 percent relative humidity and 101.3 kilopascals pressure.

Landfill gas means a gaseous by-product of the land application of municipal refuse typically formed through the anaerobic decomposition of waste materials and composed principally of methane and CO₂.

Lean burn engine means any two-stroke or four-stroke spark ignited engine that does not meet the definition of a rich burn engine.

Limited use stationary RICE means any stationary RICE that operates less than 100 hours per year.

Liquefied petroleum gas means any liquefied hydrocarbon gas obtained as a by-product in petroleum refining of natural gas production.

Liquid fuel means any fuel in liquid form at standard temperature and pressure, including but not limited to diesel, residual/crude oil, kerosene/naphtha (jet fuel), and gasoline.

Major Source, as used in this subpart, shall have the same meaning as in [§ 63.2](#), except that:

- (1) Emissions from any oil or gas exploration or production well (with its associated equipment (as defined in this section)) and emissions from any pipeline compressor station or pump station shall not be aggregated with emissions from other similar units, to determine whether

such emission points or stations are major sources, even when emission points are in a contiguous area or under common control;

(2) For oil and gas production facilities, emissions from processes, operations, or equipment that are not part of the same oil and gas production facility, as defined in [§ 63.1271](#) of [subpart HHH of this part](#), shall not be aggregated;

(3) For production field facilities, only HAP emissions from glycol dehydration units, storage vessel with the potential for flash emissions, combustion turbines and reciprocating internal combustion engines shall be aggregated for a major source determination; and

(4) Emissions from processes, operations, and equipment that are not part of the same natural gas transmission and storage facility, as defined in [§ 63.1271](#) of [subpart HHH of this part](#), shall not be aggregated.

Malfunction means any sudden, infrequent, and not reasonably preventable failure of air pollution control equipment, process equipment, or a process to operate in a normal or usual manner which causes, or has the potential to cause, the emission limitations in an applicable standard to be exceeded. Failures that are caused in part by poor maintenance or careless operation are not malfunctions.

Natural gas means a naturally occurring mixture of hydrocarbon and non-hydrocarbon gases found in geologic formations beneath the Earth's surface, of which the principal constituent is methane. Natural gas may be field or pipeline quality.

Non-selective catalytic reduction (NSCR) means an add-on catalytic nitrogen oxides (NO_x) control device for rich burn engines that, in a two-step reaction, promotes the conversion of excess oxygen, NO_x, CO, and volatile organic compounds (VOC) into CO₂, nitrogen, and water.

Oil and gas production facility as used in this subpart means any grouping of equipment where hydrocarbon liquids are processed, upgraded (*i.e.*, remove impurities or other constituents to meet contract specifications), or stored prior to the point of custody transfer; or where natural gas is processed, upgraded, or stored prior to entering the natural gas transmission and storage source category. For purposes of a major source determination, facility (including a building, structure, or installation) means oil and natural gas production and processing equipment that is located within the boundaries of an individual surface site as defined in this section. Equipment that is part of a facility will typically be located within close proximity to other equipment located at the same facility. Pieces of production equipment or groupings of equipment located on different oil and gas leases, mineral fee tracts, lease tracts, subsurface or surface unit areas, surface fee tracts, surface lease tracts, or separate surface sites, whether or not connected by a road, waterway, power line or pipeline, shall not be considered part of the same facility. Examples of facilities in the oil and natural gas production source category include, but are not limited to, well sites, satellite tank batteries, central tank batteries, a compressor station that transports natural gas to a natural gas processing plant, and natural gas processing plants.

Oxidation catalyst means an add-on catalytic control device that controls CO and VOC by oxidation.

Peaking unit or engine means any standby engine intended for use during periods of high demand that are not emergencies.

Percent load means the fractional power of an engine compared to its maximum manufacturer's design capacity at engine site conditions. Percent load may range between 0 percent to above 100 percent.

Potential to emit means the maximum capacity of a stationary source to emit a pollutant under its physical and operational design. Any physical or operational limitation on the capacity of the stationary source to emit a pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored, or processed, shall be treated as part of its design if the limitation or the effect it would have on emissions is federally enforceable. For oil and natural gas production facilities subject to [subpart HH of this part](#), the potential to emit provisions in [§ 63.760\(a\)](#) may be used. For natural gas transmission and storage facilities subject to [subpart HHH of this part](#), the maximum annual facility gas throughput for storage facilities may be determined according to [§ 63.1270\(a\)\(1\)](#) and the maximum annual throughput for transmission facilities may be determined according to [§ 63.1270\(a\)\(2\)](#).

Production field facility means those oil and gas production facilities located prior to the point of custody transfer.

Production well means any hole drilled in the earth from which crude oil, condensate, or field natural gas is extracted.

Propane means a colorless gas derived from petroleum and natural gas, with the molecular structure C₃H₈.

Remote stationary RICE means stationary RICE meeting any of the following criteria:

- (1) Stationary RICE located in an offshore area that is beyond the line of ordinary low water along that portion of the coast of the United States that is in direct contact with the open seas and beyond the line marking the seaward limit of inland waters.
- (2) Stationary RICE located on a pipeline segment that meets both of the criteria in paragraphs (2)(i) and (ii) of this definition.
 - (i) A pipeline segment with 10 or fewer buildings intended for human occupancy and no buildings with four or more stories within 220 yards (200 meters) on either side of the centerline of any continuous 1-mile (1.6 kilometers) length of pipeline. Each separate dwelling unit in a multiple dwelling unit building is counted as a separate building intended for human occupancy.

(ii) The pipeline segment does not lie within 100 yards (91 meters) of either a building or a small, well-defined outside area (such as a playground, recreation area, outdoor theater, or other place of public assembly) that is occupied by 20 or more persons on at least 5 days a week for 10 weeks in any 12-month period. The days and weeks need not be consecutive. The building or area is considered occupied for a full day if it is occupied for any portion of the day.

(iii) For purposes of this [paragraph \(2\)](#), the term pipeline segment means all parts of those physical facilities through which gas moves in transportation, including but not limited to pipe, valves, and other appurtenance attached to pipe, compressor units, metering stations, regulator stations, delivery stations, holders, and fabricated assemblies. Stationary RICE located within 50 yards (46 meters) of the pipeline segment providing power for equipment on a pipeline segment are part of the pipeline segment. Transportation of gas means the gathering, transmission, or distribution of gas by pipeline, or the storage of gas. A building is intended for human occupancy if its primary use is for a purpose involving the presence of humans.

(3) Stationary RICE that are not located on gas pipelines and that have 5 or fewer buildings intended for human occupancy and no buildings with four or more stories within a 0.25 mile radius around the engine. A building is intended for human occupancy if its primary use is for a purpose involving the presence of humans.

Residential emergency stationary RICE means an emergency stationary RICE used in residential establishments such as homes or apartment buildings.

Responsible official means responsible official as defined in [40 CFR 70.2](#).

Rich burn engine means any four-stroke spark ignited engine where the manufacturer's recommended operating air/fuel ratio divided by the stoichiometric air/fuel ratio at full load conditions is less than or equal to 1.1. Engines originally manufactured as rich burn engines, but modified prior to December 19, 2002 with passive emission control technology for NO_x (such as pre-combustion chambers) will be considered lean burn engines. Also, existing engines where there are no manufacturer's recommendations regarding air/fuel ratio will be considered a rich burn engine if the excess oxygen content of the exhaust at full load conditions is less than or equal to 2 percent.

Site-rated HP means the maximum manufacturer's design capacity at engine site conditions.

Spark ignition means relating to either: A gasoline-fueled engine; or any other type of engine with a spark plug (or other sparking device) and with operating characteristics significantly similar to the theoretical Otto combustion cycle. Spark ignition engines usually use a throttle to regulate intake air flow to control power during normal operation. Dual-fuel engines in which a liquid fuel (typically diesel fuel) is used for CI and gaseous fuel (typically natural gas) is used as the primary fuel at an annual average ratio of less than 2 parts diesel fuel to 100 parts total fuel on an energy equivalent basis are spark ignition engines.

Stationary reciprocating internal combustion engine (RICE) means any reciprocating internal combustion engine which uses reciprocating motion to convert heat energy into mechanical work and which is not mobile. Stationary RICE differ from mobile RICE in that a stationary RICE is not a non-road engine as defined at [40 CFR 1068.30](#), and is not used to propel a motor vehicle or a vehicle used solely for competition.

Stationary RICE test cell/stand means an engine test cell/stand, as defined in [subpart P of this part](#), that tests stationary RICE.

Stoichiometric means the theoretical air-to-fuel ratio required for complete combustion.

Storage vessel with the potential for flash emissions means any storage vessel that contains a hydrocarbon liquid with a stock tank gas-to-oil ratio equal to or greater than 0.31 cubic meters per liter and an American Petroleum Institute gravity equal to or greater than 40 degrees and an actual annual average hydrocarbon liquid throughput equal to or greater than 79,500 liters per day. Flash emissions occur when dissolved hydrocarbons in the fluid evolve from solution when the fluid pressure is reduced.

Subpart means [40 CFR part 63, subpart ZZZZ](#).

Surface site means any combination of one or more graded pad sites, gravel pad sites, foundations, platforms, or the immediate physical location upon which equipment is physically affixed.

Two-stroke engine means a type of engine which completes the power cycle in single crankshaft revolution by combining the intake and compression operations into one stroke and the power and exhaust operations into a second stroke. This system requires auxiliary scavenging and inherently runs lean of stoichiometric.

[[69 FR 33506](#), June 15, 2004, as amended at [71 FR 20467](#), Apr. 20, 2006; [73 FR 3607](#), Jan. 18, 2008; [75 FR 9679](#), Mar. 3, 2010; [75 FR 51592](#), Aug. 20, 2010; [76 FR 12867](#), Mar. 9, 2011; [78 FR 6706](#), Jan. 30, 2013]

Table 1a to Subpart ZZZZ of Part 63 - Emission Limitations for Existing, New, and Reconstructed Spark Ignition, 4SRB Stationary RICE >500 HP Located at a Major Source of HAP Emissions

As stated in §§ [63.6600](#) and [63.6640](#), you must comply with the following emission limitations at 100 percent load plus or minus 10 percent for existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions:

For each . . .	You must meet the following emission limitation, except during periods of startup . . .	During periods of startup you must . . .
1. 4SRB stationary RICE	<p>a. Reduce formaldehyde emissions by 76 percent or more. If you commenced construction or reconstruction between December 19, 2002 and June 15, 2004, you may reduce formaldehyde emissions by 75 percent or more until June 15, 2007 or</p> <p>b. Limit the concentration of formaldehyde in the stationary RICE exhaust to 350 ppbvd or less at 15 percent O₂</p>	Minimize the engine's time spent at idle and minimize the engine's startup time at startup to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes, after which time the non-startup emission limitations apply. ¹

¹ Sources can petition the Administrator pursuant to the requirements of [40 CFR 63.6\(g\)](#) for alternative work practices.

[[75 FR 9679](#), Mar. 3, 2010, as amended at [75 FR 51592](#), Aug. 20, 2010]

Table 1b to Subpart ZZZZ of Part 63 - Operating Limitations for Existing, New, and Reconstructed SI 4SRB Stationary RICE >500 HP Located at a Major Source of HAP Emissions

As stated in [§§ 63.6600](#), [63.6603](#), [63.6630](#) and [63.6640](#), you must comply with the following operating limitations for existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions:

For each . . .	You must meet the following operating limitation, except during periods of startup . . .
1. existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions complying with the requirement to reduce formaldehyde emissions by 76 percent or more (or by 75 percent or more, if applicable) and using NSCR; or	a. maintain your catalyst so that the pressure drop across the catalyst does not change by more than 2 inches of water at 100 percent load plus or minus 10 percent from the pressure drop across the catalyst measured during the initial performance test; and

For each . . .	You must meet the following operating limitation, except during periods of startup . . .
----------------	--

existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions complying with the requirement to limit the concentration of formaldehyde in the stationary RICE exhaust to 350 ppbvd or less at 15 percent O₂ and using NSCR;

b. maintain the temperature of your stationary RICE exhaust so that the catalyst inlet temperature is greater than or equal to 750 °F and less than or equal to 1250 °F.¹

2. existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions complying with the requirement to reduce formaldehyde emissions by 76 percent or more (or by 75 percent or more, if applicable) and not using NSCR; or

Comply with any operating limitations approved by the Administrator.

existing, new and reconstructed 4SRB stationary RICE >500 HP located at a major source of HAP emissions complying with the requirement to limit the concentration of formaldehyde in the stationary RICE exhaust to 350 ppbvd or less at 15 percent O₂ and not using NSCR.

¹ Sources can petition the Administrator pursuant to the requirements of [40 CFR 63.8\(f\)](#) for a different temperature range.

[[78 FR 6706](#), Jan. 30, 2013]

Table 2a to Subpart ZZZZ of Part 63 - Emission Limitations for New and Reconstructed 2SLB and Compression Ignition Stationary RICE >500 HP and New and Reconstructed 4SLB Stationary RICE ≥250 HP Located at a Major Source of HAP Emissions

As stated in [§§ 63.6600](#) and [63.6640](#), you must comply with the following emission limitations for new and reconstructed lean burn and new and reconstructed compression ignition stationary RICE at 100 percent load plus or minus 10 percent:

For each . ..	You must meet the following emission limitation, except during periods of startup . ..	During periods of startup you must . . .
1. 2SLB stationary RICE	a. Reduce CO emissions by 58 percent or more; or b. Limit concentration of formaldehyde in the stationary RICE exhaust to 12 ppmvd or less at 15 percent O ₂ . If you commenced construction or reconstruction between December 19, 2002 and June 15, 2004, you may limit concentration of formaldehyde to 17 ppmvd or less at 15 percent O ₂ until June 15, 2007	Minimize the engine's time spent at idle and minimize the engine's startup time at startup to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes, after which time the non-startup emission limitations apply. ¹
2. 4SLB stationary RICE	a. Reduce CO emissions by 93 percent or more; or b. Limit concentration of formaldehyde in the stationary RICE exhaust to 14 ppmvd or less at 15 percent O ₂	
3. CI stationary RICE	a. Reduce CO emissions by 70 percent or more; or b. Limit concentration of formaldehyde in the stationary RICE exhaust to 580 ppbvd or less at 15 percent O ₂	

¹ Sources can petition the Administrator pursuant to the requirements of [40 CFR 63.6\(g\)](#) for alternative work practices.

[[75 FR 9680](#), Mar. 3, 2010]

Table 2b to Subpart ZZZZ of Part 63 - Operating Limitations for New and Reconstructed 2SLB and CI Stationary RICE >500 HP Located at a Major Source of HAP Emissions, New and Reconstructed 4SLB Stationary

RICE \geq 250 HP Located at a Major Source of HAP Emissions, Existing CI Stationary RICE >500 HP

As stated in §§ 63.6600, 63.6601, 63.6603, 63.6630, and 63.6640, you must comply with the following operating limitations for new and reconstructed 2SLB and CI stationary RICE >500 HP located at a major source of HAP emissions; new and reconstructed 4SLB stationary RICE \geq 250 HP located at a major source of HAP emissions; and existing CI stationary RICE >500 HP:

For each . . .	You must meet the following operating limitation, except during periods of startup . . .
<p>1. New and reconstructed 2SLB and CI stationary RICE >500 HP located at a major source of HAP emissions and new and reconstructed 4SLB stationary RICE \geq250 HP located at a major source of HAP emissions complying with the requirement to reduce CO emissions and using an oxidation catalyst; and</p> <p>New and reconstructed 2SLB and CI stationary RICE >500 HP located at a major source of HAP emissions and new and reconstructed 4SLB stationary RICE \geq250 HP located at a major source of HAP emissions complying with the requirement to limit the concentration of formaldehyde in the stationary RICE exhaust and using an oxidation catalyst.</p>	<p>a. maintain your catalyst so that the pressure drop across the catalyst does not change by more than 2 inches of water at 100 percent load plus or minus 10 percent from the pressure drop across the catalyst that was measured during the initial performance test; and</p> <p>b. maintain the temperature of your stationary RICE exhaust so that the catalyst inlet temperature is greater than or equal to 450 °F and less than or equal to 1350 °F.¹</p>
<p>2. Existing CI stationary RICE >500 HP complying with the requirement to limit or reduce the concentration of CO in the stationary RICE exhaust and using an oxidation catalyst</p>	<p>a. maintain your catalyst so that the pressure drop across the catalyst does not change by more than 2 inches of water from the pressure drop across the catalyst that was measured during the initial performance test; and</p> <p>b. maintain the temperature of your stationary RICE exhaust so that the catalyst inlet temperature is greater than or equal to 450 °F and less than or equal to 1350 °F.¹</p>
<p>3. New and reconstructed 2SLB and CI stationary</p>	<p>Comply with any operating limitations</p>

For each . . .	You must meet the following operating limitation, except during periods of startup . . .
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RICE >500 HP located at a major source of HAP emissions and new and reconstructed 4SLB stationary RICE \geq 250 HP located at a major source of HAP emissions complying with the requirement to reduce CO emissions and not using an oxidation catalyst; and

approved by the Administrator.

New and reconstructed 2SLB and CI stationary RICE >500 HP located at a major source of HAP emissions and new and reconstructed 4SLB stationary RICE \geq 250 HP located at a major source of HAP emissions complying with the requirement to limit the concentration of formaldehyde in the stationary RICE exhaust and not using an oxidation catalyst; and

existing CI stationary RICE >500 HP complying with the requirement to limit or reduce the concentration of CO in the stationary RICE exhaust and not using an oxidation catalyst.

¹ Sources can petition the Administrator pursuant to the requirements of [40 CFR 63.8\(f\)](#) for a different temperature range.

[\[78 FR 6707\]](#), Jan. 30, 2013]

Table 2c to Subpart ZZZZ of Part 63 - Requirements for Existing Compression Ignition Stationary RICE Located at a Major Source of HAP Emissions and Existing Spark Ignition Stationary RICE \leq 500 HP Located at a Major Source of HAP Emissions

As stated in [§§ 63.6600](#), [63.6602](#), and [63.6640](#), you must comply with the following requirements for existing compression ignition stationary RICE located at a major source of HAP emissions and existing spark ignition stationary RICE \leq 500 HP located at a major source of HAP emissions:

For each . . .	You must meet the following requirement, except during periods of startup . . .	During periods of startup you must . . .
1. Emergency stationary CI RICE and black start stationary CI RICE ¹	a. Change oil and filter every 500 hours of operation or annually, whichever comes first. ² b. Inspect air cleaner every 1,000 hours of operation or annually, whichever comes first, and replace as necessary; c. Inspect all hoses and belts every 500 hours of operation or annually, whichever comes first, and replace as necessary. ³	Minimize the engine's time spent at idle and minimize the engine's startup time at startup to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes, after which time the non-startup emission limitations apply. ³
2. Non-Emergency, non-black start stationary CI RICE <100 HP	a. Change oil and filter every 1,000 hours of operation or annually, whichever comes first. ² b. Inspect air cleaner every 1,000 hours of operation or annually, whichever comes first, and replace as necessary; c. Inspect all hoses and belts every 500 hours of operation or annually, whichever comes first, and replace as necessary. ³	
3. Non-Emergency, non-black start CI stationary RICE 100≤HP≤300 HP	Limit concentration of CO in the stationary RICE exhaust to 230 ppmvd or less at 15 percent O ₂ .	

For each . . .	You must meet the following requirement, except during periods of startup . . .	During periods of startup you must . . .
4. Non-Emergency, non-black start CI stationary RICE $300 < \text{HP} \leq 500$	<ul style="list-style-type: none"> a. Limit concentration of CO in the stationary RICE exhaust to 49 ppmvd or less at 15 percent O₂; or b. Reduce CO emissions by 70 percent or more. 	
5. Non-Emergency, non-black start stationary CI RICE > 500 HP	<ul style="list-style-type: none"> a. Limit concentration of CO in the stationary RICE exhaust to 23 ppmvd or less at 15 percent O₂; or b. Reduce CO emissions by 70 percent or more. 	
6. Emergency stationary SI RICE and black start stationary SI RICE. ¹	<ul style="list-style-type: none"> a. Change oil and filter every 500 hours of operation or annually, whichever comes first;² b. Inspect spark plugs every 1,000 hours of operation or annually, whichever comes first, and replace as necessary; c. Inspect all hoses and belts every 500 hours of operation or annually, whichever comes first, and replace as necessary.³ 	
7. Non-Emergency, non-black start stationary SI RICE < 100 HP that are not 2SLB stationary RICE	<ul style="list-style-type: none"> a. Change oil and filter every 1,440 hours of operation or annually, whichever comes first;² b. Inspect spark plugs 	

For each . . .	You must meet the following requirement, except during periods of startup . . .	During periods of startup you must . . .
<p>8. Non-Emergency, non-black start 2SLB stationary SI RICE <100 HP</p>	<p>every 1,440 hours of operation or annually, whichever comes first, and replace as necessary;</p> <p>c. Inspect all hoses and belts every 1,440 hours of operation or annually, whichever comes first, and replace as necessary.³</p> <p>a. Change oil and filter every 4,320 hours of operation or annually, whichever comes first;²</p> <p>b. Inspect spark plugs every 4,320 hours of operation or annually, whichever comes first, and replace as necessary;</p> <p>c. Inspect all hoses and belts every 4,320 hours of operation or annually, whichever comes first, and replace as necessary.³</p>	
<p>9. Non-emergency, non-black start 2SLB stationary RICE $100 \leq \text{HP} \leq 500$</p>	<p>Limit concentration of CO in the stationary RICE exhaust to 225 ppmvd or less at 15 percent O₂.</p>	
<p>10. Non-emergency, non-black start 4SLB stationary RICE $100 \leq \text{HP} \leq 500$</p>	<p>Limit concentration of CO in the stationary RICE exhaust to 47</p>	

For each . . .	You must meet the following requirement, except during periods of startup . . .	During periods of startup you must . . .
	ppmvd or less at 15 percent O ₂ .	
11. Non-emergency, non-black start 4SRB stationary RICE 100≤HP≤500	Limit concentration of formaldehyde in the stationary RICE exhaust to 10.3 ppmvd or less at 15 percent O ₂ .	
12. Non-emergency, non-black start stationary RICE 100≤HP≤500 which combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis	Limit concentration of CO in the stationary RICE exhaust to 177 ppmvd or less at 15 percent O ₂ .	

¹ If an emergency engine is operating during an emergency and it is not possible to shut down the engine in order to perform the work practice requirements on the schedule required in Table 2c of this subpart, or if performing the work practice on the required schedule would otherwise pose an unacceptable risk under federal, state, or local law, the work practice can be delayed until the emergency is over or the unacceptable risk under federal, state, or local law has abated. The work practice should be performed as soon as practicable after the emergency has ended or the unacceptable risk under federal, state, or local law has abated. Sources must report any failure to perform the work practice on the schedule required and the federal, state or local law under which the risk was deemed unacceptable.

² Sources have the option to utilize an oil analysis program as described in [§ 63.6625\(i\)](#) or [\(j\)](#) in order to extend the specified oil change requirement in Table 2c of this subpart.

³ Sources can petition the Administrator pursuant to the requirements of [40 CFR 63.6\(g\)](#) for alternative work practices.

[[78 FR 6708](#), Jan. 30, 2013, as amended at [78 FR 14457](#), Mar. 6, 2013]

Table 2d to Subpart ZZZZ of Part 63 - Requirements for Existing Stationary RICE Located at Area Sources of HAP Emissions

As stated in §§ 63.6603 and 63.6640, you must comply with the following requirements for existing stationary RICE located at area sources of HAP emissions:

For each . . .	You must meet the following requirement, except during periods of startup . . .	During periods of startup you must . . .
1. Non-Emergency, non-black start CI stationary RICE ≤ 300 HP	a. Change oil and filter every 1,000 hours of operation or annually, whichever comes first; ¹ b. Inspect air cleaner every 1,000 hours of operation or annually, whichever comes first, and replace as necessary; c. Inspect all hoses and belts every 500 hours of operation or annually, whichever comes first, and replace as necessary.	Minimize the engine's time spent at idle and minimize the engine's startup time at startup to a period needed for appropriate and safe loading of the engine, not to exceed 30 minutes, after which time the non-startup emission limitations apply.
2. Non-Emergency, non-black start CI stationary RICE $300 < \text{HP} \leq 500$	a. Limit concentration of CO in the stationary RICE exhaust to 49 ppmvd at 15 percent O ₂ ; or b. Reduce CO emissions by 70 percent or more.	

For each . . .	You must meet the following requirement, except during periods of startup . . .	During periods of startup you must . . .
3. Non-Emergency, non-black start CI stationary RICE >500 HP	<ul style="list-style-type: none"> a. Limit concentration of CO in the stationary RICE exhaust to 23 ppmvd at 15 percent O₂; or b. Reduce CO emissions by 70 percent or more. 	
4. Emergency stationary CI RICE and black start stationary CI RICE. ²	<ul style="list-style-type: none"> a. Change oil and filter every 500 hours of operation or annually, whichever comes first;¹ b. Inspect air cleaner every 1,000 hours of operation or annually, whichever comes first, and replace as necessary; and c. Inspect all hoses and belts every 500 hours of operation or annually, whichever comes first, and replace as necessary. 	
5. Emergency stationary SI RICE; black start stationary SI RICE; non-emergency, non-black start 4SLB stationary RICE >500 HP that operate 24 hours or less per calendar year; non-emergency, non-black start 4SRB	<ul style="list-style-type: none"> a. Change oil and filter every 500 hours of operation or annually, whichever comes first;¹; b. Inspect spark plugs 	

For each . . .	You must meet the following requirement, except during periods of startup . . .	During periods of startup you must . . .
stationary RICE >500 HP that operate 24 hours or less per calendar year. ²	every 1,000 hours of operation or annually, whichever comes first, and replace as necessary; and c. Inspect all hoses and belts every 500 hours of operation or annually, whichever comes first, and replace as necessary.	
6. Non-emergency, non-black start 2SLB stationary RICE	a. Change oil and filter every 4,320 hours of operation or annually, whichever comes first; ¹ b. Inspect spark plugs every 4,320 hours of operation or annually, whichever comes first, and replace as necessary; and c. Inspect all hoses and belts every 4,320 hours of operation or annually, whichever comes first, and replace as necessary.	
7. Non-emergency, non-black start 4SLB stationary RICE ≤500 HP	a. Change oil and filter every 1,440 hours of operation or annually,	

For each . . .	You must meet the following requirement, except during periods of startup . . .	During periods of startup you must . . .
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whichever comes first;¹

b. Inspect spark plugs every 1,440 hours of operation or annually, whichever comes first, and replace as necessary; and

c. Inspect all hoses and belts every 1,440 hours of operation or annually, whichever comes first, and replace as necessary.

8. Non-emergency, non-black start
4SLB remote stationary RICE >500
HP

a. Change oil and filter every 2,160 hours of operation or annually, whichever comes first;¹

b. Inspect spark plugs every 2,160 hours of operation or annually, whichever comes first, and replace as necessary; and

c. Inspect all hoses and belts every 2,160 hours of operation or annually, whichever comes first, and replace as necessary.

For each . . .	You must meet the following requirement, except during periods of startup . . .	During periods of startup you must . . .
9. Non-emergency, non-black start 4SLB stationary RICE >500 HP that are not remote stationary RICE and that operate more than 24 hours per calendar year	Install an oxidation catalyst to reduce HAP emissions from the stationary RICE.	
10. Non-emergency, non-black start 4SRB stationary RICE \leq 500 HP	<p>a. Change oil and filter every 1,440 hours of operation or annually, whichever comes first;¹</p> <p>b. Inspect spark plugs every 1,440 hours of operation or annually, whichever comes first, and replace as necessary; and</p> <p>c. Inspect all hoses and belts every 1,440 hours of operation or annually, whichever comes first, and replace as necessary.</p>	
11. Non-emergency, non-black start 4SRB remote stationary RICE >500 HP	<p>a. Change oil and filter every 2,160 hours of operation or annually, whichever comes first;¹</p> <p>b. Inspect spark plugs every 2,160 hours of operation or annually, whichever comes first, and replace as</p>	

For each . . .	You must meet the following requirement, except during periods of startup . . .	During periods of startup you must . . .
	<p>necessary; and</p> <p>c. Inspect all hoses and belts every 2,160 hours of operation or annually, whichever comes first, and replace as necessary.</p>	
<p>12. Non-emergency, non-black start 4SRB stationary RICE >500 HP that are not remote stationary RICE and that operate more than 24 hours per calendar year</p>	<p>Install NSCR to reduce HAP emissions from the stationary RICE.</p>	
<p>13. Non-emergency, non-black start stationary RICE which combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis</p>	<p>a. Change oil and filter every 1,440 hours of operation or annually, whichever comes first;¹</p> <p>b. Inspect spark plugs every 1,440 hours of operation or annually, whichever comes first, and replace as necessary; and</p> <p>c. Inspect all hoses and belts every 1,440 hours of operation or annually, whichever comes first, and replace as necessary.</p>	

¹ Sources have the option to utilize an oil analysis program as described in [§ 63.6625\(i\)](#) or [\(j\)](#) in order to extend the specified oil change requirement in Table 2d of this subpart.

² If an emergency engine is operating during an emergency and it is not possible to shut down the engine in order to perform the management practice requirements on the schedule required in Table 2d of this subpart, or if performing the management practice on the required schedule would otherwise pose an unacceptable risk under federal, state, or local law, the management practice can be delayed until the emergency is over or the unacceptable risk under federal, state, or local law has abated. The management practice should be performed as soon as practicable after the emergency has ended or the unacceptable risk under federal, state, or local law has abated. Sources must report any failure to perform the management practice on the schedule required and the federal, state or local law under which the risk was deemed unacceptable.

[78 FR 6709, Jan. 30, 2013]

Table 3 to Subpart ZZZZ of Part 63 - Subsequent Performance Tests

As stated in §§ 63.6615 and 63.6620, you must comply with the following subsequent performance test requirements:

For each . . .	Complying with the requirement to . . .	You must . . .
1. New or reconstructed 2SLB stationary RICE >500 HP located at major sources; new or reconstructed 4SLB stationary RICE ≥250 HP located at major sources; and new or reconstructed CI stationary RICE >500 HP located at major sources	Reduce CO emissions and not using a CEMS	Conduct subsequent performance tests semiannually. ¹
2. 4SRB stationary RICE ≥5,000 HP located at major sources	Reduce formaldehyde emissions	Conduct subsequent performance tests semiannually. ¹
3. Stationary RICE >500 HP located at major sources and new or reconstructed 4SLB stationary RICE 250≤HP≤500 located at major sources	Limit the concentration of formaldehyde in the stationary RICE exhaust	Conduct subsequent performance tests semiannually. ¹
4. Existing non-emergency, non-black start CI stationary RICE >500 HP that are not limited use stationary RICE	Limit or reduce CO emissions and not using a CEMS	Conduct subsequent performance tests every 8,760 hours or 3 years, whichever comes first.

For each . . .	Complying with the requirement to . . .	You must . . .
5. Existing non-emergency, non-black start CI stationary RICE >500 HP that are limited use stationary RICE	Limit or reduce CO emissions and not using a CEMS	Conduct subsequent performance tests every 8,760 hours or 5 years, whichever comes first.

¹ After you have demonstrated compliance for two consecutive tests, you may reduce the frequency of subsequent performance tests to annually. If the results of any subsequent annual performance test indicate the stationary RICE is not in compliance with the CO or formaldehyde emission limitation, or you deviate from any of your operating limitations, you must resume semiannual performance tests.

[78 FR 6711, Jan. 30, 2013]

Table 4 to Subpart ZZZZ of Part 63 - Requirements for Performance Tests

As stated in §§ 63.6610, 63.6611, 63.6620, and 63.6640, you must comply with the following requirements for performance tests for stationary RICE:

For each . . .	Complying with the requirement to . . .	You must . . .	Using . . .	According to the following requirements . . .
1. 2SLB, 4SLB, and CI stationary RICE	a. reduce CO emissions	i. Select the sampling port location and the number/location of traverse points at the inlet and outlet of the control device; and		(a) For CO and O ₂ measurement, ducts ≤6 inches in diameter may be sampled at a single point located at the duct centroid and ducts >6 and ≤12 inches in diameter may be sampled at 3 traverse points located at 16.7, 50.0, and 83.3% of the measurement line ('3-point long line'). If the duct is >12 inches in

For each . ..	Complying with the requirement to ...	You must ...	Using ...	According to the following requirements ...
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diameter *and* the sampling port location meets the two and half-diameter criterion of [Section 11.1.1](#) of Method 1 of [40 CFR part 60, appendix A-1](#), the duct may be sampled at '3-point long line'; otherwise, conduct the stratification testing and select sampling points according to [Section 8.1.2](#) of Method 7E of [40 CFR part 60, appendix A-4](#).

ii. Measure the O₂ at the inlet and outlet of the control device; and
 (1) Method 3 or 3A or 3B of [40 CFR part 60, appendix A-2](#), or ASTM Method D6522-00 (Reapproved 2005)^a (heated probe not necessary)
 (b) Measurements to determine O₂ must be made at the same time as the measurements for CO concentration.

iii. Measure the CO at the inlet and the outlet of the control device
 (1) ASTM D6522-00 (Reapproved 2005)^{a b c} (heated probe not necessary) or Method 10 of [40 CFR part 60, appendix A-4](#)
 (c) The CO concentration must be at 15 percent O₂, dry basis.

2. 4SRB a. reduce

i. Select the

(a) For formaldehyde,

For each . ..	Complying with the requirement to ...	You must ...	Using ...	According to the following requirements ...
stationary RICE	formaldehyde emissions	sampling port location and the number/location of traverse points at the inlet and outlet of the control device; and	<p data-bbox="837 1703 1097 1869">ii. Measure O₂ at the inlet and outlet of the control device; and (1) Method 3 or 3A or 3B of 40 CFR part 60, appendix A-2, or ASTM</p>	<p data-bbox="1102 401 1435 1654">O₂, and moisture measurement, ducts ≤6 inches in diameter may be sampled at a single point located at the duct centroid and ducts >6 and ≤12 inches in diameter may be sampled at 3 traverse points located at 16.7, 50.0, and 83.3% of the measurement line ('3- point long line'). If the duct is >12 inches in diameter <i>and</i> the sampling port location meets the two and half- diameter criterion of Section 11.1.1 of Method 1 of 40 CFR part 60, appendix A, the duct may be sampled at '3- point long line'; otherwise, conduct the stratification testing and select sampling points according to Section 8.1.2 of Method 7E of 40 CFR part 60, appendix A.</p> <p data-bbox="1102 1703 1435 1869">(a) Measurements to determine O₂ concentration must be made at the same time as</p>

For each . ..	Complying with the requirement to ...	You must ...	Using ...	According to the following requirements ...
			Method D6522-00 (Reapproved 2005) ^a (heated probe not necessary)	the measurements for formaldehyde or THC concentration.
		iii. Measure moisture content at the inlet and outlet of the control device; and	(1) Method 4 of 40 CFR part 60, appendix A-3 , or Method 320 of 40 CFR part 63, appendix A , or ASTM D 6348-03 ^a	(a) Measurements to determine moisture content must be made at the same time and location as the measurements for formaldehyde or THC concentration.
		iv. If demonstrating compliance with the formaldehyde percent reduction requirement, measure formalde- hyde at the inlet and the outlet of the control device	(1) Method 320 or 323 of 40 CFR part 63, appendix A ; or ASTM D6348-03 ^a , provided in ASTM D6348-03 Annex A5 (Analyte Spiking Technique), the percent R must be greater than or equal to 70 and less than or equal to 130	(a) Formaldehyde concentration must be at 15 percent O ₂ , dry basis. Results of this test consist of the average of the three 1-hour or longer runs.
		v. If demonstrating compliance with the THC percent reduction requirement, measure THC at the inlet and the outlet of the control device	(1) Method 25A, reported as propane, of 40 CFR part 60, appendix A-7	(a) THC concentration must be at 15 percent O ₂ , dry basis. Results of this test consist of the average of the three 1- hour or longer runs.

For each . ..	Complying with the requirement to ...	You must ...	Using ...	According to the following requirements ...
3. Stationary RICE	a. limit the concentration of formalde- hyde or CO in the stationary RICE exhaust	i. Select the sampling port location and the number/location of traverse points at the exhaust of the stationary RICE; and		(a) For formaldehyde, CO, O ₂ , and moisture measurement, ducts ≤6 inches in diameter may be sampled at a single point located at the duct centroid and ducts >6 and ≤12 inches in diameter may be sampled at 3 traverse points located at 16.7, 50.0, and 83.3% of the measurement line ('3- point long line'). If the duct is >12 inches in diameter <i>and</i> the sampling port location meets the two and half- diameter criterion of Section 11.1.1 of Method 1 of 40 CFR part 60, appendix A , the duct may be sampled at '3- point long line'; otherwise, conduct the stratification testing and select sampling points according to Section 8.1.2 of Method 7E of 40 CFR part 60, appendix A . If using a control device, the sampling site must be located at the outlet of the control device.

For each . ..	Complying with the requirement to ...	You must ...	Using ...	According to the following requirements ...
		ii. Determine the O ₂ concentration of the stationary RICE exhaust at the sampling port location; and	(1) Method 3 or 3A or 3B of 40 CFR part 60, appendix A-2 , or ASTM Method D6522-00 (Reapproved 2005) ^a (heated probe not necessary)	(a) Measurements to determine O ₂ concentration must be made at the same time and location as the measurements for formaldehyde or CO concentration.
		iii. Measure moisture content of the station-ary RICE exhaust at the sampling port location; and	(1) Method 4 of 40 CFR part 60, appendix A-3 , or Method 320 of 40 CFR part 63, appendix A , or ASTM D 6348-03 ^a	(a) Measurements to determine moisture content must be made at the same time and location as the measurements for formaldehyde or CO concentration.
		iv. Measure formalde-hyde at the exhaust of the station-ary RICE; or	(1) Method 320 or 323 of 40 CFR part 63, appendix A ; or ASTM D6348-03 ^a , provided in ASTM D6348-03 Annex A5 (Analyte Spiking Technique), the percent R must be greater than or equal to 70 and less than or equal to 130	(a) Formaldehyde concentration must be at 15 percent O ₂ , dry basis. Results of this test consist of the average of the three 1-hour or longer runs.
		v. measure CO at the exhaust of the station-ary RICE	(1) Method 10 of 40 CFR part 60, appendix A-4 , ASTM Method D6522-00 (2005) ^{a c} ,	(a) CO concentration must be at 15 percent O ₂ , dry basis. Results of this test consist of the average of the three 1-

For each . . .	Complying with the requirement to . . .	You must . . .	Using . . .	According to the following requirements . . .
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Method 320 of [40](#) hour or longer runs.
[CFR part 63](#),
[appendix A](#), or
 ASTM D6348-03^a

^a You may also use Methods 3A and 10 as options to ASTM-D6522-00 (2005). You may obtain a copy of ASTM-D6522-00 (2005) from at least one of the following addresses: American Society for Testing and Materials, 100 Barr Harbor Drive, West Conshohocken, PA 19428-2959, or University Microfilms International, 300 North Zeeb Road, Ann Arbor, MI 48106.

^b You may obtain a copy of ASTM-D6348-03 from at least one of the following addresses: American Society for Testing and Materials, 100 Barr Harbor Drive, West Conshohocken, PA 19428-2959, or University Microfilms International, 300 North Zeeb Road, Ann Arbor, MI 48106.

[[79 FR 11290](#), Feb. 27, 2014]

Table 5 to Subpart ZZZZ of Part 63 - Initial Compliance With Emission Limitations, Operating Limitations, and Other Requirements

As stated in [§§ 63.6612](#), [63.6625](#) and [63.6630](#), you must initially comply with the emission and operating limitations as required by the following:

For each . . .	Complying with the requirement to . . .	You have demonstrated initial compliance if . . .
1. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE ≥250 HP located at a major source of HAP, non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non-	a. Reduce CO emissions and using oxidation catalyst, and using a CPMS	i. The average reduction of emissions of CO determined from the initial performance test achieves the required CO percent reduction; and ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according to the requirements in § 63.6625(b) ; and

For each . . .	Complying with the requirement to . . .	You have demonstrated initial compliance if . . .
emergency stationary CI RICE >500 HP located at an area source of HAP		iii. You have recorded the catalyst pressure drop and catalyst inlet temperature during the initial performance test.
2. Non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non-emergency stationary CI RICE >500 HP located at an area source of HAP	a. Limit the concentration of CO, using oxidation catalyst, and using a CPMS	i. The average CO concentration determined from the initial performance test is less than or equal to the CO emission limitation; and ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according to the requirements in § 63.6625(b) ; and iii. You have recorded the catalyst pressure drop and catalyst inlet temperature during the initial performance test.
3. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE ≥250 HP located at a major source of HAP, non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non-emergency stationary CI RICE >500 HP located at an area source of HAP	a. Reduce CO emissions and not using oxidation catalyst	i. The average reduction of emissions of CO determined from the initial performance test achieves the required CO percent reduction; and ii. You have installed a CPMS to continuously monitor operating parameters approved by the Administrator (if any) according to the requirements in § 63.6625(b) ; and iii. You have recorded the approved operating parameters (if any) during the initial performance test.
4. Non-emergency stationary CI RICE >500 HP located at a major	a. Limit the concentration of CO,	i. The average CO concentration determined from the initial

For each . . .	Complying with the requirement to . . .	You have demonstrated initial compliance if . . .
source of HAP, and existing non-emergency stationary CI RICE >500 HP located at an area source of HAP	and not using oxidation catalyst	<p>performance test is less than or equal to the CO emission limitation; and</p> <p>ii. You have installed a CPMS to continuously monitor operating parameters approved by the Administrator (if any) according to the requirements in § 63.6625(b); and</p> <p>iii. You have recorded the approved operating parameters (if any) during the initial performance test.</p>
<p>5. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE ≥250 HP located at a major source of HAP, non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non-emergency stationary CI RICE >500 HP located at an area source of HAP</p>	<p>a. Reduce CO emissions, and using a CEMS</p>	<p>i. You have installed a CEMS to continuously monitor CO and either O₂ or CO₂ at both the inlet and outlet of the oxidation catalyst according to the requirements in § 63.6625(a); and</p> <p>ii. You have conducted a performance evaluation of your CEMS using PS 3 and 4A of 40 CFR part 60, appendix B; and</p> <p>iii. The average reduction of CO calculated using § 63.6620 equals or exceeds the required percent reduction. The initial test comprises the first 4-hour period after successful validation of the CEMS. Compliance is based on the average percent reduction achieved during the 4-hour period.</p>
<p>6. Non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non-</p>	<p>a. Limit the concentration of CO,</p>	<p>i. You have installed a CEMS to continuously monitor CO and either O₂ or CO₂ at the outlet of the</p>

For each . . .	Complying with the requirement to . . .	You have demonstrated initial compliance if . . .
<p>emergency stationary CI RICE >500 HP located at an area source of HAP</p>	<p>and using a CEMS</p>	<p>oxidation catalyst according to the requirements in § 63.6625(a); and</p> <p>ii. You have conducted a performance evaluation of your CEMS using PS 3 and 4A of 40 CFR part 60, appendix B; and</p> <p>iii. The average concentration of CO calculated using § 63.6620 is less than or equal to the CO emission limitation. The initial test comprises the first 4-hour period after successful validation of the CEMS. Compliance is based on the average concentration measured during the 4-hour period.</p>
<p>7. Non-emergency 4SRB stationary RICE >500 HP located at a major source of HAP</p>	<p>a. Reduce formaldehyde emissions and using NSCR</p>	<p>i. The average reduction of emissions of formaldehyde determined from the initial performance test is equal to or greater than the required formaldehyde percent reduction, or the average reduction of emissions of THC determined from the initial performance test is equal to or greater than 30 percent; and</p> <p>ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according to the requirements in § 63.6625(b); and</p> <p>iii. You have recorded the catalyst pressure drop and catalyst inlet temperature during the initial performance test.</p>

For each . . .	Complying with the requirement to . . .	You have demonstrated initial compliance if . . .
8. Non-emergency 4SRB stationary RICE >500 HP located at a major source of HAP	a. Reduce formaldehyde emissions and not using NSCR	<p>i. The average reduction of emissions of formaldehyde determined from the initial performance test is equal to or greater than the required formaldehyde percent reduction or the average reduction of emissions of THC determined from the initial performance test is equal to or greater than 30 percent; and</p> <p>ii. You have installed a CPMS to continuously monitor operating parameters approved by the Administrator (if any) according to the requirements in § 63.6625(b); and</p> <p>iii. You have recorded the approved operating parameters (if any) during the initial performance test.</p>
9. New or reconstructed non-emergency stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE $250 \leq \text{HP} \leq 500$ located at a major source of HAP, and existing non-emergency 4SRB stationary RICE >500 HP located at a major source of HAP	a. Limit the concentration of formaldehyde in the stationary RICE exhaust and using oxidation catalyst or NSCR	<p>i. The average formaldehyde concentration, corrected to 15 percent O₂, dry basis, from the three test runs is less than or equal to the formaldehyde emission limitation; and</p> <p>ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according to the requirements in § 63.6625(b); and</p> <p>iii. You have recorded the catalyst pressure drop and catalyst inlet temperature during the initial performance test.</p>

For each . . .	Complying with the requirement to . . .	You have demonstrated initial compliance if . . .
<p>10. New or reconstructed non-emergency stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE $250 \leq \text{HP} \leq 500$ located at a major source of HAP, and existing non-emergency 4SRB stationary RICE >500 HP located at a major source of HAP</p>	<p>a. Limit the concentration of formaldehyde in the stationary RICE exhaust and not using oxidation catalyst or NSCR</p>	<p>i. The average formaldehyde concentration, corrected to 15 percent O₂, dry basis, from the three test runs is less than or equal to the formaldehyde emission limitation; and ii. You have installed a CPMS to continuously monitor operating parameters approved by the Administrator (if any) according to the requirements in § 63.6625(b); and</p>
<p>11. Existing non-emergency stationary RICE $100 \leq \text{HP} \leq 500$ located at a major source of HAP, and existing non-emergency stationary CI RICE $300 < \text{HP} \leq 500$ located at an area source of HAP</p>	<p>a. Reduce CO emissions</p>	<p>iii. You have recorded the approved operating parameters (if any) during the initial performance test.</p> <p>i. The average reduction of emissions of CO or formaldehyde, as applicable determined from the initial performance test is equal to or greater than the required CO or formaldehyde, as applicable, percent reduction.</p>
<p>12. Existing non-emergency stationary RICE $100 \leq \text{HP} \leq 500$ located at a major source of HAP, and existing non-emergency stationary CI RICE $300 < \text{HP} \leq 500$ located at an area source of HAP</p>	<p>a. Limit the concentration of formaldehyde or CO in the stationary RICE exhaust</p>	<p>i. The average formaldehyde or CO concentration, as applicable, corrected to 15 percent O₂, dry basis, from the three test runs is less than or equal to the formaldehyde or CO emission limitation, as applicable.</p>
<p>13. Existing non-emergency 4SLB stationary RICE >500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per</p>	<p>a. Install an oxidation catalyst</p>	<p>i. You have conducted an initial compliance demonstration as specified in § 63.6630(e) to show that the average reduction of emissions of CO is 93 percent or more, or the average CO</p>

For each . . .	Complying with the requirement to . . .	You have demonstrated initial compliance if . . .
calendar year		<p>concentration is less than or equal to 47 ppmvd at 15 percent O₂;</p> <p>ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according to the requirements in § 63.6625(b), or you have installed equipment to automatically shut down the engine if the catalyst inlet temperature exceeds 1350 °F.</p> <p>i. You have conducted an initial compliance demonstration as specified in § 63.6630(e) to show that the average reduction of emissions of CO is 75 percent or more, the average CO concentration is less than or equal to 270 ppmvd at 15 percent O₂, or the average reduction of emissions of THC is 30 percent or more;</p> <p>ii. You have installed a CPMS to continuously monitor catalyst inlet temperature according to the requirements in § 63.6625(b), or you have installed equipment to automatically shut down the engine if the catalyst inlet temperature exceeds 1250 °F.</p>
<p>14. Existing non-emergency 4SRB stationary RICE >500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per calendar year</p>	<p>a. Install NSCR</p>	

[[78 FR 6712](#), Jan. 30, 2013]

Table 6 to Subpart ZZZZ of Part 63 - Continuous Compliance With Emission Limitations, and Other Requirements

As stated in [§ 63.6640](#), you must continuously comply with the emissions and operating limitations and work or management practices as required by the following:

For each . . .	Complying with the requirement to . . .	You must demonstrate continuous compliance by . . .
<p>1. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE ≥250 HP located at a major source of HAP, and new or reconstructed non-emergency CI stationary RICE >500 HP located at a major source of HAP</p>	<p>a. Reduce CO emissions and using an oxidation catalyst, and using a CPMS</p>	<p>i. Conducting semiannual performance tests for CO to demonstrate that the required CO percent reduction is achieved^a; and</p> <p>ii. Collecting the catalyst inlet temperature data according to § 63.6625(b); and</p> <p>iii. Reducing these data to 4-hour rolling averages; and</p> <p>iv. Maintaining the 4-hour rolling averages within the operating limitations for the catalyst inlet temperature; and</p> <p>v. Measuring the pressure drop across the catalyst once per month and demonstrating that the pressure drop across the catalyst is within the operating limitation established during the performance test.</p>
<p>2. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE ≥250 HP located at a major source of HAP, and new or reconstructed non-emergency CI stationary RICE >500 HP located at a major source of HAP</p>	<p>a. Reduce CO emissions and not using an oxidation catalyst, and using a CPMS</p>	<p>i. Conducting semiannual performance tests for CO to demonstrate that the required CO percent reduction is achieved^a; and</p> <p>ii. Collecting the approved operating parameter (if any) data according to § 63.6625(b); and</p> <p>iii. Reducing these data to 4-hour rolling averages; and</p> <p>iv. Maintaining the 4-hour rolling</p>

For each . . .	Complying with the requirement to . . .	You must demonstrate continuous compliance by . . .
<p>3. New or reconstructed non-emergency 2SLB stationary RICE >500 HP located at a major source of HAP, new or reconstructed non-emergency 4SLB stationary RICE ≥250 HP located at a major source of HAP, new or reconstructed non-emergency stationary CI RICE >500 HP located at a major source of HAP, and existing non-emergency stationary CI RICE >500 HP</p>	<p>a. Reduce CO emissions or limit the concentration of CO in the stationary RICE exhaust, and using a CEMS</p>	<p>averages within the operating limitations for the operating parameters established during the performance test.</p> <p>i. Collecting the monitoring data according to § 63.6625(a), reducing the measurements to 1-hour averages, calculating the percent reduction or concentration of CO emissions according to § 63.6620; and</p> <p>ii. Demonstrating that the catalyst achieves the required percent reduction of CO emissions over the 4-hour averaging period, or that the emission remain at or below the CO concentration limit; and</p> <p>iii. Conducting an annual RATA of your CEMS using PS 3 and 4A of 40 CFR part 60, appendix B, as well as daily and periodic data quality checks in accordance with 40 CFR part 60, appendix F, procedure 1.</p>
<p>4. Non-emergency 4SRB stationary RICE >500 HP located at a major source of HAP</p>	<p>a. Reduce formaldehyde emissions and using NSCR</p>	<p>i. Collecting the catalyst inlet temperature data according to § 63.6625(b); and</p> <p>ii. Reducing these data to 4-hour rolling averages; and</p> <p>iii. Maintaining the 4-hour rolling averages within the operating limitations for the catalyst inlet temperature; and</p>

For each . . .	Complying with the requirement to . . .	You must demonstrate continuous compliance by . . .
5. Non-emergency 4SRB stationary RICE >500 HP located at a major source of HAP	a. Reduce formaldehyde emissions and not using NSCR	<p>iv. Measuring the pressure drop across the catalyst once per month and demonstrating that the pressure drop across the catalyst is within the operating limitation established during the performance test.</p> <p>i. Collecting the approved operating parameter (if any) data according to § 63.6625(b); and</p> <p>ii. Reducing these data to 4-hour rolling averages; and</p> <p>iii. Maintaining the 4-hour rolling averages within the operating limitations for the operating parameters established during the performance test.</p> <p>Conducting semiannual performance tests for formaldehyde to demonstrate that the required formaldehyde percent reduction is achieved, or to demonstrate that the average reduction of emissions of THC determined from the performance test is equal to or greater than 30 percent.^a</p>
6. Non-emergency 4SRB stationary RICE with a brake HP $\geq 5,000$ located at a major source of HAP	a. Reduce formaldehyde emissions	<p>Conducting semiannual performance tests for formaldehyde to demonstrate that the required formaldehyde percent reduction is achieved, or to demonstrate that the average reduction of emissions of THC determined from the performance test is equal to or greater than 30 percent.^a</p>
7. New or reconstructed non-emergency stationary RICE >500 HP located at a major source of HAP and new or reconstructed non-emergency 4SLB stationary RICE $250 \leq \text{HP} \leq 500$ located at a major source of HAP	a. Limit the concentration of formaldehyde in the stationary RICE exhaust and using oxidation catalyst or NSCR	<p>i. Conducting semiannual performance tests for formaldehyde to demonstrate that your emissions remain at or below the formaldehyde concentration limit^a; and</p> <p>ii. Collecting the catalyst inlet temperature data according to §</p>

For each . . .	Complying with the requirement to . . .	You must demonstrate continuous compliance by . . .
<p>8. New or reconstructed non-emergency stationary RICE >500 HP located at a major source of HAP and new or reconstructed non-emergency 4SLB stationary RICE $250 \leq \text{HP} \leq 500$ located at a major source of HAP</p>	<p>a. Limit the concentration of formaldehyde in the stationary RICE exhaust and not using oxidation catalyst or NSCR</p>	<p>63.6625(b); and</p> <p>iii. Reducing these data to 4-hour rolling averages; and</p> <p>iv. Maintaining the 4-hour rolling averages within the operating limitations for the catalyst inlet temperature; and</p> <p>v. Measuring the pressure drop across the catalyst once per month and demonstrating that the pressure drop across the catalyst is within the operating limitation established during the performance test.</p> <p>i. Conducting semiannual performance tests for formaldehyde to demonstrate that your emissions remain at or below the formaldehyde concentration limit^a; and</p> <p>ii. Collecting the approved operating parameter (if any) data according to § 63.6625(b); and</p> <p>iii. Reducing these data to 4-hour rolling averages; and</p> <p>iv. Maintaining the 4-hour rolling averages within the operating limitations for the operating parameters established during the performance test.</p>
<p>9. Existing emergency and black start stationary RICE ≤ 500 HP located at a major source of HAP, existing non-emergency stationary</p>	<p>a. Work or Management practices</p>	<p>i. Operating and maintaining the stationary RICE according to the manufacturer's emission-related operation and maintenance</p>

For each . . .	Complying with the requirement to . . .	You must demonstrate continuous compliance by . . .
<p>RICE <100 HP located at a major source of HAP, existing emergency and black start stationary RICE located at an area source of HAP, existing non-emergency stationary CI RICE ≤300 HP located at an area source of HAP, existing non-emergency 2SLB stationary RICE located at an area source of HAP, existing non-emergency stationary SI RICE located at an area source of HAP which combusts landfill or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis, existing non-emergency 4SLB and 4SRB stationary RICE ≤500 HP located at an area source of HAP, existing non-emergency 4SLB and 4SRB stationary RICE >500 HP located at an area source of HAP that operate 24 hours or less per calendar year, and existing non-emergency 4SLB and 4SRB stationary RICE >500 HP located at an area source of HAP that are remote stationary RICE</p>	<p>a. Reduce CO emissions, or limit the concentration of CO in the stationary RICE exhaust, and using oxidation catalyst</p>	<p>instructions; or ii. Develop and follow your own maintenance plan which must provide to the extent practicable for the maintenance and operation of the engine in a manner consistent with good air pollution control practice for minimizing emissions.</p> <p>i. Conducting performance tests every 8,760 hours or 3 years, whichever comes first, for CO or formaldehyde, as appropriate, to demonstrate that the required CO or formaldehyde, as appropriate, percent reduction is achieved or that your emissions remain at or below the CO or formaldehyde concentration limit; and</p>
<p>10. Existing stationary CI RICE >500 HP that are not limited use stationary RICE</p>		

For each . . .	Complying with the requirement to . . .	You must demonstrate continuous compliance by . . .
<p>11. Existing stationary CI RICE >500 HP that are not limited use stationary RICE</p>	<p>a. Reduce CO emissions, or limit the concentration of CO in the stationary RICE exhaust, and not using oxidation catalyst</p>	<p>ii. Collecting the catalyst inlet temperature data according to § 63.6625(b); and</p> <p>iii. Reducing these data to 4-hour rolling averages; and</p> <p>iv. Maintaining the 4-hour rolling averages within the operating limitations for the catalyst inlet temperature; and</p> <p>v. Measuring the pressure drop across the catalyst once per month and demonstrating that the pressure drop across the catalyst is within the operating limitation established during the performance test.</p> <p>i. Conducting performance tests every 8,760 hours or 3 years, whichever comes first, for CO or formaldehyde, as appropriate, to demonstrate that the required CO or formaldehyde, as appropriate, percent reduction is achieved or that your emissions remain at or below the CO or formaldehyde concentration limit; and</p> <p>ii. Collecting the approved operating parameter (if any) data according to § 63.6625(b); and</p> <p>iii. Reducing these data to 4-hour rolling averages; and</p> <p>iv. Maintaining the 4-hour rolling averages within the operating</p>

For each . . .	Complying with the requirement to . . .	You must demonstrate continuous compliance by . . .
12. Existing limited use CI stationary RICE >500 HP	a. Reduce CO emissions or limit the concentration of CO in the stationary RICE exhaust, and using an oxidation catalyst	<p>limitations for the operating parameters established during the performance test.</p> <p>i. Conducting performance tests every 8,760 hours or 5 years, whichever comes first, for CO or formaldehyde, as appropriate, to demonstrate that the required CO or formaldehyde, as appropriate, percent reduction is achieved or that your emissions remain at or below the CO or formaldehyde concentration limit; and</p> <p>ii. Collecting the catalyst inlet temperature data according to § 63.6625(b); and</p> <p>iii. Reducing these data to 4-hour rolling averages; and</p> <p>iv. Maintaining the 4-hour rolling averages within the operating limitations for the catalyst inlet temperature; and</p> <p>v. Measuring the pressure drop across the catalyst once per month and demonstrating that the pressure drop across the catalyst is within the operating limitation established during the performance test.</p>
13. Existing limited use CI stationary RICE >500 HP	a. Reduce CO emissions or limit the concentration of CO in the stationary	i. Conducting performance tests every 8,760 hours or 5 years, whichever comes first, for CO or formaldehyde, as appropriate, to

For each . . .	Complying with the requirement to . . .	You must demonstrate continuous compliance by . . .
<p>14. Existing non-emergency 4SLB stationary RICE >500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per calendar year</p>	<p>RICE exhaust, and not using an oxidation catalyst</p> <p>a. Install an oxidation catalyst</p>	<p>demonstrate that the required CO or formaldehyde, as appropriate, percent reduction is achieved or that your emissions remain at or below the CO or formaldehyde concentration limit; and</p> <p>ii. Collecting the approved operating parameter (if any) data according to § 63.6625(b); and</p> <p>iii. Reducing these data to 4-hour rolling averages; and</p> <p>iv. Maintaining the 4-hour rolling averages within the operating limitations for the operating parameters established during the performance test.</p> <p>i. Conducting annual compliance demonstrations as specified in § 63.6640(c) to show that the average reduction of emissions of CO is 93 percent or more, or the average CO concentration is less than or equal to 47 ppmvd at 15 percent O₂; and either</p> <p>ii. Collecting the catalyst inlet temperature data according to § 63.6625(b), reducing these data to 4-hour rolling averages; and maintaining the 4-hour rolling averages within the limitation of greater than 450 °F and less than or equal to 1350 °F for the catalyst inlet temperature; or</p> <p>iii. Immediately shutting down the</p>

For each . . .	Complying with the requirement to . . .	You must demonstrate continuous compliance by . . .
<p>15. Existing non-emergency 4SRB stationary RICE >500 HP located at an area source of HAP that are not remote stationary RICE and that are operated more than 24 hours per calendar year</p>	<p>a. Install NSCR</p>	<p>engine if the catalyst inlet temperature exceeds 1350 °F.</p> <p>i. Conducting annual compliance demonstrations as specified in § 63.6640(c) to show that the average reduction of emissions of CO is 75 percent or more, the average CO concentration is less than or equal to 270 ppmvd at 15 percent O₂, or the average reduction of emissions of THC is 30 percent or more; and either</p> <p>ii. Collecting the catalyst inlet temperature data according to § 63.6625(b), reducing these data to 4-hour rolling averages; and maintaining the 4-hour rolling averages within the limitation of greater than or equal to 750 °F and less than or equal to 1250 °F for the catalyst inlet temperature; or</p> <p>iii. Immediately shutting down the engine if the catalyst inlet temperature exceeds 1250 °F.</p>

^a After you have demonstrated compliance for two consecutive tests, you may reduce the frequency of subsequent performance tests to annually. If the results of any subsequent annual performance test indicate the stationary RICE is not in compliance with the CO or formaldehyde emission limitation, or you deviate from any of your operating limitations, you must resume semiannual performance tests.

[[78 FR 6715](#), Jan. 30, 2013]

Table 7 to Subpart ZZZZ of Part 63 - Requirements for Reports

As stated in [§ 63.6650](#), you must comply with the following requirements for reports:

For each . . .	You must submit a . . .	The report must contain . . .	You must submit the report . . .
<p>1. Existing non-emergency, non-black start stationary RICE $100 \leq \text{HP} \leq 500$ located at a major source of HAP; existing non-emergency, non-black start stationary CI RICE > 500 HP located at a major source of HAP; existing non-emergency 4SRB stationary RICE > 500 HP located at a major source of HAP; existing non-emergency, non-black start stationary CI RICE > 300 HP located at an area source of HAP; new or reconstructed non-emergency stationary RICE > 500 HP located at a major source of HAP; and new or reconstructed non-emergency 4SLB stationary RICE $250 \leq \text{HP} \leq 500$ located at a major source of HAP</p>	<p>Compliance report</p>	<p>a. If there are no deviations from any emission limitations or operating limitations that apply to you, a statement that there were no deviations from the emission limitations or operating limitations during the reporting period. If there were no periods during which the CMS, including CEMS and CPMS, was out-of-control, as specified in § 63.8(c)(7), a statement that there were not periods during which the CMS was out-of-control during the reporting period; or</p> <p>b. If you had a deviation from any emission limitation or operating limitation during the reporting period, the information in § 63.6650(d). If there were periods during which the CMS, including CEMS and CPMS, was out-of-control, as specified in § 63.8(c)(7), the information in § 63.6650(e); or</p> <p>c. If you had a malfunction during the reporting period,</p>	<p>i. Semiannually according to the requirements in § 63.6650(b)(1)-(5) for engines that are not limited use stationary RICE subject to numerical emission limitations; and</p> <p>ii. Annually according to the requirements in § 63.6650(b)(6)-(9) for engines that are limited use stationary RICE subject to numerical emission limitations.</p> <p>i. Semiannually according to the requirements in § 63.6650(b).</p> <p>i. Semiannually according to the</p>

For each . . .	You must submit a . . .	The report must contain . . .	You must submit the report . . .
<p>2. New or reconstructed non-emergency stationary RICE that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis</p>	<p>Report</p>	<p>the information in § 63.6650(c)(4).</p> <p>a. The fuel flow rate of each fuel and the heating values that were used in your calculations, and you must demonstrate that the percentage of heat input provided by landfill gas or digester gas, is equivalent to 10 percent or more of the gross heat input on an annual basis; and</p> <p>b. The operating limits provided in your federally enforceable permit, and any deviations from these limits; and</p> <p>c. Any problems or errors suspected with the meters.</p>	<p>requirements in § 63.6650(b).</p> <p>i. Annually, according to the requirements in § 63.6650.</p> <p>i. See item 2.a.i.</p> <p>i. See item 2.a.i.</p>
<p>3. Existing non-emergency, non-black start 4SLB and 4SRB stationary RICE >500 HP located at an area source of HAP that are not remote stationary RICE and that operate more than 24 hours per calendar year</p>	<p>Compliance report</p>	<p>a. The results of the annual compliance demonstration, if conducted during the reporting period.</p>	<p>i. Semiannually according to the requirements in § 63.6650(b)(1)-(5).</p>
<p>4. Emergency stationary RICE that operate or are contractually obligated to be available for more than 15</p>	<p>Report</p>	<p>a. The information in § 63.6650(h)(1)</p>	<p>i. annually according to the requirements in § 63.6650(h)(2)-(3).</p>

For each . . .	You must submit a . . .	The report must contain . . .	You must submit the report . . .
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hours per year for the purposes specified in [§ 63.6640\(f\)\(2\)\(ii\)](#) and [\(iii\)](#) or that operate for the purposes specified in [§ 63.6640\(f\)\(4\)\(ii\)](#)

[[78 FR 6719](#), Jan. 30, 2013]

Table 8 to Subpart ZZZZ of Part 63 - Applicability of General Provisions to Subpart ZZZZ.

As stated in [§ 63.6665](#), you must comply with the following applicable general provisions.

General provisions citation	Subject of citation	Applies to subpart	Explanation
§ 63.1	General applicability of the General Provisions	Yes.	
§ 63.2	Definitions	Yes	Additional terms defined in § 63.6675 .
§ 63.3	Units and abbreviations	Yes.	
§ 63.4	Prohibited activities and circumvention	Yes.	
§ 63.5	Construction and reconstruction	Yes.	
§ 63.6(a)	Applicability	Yes.	
§ 63.6(b)(1)-(4)	Compliance dates for new and reconstructed sources	Yes.	

General provisions citation	Subject of citation	Applies to subpart	Explanation
§ 63.6(b)(5)	Notification	Yes.	
§ 63.6(b)(6)	[Reserved]		
§ 63.6(b)(7)	Compliance dates for new and reconstructed area sources that become major sources	Yes.	
§ 63.6(c)(1)-(2)	Compliance dates for existing sources	Yes.	
§ 63.6(c)(3)-(4)	[Reserved]		
§ 63.6(c)(5)	Compliance dates for existing area sources that become major sources	Yes.	
§ 63.6(d)	[Reserved]		
§ 63.6(e)	Operation and maintenance	No.	
§ 63.6(f)(1)	Applicability of standards	No.	
§ 63.6(f)(2)	Methods for determining compliance	Yes.	
§ 63.6(f)(3)	Finding of compliance	Yes.	
§ 63.6(g)(1)-(3)	Use of alternate standard	Yes.	
§ 63.6(h)	Opacity and visible emission standards	No	Subpart ZZZZ does not contain opacity or visible emission standards.
§ 63.6(i)	Compliance extension procedures and criteria	Yes.	
§ 63.6(j)	Presidential compliance	Yes.	

General provisions citation	Subject of citation	Applies to subpart	Explanation
	exemption		
§ 63.7(a)(1)-(2)	Performance test dates	Yes	Subpart ZZZZ contains performance test dates at §§ 63.6610 , 63.6611 , and 63.6612 .
§ 63.7(a)(3)	CAA section 114 authority	Yes.	
§ 63.7(b)(1)	Notification of performance test	Yes	Except that § 63.7(b)(1) only applies as specified in § 63.6645 .
§ 63.7(b)(2)	Notification of rescheduling	Yes	Except that § 63.7(b)(2) only applies as specified in § 63.6645 .
§ 63.7(c)	Quality assurance/test plan	Yes	Except that § 63.7(c) only applies as specified in § 63.6645 .
§ 63.7(d)	Testing facilities	Yes.	
§ 63.7(e)(1)	Conditions for conducting performance tests	No.	Subpart ZZZZ specifies conditions for conducting performance tests at § 63.6620 .
§ 63.7(e)(2)	Conduct of performance tests and reduction of data	Yes	Subpart ZZZZ specifies test methods at § 63.6620 .
§ 63.7(e)(3)	Test run duration	Yes.	
§ 63.7(e)(4)	Administrator may require other testing under section 114 of the CAA	Yes.	
§ 63.7(f)	Alternative test method provisions	Yes.	

General provisions citation	Subject of citation	Applies to subpart	Explanation
§ 63.7(g)	Performance test data analysis, recordkeeping, and reporting	Yes.	
§ 63.7(h)	Waiver of tests	Yes.	
§ 63.8(a)(1)	Applicability of monitoring requirements	Yes	Subpart ZZZZ contains specific requirements for monitoring at § 63.6625 .
§ 63.8(a)(2)	Performance specifications	Yes.	
§ 63.8(a)(3)	[Reserved]		
§ 63.8(a)(4)	Monitoring for control devices	No.	
§ 63.8(b)(1)	Monitoring	Yes.	
§ 63.8(b)(2)-(3)	Multiple effluents and multiple monitoring systems	Yes.	
§ 63.8(c)(1)	Monitoring system operation and maintenance	Yes.	
§ 63.8(c)(1)(i)	Routine and predictable SSM	No	
§ 63.8(c)(1)(ii)	SSM not in Startup Shutdown Malfunction Plan	Yes.	
§ 63.8(c)(1)(iii)	Compliance with operation and maintenance requirements	No	
§ 63.8(c)(2)-(3)	Monitoring system installation	Yes.	
§ 63.8(c)(4)	Continuous monitoring system (CMS) requirements	Yes	Except that subpart ZZZZ does not require Continuous Opacity Monitoring System (COMS).

General provisions citation	Subject of citation	Applies to subpart	Explanation
§ 63.8(c)(5)	COMS minimum procedures	No	Subpart ZZZZ does not require COMS.
§ 63.8(c)(6)-(8)	CMS requirements	Yes	Except that subpart ZZZZ does not require COMS.
§ 63.8(d)	CMS quality control	Yes.	
§ 63.8(e)	CMS performance evaluation	Yes	Except for § 63.8(e)(5)(ii) , which applies to COMS.
		Except that § 63.8(e) only applies as specified in § 63.6645 .	
§ 63.8(f)(1)-(5)	Alternative monitoring method	Yes	Except that § 63.8(f)(4) only applies as specified in § 63.6645 .
§ 63.8(f)(6)	Alternative to relative accuracy test	Yes	Except that § 63.8(f)(6) only applies as specified in § 63.6645 .
§ 63.8(g)	Data reduction	Yes	Except that provisions for COMS are not applicable. Averaging periods for demonstrating compliance are specified at §§ 63.6635 and 63.6640 .
§ 63.9(a)	Applicability and State delegation of notification requirements	Yes.	
§ 63.9(b)(1)-(5)	Initial notifications	Yes	Except that § 63.9(b)(3) is

General provisions citation	Subject of citation	Applies to subpart	Explanation
			reserved.
		Except that § 63.9(b) only applies as specified in § 63.6645 .	
§ 63.9(c)	Request for compliance extension	Yes	Except that § 63.9(c) only applies as specified in § 63.6645 .
§ 63.9(d)	Notification of special compliance requirements for new sources	Yes	Except that § 63.9(d) only applies as specified in § 63.6645 .
§ 63.9(e)	Notification of performance test	Yes	Except that § 63.9(e) only applies as specified in § 63.6645 .
§ 63.9(f)	Notification of visible emission (VE)/opacity test	No	Subpart ZZZZ does not contain opacity or VE standards.
§ 63.9(g)(1)	Notification of performance evaluation	Yes	Except that § 63.9(g) only applies as specified in § 63.6645 .
§ 63.9(g)(2)	Notification of use of COMS data	No	Subpart ZZZZ does not contain opacity or VE standards.
§ 63.9(g)(3)	Notification that criterion for alternative to RATA is exceeded	Yes	If alternative is in use.
		Except that § 63.9(g) only applies as specified in §	

General provisions citation	Subject of citation	Applies to subpart	Explanation
			63.6645.
§ 63.9(h)(1)-(6)	Notification of compliance status	Yes	Except that notifications for sources using a CEMS are due 30 days after completion of performance evaluations. § 63.9(h)(4) is reserved.
			Except that § 63.9(h) only applies as specified in § 63.6645.
§ 63.9(i)	Adjustment of submittal deadlines	Yes.	
§ 63.9(j)	Change in previous information	Yes.	
§ 63.9(k)	Electronic reporting procedures	Yes	Only as specified in § 63.9(j) .
§ 63.10(a)	Administrative provisions for recordkeeping/reporting	Yes.	
§ 63.10(b)(1)	Record retention	Yes	Except that the most recent 2 years of data do not have to be retained on site.
§ 63.10(b)(2)(i)-(v)	Records related to SSM	No.	
§ 63.10(b)(2)(vi)-(xi)	Records	Yes.	
§ 63.10(b)(2)(xii)	Record when under waiver	Yes.	
§ 63.10(b)(2)(xiii)	Records when using alternative to RATA	Yes	For CO standard if using RATA alternative.

General provisions citation	Subject of citation	Applies to subpart	Explanation
§ 63.10(b)(2)(xiv)	Records of supporting documentation	Yes.	
§ 63.10(b)(3)	Records of applicability determination	Yes.	
§ 63.10(c)	Additional records for sources using CEMS	Yes	Except that § 63.10(c)(2)-(4) and (9) are reserved.
§ 63.10(d)(1)	General reporting requirements	Yes.	
§ 63.10(d)(2)	Report of performance test results	Yes.	
§ 63.10(d)(3)	Reporting opacity or VE observations	No	Subpart ZZZZ does not contain opacity or VE standards.
§ 63.10(d)(4)	Progress reports	Yes.	
§ 63.10(d)(5)	Startup, shutdown, and malfunction reports	No.	
§ 63.10(e)(1) and (2)(i)	Additional CMS Reports	Yes.	
§ 63.10(e)(2)(ii)	COMS-related report	No	Subpart ZZZZ does not require COMS.
§ 63.10(e)(3)	Excess emission and parameter exceedances reports	Yes.	Except that § 63.10(e)(3)(i)(C) is reserved.
§ 63.10(e)(4)	Reporting COMS data	No	Subpart ZZZZ does not require COMS.
§ 63.10(f)	Waiver for recordkeeping/reporting	Yes.	

General provisions citation	Subject of citation	Applies to subpart	Explanation
§ 63.11	Flares	No.	
§ 63.12	State authority and delegations	Yes.	
§ 63.13	Addresses	Yes.	
§ 63.14	Incorporation by reference	Yes.	
§ 63.15	Availability of information	Yes.	

[[75 FR 9688](#), Mar. 3, 2010, as amended at [78 FR 6720](#), Jan. 30, 2013; [85 FR 73912](#), Nov. 19, 2020]

Appendix A to Subpart ZZZZ of Part 63 - Protocol for Using an Electrochemical Analyzer to Determine Oxygen and Carbon Monoxide Concentrations From Certain Engines

1.0 Scope and Application. What is this Protocol?

This protocol is a procedure for using portable electrochemical (EC) cells for measuring carbon monoxide (CO) and oxygen (O₂) concentrations in controlled and uncontrolled emissions from existing stationary 4-stroke lean burn and 4-stroke rich burn reciprocating internal combustion engines as specified in the applicable rule.

1.1 Analytes. What does this protocol determine?

This protocol measures the engine exhaust gas concentrations of carbon monoxide (CO) and oxygen (O₂).

Analyte	CAS No.	Sensitivity
Carbon monoxide (CO)	630-08-0	Minimum detectable limit should be 2 percent of the nominal range or 1 ppm, whichever is less restrictive.
Oxygen (O ₂)	7782-	

Analyte	CAS No.	Sensitivity
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1.2 Applicability. When is this protocol acceptable?

This protocol is applicable to [40 CFR part 63, subpart ZZZZ](#). Because of inherent cross sensitivities of EC cells, you must not apply this protocol to other emissions sources without specific instruction to that effect.

1.3 Data Quality Objectives. How good must my collected data be?

Refer to Section 13 to verify and document acceptable analyzer performance.

1.4 Range. What is the targeted analytical range for this protocol?

The measurement system and EC cell design(s) conforming to this protocol will determine the analytical range for each gas component. The nominal ranges are defined by choosing up-scale calibration gas concentrations near the maximum anticipated flue gas concentrations for CO and O₂, or no more than twice the permitted CO level.

1.5 Sensitivity. What minimum detectable limit will this protocol yield for a particular gas component?

The minimum detectable limit depends on the nominal range and resolution of the specific EC cell used, and the signal to noise ratio of the measurement system. The minimum detectable limit should be 2 percent of the nominal range or 1 ppm, whichever is less restrictive.

2.0 Summary of Protocol

In this protocol, a gas sample is extracted from an engine exhaust system and then conveyed to a portable EC analyzer for measurement of CO and O₂ gas concentrations. This method provides measurement system performance specifications and sampling protocols to ensure reliable data. You may use additions to, or modifications of vendor supplied measurement systems (e.g., heated or unheated sample lines, thermocouples, flow meters, selective gas scrubbers, etc.) to meet the design specifications of this protocol. Do not make changes to the measurement system from the as-verified configuration ([Section 3.12](#)).

3.0 Definitions

3.1 Measurement System. The total equipment required for the measurement of CO and O₂ concentrations. The measurement system consists of the following major subsystems:

3.1.1 Data Recorder. A strip chart recorder, computer or digital recorder for logging measurement data from the analyzer output. You may record measurement data from the digital data display manually or electronically.

3.1.2 Electrochemical (EC) Cell. A device, similar to a fuel cell, used to sense the presence of a specific analyte and generate an electrical current output proportional to the analyte concentration.

3.1.3 Interference Gas Scrubber. A device used to remove or neutralize chemical compounds that may interfere with the selective operation of an EC cell.

3.1.4 Moisture Removal System. Any device used to reduce the concentration of moisture in the sample stream so as to protect the EC cells from the damaging effects of condensation and to minimize errors in measurements caused by the scrubbing of soluble gases.

3.1.5 Sample Interface. The portion of the system used for one or more of the following: sample acquisition; sample transport; sample conditioning or protection of the EC cell from any degrading effects of the engine exhaust effluent; removal of particulate matter and condensed moisture.

3.2 Nominal Range. The range of analyte concentrations over which each EC cell is operated (normally 25 percent to 150 percent of up-scale calibration gas value). Several nominal ranges can be used for any given cell so long as the calibration and repeatability checks for that range remain within specifications.

3.3 Calibration Gas. A vendor certified concentration of a specific analyte in an appropriate balance gas.

3.4 Zero Calibration Error. The analyte concentration output exhibited by the EC cell in response to zero-level calibration gas.

3.5 Up-Scale Calibration Error. The mean of the difference between the analyte concentration exhibited by the EC cell and the certified concentration of the up-scale calibration gas.

3.6 Interference Check. A procedure for quantifying analytical interference from components in the engine exhaust gas other than the targeted analytes.

3.7 Repeatability Check. A protocol for demonstrating that an EC cell operated over a given nominal analyte concentration range provides a stable and consistent response and is not significantly affected by repeated exposure to that gas.

3.8 Sample Flow Rate. The flow rate of the gas sample as it passes through the EC cell. In some situations, EC cells can experience drift with changes in flow rate. The flow rate must be monitored and documented during all phases of a sampling run.

3.9 Sampling Run. A timed three-phase event whereby an EC cell's response rises and plateaus in a sample conditioning phase, remains relatively constant during a measurement data phase, then declines during a refresh phase. The sample conditioning phase exposes the EC cell to the gas sample for a length of time sufficient to reach a constant response. The measurement data phase is the time interval during which gas sample measurements can be made that meet the acceptance criteria of this protocol. The refresh phase then purges the EC cells with CO-free air. The refresh phase replenishes requisite O₂ and moisture in the electrolyte reserve and provides a mechanism to de-gas or desorb any interference gas scrubbers or filters so as to enable a stable CO EC cell response. There are four primary types of sampling runs: pre- sampling calibrations; stack gas sampling; post-sampling calibration checks; and measurement system repeatability checks. Stack gas sampling runs can be chained together for extended evaluations, providing all other procedural specifications are met.

3.10 Sampling Day. A time not to exceed twelve hours from the time of the pre-sampling calibration to the post-sampling calibration check. During this time, stack gas sampling runs can be repeated without repeated recalibrations, providing all other sampling specifications have been met.

3.11 Pre-Sampling Calibration/Post-Sampling Calibration Check. The protocols executed at the beginning and end of each sampling day to bracket measurement readings with controlled performance checks.

3.12 Performance-Established Configuration. The EC cell and sampling system configuration that existed at the time that it initially met the performance requirements of this protocol.

4.0 Interferences.

When present in sufficient concentrations, NO and NO₂ are two gas species that have been reported to interfere with CO concentration measurements. In the likelihood of this occurrence, it is the protocol user's responsibility to employ and properly maintain an appropriate CO EC cell filter or scrubber for removal of these gases, as described in [Section 6.2.12](#).

5.0 Safety. [Reserved]

6.0 Equipment and Supplies.

6.1 What equipment do I need for the measurement system?

The system must maintain the gas sample at conditions that will prevent moisture condensation in the sample transport lines, both before and as the sample gas contacts the EC cells. The essential components of the measurement system are described below.

6.2 Measurement System Components.

6.2.1 Sample Probe. A single extraction-point probe constructed of glass, stainless steel or other non-reactive material, and of length sufficient to reach any designated sampling point. The sample probe must be designed to prevent plugging due to condensation or particulate matter.

6.2.2 Sample Line. Non-reactive tubing to transport the effluent from the sample probe to the EC cell.

6.2.3 Calibration Assembly (optional). A three-way valve assembly or equivalent to introduce calibration gases at ambient pressure at the exit end of the sample probe during calibration checks. The assembly must be designed such that only stack gas or calibration gas flows in the sample line and all gases flow through any gas path filters.

6.2.4 Particulate Filter (optional). Filters before the inlet of the EC cell to prevent accumulation of particulate material in the measurement system and extend the useful life of the components. All filters must be fabricated of materials that are non-reactive to the gas mixtures being sampled.

6.2.5 Sample Pump. A leak-free pump to provide undiluted sample gas to the system at a flow rate sufficient to minimize the response time of the measurement system. If located upstream of the EC cells, the pump must be constructed of a material that is non-reactive to the gas mixtures being sampled.

6.2.8 Sample Flow Rate Monitoring. An adjustable rotameter or equivalent device used to adjust and maintain the sample flow rate through the analyzer as prescribed.

6.2.9 Sample Gas Manifold (optional). A manifold to divert a portion of the sample gas stream to the analyzer and the remainder to a by-pass discharge vent. The sample gas manifold may also include provisions for introducing calibration gases directly to the analyzer. The manifold must be constructed of a material that is non-reactive to the gas mixtures being sampled.

6.2.10 EC cell. A device containing one or more EC cells to determine the CO and O₂ concentrations in the sample gas stream. The EC cell(s) must meet the applicable performance specifications of Section 13 of this protocol.

6.2.11 Data Recorder. A strip chart recorder, computer or digital recorder to make a record of analyzer output data. The data recorder resolution (i.e., readability) must be no greater than 1 ppm for CO; 0.1 percent for O₂; and one degree (either °C or °F) for temperature. Alternatively, you may use a digital or analog meter having the same resolution to observe and manually record the analyzer responses.

6.2.12 Interference Gas Filter or Scrubber. A device to remove interfering compounds upstream of the CO EC cell. Specific interference gas filters or scrubbers used in the performance-established configuration of the analyzer must continue to be used. Such a filter or scrubber must have a means to determine when the removal agent is exhausted. Periodically replace or replenish it in accordance with the manufacturer's recommendations.

7.0 Reagents and Standards. What calibration gases are needed?

7.1 Calibration Gases. CO calibration gases for the EC cell must be CO in nitrogen or CO in a mixture of nitrogen and O₂. Use CO calibration gases with labeled concentration values certified by the manufacturer to be within ±5 percent of the label value. Dry ambient air (20.9 percent O₂) is acceptable for calibration of the O₂ cell. If needed, any lower percentage O₂ calibration gas must be a mixture of O₂ in nitrogen.

7.1.1 Up-Scale CO Calibration Gas Concentration. Choose one or more up-scale gas concentrations such that the average of the stack gas measurements for each stack gas sampling run are between 25 and 150 percent of those concentrations. Alternatively, choose an up-scale gas that does not exceed twice the concentration of the applicable outlet standard. If a measured gas value exceeds 150 percent of the up-scale CO calibration gas value at any time during the stack gas sampling run, the run must be discarded and repeated.

7.1.2 Up-Scale O₂ Calibration Gas Concentration.

Select an O₂ gas concentration such that the difference between the gas concentration and the average stack gas measurement or reading for each sample run is less than 15 percent O₂. When the average exhaust gas O₂ readings are above 6 percent, you may use dry ambient air (20.9 percent O₂) for the up-scale O₂ calibration gas.

7.1.3 Zero Gas. Use an inert gas that contains less than 0.25 percent of the up-scale CO calibration gas concentration. You may use dry air that is free from ambient CO and other combustion gas products (e.g., CO₂).

8.0 Sample Collection and Analysis

8.1 Selection of Sampling Sites.

8.1.1 Control Device Inlet. Select a sampling site sufficiently downstream of the engine so that the combustion gases should be well mixed. Use a single sampling extraction point near the center of the duct (e.g., within the 10 percent centroidal area), unless instructed otherwise.

8.1.2 Exhaust Gas Outlet. Select a sampling site located at least two stack diameters downstream of any disturbance (e.g., turbocharger exhaust, crossover junction or recirculation take-off) and at least one-half stack diameter upstream of the gas discharge to the atmosphere. Use a single sampling extraction point near the center of the duct (e.g., within the 10 percent centroidal area), unless instructed otherwise.

8.2 Stack Gas Collection and Analysis. Prior to the first stack gas sampling run, conduct that the pre-sampling calibration in accordance with [Section 10.1](#). Use Figure 1 to record all data. Zero the analyzer with zero gas. Confirm and record that the scrubber media color is correct and not exhausted. Then position the probe at the sampling point and begin the sampling run at the same flow rate used during the up-scale calibration. Record the start time. Record all EC cell output responses and the flow rate during the “sample conditioning phase” once per minute until

constant readings are obtained. Then begin the “measurement data phase” and record readings every 15 seconds for at least two minutes (or eight readings), or as otherwise required to achieve two continuous minutes of data that meet the specification given in [Section 13.1](#). Finally, perform the “refresh phase” by introducing dry air, free from CO and other combustion gases, until several minute-to-minute readings of consistent value have been obtained. For each run use the “measurement data phase” readings to calculate the average stack gas CO and O₂ concentrations.

8.3 EC Cell Rate. Maintain the EC cell sample flow rate so that it does not vary by more than ± 10 percent throughout the pre-sampling calibration, stack gas sampling and post-sampling calibration check. Alternatively, the EC cell sample flow rate can be maintained within a tolerance range that does not affect the gas concentration readings by more than ± 3 percent, as instructed by the EC cell manufacturer.

9.0 Quality Control (Reserved)

10.0 Calibration and Standardization

10.1 Pre-Sampling Calibration. Conduct the following protocol once for each nominal range to be used on each EC cell before performing a stack gas sampling run on each field sampling day. Repeat the calibration if you replace an EC cell before completing all of the sampling runs. There is no prescribed order for calibration of the EC cells; however, each cell must complete the measurement data phase during calibration. Assemble the measurement system by following the manufacturer's recommended protocols including for preparing and preconditioning the EC cell. Assure the measurement system has no leaks and verify the gas scrubbing agent is not depleted. Use Figure 1 to record all data.

10.1.1 Zero Calibration. For both the O₂ and CO cells, introduce zero gas to the measurement system (e.g., at the calibration assembly) and record the concentration reading every minute until readings are constant for at least two consecutive minutes. Include the time and sample flow rate. Repeat the steps in this section at least once to verify the zero calibration for each component gas.

10.1.2 Zero Calibration Tolerance. For each zero gas introduction, the zero level output must be less than or equal to ± 3 percent of the up-scale gas value or ± 1 ppm, whichever is less restrictive, for the CO channel and less than or equal to ± 0.3 percent O₂ for the O₂ channel.

10.1.3 Up-Scale Calibration. Individually introduce each calibration gas to the measurement system (e.g., at the calibration assembly) and record the start time. Record all EC cell output responses and the flow rate during this “sample conditioning phase” once per minute until readings are constant for at least two minutes. Then begin the “measurement data phase” and record readings every 15 seconds for a total of two minutes, or as otherwise required. Finally, perform the “refresh phase” by introducing dry air, free from CO and other combustion gases, until readings are constant for at least two consecutive minutes. Then repeat the steps in this section at least once to verify the calibration for each component gas. Introduce all gases to flow

through the entire sample handling system (i.e., at the exit end of the sampling probe or the calibration assembly).

10.1.4 Up-Scale Calibration Error. The mean of the difference of the “measurement data phase” readings from the reported standard gas value must be less than or equal to ± 5 percent or ± 1 ppm for CO or ± 0.5 percent O₂, whichever is less restrictive, respectively. The maximum allowable deviation from the mean measured value of any single “measurement data phase” reading must be less than or equal to ± 2 percent or ± 1 ppm for CO or ± 0.5 percent O₂, whichever is less restrictive, respectively.

10.2 Post-Sampling Calibration Check. Conduct a stack gas post-sampling calibration check after the stack gas sampling run or set of runs and within 12 hours of the initial calibration. Conduct up-scale and zero calibration checks using the protocol in [Section 10.1](#). Make no changes to the sampling system or EC cell calibration until all post-sampling calibration checks have been recorded. If either the zero or up-scale calibration error exceeds the respective specification in Sections 10.1.2 and 10.1.4 then all measurement data collected since the previous successful calibrations are invalid and re-calibration and re-sampling are required. If the sampling system is disassembled or the EC cell calibration is adjusted, repeat the calibration check before conducting the next analyzer sampling run.

11.0 Analytical Procedure

The analytical procedure is fully discussed in Section 8.

12.0 Calculations and Data Analysis

Determine the CO and O₂ concentrations for each stack gas sampling run by calculating the mean gas concentrations of the data recorded during the “measurement data phase”.

13.0 Protocol Performance

Use the following protocols to verify consistent analyzer performance during each field sampling day.

13.1 Measurement Data Phase Performance Check. Calculate the mean of the readings from the “measurement data phase”. The maximum allowable deviation from the mean for each of the individual readings is ± 2 percent, or ± 1 ppm, whichever is less restrictive. Record the mean value and maximum deviation for each gas monitored. Data must conform to [Section 10.1.4](#). The EC cell flow rate must conform to the specification in [Section 8.3](#).

Example:

A measurement data phase is invalid if the maximum deviation of any single reading comprising that mean is greater than ± 2 percent *or* ± 1 ppm (the default criteria). For example, if the mean = 30 ppm, single readings of below 29 ppm and above 31 ppm are disallowed).

13.2 Interference Check. Before the initial use of the EC cell and interference gas scrubber in the field, and semi-annually thereafter, challenge the interference gas scrubber with NO and NO₂ gas standards that are generally recognized as representative of diesel-fueled engine NO and NO₂ emission values. Record the responses displayed by the CO EC cell and other pertinent data on Figure 1 or a similar form.

13.2.1 Interference Response. The combined NO and NO₂ interference response should be less than or equal to ± 5 percent of the up-scale CO calibration gas concentration.

13.3 Repeatability Check. Conduct the following check once for each nominal range that is to be used on the CO EC cell within 5 days prior to each field sampling program. If a field sampling program lasts longer than 5 days, repeat this check every 5 days. Immediately repeat the check if the EC cell is replaced or if the EC cell is exposed to gas concentrations greater than 150 percent of the highest up-scale gas concentration.

13.3.1 Repeatability Check Procedure. Perform a complete EC cell sampling run (all three phases) by introducing the CO calibration gas to the measurement system and record the response. Follow [Section 10.1.3](#). Use Figure 1 to record all data. Repeat the run three times for a total of four complete runs. During the four repeatability check runs, do not adjust the system except where necessary to achieve the correct calibration gas flow rate at the analyzer.

13.3.2 Repeatability Check Calculations. Determine the highest and lowest average “measurement data phase” CO concentrations from the four repeatability check runs and record the results on Figure 1 or a similar form. The absolute value of the difference between the maximum and minimum average values recorded must not vary more than ± 3 percent or ± 1 ppm of the up-scale gas value, whichever is less restrictive.

14.0 Pollution Prevention (Reserved)

15.0 Waste Management (Reserved)

16.0 Alternative Procedures (Reserved)

17.0 References

(1) “Development of an Electrochemical Cell Emission Analyzer Test Protocol”, Topical Report, Phil Juneau, Emission Monitoring, Inc., July 1997.

(2) “Determination of Nitrogen Oxides, Carbon Monoxide, and Oxygen Emissions from Natural Gas-Fired Engines, Boilers, and Process Heaters Using Portable Analyzers”, EMC Conditional Test Protocol 30 (CTM-30), Gas Research Institute Protocol GRI-96/0008, Revision 7, October 13, 1997.

(3) “ICAC Test Protocol for Periodic Monitoring”, EMC Conditional Test Protocol 34 (CTM-034), The Institute of Clean Air Companies, September 8, 1999.

(4) "Code of Federal Regulations", Protection of Environment, 40 CFR, Part 60, Appendix A, Methods 1-4; 10.

Table 1: Appendix A - Sampling Run Data.

Facility_____ Engine I.D._____ Date_____										
Run Type:	<input type="checkbox"/>		<input type="checkbox"/>		<input type="checkbox"/>		<input type="checkbox"/>		<input type="checkbox"/>	
(X)	Pre-Sample Calibration				Stack Gas Sample				Post-Sample Cal. Check	Repeatability Check
Run #	1	1	2	2	3	3	4	4	Time Scrub. OK	Flow-Rate
Gas	O ₂	CO	O ₂	CO	O ₂	CO	O ₂	CO		
Sample Cond. Phase										
"										
"										
"										
"										
Measurement Data Phase										
"										
"										
"										
"										
"										
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Mean

Refresh
Phase

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[[78 FR 6721](#), Jan. 30, 2013]

Appendix F

40 C.F.R. Part 63 Subpart DDDDD

National Emission Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters

Subpart DDDDD - National Emission Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters

Source: [76 FR 15664](#), Mar. 21, 2011, unless otherwise noted.

What This Subpart Covers

§ 63.7480 What is the purpose of this subpart?

This subpart establishes national emission limitations and work practice standards for hazardous air pollutants (HAP) emitted from industrial, commercial, and institutional boilers and process heaters located at major sources of HAP. This subpart also establishes requirements to demonstrate initial and continuous compliance with the emission limitations and work practice standards.

§ 63.7485 Am I subject to this subpart?

You are subject to this subpart if you own or operate an industrial, commercial, or institutional boiler or process heater as defined in [§ 63.7575](#) that is located at, or is part of, a major source of HAP, except as specified in [§ 63.7491](#). For purposes of this subpart, a major source of HAP is as defined in [§ 63.2](#), except that for oil and natural gas production facilities, a major source of HAP is as defined in [§ 63.7575](#).

[[78 FR 7162](#), Jan. 31, 2013]

§ 63.7490 What is the affected source of this subpart?

(a) This subpart applies to new, reconstructed, and existing affected sources as described in [paragraphs \(a\)\(1\)](#) and [\(2\)](#) of this section.

(1) The affected source of this subpart is the collection at a major source of all existing industrial, commercial, and institutional boilers and process heaters within a subcategory as defined in [§ 63.7575](#).

(2) The affected source of this subpart is each new or reconstructed industrial, commercial, or institutional boiler or process heater, as defined in [§ 63.7575](#), located at a major source.

(b) A boiler or process heater is new if you commence construction of the boiler or process heater after June 4, 2010, and you meet the applicability criteria at the time you commence construction.

(c) A boiler or process heater is reconstructed if you meet the reconstruction criteria as defined in [§ 63.2](#), you commence reconstruction after June 4, 2010, and you meet the applicability criteria at the time you commence reconstruction.

(d) A boiler or process heater is existing if it is not new or reconstructed.

(e) An existing electric utility steam generating unit (EGU) that meets the applicability requirements of this subpart after the effective date of this final rule due to a change (e.g., fuel switch) is considered to be an existing source under this subpart.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7162](#), Jan. 31, 2013]

§ 63.7491 Are any boilers or process heaters not subject to this subpart?

The types of boilers and process heaters listed in [paragraphs \(a\)](#) through [\(n\)](#) of this section are not subject to this subpart.

(a) An electric utility steam generating unit (EGU) covered by [subpart UUUUU of this part](#) or a natural gas-fired EGU as defined in [subpart UUUUU of this part](#) firing at least 85 percent natural gas on an annual heat input basis.

(b) A recovery boiler or furnace covered by [subpart MM of this part](#).

(c) A boiler or process heater that is used specifically for research and development, including test steam boilers used to provide steam for testing the propulsion systems on military vessels. This does not include units that provide heat or steam to a process at a research and development facility.

(d) A hot water heater as defined in this subpart.

(e) A refining kettle covered by [subpart X of this part](#).

(f) An ethylene cracking furnace covered by [subpart YY of this part](#).

(g) Blast furnace stoves as described in EPA-453/R-01-005 (incorporated by reference, see [§ 63.14](#)).

(h) Any boiler or process heater that is part of the affected source subject to another subpart of this part, such as boilers and process heaters used as control devices to comply with [subparts JJJ](#), [OOO](#), [PPP](#), and [U of this part](#).

(i) Any boiler or process heater that is used as a control device to comply with another subpart of this [part](#), or [part 60](#), [part 61](#), or [part 65 of this chapter](#) provided that at least 50 percent of the average annual heat input during any 3 consecutive calendar years to the boiler or process heater is provided by regulated gas streams that are subject to another standard.

(j) Temporary boilers and process heaters as defined in this subpart.

- (k) Blast furnace gas fuel-fired boilers and process heaters as defined in this subpart.
- (l) Any boiler or process heater specifically listed as an affected source in any standard(s) established under section 129 of the Clean Air Act.
- (m) A unit that burns hazardous waste covered by [Subpart EEE of this part](#). A unit that is exempt from Subpart EEE as specified in [§ 63.1200\(b\)](#) is not covered by Subpart EEE.
- (n) Residential boilers as defined in this subpart.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7162](#), Jan. 31, 2013; [80 FR 72806](#), Nov. 20, 2015]

§ 63.7495 When do I have to comply with this subpart?

- (a) If you have a new or reconstructed boiler or process heater, you must comply with this subpart by April 1, 2013, or upon startup of your boiler or process heater, whichever is later.
- (b) If you have an existing boiler or process heater, you must comply with this subpart no later than January 31, 2016, except as provided in [§ 63.6\(i\)](#).
- (c) If you have an area source that increases its emissions or its potential to emit such that it becomes a major source of HAP, [paragraphs \(c\)\(1\) and \(2\)](#) of this section apply to you.
 - (1) Any new or reconstructed boiler or process heater at the existing source must be in compliance with this subpart upon startup.
 - (2) Any existing boiler or process heater at the existing source must be in compliance with this subpart within 3 years after the source becomes a major source.
- (d) You must meet the notification requirements in [§ 63.7545](#) according to the schedule in [§ 63.7545](#) and in [subpart A of this part](#). Some of the notifications must be submitted before you are required to comply with the emission limits and work practice standards in this subpart.
- (e) If you own or operate an industrial, commercial, or institutional boiler or process heater and would be subject to this subpart except for the exemption in [§ 63.7491\(l\)](#) for commercial and industrial solid waste incineration units covered by part 60, subpart CCCC or subpart DDDD, and you cease combusting solid waste, you must be in compliance with this subpart and are no longer subject to part 60, subparts CCCC or DDDD beginning on the effective date of the switch as identified under the provisions of [§ 60.2145\(a\)\(2\) and \(3\)](#) or [§ 60.2710\(a\)\(2\) and \(3\)](#).
- (f) If you own or operate an existing EGU that becomes subject to this subpart after January 31, 2016, you must be in compliance with the applicable existing source provisions of this subpart on the effective date such unit becomes subject to this subpart.

(g) If you own or operate an existing industrial, commercial, or institutional boiler or process heater and would be subject to this subpart except for an exemption in [§ 63.7491\(i\)](#) that becomes subject to this subpart after January 31, 2013, you must be in compliance with the applicable existing source provisions of this subpart within 3 years after such unit becomes subject to this subpart.

(h) If you own or operate an existing industrial, commercial, or institutional boiler or process heater and have switched fuels or made a physical change to the boiler or process heater that resulted in the applicability of a different subcategory after the compliance date of this subpart, you must be in compliance with the applicable existing source provisions of this subpart on the effective date of the fuel switch or physical change.

(i) If you own or operate a new industrial, commercial, or institutional boiler or process heater and have switched fuels or made a physical change to the boiler or process heater that resulted in the applicability of a different subcategory, you must be in compliance with the applicable new source provisions of this subpart on the effective date of the fuel switch or physical change.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7162](#), Jan. 31, 2013; [80 FR 72807](#), Nov. 20, 2015]

Emission Limitations and Work Practice Standards

§ 63.7499 What are the subcategories of boilers and process heaters?

The subcategories of boilers and process heaters, as defined in [§ 63.7575](#) are:

- (a) Pulverized coal/solid fossil fuel units.
- (b) Stokers designed to burn coal/solid fossil fuel.
- (c) Fluidized bed units designed to burn coal/solid fossil fuel.
- (d) Stokers/sloped grate/other units designed to burn kiln dried biomass/bio-based solid.
- (e) Fluidized bed units designed to burn biomass/bio-based solid.
- (f) Suspension burners designed to burn biomass/bio-based solid.
- (g) Fuel cells designed to burn biomass/bio-based solid.
- (h) Hybrid suspension/grate burners designed to burn wet biomass/bio-based solid.
- (i) Stokers/sloped grate/other units designed to burn wet biomass/bio-based solid.

- (j) Dutch ovens/pile burners designed to burn biomass/bio-based solid.
- (k) Units designed to burn liquid fuel that are non-continental units.
- (l) Units designed to burn gas 1 fuels.
- (m) Units designed to burn gas 2 (other) gases.
- (n) Metal process furnaces.
- (o) Limited-use boilers and process heaters.
- (p) Units designed to burn solid fuel.
- (q) Units designed to burn liquid fuel.
- (r) Units designed to burn coal/solid fossil fuel.
- (s) Fluidized bed units with an integrated fluidized bed heat exchanger designed to burn coal/solid fossil fuel.
- (t) Units designed to burn heavy liquid fuel.
- (u) Units designed to burn light liquid fuel.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7163](#), Jan. 31, 2013]

§ 63.7500 What emission limitations, work practice standards, and operating limits must I meet?

(a) You must meet the requirements in [paragraphs \(a\)\(1\)](#) through [\(3\)](#) of this section, except as provided in [paragraphs \(b\)](#), through [\(e\)](#) of this section. You must meet these requirements at all times the affected unit is operating, except as provided in [paragraph \(f\)](#) of this section.

(1) You must meet each emission limit and work practice standard in Tables 1 through 3, and 11 through 13 to this subpart that applies to your boiler or process heater, for each boiler or process heater at your source, except as provided under [§ 63.7522](#). The output-based emission limits, in units of pounds per million Btu of steam output, in Tables 1 or 2 to this subpart are an alternative applicable only to boilers and process heaters that generate either steam, cogenerate steam with electricity, or both. The output-based emission limits, in units of pounds per megawatt-hour, in Tables 1 or 2 to this subpart are an alternative applicable only to boilers that generate only electricity. Boilers that perform multiple functions (cogeneration and electricity generation) or supply steam to common headers would calculate a total steam energy output using equation 21 of [§ 63.7575](#) to demonstrate compliance with the output-based emission limits, in units of pounds per million Btu of steam output, in

Tables 1 or 2 to this subpart. If you operate a new boiler or process heater, you can choose to comply with alternative limits as discussed in [paragraphs \(a\)\(1\)\(i\) through \(iii\)](#) of this section, but on or after January 31, 2016, you must comply with the emission limits in Table 1 to this subpart.

(i) If your boiler or process heater commenced construction or reconstruction after June 4, 2010 and before May 20, 2011, you may comply with the emission limits in Table 1 or 11 to this subpart until January 31, 2016.

(ii) If your boiler or process heater commenced construction or reconstruction on or after May 20, 2011 and before December 23, 2011, you may comply with the emission limits in Table 1 or 12 to this subpart until January 31, 2016.

(iii) If your boiler or process heater commenced construction or reconstruction on or after December 23, 2011 and before April 1, 2013, you may comply with the emission limits in Table 1 or 13 to this subpart until January 31, 2016.

(2) You must meet each operating limit in Table 4 to this subpart that applies to your boiler or process heater. If you use a control device or combination of control devices not covered in Table 4 to this subpart, or you wish to establish and monitor an alternative operating limit or an alternative monitoring parameter, you must apply to the EPA Administrator for approval of alternative monitoring under [§ 63.8\(f\)](#).

(3) At all times, you must operate and maintain any affected source (as defined in [§ 63.7490](#)), including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions. Determination of whether such operation and maintenance procedures are being used will be based on information available to the Administrator that may include, but is not limited to, monitoring results, review of operation and maintenance procedures, review of operation and maintenance records, and inspection of the source.

(b) As provided in [§ 63.6\(g\)](#), EPA may approve use of an alternative to the work practice standards in this section.

(c) Limited-use boilers and process heaters must complete a tune-up every 5 years as specified in [§ 63.7540](#). They are not subject to the emission limits in Tables 1 and 2 or 11 through 13 to this subpart, the annual tune-up, or the energy assessment requirements in Table 3 to this subpart, or the operating limits in Table 4 to this subpart.

(d) Boilers and process heaters with a heat input capacity of less than or equal to 5 million Btu per hour in the units designed to burn gas 2 (other) fuels subcategory or units designed to burn light liquid fuels subcategory must complete a tune-up every 5 years as specified in [§ 63.7540](#).

(e) Boilers and process heaters in the units designed to burn gas 1 fuels subcategory with a heat input capacity of less than or equal to 5 million Btu per hour must complete a tune-up every 5 years as specified in [§ 63.7540](#). Boilers and process heaters in the units designed to burn gas 1

fuels subcategory with a heat input capacity greater than 5 million Btu per hour and less than 10 million Btu per hour must complete a tune-up every 2 years as specified in [§ 63.7540](#). Boilers and process heaters in the units designed to burn gas 1 fuels subcategory are not subject to the emission limits in Tables 1 and 2 or 11 through 13 to this subpart, or the operating limits in Table 4 to this subpart.

(f) These standards apply at all times the affected unit is operating, except during periods of startup and shutdown during which time you must comply only with items 5 and 6 of Table 3 to this subpart.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7163](#), Jan. 31, 2013; [80 FR 72807](#), Nov. 20, 2015]

§ 63.7501 [Reserved]

General Compliance Requirements

§ 63.7505 What are my general requirements for complying with this subpart?

(a) You must be in compliance with the emission limits, work practice standards, and operating limits in this subpart. These emission and operating limits apply to you at all times the affected unit is operating except for the periods noted in [§ 63.7500\(f\)](#).

(b) [Reserved]

(c) You must demonstrate compliance with all applicable emission limits using performance stack testing, fuel analysis, or continuous monitoring systems (CMS), including a continuous emission monitoring system (CEMS), or particulate matter continuous parameter monitoring system (PM CPMS), where applicable. You may demonstrate compliance with the applicable emission limit for hydrogen chloride (HCl), mercury, or total selected metals (TSM) using fuel analysis if the emission rate calculated according to [§ 63.7530\(c\)](#) is less than the applicable emission limit. (For gaseous fuels, you may not use fuel analyses to comply with the TSM alternative standard or the HCl standard.) Otherwise, you must demonstrate compliance for HCl, mercury, or TSM using performance stack testing, if subject to an applicable emission limit listed in Tables 1, 2, or 11 through 13 to this subpart.

(d) If you demonstrate compliance with any applicable emission limit through performance testing and subsequent compliance with operating limits through the use of CPMS, or with a CEMS or COMS, you must develop a site-specific monitoring plan according to the requirements in [paragraphs \(d\)\(1\) through \(4\)](#) of this section for the use of any CEMS, COMS, or CPMS. This requirement also applies to you if you petition the EPA Administrator for alternative monitoring parameters under [§ 63.8\(f\)](#).

(1) For each CMS required in this section (including CEMS, COMS, or CPMS), you must develop, and submit to the Administrator for approval upon request, a site-specific monitoring plan that addresses design, data collection, and the quality assurance and quality control elements outlined in [§ 63.8\(d\)](#) and the elements described in [paragraphs \(d\)\(1\)\(i\)](#) through [\(iii\)](#) of this section. You must submit this site-specific monitoring plan, if requested, at least 60 days before your initial performance evaluation of your CMS. This requirement to develop and submit a site specific monitoring plan does not apply to affected sources with existing CEMS or COMS operated according to the performance specifications under appendix B to [part 60 of this chapter](#) and that meet the requirements of [§ 63.7525](#). Using the process described in [§ 63.8\(f\)\(4\)](#), you may request approval of alternative monitoring system quality assurance and quality control procedures in place of those specified in this paragraph and, if approved, include the alternatives in your site-specific monitoring plan.

(i) Installation of the CMS sampling probe or other interface at a measurement location relative to each affected process unit such that the measurement is representative of control of the exhaust emissions (e.g., on or downstream of the last control device);

(ii) Performance and equipment specifications for the sample interface, the pollutant concentration or parametric signal analyzer, and the data collection and reduction systems; and

(iii) Performance evaluation procedures and acceptance criteria (e.g., calibrations, accuracy audits, analytical drift).

(2) In your site-specific monitoring plan, you must also address [paragraphs \(d\)\(2\)\(i\)](#) through [\(iii\)](#) of this section.

(i) Ongoing operation and maintenance procedures in accordance with the general requirements of [§ 63.8\(c\)\(1\)\(ii\)](#), [\(c\)\(3\)](#), and [\(c\)\(4\)\(ii\)](#);

(ii) Ongoing data quality assurance procedures in accordance with the general requirements of [§ 63.8\(d\)](#); and

(iii) Ongoing recordkeeping and reporting procedures in accordance with the general requirements of [§ 63.10\(c\)](#) (as applicable in Table 10 to this subpart), [\(e\)\(1\)](#), and [\(e\)\(2\)\(i\)](#).

(3) You must conduct a performance evaluation of each CMS in accordance with your site-specific monitoring plan.

(4) You must operate and maintain the CMS in continuous operation according to the site-specific monitoring plan.

(e) If you have an applicable emission limit, and you choose to comply using definition (2) of “startup” in [§ 63.7575](#), you must develop and implement a written startup and shutdown plan (SSP) according to the requirements in Table 3 to this subpart. The SSP must be maintained onsite and available upon request for public inspection.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7164](#), Jan. 31, 2013; [80 FR 72807](#), Nov. 20, 2015]

Testing, Fuel Analyses, and Initial Compliance Requirements

§ 63.7510 What are my initial compliance requirements and by what date must I conduct them?

(a) For each boiler or process heater that is required or that you elect to demonstrate compliance with any of the applicable emission limits in Tables 1 or 2 or 11 through 13 of this subpart through performance (stack) testing, your initial compliance requirements include all the following:

(1) Conduct performance tests according to [§ 63.7520](#) and Table 5 to this subpart.

(2) Conduct a fuel analysis for each type of fuel burned in your boiler or process heater according to [§ 63.7521](#) and Table 6 to this subpart, except as specified in [paragraphs \(a\)\(2\)\(i\) through \(iii\)](#) of this section.

(i) For each boiler or process heater that burns a single type of fuel, you are not required to conduct a fuel analysis for each type of fuel burned in your boiler or process heater according to [§ 63.7521](#) and Table 6 to this subpart. For purposes of this subpart, units that use a supplemental fuel only for startup, unit shutdown, and transient flame stability purposes still qualify as units that burn a single type of fuel, and the supplemental fuel is not subject to the fuel analysis requirements under [§ 63.7521](#) and Table 6 to this subpart.

(ii) When natural gas, refinery gas, or other gas 1 fuels are co-fired with other fuels, you are not required to conduct a fuel analysis of those Gas 1 fuels according to [§ 63.7521](#) and Table 6 to this subpart. If gaseous fuels other than natural gas, refinery gas, or other gas 1 fuels are co-fired with other fuels and those non-Gas 1 gaseous fuels are subject to another subpart of this part, part 60, part 61, or part 65, you are not required to conduct a fuel analysis of those non-Gas 1 fuels according to [§ 63.7521](#) and Table 6 to this subpart.

(iii) You are not required to conduct a chlorine fuel analysis for any gaseous fuels. You must conduct a fuel analysis for mercury on gaseous fuels unless the fuel is exempted in [paragraphs \(a\)\(2\)\(i\) and \(ii\)](#) of this section.

(3) Establish operating limits according to [§ 63.7530](#) and Table 7 to this subpart.

(4) Conduct CMS performance evaluations according to [§ 63.7525](#).

(b) For each boiler or process heater that you elect to demonstrate compliance with the applicable emission limits in Tables 1 or 2 or 11 through 13 to this subpart for HCl, mercury, or TSM through fuel analysis, your initial compliance requirement is to conduct a fuel analysis for each type of fuel burned in your boiler or process heater according to [§ 63.7521](#) and Table

6 to this subpart and establish operating limits according to [§ 63.7530](#) and Table 8 to this subpart. The fuels described in [paragraph \(a\)\(2\)\(i\)](#) and [\(ii\)](#) of this section are exempt from these fuel analysis and operating limit requirements. The fuels described in [paragraph \(a\)\(2\)\(ii\)](#) of this section are exempt from the chloride fuel analysis and operating limit requirements. Boilers and process heaters that use a CEMS for mercury or HCl are exempt from the performance testing and operating limit requirements specified in [paragraph \(a\)](#) of this section for the HAP for which CEMS are used.

(c) If your boiler or process heater is subject to a carbon monoxide (CO) limit, your initial compliance demonstration for CO is to conduct a performance test for CO according to Table 5 to this subpart or conduct a performance evaluation of your continuous CO monitor, if applicable, according to [§ 63.7525\(a\)](#). Boilers and process heaters that use a CO CEMS to comply with the applicable alternative CO CEMS emission standard listed in Tables 1, 2, or 11 through 13 to this subpart, as specified in [§ 63.7525\(a\)](#), are exempt from the initial CO performance testing and oxygen concentration operating limit requirements specified in [paragraph \(a\)](#) of this section.

(d) If your boiler or process heater is subject to a PM limit, your initial compliance demonstration for PM is to conduct a performance test in accordance with [§ 63.7520](#) and Table 5 to this subpart.

(e) For existing affected sources (as defined in [§ 63.7490](#)), you must complete the initial compliance demonstrations, as specified in [paragraphs \(a\)](#) through [\(d\)](#) of this section, no later than 180 days after the compliance date that is specified for your source in [§ 63.7495](#) and according to the applicable provisions in [§ 63.7\(a\)\(2\)](#) as cited in Table 10 to this subpart, except as specified in [paragraph \(j\)](#) of this section. You must complete an initial tune-up by following the procedures described in [§ 63.7540\(a\)\(10\)\(i\)](#) through [\(vi\)](#) no later than the compliance date specified in [§ 63.7495](#), except as specified in [paragraph \(j\)](#) of this section. You must complete the one-time energy assessment specified in Table 3 to this subpart no later than the compliance date specified in [§ 63.7495](#).

(f) For new or reconstructed affected sources (as defined in [§ 63.7490](#)), you must complete the initial compliance demonstration with the emission limits no later than July 30, 2013 or within 180 days after startup of the source, whichever is later. If you are demonstrating compliance with an emission limit in Tables 11 through 13 to this subpart that is less stringent (that is, higher) than the applicable emission limit in Table 1 to this subpart, you must demonstrate compliance with the applicable emission limit in Table 1 no later than July 29, 2016.

(g) For new or reconstructed affected sources (as defined in [§ 63.7490](#)), you must demonstrate initial compliance with the applicable work practice standards in Table 3 to this subpart within the applicable annual, biennial, or 5-year schedule as specified in [§ 63.7515\(d\)](#) following the initial compliance date specified in [§ 63.7495\(a\)](#). Thereafter, you are required to complete the applicable annual, biennial, or 5-year tune-up as specified in [§ 63.7515\(d\)](#).

(h) For affected sources (as defined in [§ 63.7490](#)) that ceased burning solid waste consistent with [§ 63.7495\(e\)](#) and for which the initial compliance date has passed, you must demonstrate

compliance within 60 days of the effective date of the waste-to-fuel switch. If you have not conducted your compliance demonstration for this subpart within the previous 12 months, you must complete all compliance demonstrations for this subpart before you commence or recommence combustion of solid waste.

(i) For an existing EGU that becomes subject after January 31, 2016, you must demonstrate compliance within 180 days after becoming an affected source.

(j) For existing affected sources (as defined in [§ 63.7490](#)) that have not operated between the effective date of the rule and the compliance date that is specified for your source in [§ 63.7495](#), you must complete the initial compliance demonstration, if subject to the emission limits in Table 2 to this subpart, as specified in [paragraphs \(a\)](#) through [\(d\)](#) of this section, no later than 180 days after the re-start of the affected source and according to the applicable provisions in [§ 63.7\(a\)\(2\)](#) as cited in Table 10 to this subpart. You must complete an initial tune-up by following the procedures described in [§ 63.7540\(a\)\(10\)\(i\)](#) through [\(vi\)](#) no later than 30 days after the re-start of the affected source and, if applicable, complete the one-time energy assessment specified in Table 3 to this subpart, no later than the compliance date specified in [§ 63.7495](#).

(k) For affected sources, as defined in [§ 63.7490](#), that switch subcategories consistent with [§ 63.7545\(h\)](#) after the initial compliance date, you must demonstrate compliance within 60 days of the effective date of the switch, unless you had previously conducted your compliance demonstration for this subcategory within the previous 12 months.

[[78 FR 7164](#), Jan. 31, 2013, as amended at [80 FR 72808](#), Nov. 20, 2015]

§ 63.7515 When must I conduct subsequent performance tests, fuel analyses, or tune-ups?

(a) You must conduct all applicable performance tests according to [§ 63.7520](#) on an annual basis, except as specified in [paragraphs \(b\)](#) through [\(e\)](#), [\(g\)](#), and [\(h\)](#) of this section. Annual performance tests must be completed no more than 13 months after the previous performance test, except as specified in [paragraphs \(b\)](#) through [\(e\)](#), [\(g\)](#), and [\(h\)](#) of this section.

(b) If your performance tests for a given pollutant for at least 2 consecutive years show that your emissions are at or below 75 percent of the emission limit (or, in limited instances as specified in Tables 1 and 2 or 11 through 13 to this subpart, at or below the emission limit) for the pollutant, and if there are no changes in the operation of the individual boiler or process heater or air pollution control equipment that could increase emissions, you may choose to conduct performance tests for the pollutant every third year. Each such performance test must be conducted no more than 37 months after the previous performance test. If you elect to demonstrate compliance using emission averaging under [§ 63.7522](#), you must continue to conduct performance tests annually. The requirement to test at maximum chloride input level is waived unless the stack test is conducted for HCl. The requirement to test at maximum

mercury input level is waived unless the stack test is conducted for mercury. The requirement to test at maximum TSM input level is waived unless the stack test is conducted for TSM.

(c) If a performance test shows emissions exceeded the emission limit or 75 percent of the emission limit (as specified in Tables 1 and 2 or 11 through 13 to this subpart) for a pollutant, you must conduct annual performance tests for that pollutant until all performance tests over a consecutive 2-year period meet the required level (at or below 75 percent of the emission limit, as specified in Tables 1 and 2 or 11 through 13 to this subpart).

(d) If you are required to meet an applicable tune-up work practice standard, you must conduct an annual, biennial, or 5-year performance tune-up according to [§ 63.7540\(a\)\(10\)](#), [\(11\)](#), or [\(12\)](#), respectively. Each annual tune-up specified in [§ 63.7540\(a\)\(10\)](#) must be no more than 13 months after the previous tune-up. Each biennial tune-up specified in [§ 63.7540\(a\)\(11\)](#) must be conducted no more than 25 months after the previous tune-up. Each 5-year tune-up specified in [§ 63.7540\(a\)\(12\)](#) must be conducted no more than 61 months after the previous tune-up. For a new or reconstructed affected source (as defined in [§ 63.7490](#)), the first annual, biennial, or 5-year tune-up must be no later than 13 months, 25 months, or 61 months, respectively, after April 1, 2013 or the initial startup of the new or reconstructed affected source, whichever is later.

(e) If you demonstrate compliance with the mercury, HCl, or TSM based on fuel analysis, you must conduct a monthly fuel analysis according to [§ 63.7521](#) for each type of fuel burned that is subject to an emission limit in Tables 1, 2, or 11 through 13 to this subpart. You may comply with this monthly requirement by completing the fuel analysis any time within the calendar month as long as the analysis is separated from the previous analysis by at least 14 calendar days. If you burn a new type of fuel, you must conduct a fuel analysis before burning the new type of fuel in your boiler or process heater. You must still meet all applicable continuous compliance requirements in [§ 63.7540](#). If each of 12 consecutive monthly fuel analyses demonstrates 75 percent or less of the compliance level, you may decrease the fuel analysis frequency to quarterly for that fuel. If any quarterly sample exceeds 75 percent of the compliance level or you begin burning a new type of fuel, you must return to monthly monitoring for that fuel, until 12 months of fuel analyses are again less than 75 percent of the compliance level. If sampling is conducted on one day per month, samples should be no less than 14 days apart, but if multiple samples are taken per month, the 14-day restriction does not apply.

(f) You must report the results of performance tests and the associated fuel analyses within 60 days after the completion of the performance tests. This report must also verify that the operating limits for each boiler or process heater have not changed or provide documentation of revised operating limits established according to [§ 63.7530](#) and Table 7 to this subpart, as applicable. The reports for all subsequent performance tests must include all applicable information required in [§ 63.7550](#).

(g) For affected sources (as defined in [§ 63.7490](#)) that have not operated since the previous compliance demonstration and more than one year has passed since the previous compliance demonstration, you must complete the subsequent compliance demonstration, if subject to the

emission limits in Tables 1, 2, or 11 through 13 to this subpart, no later than 180 days after the re-start of the affected source and according to the applicable provisions in [§ 63.7\(a\)\(2\)](#) as cited in Table 10 to this subpart. You must complete a subsequent tune-up by following the procedures described in [§ 63.7540\(a\)\(10\)\(i\)](#) through [\(vi\)](#) and the schedule described in [§ 63.7540\(a\)\(13\)](#) for units that are not operating at the time of their scheduled tune-up.

(h) If your affected boiler or process heater is in the unit designed to burn light liquid subcategory and you combust ultra-low sulfur liquid fuel, you do not need to conduct further performance tests (stack tests or fuel analyses) if the pollutants measured during the initial compliance performance tests meet the emission limits in Tables 1 or 2 of this subpart providing you demonstrate ongoing compliance with the emissions limits by monitoring and recording the type of fuel combusted on a monthly basis. If you intend to use a fuel other than ultra-low sulfur liquid fuel, natural gas, refinery gas, or other gas 1 fuel, you must conduct new performance tests within 60 days of burning the new fuel type.

(i) If you operate a CO CEMS that meets the Performance Specifications outlined in [§ 63.7525\(a\)\(3\) of this subpart](#) to demonstrate compliance with the applicable alternative CO CEMS emission standard listed in Tables 1, 2, or 11 through 13 to this subpart, you are not required to conduct CO performance tests and are not subject to the oxygen concentration operating limit requirement specified in [§ 63.7510\(a\)](#).

[[78 FR 7165](#), Jan. 31, 2013, as amended at [80 FR 72808](#), Nov. 20, 2015]

§ 63.7520 What stack tests and procedures must I use?

(a) You must conduct all performance tests according to [§ 63.7\(c\)](#), [\(d\)](#), [\(f\)](#), and [\(h\)](#). You must also develop a site-specific stack test plan according to the requirements in [§ 63.7\(c\)](#). You shall conduct all performance tests under such conditions as the Administrator specifies to you based on the representative performance of each boiler or process heater for the period being tested. Upon request, you shall make available to the Administrator such records as may be necessary to determine the conditions of the performance tests.

(b) You must conduct each performance test according to the requirements in Table 5 to this subpart.

(c) You must conduct each performance test under the specific conditions listed in Tables 5 and 7 to this subpart. You must conduct performance tests at representative operating load conditions while burning the type of fuel or mixture of fuels that has the highest content of chlorine and mercury, and TSM if you are opting to comply with the TSM alternative standard and you must demonstrate initial compliance and establish your operating limits based on these performance tests. These requirements could result in the need to conduct more than one performance test. Following each performance test and until the next performance test, you must comply with the operating limit for operating load conditions specified in Table 4 to this subpart.

(d) You must conduct a minimum of three separate test runs for each performance test required in this section, as specified in [§ 63.7\(e\)\(3\)](#). Each test run must comply with the minimum applicable sampling times or volumes specified in Tables 1 and 2 or 11 through 13 to this subpart.

(e) To determine compliance with the emission limits, you must use the F-Factor methodology and equations in sections 12.2 and 12.3 of EPA Method 19 at [40 CFR part 60, appendix A-7](#) of this chapter to convert the measured particulate matter (PM) concentrations, the measured HCl concentrations, the measured mercury concentrations, and the measured TSM concentrations that result from the performance test to pounds per million Btu heat input emission rates.

(f) Except for a 30-day rolling average based on CEMS (or sorbent trap monitoring system) data, if measurement results for any pollutant are reported as below the method detection level (e.g., laboratory analytical results for one or more sample components are below the method defined analytical detection level), you must use the method detection level as the measured emissions level for that pollutant in calculating compliance. The measured result for a multiple component analysis (e.g., analytical values for multiple Method 29 fractions both for individual HAP metals and for total HAP metals) may include a combination of method detection level data and analytical data reported above the method detection level.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7166](#), Jan. 31, 2013]

§ 63.7521 What fuel analyses, fuel specification, and procedures must I use?

(a) For solid and liquid fuels, you must conduct fuel analyses for chloride and mercury according to the procedures in [paragraphs \(b\) through \(e\)](#) of this section and Table 6 to this subpart, as applicable. For solid fuels and liquid fuels, you must also conduct fuel analyses for TSM if you are opting to comply with the TSM alternative standard. For gas 2 (other) fuels, you must conduct fuel analyses for mercury according to the procedures in [paragraphs \(b\) through \(e\)](#) of this section and Table 6 to this subpart, as applicable. (For gaseous fuels, you may not use fuel analyses to comply with the TSM alternative standard or the HCl standard.) For purposes of complying with this section, a fuel gas system that consists of multiple gaseous fuels collected and mixed with each other is considered a single fuel type and sampling and analysis is only required on the combined fuel gas system that will feed the boiler or process heater. Sampling and analysis of the individual gaseous streams prior to combining is not required. You are not required to conduct fuel analyses for fuels used for only startup, unit shutdown, and transient flame stability purposes. You are required to conduct fuel analyses only for fuels and units that are subject to emission limits for mercury, HCl, or TSM in Tables 1 and 2 or 11 through 13 to this subpart. Gaseous and liquid fuels are exempt from the sampling requirements in [paragraphs \(c\) and \(d\)](#) of this section.

(b) You must develop a site-specific fuel monitoring plan according to the following procedures and requirements in [paragraphs \(b\)\(1\) and \(2\)](#) of this section, if you are required to conduct fuel analyses as specified in [§ 63.7510](#).

(1) If you intend to use an alternative analytical method other than those required by Table 6 to this subpart, you must submit the fuel analysis plan to the Administrator for review and approval no later than 60 days before the date that you intend to conduct the initial compliance demonstration described in [§ 63.7510](#).

(2) You must include the information contained in [paragraphs \(b\)\(2\)\(i\)](#) through [\(vi\)](#) of this section in your fuel analysis plan.

(i) The identification of all fuel types anticipated to be burned in each boiler or process heater.

(ii) For each anticipated fuel type, the notification of whether you or a fuel supplier will be conducting the fuel analysis.

(iii) For each anticipated fuel type, a detailed description of the sample location and specific procedures to be used for collecting and preparing the composite samples if your procedures are different from [paragraph \(c\)](#) or [\(d\)](#) of this section. Samples should be collected at a location that most accurately represents the fuel type, where possible, at a point prior to mixing with other dissimilar fuel types.

(iv) For each anticipated fuel type, the analytical methods from Table 6, with the expected minimum detection levels, to be used for the measurement of chlorine or mercury.

(v) If you request to use an alternative analytical method other than those required by Table 6 to this subpart, you must also include a detailed description of the methods and procedures that you are proposing to use. Methods in Table 6 shall be used until the requested alternative is approved.

(vi) If you will be using fuel analysis from a fuel supplier in lieu of site-specific sampling and analysis, the fuel supplier must use the analytical methods required by Table 6 to this subpart.

(c) You must obtain composite fuel samples for each fuel type according to the procedures in [paragraph \(c\)\(1\)](#) or [\(2\)](#) of this section, or the methods listed in Table 6 to this subpart, or use an automated sampling mechanism that provides representative composite fuel samples for each fuel type that includes both coarse and fine material. At a minimum, for demonstrating initial compliance by fuel analysis, you must obtain three composite samples. For monthly fuel analyses, at a minimum, you must obtain a single composite sample. For fuel analyses as part of a performance stack test, as specified in [§ 63.7510\(a\)](#), you must obtain a composite fuel sample during each performance test run.

(1) If sampling from a belt (or screw) feeder, collect fuel samples according to [paragraphs \(c\)\(1\)\(i\)](#) and [\(ii\)](#) of this section.

(i) Stop the belt and withdraw a 6-inch wide sample from the full cross-section of the stopped belt to obtain a minimum two pounds of sample. You must collect all the material

(fines and coarse) in the full cross-section. You must transfer the sample to a clean plastic bag.

(ii) Each composite sample will consist of a minimum of three samples collected at approximately equal one-hour intervals during the testing period for sampling during performance stack testing.

(2) If sampling from a fuel pile or truck, you must collect fuel samples according to [paragraphs \(c\)\(2\)\(i\)](#) through [\(iii\)](#) of this section.

(i) For each composite sample, you must select a minimum of five sampling locations uniformly spaced over the surface of the pile.

(ii) At each sampling site, you must dig into the pile to a uniform depth of approximately 18 inches. You must insert a clean shovel into the hole and withdraw a sample, making sure that large pieces do not fall off during sampling; use the same shovel to collect all samples.

(iii) You must transfer all samples to a clean plastic bag for further processing.

(d) You must prepare each composite sample according to the procedures in [paragraphs \(d\)\(1\)](#) through [\(7\)](#) of this section.

(1) You must thoroughly mix and pour the entire composite sample over a clean plastic sheet.

(2) You must break large sample pieces (e.g., larger than 3 inches) into smaller sizes.

(3) You must make a pie shape with the entire composite sample and subdivide it into four equal parts.

(4) You must separate one of the quarter samples as the first subset.

(5) If this subset is too large for grinding, you must repeat the procedure in [paragraph \(d\)\(3\)](#) of this section with the quarter sample and obtain a one-quarter subset from this sample.

(6) You must grind the sample in a mill.

(7) You must use the procedure in [paragraph \(d\)\(3\)](#) of this section to obtain a one-quarter subsample for analysis. If the quarter sample is too large, subdivide it further using the same procedure.

(e) You must determine the concentration of pollutants in the fuel (mercury and/or chlorine and/or TSM) in units of pounds per million Btu of each composite sample for each fuel type according to the procedures in Table 6 to this subpart, for use in Equations 7, 8, and 9 of this subpart.

(f) To demonstrate that a gaseous fuel other than natural gas or refinery gas qualifies as an other gas 1 fuel, as defined in [§ 63.7575](#), you must conduct a fuel specification analyses for mercury according to the procedures in [paragraphs \(g\)](#) through [\(i\)](#) of this section and Table 6 to this subpart, as applicable, except as specified in [paragraph \(f\)\(1\)](#) through [\(4\)](#) of this section, or as an alternative where fuel specification analysis is not practical, you must measure mercury concentration in the exhaust gas when firing only the gaseous fuel to be demonstrated as an other gas 1 fuel in the boiler or process heater according to the procedures in Table 6 to this subpart.

(1) You are not required to conduct the fuel specification analyses in [paragraphs \(g\)](#) through [\(i\)](#) of this section for natural gas or refinery gas.

(2) You are not required to conduct the fuel specification analyses in [paragraphs \(g\)](#) through [\(i\)](#) of this section for gaseous fuels that are subject to another subpart of this part, part 60, part 61, or part 65.

(3) You are not required to conduct the fuel specification analyses in [paragraphs \(g\)](#) through [\(i\)](#) of this section on gaseous fuels for units that are complying with the limits for units designed to burn gas 2 (other) fuels.

(4) You are not required to conduct the fuel specification analyses in [paragraphs \(g\)](#) through [\(i\)](#) of this section for gas streams directly derived from natural gas at natural gas production sites or natural gas plants.

(g) You must develop a site-specific fuel analysis plan for other gas 1 fuels according to the following procedures and requirements in [paragraphs \(g\)\(1\)](#) and [\(2\)](#) of this section.

(1) If you intend to use an alternative analytical method other than those required by Table 6 to this subpart, you must submit the fuel analysis plan to the Administrator for review and approval no later than 60 days before the date that you intend to conduct the initial compliance demonstration described in [§ 63.7510](#).

(2) You must include the information contained in [paragraphs \(g\)\(2\)\(i\)](#) through [\(vi\)](#) of this section in your fuel analysis plan.

(i) The identification of all gaseous fuel types other than those exempted from fuel specification analysis under [\(f\)\(1\)](#) through [\(3\)](#) of this section anticipated to be burned in each boiler or process heater.

(ii) For each anticipated fuel type, the identification of whether you or a fuel supplier will be conducting the fuel specification analysis.

(iii) For each anticipated fuel type, a detailed description of the sample location and specific procedures to be used for collecting and preparing the samples if your procedures are different from the sampling methods contained in Table 6 to this subpart. Samples should be collected at a location that most accurately represents the fuel type, where

possible, at a point prior to mixing with other dissimilar fuel types. If multiple boilers or process heaters are fueled by a common fuel stream it is permissible to conduct a single gas specification at the common point of gas distribution.

(iv) For each anticipated fuel type, the analytical methods from Table 6 to this subpart, with the expected minimum detection levels, to be used for the measurement of mercury.

(v) If you request to use an alternative analytical method other than those required by Table 6 to this subpart, you must also include a detailed description of the methods and procedures that you are proposing to use. Methods in Table 6 to this subpart shall be used until the requested alternative is approved.

(vi) If you will be using fuel analysis from a fuel supplier in lieu of site-specific sampling and analysis, the fuel supplier must use the analytical methods required by Table 6 to this subpart. When using a fuel supplier's fuel analysis, the owner or operator is not required to submit the information in [§ 63.7521\(g\)\(2\)\(iii\)](#).

(h) You must obtain a single fuel sample for each fuel type for fuel specification of gaseous fuels.

(i) You must determine the concentration in the fuel of mercury, in units of microgram per cubic meter, dry basis, of each sample for each other gas 1 fuel type according to the procedures in Table 6 to this subpart.

[[78 FR 7167](#), Jan. 31, 2013, as amended at [80 FR 72808](#), Nov. 20, 2015]

§ 63.7522 Can I use emissions averaging to comply with this subpart?

(a) As an alternative to meeting the requirements of [§ 63.7500](#) for PM (or TSM), HCl, or mercury on a boiler or process heater-specific basis, if you have more than one existing boiler or process heater in any subcategories located at your facility, you may demonstrate compliance by emissions averaging, if your averaged emissions are not more than 90 percent of the applicable emission limit, according to the procedures in this section. You may not include new boilers or process heaters in an emissions average.

(b) For a group of two or more existing boilers or process heaters in the same subcategory that each vent to a separate stack, you may average PM (or TSM), HCl, or mercury emissions among existing units to demonstrate compliance with the limits in Table 2 to this subpart as specified in [paragraph \(b\)\(1\)](#) through [\(3\)](#) of this section, if you satisfy the requirements in [paragraphs \(c\)](#) through [\(g\)](#) of this section.

(1) You may average units using a CEMS or PM CPMS for demonstrating compliance.

(2) For mercury and HCl, averaging is allowed as follows:

- (i) You may average among units in any of the solid fuel subcategories.
- (ii) You may average among units in any of the liquid fuel subcategories.
- (iii) You may average among units in a subcategory of units designed to burn gas 2 (other) fuels.
- (iv) You may not average across the units designed to burn liquid, units designed to burn solid fuel, and units designed to burn gas 2 (other) subcategories.

(3) For PM (or TSM), averaging is only allowed between units within each of the following subcategories and you may not average across subcategories:

- (i) Units designed to burn coal/solid fossil fuel.
- (ii) Stokers/sloped grate/other units designed to burn kiln dried biomass/bio-based solids.
- (iii) Stokers/sloped grate/other units designed to burn wet biomass/bio-based solids.
- (iv) Fluidized bed units designed to burn biomass/bio-based solid.
- (v) Suspension burners designed to burn biomass/bio-based solid.
- (vi) Dutch ovens/pile burners designed to burn biomass/bio-based solid.
- (vii) Fuel Cells designed to burn biomass/bio-based solid.
- (viii) Hybrid suspension/grate burners designed to burn wet biomass/bio-based solid.
- (ix) Units designed to burn heavy liquid fuel.
- (x) Units designed to burn light liquid fuel.
- (xi) Units designed to burn liquid fuel that are non-continental units.
- (xii) Units designed to burn gas 2 (other) gases.

(c) For each existing boiler or process heater in the averaging group, the emission rate achieved during the initial compliance test for the HAP being averaged must not exceed the emission level that was being achieved on April 1, 2013 or the control technology employed during the initial compliance test must not be less effective for the HAP being averaged than the control technology employed on April 1, 2013.

(d) The averaged emissions rate from the existing boilers and process heaters participating in the emissions averaging option must not exceed 90 percent of the limits in Table 2 to this

subpart at all times the affected units are subject to numeric emission limits following the compliance date specified in [§ 63.7495](#).

(e) You must demonstrate initial compliance according to [paragraph \(e\)\(1\)](#) or [\(2\)](#) of this section using the maximum rated heat input capacity or maximum steam generation capacity of each unit and the results of the initial performance tests or fuel analysis.

(1) You must use Equation 1a or 1b or 1c of this section to demonstrate that the PM (or TSM), HCl, or mercury emissions from all existing units participating in the emissions averaging option for that pollutant do not exceed the emission limits in Table 2 to this subpart. Use Equation 1a if you are complying with the emission limits on a heat input basis, use Equation 1b if you are complying with the emission limits on a steam generation (output) basis, and use Equation 1c if you are complying with the emission limits on a electric generation (output) basis.

$$AveWeightedEmissions = 1.1 \times \sum_{i=1}^n (Er \times Hm) \div \sum_{i=1}^n Hm \quad (Eq. 1a)$$

Where:

AveWeightedEmissions = Average weighted emissions for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of heat input.

Er = Emission rate (as determined during the initial compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per million Btu of heat input. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM using the applicable equation in [§ 63.7530\(c\)](#).

Hm = Maximum rated heat input capacity of unit, i, in units of million Btu per hour.

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

$$AveWeightedEmissions = 1.1 \times \sum_{i=1}^n (Er \times So) \div \sum_{i=1}^n So \quad (Eq. 1b)$$

Where:

AveWeightedEmissions = Average weighted emissions for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of steam output.

E_r = Emission rate (as determined during the initial compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i , in units of pounds per million Btu of steam output. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM using the applicable equation in [§ 63.7530\(c\)](#). If you are taking credit for energy conservation measures from a unit according to [§ 63.7533](#), use the adjusted emission level for that unit, E_{adj} , determined according to [§ 63.7533](#) for that unit.

S_o = Maximum steam output capacity of unit, i , in units of million Btu per hour, as defined in [§ 63.7575](#).

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

$$AveWeightedEmissions = 1.1 \times \sum_{i=1}^n (E_r \times E_o) \div \sum_{i=1}^n E_o \quad (Eq. 2)$$

Where:

$AveWeightedEmissions$ = Average weighted emissions for PM (or TSM), HCl, or mercury, in units of pounds per megawatt hour.

E_r = Emission rate (as determined during the initial compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i , in units of pounds per megawatt hour. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM using the applicable equation in [§ 63.7530\(c\)](#). If you are taking credit for energy conservation measures from a unit according to [§ 63.7533](#), use the adjusted emission level for that unit, E_{adj} , determined according to [§ 63.7533](#) for that unit.

E_o = Maximum electric generating output capacity of unit, i , in units of megawatt hour, as defined in [§ 63.7575](#).

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

(2) If you are not capable of determining the maximum rated heat input capacity of one or more boilers that generate steam, you may use Equation 2 of this section as an alternative to using Equation 1a of this section to demonstrate that the PM (or TSM), HCl, or mercury emissions from all existing units participating in the emissions averaging option do not exceed the emission limits for that pollutant in Table 2 to this subpart that are in pounds per million Btu of heat input.

$$AveWeightedEmissions = 1.1 \times \sum_{i=1}^n (Er \times Sm \times Cfi) \div \sum_{i=1}^n (Sm \times Cfi) \quad (Eq. 3a)$$

Where:

AveWeightedEmissions = Average weighted emission level for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of heat input.

Er = Emission rate (as determined during the most recent compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per million Btu of heat input. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM using the applicable equation in [§ 63.7530\(c\)](#).

Sm = Maximum steam generation capacity by unit, i, in units of pounds per hour.

Cfi = Conversion factor, calculated from the most recent compliance test, in units of million Btu of heat input per pounds of steam generated for unit, i.

1.1 = Required discount factor.

(f) After the initial compliance demonstration described in [paragraph \(e\)](#) of this section, you must demonstrate compliance on a monthly basis determined at the end of every month (12 times per year) according to [paragraphs \(f\)\(1\)](#) through [\(3\)](#) of this section. The first monthly period begins on the compliance date specified in [§ 63.7495](#). If the affected source elects to collect monthly data for up to the 11 months preceding the first monthly period, these additional data points can be used to compute the 12-month rolling average in [paragraph \(f\)\(3\)](#) of this section.

(1) For each calendar month, you must use Equation 3a or 3b or 3c of this section to calculate the average weighted emission rate for that month. Use Equation 3a and the actual heat input for the month for each existing unit participating in the emissions averaging option if you are complying with emission limits on a heat input basis. Use Equation 3b and the actual steam generation for the month if you are complying with the emission limits on a steam generation (output) basis. Use Equation 3c and the actual electrical generation for the month if you are complying with the emission limits on an electrical generation (output) basis.

$$AveWeightedEmissions = 1.1 \times \sum_{i=1}^n (Er \times Hb) \div \sum_{i=1}^n Hb \quad (Eq. 3b)$$

Where:

AveWeightedEmissions = Average weighted emission level for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of heat input, for that calendar month.

Er = Emission rate (as determined during the most recent compliance demonstration) of PM (or TSM), HCl, or mercury from unit, *i*, in units of pounds per million Btu of heat input. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM according to Table 6 to this subpart.

Hb = The heat input for that calendar month to unit, *i*, in units of million Btu.

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

$$AveWeightedEmissions = 1.1 \times \sum_{i=1}^n (Er \times So) \div \sum_{i=1}^n So \quad (\text{Eq. 3b})$$

Where:

AveWeightedEmissions = Average weighted emission level for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of steam output, for that calendar month.

Er = Emission rate (as determined during the most recent compliance demonstration) of PM (or TSM), HCl, or mercury from unit, *i*, in units of pounds per million Btu of steam output. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM according to Table 6 to this subpart. If you are taking credit for energy conservation measures from a unit according to [§ 63.7533](#), use the adjusted emission level for that unit, *E_{adj}*, determined according to [§ 63.7533](#) for that unit.

So = The steam output for that calendar month from unit, *i*, in units of million Btu, as defined in [§ 63.7575](#).

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

$$AveWeightedEmissions = 1.1 \times \sum_{i=1}^n (Er \times Eo) \div \sum_{i=1}^n Eo \quad (\text{Eq. 3c})$$

Where:

AveWeightedEmissions = Average weighted emission level for PM (or TSM), HCl, or mercury, in units of pounds per megawatt hour, for that calendar month.

Er = Emission rate (as determined during the most recent compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per megawatt hour. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM according to Table 6 to this subpart. If you are taking credit for energy conservation measures from a unit according to [§ 63.7533](#), use the adjusted emission level for that unit, E_{adj}, determined according to [§ 63.7533](#) for that unit.

Eo = The electric generating output for that calendar month from unit, i, in units of megawatt hour, as defined in [§ 63.7575](#).

n = Number of units participating in the emissions averaging option.

1.1 = Required discount factor.

(2) If you are not capable of monitoring heat input, you may use Equation 4 of this section as an alternative to using Equation 3a of this section to calculate the average weighted emission rate using the actual steam generation from the boilers participating in the emissions averaging option.

$$AveWeightedEmissions = 1.1 \times \sum_{i=1}^n (Er \times Sa \times Cfi) \div \sum_{i=1}^n (Sa \times Cfi)$$

Where:

AveWeightedEmissions = average weighted emission level for PM (or TSM), HCl, or mercury, in units of pounds per million Btu of heat input for that calendar month.

Er = Emission rate (as determined during the most recent compliance demonstration) of PM (or TSM), HCl, or mercury from unit, i, in units of pounds per million Btu of heat input. Determine the emission rate for PM (or TSM), HCl, or mercury by performance testing according to Table 5 to this subpart, or by fuel analysis for HCl or mercury or TSM according to Table 6 to this subpart.

Sa = Actual steam generation for that calendar month by boiler, i, in units of pounds.

Cfi = Conversion factor, as calculated during the most recent compliance test, in units of million Btu of heat input per pounds of steam generated for boiler, i.

1.1 = Required discount factor.

(3) Until 12 monthly weighted average emission rates have been accumulated, calculate and report only the average weighted emission rate determined under [paragraph \(f\)\(1\)](#) or [\(2\)](#) of

this section for each calendar month. After 12 monthly weighted average emission rates have been accumulated, for each subsequent calendar month, use Equation 5 of this section to calculate the 12-month rolling average of the monthly weighted average emission rates for the current calendar month and the previous 11 calendar months.

$$E_{avg} = \sum_{i=1}^n ERI \div 12 \quad (\text{Eq. 5})$$

Where:

E_{avg} = 12-month rolling average emission rate, (pounds per million Btu heat input)

ERI = Monthly weighted average, for calendar month “i” (pounds per million Btu heat input), as calculated by [paragraph \(f\)\(1\)](#) or [\(2\)](#) of this section.

(g) You must develop, and submit upon request to the applicable Administrator for review and approval, an implementation plan for emission averaging according to the following procedures and requirements in [paragraphs \(g\)\(1\)](#) through [\(4\)](#) of this section.

(1) If requested, you must submit the implementation plan no later than 180 days before the date that the facility intends to demonstrate compliance using the emission averaging option.

(2) You must include the information contained in [paragraphs \(g\)\(2\)\(i\)](#) through [\(vii\)](#) of this section in your implementation plan for all emission sources included in an emissions average:

(i) The identification of all existing boilers and process heaters in the averaging group, including for each either the applicable HAP emission level or the control technology installed as of January 31, 2013 and the date on which you are requesting emission averaging to commence;

(ii) The process parameter (heat input or steam generated) that will be monitored for each averaging group;

(iii) The specific control technology or pollution prevention measure to be used for each emission boiler or process heater in the averaging group and the date of its installation or application. If the pollution prevention measure reduces or eliminates emissions from multiple boilers or process heaters, the owner or operator must identify each boiler or process heater;

(iv) The test plan for the measurement of PM (or TSM), HCl, or mercury emissions in accordance with the requirements in [§ 63.7520](#);

(v) The operating parameters to be monitored for each control system or device consistent with [§ 63.7500](#) and Table 4, and a description of how the operating limits will be determined;

(vi) If you request to monitor an alternative operating parameter pursuant to [§ 63.7525](#), you must also include:

(A) A description of the parameter(s) to be monitored and an explanation of the criteria used to select the parameter(s); and

(B) A description of the methods and procedures that will be used to demonstrate that the parameter indicates proper operation of the control device; the frequency and content of monitoring, reporting, and recordkeeping requirements; and a demonstration, to the satisfaction of the Administrator, that the proposed monitoring frequency is sufficient to represent control device operating conditions; and

(vii) A demonstration that compliance with each of the applicable emission limit(s) will be achieved under representative operating load conditions. Following each compliance demonstration and until the next compliance demonstration, you must comply with the operating limit for operating load conditions specified in Table 4 to this subpart.

(3) If submitted upon request, the Administrator shall review and approve or disapprove the plan according to the following criteria:

(i) Whether the content of the plan includes all of the information specified in [paragraph \(g\)\(2\)](#) of this section; and

(ii) Whether the plan presents sufficient information to determine that compliance will be achieved and maintained.

(4) The applicable Administrator shall not approve an emission averaging implementation plan containing any of the following provisions:

(i) Any averaging between emissions of differing pollutants or between differing sources; or

(ii) The inclusion of any emission source other than an existing unit in the same subcategories.

(h) For a group of two or more existing affected units, each of which vents through a single common stack, you may average PM (or TSM), HCl, or mercury emissions to demonstrate compliance with the limits for that pollutant in Table 2 to this subpart if you satisfy the requirements in [paragraph \(i\)](#) or [\(j\)](#) of this section.

(i) For a group of two or more existing units in the same subcategory, each of which vents through a common emissions control system to a common stack, that does not receive

emissions from units in other subcategories or categories, you may treat such averaging group as a single existing unit for purposes of this subpart and comply with the requirements of this subpart as if the group were a single unit.

(j) For all other groups of units subject to the common stack requirements of [paragraph \(h\)](#) of this section, including situations where the exhaust of affected units are each individually controlled and then sent to a common stack, the owner or operator may elect to:

(1) Conduct performance tests according to procedures specified in [§ 63.7520](#) in the common stack if affected units from other subcategories vent to the common stack. The emission limits that the group must comply with are determined by the use of Equation 6 of this section.

$$En = \frac{\sum_{i=1}^n (ELi \times Hi)}{\sum_{i=1}^n Hi} \quad (\text{Eq. 6})$$

Where:

En = HAP emission limit, pounds per million British thermal units (lb/MMBtu) or parts per million (ppm).

Eli = Appropriate emission limit from Table 2 to this subpart for unit i, in units of lb/MMBtu or ppm.

Hi = Heat input from unit i, MMBtu.

(2) Conduct performance tests according to procedures specified in [§ 63.7520](#) in the common stack. If affected units and non-affected units vent to the common stack, the non-affected units must be shut down or vented to a different stack during the performance test unless the facility determines to demonstrate compliance with the non-affected units venting to the stack; and

(3) Meet the applicable operating limit specified in [§ 63.7540](#) and Table 8 to this subpart for each emissions control system (except that, if each unit venting to the common stack has an applicable opacity operating limit, then a single continuous opacity monitoring system may be located in the common stack instead of in each duct to the common stack).

(k) The common stack of a group of two or more existing boilers or process heaters in the same subcategories subject to [paragraph \(h\)](#) of this section may be treated as a separate stack for purposes of [paragraph \(b\)](#) of this section and included in an emissions averaging group subject to [paragraph \(b\)](#) of this section.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7168](#), Jan. 31, 2013; [80 FR 72809](#), Nov. 20, 2015]

§ 63.7525 What are my monitoring, installation, operation, and maintenance requirements?

(a) If your boiler or process heater is subject to a CO emission limit in Tables 1, 2, or 11 through 13 to this subpart, you must install, operate, and maintain an oxygen analyzer system, as defined in [§ 63.7575](#), or install, certify, operate and maintain continuous emission monitoring systems for CO and oxygen (or carbon dioxide (CO₂)) according to the procedures in [paragraphs \(a\)\(1\) through \(6\)](#) of this section.

(1) Install the CO CEMS and oxygen (or CO₂) analyzer by the compliance date specified in [§ 63.7495](#). The CO and oxygen (or CO₂) levels shall be monitored at the same location at the outlet of the boiler or process heater. An owner or operator may request an alternative test method under [§ 63.7 of this chapter](#), in order that compliance with the CO emissions limit be determined using CO₂ as a diluent correction in place of oxygen at 3 percent. EPA Method 19 F-factors and EPA Method 19 equations must be used to generate the appropriate CO₂ correction percentage for the fuel type burned in the unit, and must also take into account that the 3 percent oxygen correction is to be done on a dry basis. The alternative test method request must account for any CO₂ being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc.

(2) To demonstrate compliance with the applicable alternative CO CEMS emission standard listed in Tables 1, 2, or 11 through 13 to this subpart, you must install, certify, operate, and maintain a CO CEMS and an oxygen analyzer according to the applicable procedures under Performance Specification 4, 4A, or 4B at [40 CFR part 60, appendix B; part 75 of this chapter](#) (if an CO₂ analyzer is used); the site-specific monitoring plan developed according to [§ 63.7505\(d\)](#); and the requirements in [§ 63.7540\(a\)\(8\)](#) and [paragraph \(a\)](#) of this section. Any boiler or process heater that has a CO CEMS that is compliant with Performance Specification 4, 4A, or 4B at [40 CFR part 60, appendix B](#), a site-specific monitoring plan developed according to [§ 63.7505\(d\)](#), and the requirements in [§ 63.7540\(a\)\(8\)](#) and [paragraph \(a\)](#) of this section must use the CO CEMS to comply with the applicable alternative CO CEMS emission standard listed in Tables 1, 2, or 11 through 13 to this subpart.

(i) You must conduct a performance evaluation of each CO CEMS according to the requirements in [§ 63.8\(e\)](#) and according to Performance Specification 4, 4A, or 4B at [40 CFR part 60, appendix B](#).

(ii) During each relative accuracy test run of the CO CEMS, you must collect emission data for CO concurrently (or within a 30- to 60-minute period) by both the CO CEMS and by Method 10, 10A, or 10B at [40 CFR part 60, appendix A-4](#). The relative accuracy testing must be at representative operating conditions.

(iii) You must follow the quality assurance procedures (e.g., quarterly accuracy determinations and daily calibration drift tests) of Procedure 1 of appendix F to part 60. The measurement span value of the CO CEMS must be two times the applicable CO emission limit, expressed as a concentration.

(iv) Any CO CEMS that does not comply with [§ 63.7525\(a\)](#) cannot be used to meet any requirement in this subpart to demonstrate compliance with a CO emission limit listed in Tables 1, 2, or 11 through 13 to this subpart.

(v) For a new unit, complete the initial performance evaluation no later than July 30, 2013, or 180 days after the date of initial startup, whichever is later. For an existing unit, complete the initial performance evaluation no later than July 29, 2016.

(vi) When CO₂ is used to correct CO emissions and CO₂ is measured on a wet basis, correct for moisture as follows: Install, operate, maintain, and quality assure a continuous moisture monitoring system for measuring and recording the moisture content of the flue gases, in order to correct the measured hourly volumetric flow rates for moisture when calculating CO concentrations. The following continuous moisture monitoring systems are acceptable: A continuous moisture sensor; an oxygen analyzer (or analyzers) capable of measuring O₂ both on a wet basis and on a dry basis; or a stack temperature sensor and a moisture look-up table, *i.e.*, a psychrometric chart (for saturated gas streams following wet scrubbers or other demonstrably saturated gas streams, only). The moisture monitoring system shall include as a component the automated data acquisition and handling system (DAHS) for recording and reporting both the raw data (*e.g.*, hourly average wet-and dry basis O₂ values) and the hourly average values of the stack gas moisture content derived from those data. When a moisture look-up table is used, the moisture monitoring system shall be represented as a single component, the certified DAHS, in the monitoring plan for the unit or common stack.

(3) Complete a minimum of one cycle of CO and oxygen (or CO₂) CEMS operation (sampling, analyzing, and data recording) for each successive 15-minute period. Collect CO and oxygen (or CO₂) data concurrently. Collect at least four CO and oxygen (or CO₂) CEMS data values representing the four 15-minute periods in an hour, or at least two 15-minute data values during an hour when CEMS calibration, quality assurance, or maintenance activities are being performed.

(4) Reduce the CO CEMS data as specified in [§ 63.8\(g\)\(2\)](#).

(5) Calculate one-hour arithmetic averages, corrected to 3 percent oxygen (or corrected to an CO₂ percentage determined to be equivalent to 3 percent oxygen) from each hour of CO CEMS data in parts per million CO concentration. The one-hour arithmetic averages required shall be used to calculate the 30-day or 10-day rolling average emissions. Use Equation 19-19 in [section 12.4.1](#) of Method 19 of [40 CFR part 60, appendix A-7](#) for calculating the average CO concentration from the hourly values.

(6) For purposes of collecting CO data, operate the CO CEMS as specified in [§ 63.7535\(b\)](#). You must use all the data collected during all periods in calculating data averages and assessing compliance, except that you must exclude certain data as specified in [§ 63.7535\(c\)](#). Periods when CO data are unavailable may constitute monitoring deviations as specified in [§ 63.7535\(d\)](#).

(7) Operate an oxygen trim system with the oxygen level set no lower than the lowest hourly average oxygen concentration measured during the most recent CO performance test as the operating limit for oxygen according to Table 7 to this subpart.

(b) If your boiler or process heater is in the unit designed to burn coal/solid fossil fuel subcategory or the unit designed to burn heavy liquid subcategory and has an average annual heat input rate greater than 250 MMBtu per hour from solid fossil fuel and/or heavy liquid, and you demonstrate compliance with the PM limit instead of the alternative TSM limit, you must install, maintain, and operate a PM CPMS monitoring emissions discharged to the atmosphere and record the output of the system as specified in [paragraphs \(b\)\(1\) through \(4\)](#) of this section. As an alternative to use of a PM CPMS to demonstrate compliance with the PM limit, you may choose to use a PM CEMS. If you choose to use a PM CEMS to demonstrate compliance with the PM limit instead of the alternative TSM limit, you must install, certify, maintain, and operate a PM CEMS monitoring emissions discharged to the atmosphere and record the output of the system as specified in [paragraph \(b\)\(5\) through \(8\)](#) of this section. For other boilers or process heaters, you may elect to use a PM CPMS or PM CEMS operated in accordance with this section in lieu of using other CMS for monitoring PM compliance (*e.g.*, bag leak detectors, ESP secondary power, and PM scrubber pressure). Owners of boilers and process heaters who elect to comply with the alternative TSM limit are not required to install a PM CPMS.

(1) Install, operate, and maintain your PM CPMS according to the procedures in your approved site-specific monitoring plan developed in accordance with [§ 63.7505\(d\)](#), the requirements in [§ 63.7540\(a\)\(9\)](#), and [paragraphs \(b\)\(1\)\(i\) through \(iii\)](#) of this section.

(i) The operating principle of the PM CPMS must be based on in-stack or extractive light scatter, light scintillation, beta attenuation, or mass accumulation detection of PM in the exhaust gas or representative exhaust gas sample. The reportable measurement output from the PM CPMS must be expressed as milliamps.

(ii) The PM CPMS must have a cycle time (*i.e.*, period required to complete sampling, measurement, and reporting for each measurement) no longer than 60 minutes.

(iii) The PM CPMS must have a documented detection limit of 0.5 milligram per actual cubic meter, or less.

(2) For a new unit, complete the initial performance evaluation no later than July 30, 2013, or 180 days after the date of initial startup, whichever is later. For an existing unit, complete the initial performance evaluation no later than July 29, 2016.

(3) Collect PM CPMS hourly average output data for all boiler or process heater operating hours except as indicated in [§ 63.7535\(a\) through \(d\)](#). Express the PM CPMS output as milliamps.

(4) Calculate the arithmetic 30-day rolling average of all of the hourly average PM CPMS output data collected during all boiler or process heater operating hours (milliamps).

(5) Install, certify, operate, and maintain your PM CEMS according to the procedures in your approved site-specific monitoring plan developed in accordance with [§ 63.7505\(d\)](#), the requirements in [§ 63.7540\(a\)\(9\)](#), and [paragraphs \(b\)\(5\)\(i\) through \(iv\)](#) of this section.

(i) You shall conduct a performance evaluation of the PM CEMS according to the applicable requirements of [§ 60.8\(e\)](#), and Performance Specification 11 at [40 CFR part 60, appendix B](#) of this chapter.

(ii) During each PM correlation testing run of the CEMS required by Performance Specification 11 at [40 CFR part 60, appendix B](#) of this chapter, you shall collect PM and oxygen (or carbon dioxide) data concurrently (or within a 30-to 60-minute period) by both the CEMS and conducting performance tests using Method 5 at [40 CFR part 60, appendix A-3](#) or Method 17 at [40 CFR part 60, appendix A-6](#) of this chapter.

(iii) You shall perform quarterly accuracy determinations and daily calibration drift tests in accordance with Procedure 2 at [40 CFR part 60, appendix F](#) of this chapter. You must perform Relative Response Audits annually and perform Response Correlation Audits every 3 years.

(iv) Within 60 days after the date of completing each CEMS relative accuracy test audit or performance test conducted to demonstrate compliance with this subpart, you must submit the relative accuracy test audit data and performance test data to the EPA by successfully submitting the data electronically into the EPA's Central Data Exchange by using the Electronic Reporting Tool (see <http://www.epa.gov/ttn/chief/ert/erttool.html>).

(6) For a new unit, complete the initial performance evaluation no later than July 30, 2013, or 180 days after the date of initial startup, whichever is later. For an existing unit, complete the initial performance evaluation no later than July 29, 2016.

(7) Collect PM CEMS hourly average output data for all boiler or process heater operating hours except as indicated in [§ 63.7535\(a\)](#) through [\(d\)](#).

(8) Calculate the arithmetic 30-day rolling average of all of the hourly average PM CEMS output data collected during all boiler or process heater operating hours.

(c) If you have an applicable opacity operating limit in this rule, and are not otherwise required or elect to install and operate a PM CPMS, PM CEMS, or a bag leak detection system, you must install, operate, certify and maintain each COMS according to the procedures in [paragraphs \(c\)\(1\) through \(7\)](#) of this section by the compliance date specified in [§ 63.7495](#).

(1) Each COMS must be installed, operated, and maintained according to Performance Specification 1 at appendix B to [part 60 of this chapter](#).

(2) You must conduct a performance evaluation of each COMS according to the requirements in [§ 63.8\(e\)](#) and according to Performance Specification 1 at appendix B to [part 60 of this chapter](#).

(3) As specified in [§ 63.8\(c\)\(4\)\(i\)](#), each COMS must complete a minimum of one cycle of sampling and analyzing for each successive 10-second period and one cycle of data recording for each successive 6-minute period.

(4) The COMS data must be reduced as specified in [§ 63.8\(g\)\(2\)](#).

(5) You must include in your site-specific monitoring plan procedures and acceptance criteria for operating and maintaining each COMS according to the requirements in [§ 63.8\(d\)](#). At a minimum, the monitoring plan must include a daily calibration drift assessment, a quarterly performance audit, and an annual zero alignment audit of each COMS.

(6) You must operate and maintain each COMS according to the requirements in the monitoring plan and the requirements of [§ 63.8\(e\)](#). You must identify periods the COMS is out of control including any periods that the COMS fails to pass a daily calibration drift assessment, a quarterly performance audit, or an annual zero alignment audit. Any 6-minute period for which the monitoring system is out of control and data are not available for a required calculation constitutes a deviation from the monitoring requirements.

(7) You must determine and record all the 6-minute averages (and daily block averages as applicable) collected for periods during which the COMS is not out of control.

(d) If you have an operating limit that requires the use of a CMS other than a PM CPMS or COMS, you must install, operate, and maintain each CMS according to the procedures in [paragraphs \(d\)\(1\)](#) through [\(5\)](#) of this section by the compliance date specified in [§ 63.7495](#).

(1) The CPMS must complete a minimum of one cycle of operation every 15-minutes. You must have a minimum of four successive cycles of operation, one representing each of the four 15-minute periods in an hour, to have a valid hour of data.

(2) You must operate the monitoring system as specified in [§ 63.7535\(b\)](#), and comply with the data calculation requirements specified in [§ 63.7535\(c\)](#).

(3) Any 15-minute period for which the monitoring system is out-of-control and data are not available for a required calculation constitutes a deviation from the monitoring requirements. Other situations that constitute a monitoring deviation are specified in [§ 63.7535\(d\)](#).

(4) You must determine the 30-day rolling average of all recorded readings, except as provided in [§ 63.7535\(c\)](#).

(5) You must record the results of each inspection, calibration, and validation check.

(e) If you have an operating limit that requires the use of a flow monitoring system, you must meet the requirements in [paragraphs \(d\)](#) and [\(e\)\(1\)](#) through [\(4\)](#) of this section.

(1) You must install the flow sensor and other necessary equipment in a position that provides a representative flow.

(2) You must use a flow sensor with a measurement sensitivity of no greater than 2 percent of the design flow rate.

(3) You must minimize, consistent with good engineering practices, the effects of swirling flow or abnormal velocity distributions due to upstream and downstream disturbances.

(4) You must conduct a flow monitoring system performance evaluation in accordance with your monitoring plan at the time of each performance test but no less frequently than annually.

(f) If you have an operating limit that requires the use of a pressure monitoring system, you must meet the requirements in [paragraphs \(d\)](#) and [\(f\)\(1\)](#) through [\(6\)](#) of this section.

(1) Install the pressure sensor(s) in a position that provides a representative measurement of the pressure (*e.g.*, PM scrubber pressure drop).

(2) Minimize or eliminate pulsating pressure, vibration, and internal and external corrosion consistent with good engineering practices.

(3) Use a pressure sensor with a minimum tolerance of 1.27 centimeters of water or a minimum tolerance of 1 percent of the pressure monitoring system operating range, whichever is less.

(4) Perform checks at least once each process operating day to ensure pressure measurements are not obstructed (*e.g.*, check for pressure tap pluggage daily).

(5) Conduct a performance evaluation of the pressure monitoring system in accordance with your monitoring plan at the time of each performance test but no less frequently than annually.

(6) If at any time the measured pressure exceeds the manufacturer's specified maximum operating pressure range, conduct a performance evaluation of the pressure monitoring system in accordance with your monitoring plan and confirm that the pressure monitoring system continues to meet the performance requirements in you monitoring plan. Alternatively, install and verify the operation of a new pressure sensor.

(g) If you have an operating limit that requires a pH monitoring system, you must meet the requirements in [paragraphs \(d\)](#) and [\(g\)\(1\)](#) through [\(4\)](#) of this section.

(1) Install the pH sensor in a position that provides a representative measurement of scrubber effluent pH.

(2) Ensure the sample is properly mixed and representative of the fluid to be measured.

(3) Calibrate the pH monitoring system in accordance with your monitoring plan and according to the manufacturer's instructions. Clean the pH probe at least once each process

operating day. Maintain on-site documentation that your calibration frequency is sufficient to maintain the specified accuracy of your device.

(4) Conduct a performance evaluation (including a two-point calibration with one of the two buffer solutions having a pH within 1 of the pH of the operating limit) of the pH monitoring system in accordance with your monitoring plan at the time of each performance test but no less frequently than annually.

(h) If you have an operating limit that requires a secondary electric power monitoring system for an electrostatic precipitator (ESP) operated with a wet scrubber, you must meet the requirements in [paragraphs \(h\)\(1\)](#) and [\(2\)](#) of this section.

(1) Install sensors to measure (secondary) voltage and current to the precipitator collection plates.

(2) Conduct a performance evaluation of the electric power monitoring system in accordance with your monitoring plan at the time of each performance test but no less frequently than annually.

(i) If you have an operating limit that requires the use of a monitoring system to measure sorbent injection rate (e.g., weigh belt, weigh hopper, or hopper flow measurement device), you must meet the requirements in [paragraphs \(d\)](#) and [\(i\)\(1\)](#) through [\(2\)](#) of this section.

(1) Install the system in a position(s) that provides a representative measurement of the total sorbent injection rate.

(2) Conduct a performance evaluation of the sorbent injection rate monitoring system in accordance with your monitoring plan at the time of each performance test but no less frequently than annually.

(j) If you are not required to use a PM CPMS and elect to use a fabric filter bag leak detection system to comply with the requirements of this subpart, you must install, calibrate, maintain, and continuously operate the bag leak detection system as specified in [paragraphs \(j\)\(1\)](#) through [\(6\)](#) of this section.

(1) You must install a bag leak detection sensor(s) in a position(s) that will be representative of the relative or absolute PM loadings for each exhaust stack, roof vent, or compartment (e.g., for a positive pressure fabric filter) of the fabric filter.

(2) Conduct a performance evaluation of the bag leak detection system in accordance with your monitoring plan and consistent with the guidance provided in EPA-454/R-98-015 (incorporated by reference, see [§ 63.14](#)).

(3) Use a bag leak detection system certified by the manufacturer to be capable of detecting PM emissions at concentrations of 10 milligrams per actual cubic meter or less.

(4) Use a bag leak detection system equipped with a device to record continuously the output signal from the sensor.

(5) Use a bag leak detection system equipped with a system that will alert plant operating personnel when an increase in relative PM emissions over a preset level is detected. The alert must easily recognizable (e.g., heard or seen) by plant operating personnel.

(6) Where multiple bag leak detectors are required, the system's instrumentation and alert may be shared among detectors.

(k) For each unit that meets the definition of limited-use boiler or process heater, you must keep fuel use records for the days the boiler or process heater was operating.

(l) For each unit for which you decide to demonstrate compliance with the mercury or HCl emissions limits in Tables 1 or 2 or 11 through 13 of this subpart by use of a CEMS for mercury or HCl, you must install, certify, maintain, and operate a CEMS measuring emissions discharged to the atmosphere and record the output of the system as specified in [paragraphs \(1\)\(1\) through \(8\)](#) of this section. For HCl, this option for an affected unit takes effect on the date a final performance specification for a HCl CEMS is published in the Federal Register or the date of approval of a site-specific monitoring plan.

(1) Notify the Administrator one month before starting use of the CEMS, and notify the Administrator one month before stopping use of the CEMS.

(2) Each CEMS shall be installed, certified, operated, and maintained according to the requirements in [§ 63.7540\(a\)\(14\)](#) for a mercury CEMS and [§ 63.7540\(a\)\(15\)](#) for a HCl CEMS.

(3) For a new unit, you must complete the initial performance evaluation of the CEMS by the latest of the dates specified in [paragraph \(1\)\(3\)\(i\)](#) through [\(iii\)](#) of this section.

(i) No later than July 30, 2013.

(ii) No later 180 days after the date of initial startup.

(iii) No later 180 days after notifying the Administrator before starting to use the CEMS in place of performance testing or fuel analysis to demonstrate compliance.

(4) For an existing unit, you must complete the initial performance evaluation by the latter of the two dates specified in [paragraph \(1\)\(4\)\(i\)](#) and [\(ii\)](#) of this section.

(i) No later than July 29, 2016.

(ii) No later 180 days after notifying the Administrator before starting to use the CEMS in place of performance testing or fuel analysis to demonstrate compliance.

(5) Compliance with the applicable emissions limit shall be determined based on the 30-day rolling average of the hourly arithmetic average emissions rates using the continuous monitoring system outlet data. The 30-day rolling arithmetic average emission rate (lb/MMBtu) shall be calculated using the equations in EPA Reference Method 19 at [40 CFR part 60, appendix A-7](#), but substituting the mercury or HCl concentration for the pollutant concentrations normally used in Method 19.

(6) Collect CEMS hourly averages for all operating hours on a 30-day rolling average basis. Collect at least four CMS data values representing the four 15-minute periods in an hour, or at least two 15-minute data values during an hour when CMS calibration, quality assurance, or maintenance activities are being performed.

(7) The one-hour arithmetic averages required shall be expressed in lb/MMBtu and shall be used to calculate the boiler 30-day and 10-day rolling average emissions.

(8) You are allowed to substitute the use of the PM, mercury or HCl CEMS for the applicable fuel analysis, annual performance test, and operating limits specified in Table 4 to this subpart to demonstrate compliance with the PM, mercury or HCl emissions limit, and if you are using an acid gas wet scrubber or dry sorbent injection control technology to comply with the HCl emission limit, you are allowed to substitute the use of a sulfur dioxide (SO₂) CEMS for the applicable fuel analysis, annual performance test, and operating limits specified in Table 4 to this subpart to demonstrate compliance with HCl emissions limit.

(m) If your unit is subject to a HCl emission limit in Tables 1, 2, or 11 through 13 of this subpart and you have an acid gas wet scrubber or dry sorbent injection control technology and you elect to use an SO₂ CEMS to demonstrate continuous compliance with the HCl emission limit, you must install the monitor at the outlet of the boiler or process heater, downstream of all emission control devices, and you must install, certify, operate, and maintain the CEMS according to either [part 60](#) or [part 75 of this chapter](#).

(1) The SO₂ CEMS must be installed by the compliance date specified in [§ 63.7495](#).

(2) For on-going quality assurance (QA), the SO₂ CEMS must meet either the applicable daily and quarterly requirements in Procedure 1 of appendix F of part 60 or the applicable daily, quarterly, and semiannual or annual requirements in sections 2.1 through 2.3 of appendix B to [part 75 of this chapter](#), with the following addition: You must perform the linearity checks required in [section 2.2](#) of appendix B to [part 75 of this chapter](#) if the SO₂ CEMS has a span value of 30 ppm or less.

(3) For a new unit, the initial performance evaluation shall be completed no later than July 30, 2013, or 180 days after the date of initial startup, whichever is later. For an existing unit, the initial performance evaluation shall be completed no later than July 29, 2016.

(4) For purposes of collecting SO₂ data, you must operate the SO₂ CEMS as specified in [§ 63.7535\(b\)](#). You must use all the data collected during all periods in calculating data averages and assessing compliance, except that you must exclude certain data as specified

in [§ 63.7535\(c\)](#). Periods when SO₂ data are unavailable may constitute monitoring deviations as specified in [§ 63.7535\(d\)](#).

(5) Collect CEMS hourly averages for all operating hours on a 30-day rolling average basis.

(6) Use only unadjusted, quality-assured SO₂ concentration values in the emissions calculations; do not apply bias adjustment factors to the part 75 SO₂ data and do not use part 75 substitute data values.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7171](#), Jan. 31, 2013; [80 FR 72810](#), Nov. 20, 2015]

§ 63.7530 How do I demonstrate initial compliance with the emission limitations, fuel specifications and work practice standards?

(a) You must demonstrate initial compliance with each emission limit that applies to you by conducting initial performance tests and fuel analyses and establishing operating limits, as applicable, according to [§ 63.7520](#), [paragraphs \(b\)](#) and [\(c\)](#) of this section, and Tables 5 and 7 to this subpart. The requirement to conduct a fuel analysis is not applicable for units that burn a single type of fuel, as specified by [§ 63.7510\(a\)\(2\)](#). If applicable, you must also install, operate, and maintain all applicable CMS (including CEMS, COMS, and CPMS) according to [§ 63.7525](#).

(b) If you demonstrate compliance through performance stack testing, you must establish each site-specific operating limit in Table 4 to this subpart that applies to you according to the requirements in [§ 63.7520](#), Table 7 to this subpart, and [paragraph \(b\)\(4\)](#) of this section, as applicable. You must also conduct fuel analyses according to [§ 63.7521](#) and establish maximum fuel pollutant input levels according to [paragraphs \(b\)\(1\)](#) through [\(3\)](#) of this section, as applicable, and as specified in [§ 63.7510\(a\)\(2\)](#). (Note that [§ 63.7510\(a\)\(2\)](#) exempts certain fuels from the fuel analysis requirements.) However, if you switch fuel(s) and cannot show that the new fuel(s) does (do) not increase the chlorine, mercury, or TSM input into the unit through the results of fuel analysis, then you must repeat the performance test to demonstrate compliance while burning the new fuel(s).

(1) You must establish the maximum chlorine fuel input (Clinput) during the initial fuel analysis according to the procedures in [paragraphs \(b\)\(1\)\(i\)](#) through [\(iii\)](#) of this section.

(i) You must determine the fuel type or fuel mixture that you could burn in your boiler or process heater that has the highest content of chlorine.

(ii) During the fuel analysis for hydrogen chloride, you must determine the fraction of the total heat input for each fuel type burned (Qi) based on the fuel mixture that has the highest content of chlorine, and the average chlorine concentration of each fuel type burned (Ci).

(iii) You must establish a maximum chlorine input level using Equation 7 of this section.

$$Cl_{input} = \sum_{i=1}^n (C_i \times Q_i) \quad (\text{Eq. 7})$$

Where:

Cl_{input} = Maximum amount of chlorine entering the boiler or process heater through fuels burned in units of pounds per million Btu.

C_i = Arithmetic average concentration of chlorine in fuel type, i , analyzed according to [§ 63.7521](#), in units of pounds per million Btu.

Q_i = Fraction of total heat input from fuel type, i , based on the fuel mixture that has the highest content of chlorine during the initial compliance test. If you do not burn multiple fuel types during the performance testing, it is not necessary to determine the value of this term. Insert a value of “1” for Q_i . For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest content of chlorine.

(2) You must establish the maximum mercury fuel input level ($Mercury_{input}$) during the initial fuel analysis using the procedures in [paragraphs \(b\)\(2\)\(i\)](#) through [\(iii\)](#) of this section.

(i) You must determine the fuel type or fuel mixture that you could burn in your boiler or process heater that has the highest content of mercury.

(ii) During the compliance demonstration for mercury, you must determine the fraction of total heat input for each fuel burned (Q_i) based on the fuel mixture that has the highest content of mercury, and the average mercury concentration of each fuel type burned (HG_i).

(iii) You must establish a maximum mercury input level using Equation 8 of this section.

$$Mercury_{input} = \sum_{i=1}^n (HG_i \times Q_i) \quad (\text{Eq. 8})$$

Where:

$Mercury_{input}$ = Maximum amount of mercury entering the boiler or process heater through fuels burned in units of pounds per million Btu.

HGi = Arithmetic average concentration of mercury in fuel type, i, analyzed according to [§ 63.7521](#), in units of pounds per million Btu.

Qi = Fraction of total heat input from fuel type, i, based on the fuel mixture that has the highest mercury content during the initial compliance test. If you do not burn multiple fuel types during the performance test, it is not necessary to determine the value of this term. Insert a value of “1” for Qi. For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest content of mercury.

(3) If you opt to comply with the alternative TSM limit, you must establish the maximum TSM fuel input (TSMinput) for solid or liquid fuels during the initial fuel analysis according to the procedures in [paragraphs \(b\)\(3\)\(i\)](#) through [\(iii\)](#) of this section.

(i) You must determine the fuel type or fuel mixture that you could burn in your boiler or process heater that has the highest content of TSM.

(ii) During the fuel analysis for TSM, you must determine the fraction of the total heat input for each fuel type burned (Qi) based on the fuel mixture that has the highest content of TSM, and the average TSM concentration of each fuel type burned (TSMi).

(iii) You must establish a maximum TSM input level using Equation 9 of this section.

$$TSM_{input} = \sum_{i=1}^n (TSM_i \times Q_i) \quad (\text{Eq. 9})$$

Where:

TSMinput = Maximum amount of TSM entering the boiler or process heater through fuels burned in units of pounds per million Btu.

TSMi = Arithmetic average concentration of TSM in fuel type, i, analyzed according to [§ 63.7521](#), in units of pounds per million Btu.

Qi = Fraction of total heat input from fuel type, i, based on the fuel mixture that has the highest content of TSM during the initial compliance test. If you do not burn multiple fuel types during the performance testing, it is not necessary to determine the value of this term. Insert a value of “1” for Qi. For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest content of TSM.

(4) You must establish parameter operating limits according to [paragraphs \(b\)\(4\)\(i\) through \(ix\)](#) of this section. As indicated in Table 4 to this subpart, you are not required to establish and comply with the operating parameter limits when you are using a CEMS to monitor and demonstrate compliance with the applicable emission limit for that control device parameter.

(i) For a wet acid gas scrubber, you must establish the minimum scrubber effluent pH and liquid flow rate as defined in [§ 63.7575](#), as your operating limits during the performance test during which you demonstrate compliance with your applicable limit. If you use a wet scrubber and you conduct separate performance tests for HCl and mercury emissions, you must establish one set of minimum scrubber effluent pH, liquid flow rate, and pressure drop operating limits. The minimum scrubber effluent pH operating limit must be established during the HCl performance test. If you conduct multiple performance tests, you must set the minimum liquid flow rate operating limit at the higher of the minimum values established during the performance tests.

(ii) For any particulate control device (e.g., ESP, particulate wet scrubber, fabric filter) for which you use a PM CPMS, you must establish your PM CPMS operating limit and determine compliance with it according to [paragraphs \(b\)\(4\)\(ii\)\(A\) through \(F\)](#) of this section.

(A) Determine your operating limit as the average PM CPMS output value recorded during the most recent performance test run demonstrating compliance with the filterable PM emission limit or at the PM CPMS output value corresponding to 75 percent of the emission limit if your PM performance test demonstrates compliance below 75 percent of the emission limit. You must verify an existing or establish a new operating limit after each repeated performance test. You must repeat the performance test annually and reassess and adjust the site-specific operating limit in accordance with the results of the performance test.

(1) Your PM CPMS must provide a 4-20 milliamp output and the establishment of its relationship to manual reference method measurements must be determined in units of milliamps.

(2) Your PM CPMS operating range must be capable of reading PM concentrations from zero to a level equivalent to at least two times your allowable emission limit. If your PM CPMS is an auto-ranging instrument capable of multiple scales, the primary range of the instrument must be capable of reading PM concentration from zero to a level equivalent to two times your allowable emission limit.

(3) During the initial performance test or any such subsequent performance test that demonstrates compliance with the PM limit, record and average all milliamp output values from the PM CPMS for the periods corresponding to the compliance test runs (e.g., average all your PM CPMS output values for three corresponding 2-hour Method 5I test runs).

(B) If the average of your three PM performance test runs are below 75 percent of your PM emission limit, you must calculate an operating limit by establishing a relationship of PM CPMS signal to PM concentration using the PM CPMS instrument zero, the average PM CPMS values corresponding to the three compliance test runs, and the average PM concentration from the Method 5 or performance test with the procedures in [paragraphs \(b\)\(4\)\(ii\)\(B\)\(1\)](#) through [\(4\)](#) of this section.

(1) Determine your instrument zero output with one of the following procedures:

(i) Zero point data for *in-situ* instruments should be obtained by removing the instrument from the stack and monitoring ambient air on a test bench.

(ii) Zero point data for *extractive* instruments should be obtained by removing the extractive probe from the stack and drawing in clean ambient air.

(iii) The zero point may also be established by performing manual reference method measurements when the flue gas is free of PM emissions or contains very low PM concentrations (e.g., when your process is not operating, but the fans are operating or your source is combusting only natural gas) and plotting these with the compliance data to find the zero intercept.

(iv) If none of the steps in [paragraphs \(b\)\(4\)\(ii\)\(B\)\(1\)\(i\)](#) through [\(iii\)](#) of this section are possible, you must use a zero output value provided by the manufacturer.

(2) Determine your PM CPMS instrument average in milliamps, and the average of your corresponding three PM compliance test runs, using equation 10.

$$\bar{X} = \frac{1}{n} \sum_{i=1}^n X_i \quad \text{and} \quad \bar{Y} = \frac{1}{n} \sum_{i=1}^n Y_i \quad (\text{Eq. 10})$$

Where:

X_i = the PM CPMS data points for the three runs constituting the performance test,

Y_i = the PM concentration value for the three runs constituting the performance test, and

n = the number of data points.

(3) With your instrument zero expressed in milliamps, your three run average PM CPMS milliamp value, and your three run average PM concentration from your three compliance tests, determine a relationship of lb/MMBtu per milliamp with equation 11.

$$R = \frac{Y_1}{(X_1 - z)} \quad (\text{Eq. 11})$$

Where:

R = the relative lb/MMBtu per milliamp for your PM CPMS,

Y_1 = the three run average lb/MMBtu PM concentration,

X_1 = the three run average milliamp output from you PM CPMS, and

z = the milliamp equivalent of your instrument zero determined from (B)(i).

(4) Determine your source specific 30-day rolling average operating limit using the lb/MMBtu per milliamp value from Equation 11 in equation 12, below. This sets your operating limit at the PM CPMS output value corresponding to 75 percent of your emission limit.

$$O_1 = z + \frac{0.75(L)}{R} \quad (\text{Eq. 12})$$

Where:

O_1 = the operating limit for your PM CPMS on a 30-day rolling average, in milliamps.

L = your source emission limit expressed in lb/MMBtu,

z = your instrument zero in milliamps, determined from (B)(i), and

R = the relative lb/MMBtu per milliamp for your PM CPMS, from Equation 11.

(C) If the average of your three PM compliance test runs is at or above 75 percent of your PM emission limit you must determine your 30-day rolling average operating limit by averaging the PM CPMS milliamp output corresponding to your three PM performance test runs that demonstrate compliance with the emission limit using equation 13 and you must submit all compliance test and PM CPMS data according to the reporting requirements in [paragraph \(b\)\(4\)\(ii\)\(F\)](#) of this section.

$$O_3 = \frac{1}{n} \sum_{i=1}^n X_1 \quad (\text{Eq. 13})$$

Where:

X_i = the PM CPMS data points for all runs i ,

n = the number of data points, and

O_h = your site specific operating limit, in milliamps.

(D) To determine continuous compliance, you must record the PM CPMS output data for all periods when the process is operating and the PM CPMS is not out-of-control. You must demonstrate continuous compliance by using all quality-assured hourly average data collected by the PM CPMS for all operating hours to calculate the arithmetic average operating parameter in units of the operating limit (milliamps) on a 30-day rolling average basis, updated at the end of each new operating hour. Use Equation 14 to determine the 30-day rolling average.

$$30\text{-day} = \frac{\sum_{i=1}^n Hpvi}{n} \quad (\text{Eq. 14})$$

Where:

30-day = 30-day average.

$Hpvi$ = is the hourly parameter value for hour i

n = is the number of valid hourly parameter values collected over the previous 30 operating days.

(E) Use EPA Method 5 of appendix A to [part 60 of this chapter](#) to determine PM emissions. For each performance test, conduct three separate runs under the conditions that exist when the affected source is operating at the highest load or capacity level reasonably expected to occur. Conduct each test run to collect a minimum sample volume specified in Tables 1, 2, or 11 through 13 to this subpart, as applicable, for determining compliance with a new source limit or an existing source limit. Calculate the average of the results from three runs to determine compliance. You need not determine the PM collected in the impingers (“back half”) of the Method 5 particulate sampling train to demonstrate compliance with the PM standards of this subpart. This shall not preclude the permitting authority from requiring a determination of the “back half” for other purposes.

(F) For PM performance test reports used to set a PM CPMS operating limit, the electronic submission of the test report must also include the make and model of the PM

CPMS instrument, serial number of the instrument, analytical principle of the instrument (e.g. beta attenuation), span of the instruments primary analytical range, milliamp value equivalent to the instrument zero output, technique by which this zero value was determined, and the average milliamp signals corresponding to each PM compliance test run.

(iii) For a particulate wet scrubber, you must establish the minimum pressure drop and liquid flow rate as defined in [§ 63.7575](#), as your operating limits during the three-run performance test during which you demonstrate compliance with your applicable limit. If you use a wet scrubber and you conduct separate performance tests for PM and TSM emissions, you must establish one set of minimum scrubber liquid flow rate and pressure drop operating limits. The minimum scrubber effluent pH operating limit must be established during the HCl performance test. If you conduct multiple performance tests, you must set the minimum liquid flow rate and pressure drop operating limits at the higher of the minimum values established during the performance tests.

(iv) For an electrostatic precipitator (ESP) operated with a wet scrubber, you must establish the minimum total secondary electric power input, as defined in [§ 63.7575](#), as your operating limit during the three-run performance test during which you demonstrate compliance with your applicable limit. (These operating limits do not apply to ESP that are operated as dry controls without a wet scrubber.)

(v) For a dry scrubber, you must establish the minimum sorbent injection rate for each sorbent, as defined in [§ 63.7575](#), as your operating limit during the three-run performance test during which you demonstrate compliance with your applicable limit.

(vi) For activated carbon injection, you must establish the minimum activated carbon injection rate, as defined in [§ 63.7575](#), as your operating limit during the three-run performance test during which you demonstrate compliance with your applicable limit.

(vii) The operating limit for boilers or process heaters with fabric filters that demonstrate continuous compliance through bag leak detection systems is that a bag leak detection system be installed according to the requirements in [§ 63.7525](#), and that each fabric filter must be operated such that the bag leak detection system alert is not activated more than 5 percent of the operating time during a 6-month period.

(viii) For a minimum oxygen level, if you conduct multiple performance tests, you must set the minimum oxygen level at the lower of the minimum values established during the performance tests.

(ix) The operating limit for boilers or process heaters that demonstrate continuous compliance with the HCl emission limit using a SO₂ CEMS is to install and operate the SO₂ according to the requirements in [§ 63.7525\(m\)](#) establish a maximum SO₂ emission rate equal to the highest hourly average SO₂ measurement during the most recent three-run performance test for HCl.

(c) If you elect to demonstrate compliance with an applicable emission limit through fuel analysis, you must conduct fuel analyses according to [§ 63.7521](#) and follow the procedures in [paragraphs \(c\)\(1\)](#) through [\(5\)](#) of this section.

(1) If you burn more than one fuel type, you must determine the fuel mixture you could burn in your boiler or process heater that would result in the maximum emission rates of the pollutants that you elect to demonstrate compliance through fuel analysis.

(2) You must determine the 90th percentile confidence level fuel pollutant concentration of the composite samples analyzed for each fuel type using the one-sided t-statistic test described in Equation 15 of this section.

$$P90 = mean + (SD \times t) \quad (\text{Eq. 15})$$

Where:

P90 = 90th percentile confidence level pollutant concentration, in pounds per million Btu.

Mean = Arithmetic average of the fuel pollutant concentration in the fuel samples analyzed according to [§ 63.7521](#), in units of pounds per million Btu.

SD = Standard deviation of the mean of pollutant concentration in the fuel samples analyzed according to [§ 63.7521](#), in units of pounds per million Btu. SD is calculated as the sample standard deviation divided by the square root of the number of samples.

t = t distribution critical value for 90th percentile ($t_{0.1}$) probability for the appropriate degrees of freedom (number of samples minus one) as obtained from a t-Distribution Critical Value Table.

(3) To demonstrate compliance with the applicable emission limit for HCl, the HCl emission rate that you calculate for your boiler or process heater using Equation 16 of this section must not exceed the applicable emission limit for HCl.

$$HCl = \sum_{i=1}^n (Ci90 \times Qi \times 1.028) \quad (\text{Eq. 16})$$

Where:

HCl = HCl emission rate from the boiler or process heater in units of pounds per million Btu.

Ci90 = 90th percentile confidence level concentration of chlorine in fuel type, i, in units of pounds per million Btu as calculated according to Equation 15 of this section.

Q_i = Fraction of total heat input from fuel type, i , based on the fuel mixture that has the highest content of chlorine. If you do not burn multiple fuel types, it is not necessary to determine the value of this term. Insert a value of “1” for Q_i . For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest content of chlorine.

1.028 = Molecular weight ratio of HCl to chlorine.

(4) To demonstrate compliance with the applicable emission limit for mercury, the mercury emission rate that you calculate for your boiler or process heater using Equation 17 of this section must not exceed the applicable emission limit for mercury.

$$\text{Mercury} = \sum_{i=1}^n (Hgi90 \times Qi) \quad (\text{Eq. 17})$$

Where:

Mercury = Mercury emission rate from the boiler or process heater in units of pounds per million Btu.

Hgi90 = 90th percentile confidence level concentration of mercury in fuel, i , in units of pounds per million Btu as calculated according to Equation 15 of this section.

Q_i = Fraction of total heat input from fuel type, i , based on the fuel mixture that has the highest mercury content. If you do not burn multiple fuel types, it is not necessary to determine the value of this term. Insert a value of “1” for Q_i . For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest mercury content.

(5) To demonstrate compliance with the applicable emission limit for TSM for solid or liquid fuels, the TSM emission rate that you calculate for your boiler or process heater from solid fuels using Equation 18 of this section must not exceed the applicable emission limit for TSM.

$$\text{Metals} = \sum_{i=1}^n (TSM90i \times Qi) \quad (\text{Eq. 18})$$

Where:

Metals = TSM emission rate from the boiler or process heater in units of pounds per million Btu.

TSM_{i90} = 90th percentile confidence level concentration of TSM in fuel, i, in units of pounds per million Btu as calculated according to Equation 15 of this section.

Q_i = Fraction of total heat input from fuel type, i, based on the fuel mixture that has the highest TSM content. If you do not burn multiple fuel types, it is not necessary to determine the value of this term. Insert a value of “1” for Q_i. For continuous compliance demonstration, the actual fraction of the fuel burned during the month should be used.

n = Number of different fuel types burned in your boiler or process heater for the mixture that has the highest TSM content.

(d) [Reserved]

(e) You must include with the Notification of Compliance Status a signed certification that either the energy assessment was completed according to Table 3 to this subpart, and that the assessment is an accurate depiction of your facility at the time of the assessment, or that the maximum number of on-site technical hours specified in the definition of energy assessment applicable to the facility has been expended.

(f) You must submit the Notification of Compliance Status containing the results of the initial compliance demonstration according to the requirements in [§ 63.7545\(e\)](#).

(g) If you elect to demonstrate that a gaseous fuel meets the specifications of another gas 1 fuel as defined in [§ 63.7575](#), you must conduct an initial fuel specification analyses according to [§ 63.7521\(f\)](#) through [\(i\)](#) and according to the frequency listed in [§ 63.7540\(c\)](#) and maintain records of the results of the testing as outlined in [§ 63.7555\(g\)](#). For samples where the initial mercury specification has not been exceeded, you will include a signed certification with the Notification of Compliance Status that the initial fuel specification test meets the gas specification outlined in the definition of other gas 1 fuels.

(h) If you own or operate a unit subject to emission limits in Tables 1 or 2 or 11 through 13 to this subpart, you must meet the work practice standard according to Table 3 of this subpart. During startup and shutdown, you must only follow the work practice standards according to items 5 and 6 of Table 3 of this subpart.

(i) If you opt to comply with the alternative SO₂ CEMS operating limit in Tables 4 and 8 to this subpart, you may do so only if your affected boiler or process heater:

(1) Has a system using wet scrubber or dry sorbent injection and SO₂ CEMS installed on the unit; and

(2) At all times, you operate the wet scrubber or dry sorbent injection for acid gas control on the unit consistent with [§ 63.7500\(a\)\(3\)](#); and

(3) You establish a unit-specific maximum SO₂ operating limit by collecting the maximum hourly SO₂ emission rate on the SO₂ CEMS during the paired 3-run test for HCl. The maximum SO₂ operating limit is equal to the highest hourly average SO₂ concentration measured during the HCl performance test.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7174](#), Jan. 31, 2013; [80 FR 72811](#), Nov. 20, 2015]

§ 63.7533 Can I use efficiency credits earned from implementation of energy conservation measures to comply with this subpart?

(a) If you elect to comply with the alternative equivalent output-based emission limits, instead of the heat input-based limits listed in Table 2 to this subpart, and you want to take credit for implementing energy conservation measures identified in an energy assessment, you may demonstrate compliance using efficiency credits according to the procedures in this section. You may use this compliance approach for an existing affected boiler for demonstrating initial compliance according to [§ 63.7522\(e\)](#) and for demonstrating monthly compliance according to [§ 63.7522\(f\)](#). Owners or operators using this compliance approach must establish an emissions benchmark, calculate and document the efficiency credits, develop an Implementation Plan, comply with the general reporting requirements, and apply the efficiency credit according to the procedures in [paragraphs \(b\)](#) through [\(f\)](#) of this section. You cannot use this compliance approach for a new or reconstructed affected boiler. Additional guidance from the Department of Energy on efficiency credits is available at: <http://www.epa.gov/ttn/atw/boiler/boilerpg.html>.

(b) For each existing affected boiler for which you intend to apply emissions credits, establish a benchmark from which emission reduction credits may be generated by determining the actual annual fuel heat input to the affected boiler before initiation of an energy conservation activity to reduce energy demand (*i.e.*, fuel usage) according to [paragraphs \(b\)\(1\)](#) through [\(4\)](#) of this section. The benchmark shall be expressed in trillion Btu per year heat input.

(1) The benchmark from which efficiency credits may be generated shall be determined by using the most representative, accurate, and reliable process available for the source. The benchmark shall be established for a one-year period before the date that an energy demand reduction occurs, unless it can be demonstrated that a different time period is more representative of historical operations.

(2) Determine the starting point from which to measure progress. Inventory all fuel purchased and generated on-site (off-gases, residues) in physical units (MMBtu, million cubic feet, etc.).

(3) Document all uses of energy from the affected boiler. Use the most recent data available.

(4) Collect non-energy related facility and operational data to normalize, if necessary, the benchmark to current operations, such as building size, operating hours, etc. If possible, use actual data that are current and timely rather than estimated data.

(c) Efficiency credits can be generated if the energy conservation measures were implemented after January 1, 2008 and if sufficient information is available to determine the appropriate value of credits.

(1) The following emission points cannot be used to generate efficiency credits:

(i) Energy conservation measures implemented on or before January 1, 2008, unless the level of energy demand reduction is increased after January 1, 2008, in which case credit will be allowed only for change in demand reduction achieved after January 1, 2008.

(ii) Efficiency credits on shut-down boilers. Boilers that are shut down cannot be used to generate credits unless the facility provides documentation linking the permanent shutdown to energy conservation measures identified in the energy assessment. In this case, the bench established for the affected boiler to which the credits from the shutdown will be applied must be revised to include the benchmark established for the shutdown boiler.

(2) For all points included in calculating emissions credits, the owner or operator shall:

(i) Calculate annual credits for all energy demand points. Use Equation 19 to calculate credits. Energy conservation measures that meet the criteria of [paragraph \(c\)\(1\)](#) of this section shall not be included, except as specified in [paragraph \(c\)\(1\)\(i\)](#) of this section.

(3) Credits are generated by the difference between the benchmark that is established for each affected boiler, and the actual energy demand reductions from energy conservation measures implemented after January 1, 2008. Credits shall be calculated using Equation 19 of this section as follows:

(i) The overall equation for calculating credits is:

$$ECredits = \left(\sum_{i=1}^n EIS_{iactual} \right) \div EI_{baseline} \quad (\text{Eq. 19})$$

Where:

ECredits = Energy Input Savings for all energy conservation measures implemented for an affected boiler, expressed as a decimal fraction of the baseline energy input.

$EIS_{iactual}$ = Energy Input Savings for each energy conservation measure, i, implemented for an affected boiler, million Btu per year.

$EI_{baseline}$ = Energy Input baseline for the affected boiler, million Btu per year.

n = Number of energy conservation measures included in the efficiency credit for the affected boiler.

(ii) [Reserved]

(d) The owner or operator shall develop, and submit for approval upon request by the Administrator, an Implementation Plan containing all of the information required in this paragraph for all boilers to be included in an efficiency credit approach. The Implementation Plan shall identify all existing affected boilers to be included in applying the efficiency credits. The Implementation Plan shall include a description of the energy conservation measures implemented and the energy savings generated from each measure and an explanation of the criteria used for determining that savings. If requested, you must submit the implementation plan for efficiency credits to the Administrator for review and approval no later than 180 days before the date on which the facility intends to demonstrate compliance using the efficiency credit approach.

(e) The emissions rate as calculated using Equation 20 of this section from each existing boiler participating in the efficiency credit option must be in compliance with the limits in Table 2 to this subpart at all times the affected unit is subject to numeric emission limits, following the compliance date specified in [§ 63.7495](#).

(f) You must use Equation 20 of this section to demonstrate initial compliance by demonstrating that the emissions from the affected boiler participating in the efficiency credit compliance approach do not exceed the emission limits in Table 2 to this subpart.

$$E_{adj} = E_m \times (1 - ECredits) \quad (\text{Eq. 20})$$

Where:

E_{adj} = Emission level adjusted by applying the efficiency credits earned, lb per million Btu steam output (or lb per MWh) for the affected boiler.

E_m = Emissions measured during the performance test, lb per million Btu steam output (or lb per MWh) for the affected boiler.

ECredits = Efficiency credits from Equation 19 for the affected boiler.

(g) As part of each compliance report submitted as required under [§ 63.7550](#), you must include documentation that the energy conservation measures implemented continue to generate the credit for use in demonstrating compliance with the emission limits.

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Continuous Compliance Requirements

§ 63.7535 Is there a minimum amount of monitoring data I must obtain?

(a) You must monitor and collect data according to this section and the site-specific monitoring plan required by [§ 63.7505\(d\)](#).

(b) You must operate the monitoring system and collect data at all required intervals at all times that each boiler or process heater is operating and compliance is required, except for periods of monitoring system malfunctions or out of control periods (see [§ 63.8\(c\)\(7\) of this part](#)), and required monitoring system quality assurance or control activities, including, as applicable, calibration checks, required zero and span adjustments, and scheduled CMS maintenance as defined in your site-specific monitoring plan. A monitoring system malfunction is any sudden, infrequent, not reasonably preventable failure of the monitoring system to provide valid data. Monitoring system failures that are caused in part by poor maintenance or careless operation are not malfunctions. You are required to complete monitoring system repairs in response to monitoring system malfunctions or out-of-control periods and to return the monitoring system to operation as expeditiously as practicable.

(c) You may not use data recorded during periods of startup and shutdown, monitoring system malfunctions or out-of-control periods, repairs associated with monitoring system malfunctions or out-of-control periods, or required monitoring system quality assurance or control activities in data averages and calculations used to report emissions or operating levels. You must record and make available upon request results of CMS performance audits and dates and duration of periods when the CMS is out of control to completion of the corrective actions necessary to return the CMS to operation consistent with your site-specific monitoring plan. You must use all the data collected during all other periods in assessing compliance and the operation of the control device and associated control system.

(d) Except for periods of monitoring system malfunctions, repairs associated with monitoring system malfunctions, and required monitoring system quality assurance or quality control activities (including, as applicable, system accuracy audits, calibration checks, and required zero and span adjustments), failure to collect required data is a deviation of the monitoring requirements. In calculating monitoring results, do not use any data collected during periods of startup and shutdown, when the monitoring system is out of control as specified in your site-specific monitoring plan, while conducting repairs associated with periods when the monitoring system is out of control, or while conducting required monitoring system quality assurance or quality control activities. You must calculate monitoring results using all other monitoring data collected while the process is operating. You must report all periods when the monitoring system is out of control in your semi-annual report.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7179](#), Jan. 31, 2013; [80 FR 72812](#), Nov. 20, 2015]

§ 63.7540 How do I demonstrate continuous compliance with the emission limitations, fuel specifications and work practice standards?

(a) You must demonstrate continuous compliance with each emission limit in Tables 1 and 2 or 11 through 13 to this subpart, the work practice standards in Table 3 to this subpart, and the operating limits in Table 4 to this subpart that applies to you according to the methods specified in Table 8 to this subpart and [paragraphs \(a\)\(1\)](#) through [\(19\)](#) of this section.

(1) Following the date on which the initial compliance demonstration is completed or is required to be completed under [§§ 63.7](#) and [63.7510](#), whichever date comes first, operation above the established maximum or below the established minimum operating limits shall constitute a deviation of established operating limits listed in Table 4 of this subpart except during performance tests conducted to determine compliance with the emission limits or to establish new operating limits. Operating limits must be confirmed or reestablished during performance tests.

(2) As specified in [§ 63.7555\(d\)](#), you must keep records of the type and amount of all fuels burned in each boiler or process heater during the reporting period to demonstrate that all fuel types and mixtures of fuels burned would result in either of the following:

(i) Equal to or lower emissions of HCl, mercury, and TSM than the applicable emission limit for each pollutant, if you demonstrate compliance through fuel analysis.

(ii) Equal to or lower fuel input of chlorine, mercury, and TSM than the maximum values calculated during the last performance test, if you demonstrate compliance through performance testing.

(3) If you demonstrate compliance with an applicable HCl emission limit through fuel analysis for a solid or liquid fuel and you plan to burn a new type of solid or liquid fuel, you must recalculate the HCl emission rate using Equation 16 of [§ 63.7530](#) according to [paragraphs \(a\)\(3\)\(i\)](#) through [\(iii\)](#) of this section. You are not required to conduct fuel analyses for the fuels described in [§ 63.7510\(a\)\(2\)\(i\)](#) through [\(iii\)](#). You may exclude the fuels described in [§ 63.7510\(a\)\(2\)\(i\)](#) through [\(iii\)](#) when recalculating the HCl emission rate.

(i) You must determine the chlorine concentration for any new fuel type in units of pounds per million Btu, based on supplier data or your own fuel analysis, according to the provisions in your site-specific fuel analysis plan developed according to [§ 63.7521\(b\)](#).

(ii) You must determine the new mixture of fuels that will have the highest content of chlorine.

(iii) Recalculate the HCl emission rate from your boiler or process heater under these new conditions using Equation 16 of [§ 63.7530](#). The recalculated HCl emission rate must be less than the applicable emission limit.

(4) If you demonstrate compliance with an applicable HCl emission limit through performance testing and you plan to burn a new type of fuel or a new mixture of fuels, you must recalculate the maximum chlorine input using Equation 7 of [§ 63.7530](#). If the results of recalculating the maximum chlorine input using Equation 7 of [§ 63.7530](#) are greater than the maximum chlorine input level established during the previous performance test, then you must conduct a new performance test within 60 days of burning the new fuel type or fuel mixture according to the procedures in [§ 63.7520](#) to demonstrate that the HCl emissions do not exceed the emission limit. You must also establish new operating limits based on this performance test according to the procedures in [§ 63.7530\(b\)](#). In recalculating the maximum chlorine input and establishing the new operating limits, you are not required to conduct fuel analyses for and include the fuels described in [§ 63.7510\(a\)\(2\)\(i\)](#) through [\(iii\)](#).

(5) If you demonstrate compliance with an applicable mercury emission limit through fuel analysis, and you plan to burn a new type of fuel, you must recalculate the mercury emission rate using Equation 17 of [§ 63.7530](#) according to the procedures specified in [paragraphs \(a\)\(5\)\(i\)](#) through [\(iii\)](#) of this section. You are not required to conduct fuel analyses for the fuels described in [§ 63.7510\(a\)\(2\)\(i\)](#) through [\(iii\)](#). You may exclude the fuels described in [§ 63.7510\(a\)\(2\)\(i\)](#) through [\(iii\)](#) when recalculating the mercury emission rate.

(i) You must determine the mercury concentration for any new fuel type in units of pounds per million Btu, based on supplier data or your own fuel analysis, according to the provisions in your site-specific fuel analysis plan developed according to [§ 63.7521\(b\)](#).

(ii) You must determine the new mixture of fuels that will have the highest content of mercury.

(iii) Recalculate the mercury emission rate from your boiler or process heater under these new conditions using Equation 17 of [§ 63.7530](#). The recalculated mercury emission rate must be less than the applicable emission limit.

(6) If you demonstrate compliance with an applicable mercury emission limit through performance testing, and you plan to burn a new type of fuel or a new mixture of fuels, you must recalculate the maximum mercury input using Equation 8 of [§ 63.7530](#). If the results of recalculating the maximum mercury input using Equation 8 of [§ 63.7530](#) are higher than the maximum mercury input level established during the previous performance test, then you must conduct a new performance test within 60 days of burning the new fuel type or fuel mixture according to the procedures in [§ 63.7520](#) to demonstrate that the mercury emissions do not exceed the emission limit. You must also establish new operating limits based on this performance test according to the procedures in [§ 63.7530\(b\)](#). You are not required to conduct fuel analyses for the fuels described in [§ 63.7510\(a\)\(2\)\(i\)](#) through [\(iii\)](#). You may exclude the fuels described in [§ 63.7510\(a\)\(2\)\(i\)](#) through [\(iii\)](#) when recalculating the mercury emission rate.

(7) If your unit is controlled with a fabric filter, and you demonstrate continuous compliance using a bag leak detection system, you must initiate corrective action within 1 hour of a bag leak detection system alert and complete corrective actions as soon as practical, and operate and maintain the fabric filter system such that the periods which would cause an alert are no more than 5 percent of the operating time during a 6-month period. You must also keep records of the date, time, and duration of each alert, the time corrective action was initiated and completed, and a brief description of the cause of the alert and the corrective action taken. You must also record the percent of the operating time during each 6-month period that the conditions exist for an alert. In calculating this operating time percentage, if inspection of the fabric filter demonstrates that no corrective action is required, no alert time is counted. If corrective action is required, each alert shall be counted as a minimum of 1 hour. If you take longer than 1 hour to initiate corrective action, the alert time shall be counted as the actual amount of time taken to initiate corrective action.

(8) To demonstrate compliance with the applicable alternative CO CEMS emission limit listed in Tables 1, 2, or 11 through 13 to this subpart, you must meet the requirements in [paragraphs \(a\)\(8\)\(i\)](#) through [\(iv\)](#) of this section.

(i) Continuously monitor CO according to [§§ 63.7525\(a\)](#) and [63.7535](#).

(ii) Maintain a CO emission level below or at your applicable alternative CO CEMS-based standard in Tables 1 or 2 or 11 through 13 to this subpart at all times the affected unit is subject to numeric emission limits.

(iii) Keep records of CO levels according to [§ 63.7555\(b\)](#).

(iv) You must record and make available upon request results of CO CEMS performance audits, dates and duration of periods when the CO CEMS is out of control to completion of the corrective actions necessary to return the CO CEMS to operation consistent with your site-specific monitoring plan.

(9) The owner or operator of a boiler or process heater using a PM CPMS or a PM CEMS to meet requirements of this subpart shall install, certify, operate, and maintain the PM CPMS or PM CEMS in accordance with your site-specific monitoring plan as required in [§ 63.7505\(d\)](#).

(10) If your boiler or process heater has a heat input capacity of 10 million Btu per hour or greater, you must conduct an annual tune-up of the boiler or process heater to demonstrate continuous compliance as specified in [paragraphs \(a\)\(10\)\(i\)](#) through [\(vi\)](#) of this section. You must conduct the tune-up while burning the type of fuel (or fuels in case of units that routinely burn a mixture) that provided the majority of the heat input to the boiler or process heater over the 12 months prior to the tune-up. This frequency does not apply to limited-use boilers and process heaters, as defined in [§ 63.7575](#), or units with continuous oxygen trim systems that maintain an optimum air to fuel ratio.

(i) As applicable, inspect the burner, and clean or replace any components of the burner as necessary (you may perform the burner inspection any time prior to the tune-up or delay the burner inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the burner inspection until the first outage, not to exceed 36 months from the previous inspection. At units where entry into a piece of process equipment or into a storage vessel is required to complete the tune-up inspections, inspections are required only during planned entries into the storage vessel or process equipment;

(ii) Inspect the flame pattern, as applicable, and adjust the burner as necessary to optimize the flame pattern. The adjustment should be consistent with the manufacturer's specifications, if available;

(iii) Inspect the system controlling the air-to-fuel ratio, as applicable, and ensure that it is correctly calibrated and functioning properly (you may delay the inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the inspection until the first outage, not to exceed 36 months from the previous inspection;

(iv) Optimize total emissions of CO. This optimization should be consistent with the manufacturer's specifications, if available, and with any NO_x requirement to which the unit is subject;

(v) Measure the concentrations in the effluent stream of CO in parts per million, by volume, and oxygen in volume percent, before and after the adjustments are made (measurements may be either on a dry or wet basis, as long as it is the same basis before and after the adjustments are made). Measurements may be taken using a portable CO analyzer; and

(vi) Maintain on-site and submit, if requested by the Administrator, a report containing the information in [paragraphs \(a\)\(10\)\(vi\)\(A\) through \(C\)](#) of this section,

(A) The concentrations of CO in the effluent stream in parts per million by volume, and oxygen in volume percent, measured at high fire or typical operating load, before and after the tune-up of the boiler or process heater;

(B) A description of any corrective actions taken as a part of the tune-up; and

(C) The type and amount of fuel used over the 12 months prior to the tune-up, but only if the unit was physically and legally capable of using more than one type of fuel during that period. Units sharing a fuel meter may estimate the fuel used by each unit.

(11) If your boiler or process heater has a heat input capacity of less than 10 million Btu per hour (except as specified in [paragraph \(a\)\(12\)](#) of this section), you must conduct a biennial tune-up of the boiler or process heater as specified in [paragraphs \(a\)\(10\)\(i\) through \(vi\)](#) of this section to demonstrate continuous compliance.

(12) If your boiler or process heater has a continuous oxygen trim system that maintains an optimum air to fuel ratio, or a heat input capacity of less than or equal to 5 million Btu per hour and the unit is in the units designed to burn gas 1; units designed to burn gas 2 (other); or units designed to burn light liquid subcategories, or meets the definition of limited-use boiler or process heater in [§ 63.7575](#), you must conduct a tune-up of the boiler or process heater every 5 years as specified in [paragraphs \(a\)\(10\)\(i\)](#) through [\(vi\)](#) of this section to demonstrate continuous compliance. You may delay the burner inspection specified in [paragraph \(a\)\(10\)\(i\)](#) of this section until the next scheduled or unscheduled unit shutdown, but you must inspect each burner at least once every 72 months. If an oxygen trim system is utilized on a unit without emission standards to reduce the tune-up frequency to once every 5 years, set the oxygen level no lower than the oxygen concentration measured during the most recent tune-up.

(13) If the unit is not operating on the required date for a tune-up, the tune-up must be conducted within 30 calendar days of startup.

(14) If you are using a CEMS measuring mercury emissions to meet requirements of this subpart you must install, certify, operate, and maintain the mercury CEMS as specified in [paragraphs \(a\)\(14\)\(i\)](#) and [\(ii\)](#) of this section.

(i) Operate the mercury CEMS in accordance with performance specification 12A of [40 CFR part 60, appendix B](#) or operate a sorbent trap based integrated monitor in accordance with performance specification 12B of [40 CFR part 60, appendix B](#). The duration of the performance test must be 30 operating days if you specified a 30 operating day basis in [§ 63.7545\(e\)\(2\)\(iii\)](#) for mercury CEMS or it must be 720 hours if you specified a 720 hour basis in [§ 63.7545\(e\)\(2\)\(iii\)](#) for mercury CEMS. For each day in which the unit operates, you must obtain hourly mercury concentration data, and stack gas volumetric flow rate data.

(ii) If you are using a mercury CEMS, you must install, operate, calibrate, and maintain an instrument for continuously measuring and recording the mercury mass emissions rate to the atmosphere according to the requirements of performance specifications 6 and 12A of [40 CFR part 60, appendix B](#), and quality assurance procedure 6 of [40 CFR part 60, appendix F](#).

(15) If you are using a CEMS to measure HCl emissions to meet requirements of this subpart, you must install, certify, operate, and maintain the HCl CEMS as specified in [paragraphs \(a\)\(15\)\(i\)](#) and [\(ii\)](#) of this section. This option for an affected unit takes effect on the date a final performance specification for an HCl CEMS is published in the Federal Register or the date of approval of a site-specific monitoring plan.

(i) Operate the continuous emissions monitoring system in accordance with the applicable performance specification in [40 CFR part 60, appendix B](#). The duration of the performance test must be 30 operating days if you specified a 30 operating day basis in [§ 63.7545\(e\)\(2\)\(iii\)](#) for HCl CEMS or it must be 720 hours if you specified a 720 hour basis

in [§ 63.7545\(e\)\(2\)\(iii\)](#) for HCl CEMS. For each day in which the unit operates, you must obtain hourly HCl concentration data, and stack gas volumetric flow rate data.

(ii) If you are using a HCl CEMS, you must install, operate, calibrate, and maintain an instrument for continuously measuring and recording the HCl mass emissions rate to the atmosphere according to the requirements of the applicable performance specification of [40 CFR part 60, appendix B](#), and the quality assurance procedures of [40 CFR part 60, appendix F](#).

(16) If you demonstrate compliance with an applicable TSM emission limit through performance testing, and you plan to burn a new type of fuel or a new mixture of fuels, you must recalculate the maximum TSM input using Equation 9 of [§ 63.7530](#). If the results of recalculating the maximum TSM input using Equation 9 of [§ 63.7530](#) are higher than the maximum total selected input level established during the previous performance test, then you must conduct a new performance test within 60 days of burning the new fuel type or fuel mixture according to the procedures in [§ 63.7520](#) to demonstrate that the TSM emissions do not exceed the emission limit. You must also establish new operating limits based on this performance test according to the procedures in [§ 63.7530\(b\)](#). You are not required to conduct fuel analyses for the fuels described in [§ 63.7510\(a\)\(2\)\(i\)](#) through [\(iii\)](#). You may exclude the fuels described in [§ 63.7510\(a\)\(2\)\(i\)](#) through [\(iii\)](#) when recalculating the TSM emission rate.

(17) If you demonstrate compliance with an applicable TSM emission limit through fuel analysis for solid or liquid fuels, and you plan to burn a new type of fuel, you must recalculate the TSM emission rate using Equation 18 of [§ 63.7530](#) according to the procedures specified in [paragraphs \(a\)\(5\)\(i\)](#) through [\(iii\)](#) of this section. You are not required to conduct fuel analyses for the fuels described in [§ 63.7510\(a\)\(2\)\(i\)](#) through [\(iii\)](#). You may exclude the fuels described in [§ 63.7510\(a\)\(2\)\(i\)](#) through [\(iii\)](#) when recalculating the TSM emission rate.

(i) You must determine the TSM concentration for any new fuel type in units of pounds per million Btu, based on supplier data or your own fuel analysis, according to the provisions in your site-specific fuel analysis plan developed according to [§ 63.7521\(b\)](#).

(ii) You must determine the new mixture of fuels that will have the highest content of TSM.

(iii) Recalculate the TSM emission rate from your boiler or process heater under these new conditions using Equation 18 of [§ 63.7530](#). The recalculated TSM emission rate must be less than the applicable emission limit.

(18) If you demonstrate continuous PM emissions compliance with a PM CPMS you will use a PM CPMS to establish a site-specific operating limit corresponding to the results of the performance test demonstrating compliance with the PM limit. You will conduct your performance test using the test method criteria in Table 5 of this subpart. You will use the PM CPMS to demonstrate continuous compliance with this operating limit. You must repeat

the performance test annually and reassess and adjust the site-specific operating limit in accordance with the results of the performance test.

(i) To determine continuous compliance, you must record the PM CPMS output data for all periods when the process is operating and the PM CPMS is not out-of-control. You must demonstrate continuous compliance by using all quality-assured hourly average data collected by the PM CPMS for all operating hours to calculate the arithmetic average operating parameter in units of the operating limit (milliamperes) on a 30-day rolling average basis.

(ii) For any deviation of the 30-day rolling PM CPMS average value from the established operating parameter limit, you must:

(A) Within 48 hours of the deviation, visually inspect the air pollution control device (APCD);

(B) If inspection of the APCD identifies the cause of the deviation, take corrective action as soon as possible and return the PM CPMS measurement to within the established value; and

(C) Within 30 days of the deviation or at the time of the annual compliance test, whichever comes first, conduct a PM emissions compliance test to determine compliance with the PM emissions limit and to verify or re-establish the CPMS operating limit. You are not required to conduct additional testing for any deviations that occur between the time of the original deviation and the PM emissions compliance test required under this paragraph.

(iii) PM CPMS deviations from the operating limit leading to more than four required performance tests in a 12-month operating period constitute a separate violation of this subpart.

(19) If you choose to comply with the PM filterable emissions limit by using PM CEMS you must install, certify, operate, and maintain a PM CEMS and record the output of the PM CEMS as specified in [paragraphs \(a\)\(19\)\(i\) through \(vii\)](#) of this section. The compliance limit will be expressed as a 30-day rolling average of the numerical emissions limit value applicable for your unit in Tables 1 or 2 or 11 through 13 of this subpart.

(i) Install and certify your PM CEMS according to the procedures and requirements in Performance Specification 11 - Specifications and Test Procedures for Particulate Matter Continuous Emission Monitoring Systems at Stationary Sources in Appendix B to [part 60 of this chapter](#), using test criteria outlined in Table V of this rule. The reportable measurement output from the PM CEMS must be expressed in units of the applicable emissions limit (e.g., lb/MMBtu, lb/MWh).

(ii) Operate and maintain your PM CEMS according to the procedures and requirements in Procedure 2 - Quality Assurance Requirements for Particulate Matter Continuous Emission Monitoring Systems at Stationary Sources in Appendix F to [part 60 of this chapter](#).

(A) You must conduct the relative response audit (RRA) for your PM CEMS at least once annually.

(B) You must conduct the relative correlation audit (RCA) for your PM CEMS at least once every 3 years.

(iii) Collect PM CEMS hourly average output data for all boiler operating hours except as indicated in [paragraph \(v\)](#) of this section.

(iv) Calculate the arithmetic 30-day rolling average of all of the hourly average PM CEMS output data collected during all nonexempt boiler or process heater operating hours.

(v) You must collect data using the PM CEMS at all times the unit is operating and at the intervals specified in this [paragraph \(a\)](#), except for periods of monitoring system malfunctions, repairs associated with monitoring system malfunctions, and required monitoring system quality assurance or quality control activities.

(vi) You must use all the data collected during all boiler or process heater operating hours in assessing the compliance with your operating limit except:

(A) Any data collected during monitoring system malfunctions, repairs associated with monitoring system malfunctions, or required monitoring system quality assurance or control activities conducted during monitoring system malfunctions in calculations and report any such periods in your annual deviation report;

(B) Any data collected during periods when the monitoring system is out of control as specified in your site-specific monitoring plan, repairs associated with periods when the monitoring system is out of control, or required monitoring system quality assurance or control activities conducted during out of control periods in calculations used to report emissions or operating levels and report any such periods in your annual deviation report;

(C) Any data recorded during periods of startup or shutdown.

(vii) You must record and make available upon request results of PM CEMS system performance audits, dates and duration of periods when the PM CEMS is out of control to completion of the corrective actions necessary to return the PM CEMS to operation consistent with your site-specific monitoring plan.

(b) You must report each instance in which you did not meet each emission limit and operating limit in Tables 1 through 4 or 11 through 13 to this subpart that apply to you. These instances are deviations from the emission limits or operating limits, respectively, in this subpart. These deviations must be reported according to the requirements in [§ 63.7550](#).

(c) If you elected to demonstrate that the unit meets the specification for mercury for the unit designed to burn gas 1 subcategory, you must follow the sampling frequency specified in [paragraphs \(c\)\(1\) through \(4\)](#) of this section and conduct this sampling according to the procedures in [§ 63.7521\(f\)](#) through [\(i\)](#).

(1) If the initial mercury constituents in the gaseous fuels are measured to be equal to or less than half of the mercury specification as defined in [§ 63.7575](#), you do not need to conduct further sampling.

(2) If the initial mercury constituents are greater than half but equal to or less than 75 percent of the mercury specification as defined in [§ 63.7575](#), you will conduct semi-annual sampling. If 6 consecutive semi-annual fuel analyses demonstrate 50 percent or less of the mercury specification, you do not need to conduct further sampling. If any semi-annual sample exceeds 75 percent of the mercury specification, you must return to monthly sampling for that fuel, until 12 months of fuel analyses again are less than 75 percent of the compliance level.

(3) If the initial mercury constituents are greater than 75 percent of the mercury specification as defined in [§ 63.7575](#), you will conduct monthly sampling. If 12 consecutive monthly fuel analyses demonstrate 75 percent or less of the mercury specification, you may decrease the fuel analysis frequency to semi-annual for that fuel.

(4) If the initial sample exceeds the mercury specification as defined in [§ 63.7575](#), each affected boiler or process heater combusting this fuel is not part of the unit designed to burn gas 1 subcategory and must be in compliance with the emission and operating limits for the appropriate subcategory. You may elect to conduct additional monthly sampling while complying with these emissions and operating limits to demonstrate that the fuel qualifies as another gas 1 fuel. If 12 consecutive monthly fuel analyses samples are at or below the mercury specification as defined in [§ 63.7575](#), each affected boiler or process heater combusting the fuel can elect to switch back into the unit designed to burn gas 1 subcategory until the mercury specification is exceeded.

(d) For startup and shutdown, you must meet the work practice standards according to items 5 and 6 of Table 3 of this subpart.

[[78 FR 7179](#), Jan. 31, 2013, as amended at [80 FR 72813](#), Nov. 20, 2015]

§ 63.7541 How do I demonstrate continuous compliance under the emissions averaging provision?

(a) Following the compliance date, the owner or operator must demonstrate compliance with this subpart on a continuous basis by meeting the requirements of [paragraphs \(a\)\(1\) through \(5\)](#) of this section.

(1) For each calendar month, demonstrate compliance with the average weighted emissions limit for the existing units participating in the emissions averaging option as determined in [§ 63.7522\(f\)](#) and [\(g\)](#).

(2) You must maintain the applicable opacity limit according to [paragraphs \(a\)\(2\)\(i\)](#) and [\(ii\)](#) of this section.

(i) For each existing unit participating in the emissions averaging option that is equipped with a dry control system and not vented to a common stack, maintain opacity at or below the applicable limit.

(ii) For each group of units participating in the emissions averaging option where each unit in the group is equipped with a dry control system and vented to a common stack that does not receive emissions from non-affected units, maintain opacity at or below the applicable limit at the common stack.

(3) For each existing unit participating in the emissions averaging option that is equipped with a wet scrubber, maintain the 30-day rolling average parameter values at or above the operating limits established during the most recent performance test.

(4) For each existing unit participating in the emissions averaging option that has an approved alternative operating parameter, maintain the 30-day rolling average parameter values consistent with the approved monitoring plan.

(5) For each existing unit participating in the emissions averaging option venting to a common stack configuration containing affected units from other subcategories, maintain the appropriate operating limit for each unit as specified in Table 4 to this subpart that applies.

(b) Any instance where the owner or operator fails to comply with the continuous monitoring requirements in [paragraphs \(a\)\(1\)](#) through [\(5\)](#) of this section is a deviation.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7182](#), Jan. 31, 2013]

Notification, Reports, and Records

§ 63.7545 What notifications must I submit and when?

(a) You must submit to the Administrator all of the notifications in [§§ 63.7\(b\)](#) and [\(c\)](#), [63.8\(e\)](#), [\(f\)\(4\)](#) and [\(6\)](#), and [63.9\(b\)](#) through [\(h\)](#) that apply to you by the dates specified.

(b) As specified in [§ 63.9\(b\)\(2\)](#), if you startup your affected source before January 31, 2013, you must submit an Initial Notification not later than 120 days after January 31, 2013, or no later than 120 days after the source becomes subject to this subpart, whichever is later.

(c) As specified in [§ 63.9\(b\)\(4\)](#) and [\(5\)](#), if you startup your new or reconstructed affected source on or after January 31, 2013, you must submit an Initial Notification not later than 15

days after the actual date of startup of the affected source. For a new or reconstructed affected source that has reclassified to major source status, you must submit an Initial Notification not later 120 days after the source becomes subject to this subpart.

(d) If you are required to conduct a performance test you must submit a Notification of Intent to conduct a performance test at least 60 days before the performance test is scheduled to begin.

(e) If you are required to conduct an initial compliance demonstration as specified in [§ 63.7530](#), you must submit a Notification of Compliance Status according to [§ 63.9\(h\)\(2\)\(ii\)](#). For the initial compliance demonstration for each boiler or process heater, you must submit the Notification of Compliance Status, including all performance test results and fuel analyses, before the close of business on the 60th day following the completion of all performance test and/or other initial compliance demonstrations for all boiler or process heaters at the facility according to [§ 63.10\(d\)\(2\)](#). The Notification of Compliance Status report must contain all the information specified in [paragraphs \(e\)\(1\) through \(8\)](#) of this section, as applicable. If you are not required to conduct an initial compliance demonstration as specified in [§ 63.7530\(a\)](#), the Notification of Compliance Status must only contain the information specified in [paragraphs \(e\)\(1\) and \(8\)](#) of this section and must be submitted within 60 days of the compliance date specified at [§ 63.7495\(b\)](#).

(1) A description of the affected unit(s) including identification of which subcategories the unit is in, the design heat input capacity of the unit, a description of the add-on controls used on the unit to comply with this subpart, description of the fuel(s) burned, including whether the fuel(s) were a secondary material determined by you or the EPA through a petition process to be a non-waste under [§ 241.3 of this chapter](#), whether the fuel(s) were a secondary material processed from discarded non-hazardous secondary materials within the meaning of [§ 241.3 of this chapter](#), and justification for the selection of fuel(s) burned during the compliance demonstration.

(2) Summary of the results of all performance tests and fuel analyses, and calculations conducted to demonstrate initial compliance including all established operating limits, and including:

(i) Identification of whether you are complying with the PM emission limit or the alternative TSM emission limit.

(ii) Identification of whether you are complying with the output-based emission limits or the heat input-based (i.e., lb/MMBtu or ppm) emission limits,

(iii) Identification of whether you are complying the arithmetic mean of all valid hours of data from the previous 30 operating days or of the previous 720 hours. This identification shall be specified separately for each operating parameter.

(3) A summary of the maximum CO emission levels recorded during the performance test to show that you have met any applicable emission standard in Tables 1, 2, or 11 through 13 to this subpart, if you are not using a CO CEMS to demonstrate compliance.

(4) Identification of whether you plan to demonstrate compliance with each applicable emission limit through performance testing, a CEMS, or fuel analysis.

(5) Identification of whether you plan to demonstrate compliance by emissions averaging and identification of whether you plan to demonstrate compliance by using efficiency credits through energy conservation:

(i) If you plan to demonstrate compliance by emission averaging, report the emission level that was being achieved or the control technology employed on January 31, 2013.

(ii) [Reserved]

(6) A signed certification that you have met all applicable emission limits and work practice standards.

(7) If you had a deviation from any emission limit, work practice standard, or operating limit, you must also submit a description of the deviation, the duration of the deviation, and the corrective action taken in the Notification of Compliance Status report.

(8) In addition to the information required in [§ 63.9\(h\)\(2\)](#), your notification of compliance status must include the following certification(s) of compliance, as applicable, and signed by a responsible official:

(i) “This facility completed the required initial tune-up for all of the boilers and process heaters covered by [40 CFR part 63 subpart DDDDD](#) at this site according to the procedures in [§ 63.7540\(a\)\(10\)\(i\)](#) through [\(vi\)](#).”

(ii) “This facility has had an energy assessment performed according to [§ 63.7530\(e\)](#).”

(iii) Except for units that burn only natural gas, refinery gas, or other gas 1 fuel, or units that qualify for a statutory exemption as provided in section 129(g)(1) of the Clean Air Act, include the following: “No secondary materials that are solid waste were combusted in any affected unit.”

(f) If you operate a unit designed to burn natural gas, refinery gas, or other gas 1 fuels that is subject to this subpart, and you intend to use a fuel other than natural gas, refinery gas, gaseous fuel subject to another subpart of this part, part 60, 61, or 65, or other gas 1 fuel to fire the affected unit during a period of natural gas curtailment or supply interruption, as defined in [§ 63.7575](#), you must submit a notification of alternative fuel use within 48 hours of the declaration of each period of natural gas curtailment or supply interruption, as defined in [§ 63.7575](#). The notification must include the information specified in [paragraphs \(f\)\(1\) through \(5\)](#) of this section.

- (1) Company name and address.
- (2) Identification of the affected unit.
- (3) Reason you are unable to use natural gas or equivalent fuel, including the date when the natural gas curtailment was declared or the natural gas supply interruption began.
- (4) Type of alternative fuel that you intend to use.
- (5) Dates when the alternative fuel use is expected to begin and end.

(g) If you intend to commence or recommence combustion of solid waste, you must provide 30 days prior notice of the date upon which you will commence or recommence combustion of solid waste. The notification must identify:

- (1) The name of the owner or operator of the affected source, as defined in [§ 63.7490](#), the location of the source, the boiler(s) or process heater(s) that will commence burning solid waste, and the date of the notice.
- (2) The currently applicable subcategories under this subpart.
- (3) The date on which you became subject to the currently applicable emission limits.
- (4) The date upon which you will commence combusting solid waste.

(h) If you have switched fuels or made a physical change to the boiler or process heater and the fuel switch or physical change resulted in the applicability of a different subcategory, you must provide notice of the date upon which you switched fuels or made the physical change within 30 days of the switch/change. The notification must identify:

- (1) The name of the owner or operator of the affected source, as defined in [§ 63.7490](#), the location of the source, the boiler(s) and process heater(s) that have switched fuels, were physically changed, and the date of the notice.
- (2) The currently applicable subcategory under this subpart.
- (3) The date upon which the fuel switch or physical change occurred.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7183](#), Jan. 31, 2013; [80 FR 72814](#), Nov. 20, 2015; [85 FR 73913](#), Nov. 19, 2020; [85 FR 84262](#), Dec. 28, 2020]

§ 63.7550 What reports must I submit and when?

- (a) You must submit each report in Table 9 to this subpart that applies to you.

(b) Unless the EPA Administrator has approved a different schedule for submission of reports under [§ 63.10\(a\)](#), you must submit each report, according to [paragraph \(h\)](#) of this section, by the date in Table 9 to this subpart and according to the requirements in [paragraphs \(b\)\(1\) through \(4\)](#) of this section. For units that are subject only to a requirement to conduct subsequent annual, biennial, or 5-year tune-up according to [§ 63.7540\(a\)\(10\)](#), [\(11\)](#), or [\(12\)](#), respectively, and not subject to emission limits or Table 4 operating limits, you may submit only an annual, biennial, or 5-year compliance report, as applicable, as specified in [paragraphs \(b\)\(1\) through \(4\)](#) of this section, instead of a semi-annual compliance report.

(1) The first semi-annual compliance report must cover the period beginning on the compliance date that is specified for each boiler or process heater in [§ 63.7495](#) and ending on June 30 or December 31, whichever date is the first date that occurs at least 180 days after the compliance date that is specified for your source in [§ 63.7495](#). If submitting an annual, biennial, or 5-year compliance report, the first compliance report must cover the period beginning on the compliance date that is specified for each boiler or process heater in [§ 63.7495](#) and ending on December 31 within 1, 2, or 5 years, as applicable, after the compliance date that is specified for your source in [§ 63.7495](#).

(2) The first semi-annual compliance report must be postmarked or submitted no later than July 31 or January 31, whichever date is the first date following the end of the first calendar half after the compliance date that is specified for each boiler or process heater in [§ 63.7495](#). The first annual, biennial, or 5-year compliance report must be postmarked or submitted no later than January 31.

(3) Each subsequent semi-annual compliance report must cover the semiannual reporting period from January 1 through June 30 or the semiannual reporting period from July 1 through December 31. Annual, biennial, and 5-year compliance reports must cover the applicable 1-, 2-, or 5-year periods from January 1 to December 31.

(4) Each subsequent semi-annual compliance report must be postmarked or submitted no later than July 31 or January 31, whichever date is the first date following the end of the semiannual reporting period. Annual, biennial, and 5-year compliance reports must be postmarked or submitted no later than January 31.

(5) For each affected source that is subject to permitting regulations pursuant to [part 70](#) or [part 71 of this chapter](#), and if the permitting authority has established dates for submitting semiannual reports pursuant to 70.6(a)(3)(iii)(A) or 71.6(a)(3)(iii)(A), you may submit the first and subsequent compliance reports according to the dates the permitting authority has established in the permit instead of according to the dates in [paragraphs \(b\)\(1\) through \(4\)](#) of this section.

(c) A compliance report must contain the following information depending on how the facility chooses to comply with the limits set in this rule.

(1) If the facility is subject to the requirements of a tune up you must submit a compliance report with the information in [paragraphs \(c\)\(5\)\(i\) through \(iii\)](#) of this section, (xiv) and

(xvii) of this section, and [paragraph \(c\)\(5\)\(iv\)](#) of this section for limited-use boiler or process heater.

(2) If you are complying with the fuel analysis you must submit a compliance report with the information in paragraphs (c)(5)(i) through (iii), (vi), (x), (xi), (xiii), (xv), (xvii), (xviii) and [paragraph \(d\)](#) of this section.

(3) If you are complying with the applicable emissions limit with performance testing you must submit a compliance report with the information in (c)(5)(i) through (iii), (vi), (vii), (viii), (ix), (xi), (xiii), (xv), (xvii), (xviii) and [paragraph \(d\)](#) of this section.

(4) If you are complying with an emissions limit using a CMS the compliance report must contain the information required in paragraphs (c)(5)(i) through (iii), (v), (vi), (xi) through (xiii), (xv) through (xviii), and [paragraph \(e\)](#) of this section.

(5)

(i) Company and Facility name and address.

(ii) Process unit information, emissions limitations, and operating parameter limitations.

(iii) Date of report and beginning and ending dates of the reporting period.

(iv) The total operating time during the reporting period.

(v) If you use a CMS, including CEMS, COMS, or CPMS, you must include the monitoring equipment manufacturer(s) and model numbers and the date of the last CMS certification or audit.

(vi) The total fuel use by each individual boiler or process heater subject to an emission limit within the reporting period, including, but not limited to, a description of the fuel, whether the fuel has received a non-waste determination by the EPA or your basis for concluding that the fuel is not a waste, and the total fuel usage amount with units of measure.

(vii) If you are conducting performance tests once every 3 years consistent with [§ 63.7515\(b\)](#) or [\(c\)](#), the date of the last 2 performance tests and a statement as to whether there have been any operational changes since the last performance test that could increase emissions.

(viii) A statement indicating that you burned no new types of fuel in an individual boiler or process heater subject to an emission limit. Or, if you did burn a new type of fuel and are subject to a HCl emission limit, you must submit the calculation of chlorine input, using Equation 7 of [§ 63.7530](#), that demonstrates that your source is still within its maximum chlorine input level established during the previous performance testing (for sources that demonstrate compliance through performance testing) or you must submit the calculation

of HCl emission rate using Equation 16 of [§ 63.7530](#) that demonstrates that your source is still meeting the emission limit for HCl emissions (for boilers or process heaters that demonstrate compliance through fuel analysis). If you burned a new type of fuel and are subject to a mercury emission limit, you must submit the calculation of mercury input, using Equation 8 of [§ 63.7530](#), that demonstrates that your source is still within its maximum mercury input level established during the previous performance testing (for sources that demonstrate compliance through performance testing), or you must submit the calculation of mercury emission rate using Equation 17 of [§ 63.7530](#) that demonstrates that your source is still meeting the emission limit for mercury emissions (for boilers or process heaters that demonstrate compliance through fuel analysis). If you burned a new type of fuel and are subject to a TSM emission limit, you must submit the calculation of TSM input, using Equation 9 of [§ 63.7530](#), that demonstrates that your source is still within its maximum TSM input level established during the previous performance testing (for sources that demonstrate compliance through performance testing), or you must submit the calculation of TSM emission rate, using Equation 18 of [§ 63.7530](#), that demonstrates that your source is still meeting the emission limit for TSM emissions (for boilers or process heaters that demonstrate compliance through fuel analysis).

(ix) If you wish to burn a new type of fuel in an individual boiler or process heater subject to an emission limit and you cannot demonstrate compliance with the maximum chlorine input operating limit using Equation 7 of [§ 63.7530](#) or the maximum mercury input operating limit using Equation 8 of [§ 63.7530](#), or the maximum TSM input operating limit using Equation 9 of [§ 63.7530](#) you must include in the compliance report a statement indicating the intent to conduct a new performance test within 60 days of starting to burn the new fuel.

(x) A summary of any monthly fuel analyses conducted to demonstrate compliance according to [§§ 63.7521](#) and [63.7530](#) for individual boilers or process heaters subject to emission limits, and any fuel specification analyses conducted according to [§§ 63.7521\(f\)](#) and [63.7530\(g\)](#).

(xi) If there are no deviations from any emission limits or operating limits in this subpart that apply to you, a statement that there were no deviations from the emission limits or operating limits during the reporting period.

(xii) If there were no deviations from the monitoring requirements including no periods during which the CMSs, including CEMS, COMS, and CPMS, were out of control as specified in [§ 63.8\(c\)\(7\)](#), a statement that there were no deviations and no periods during which the CMS were out of control during the reporting period.

(xiii) If a malfunction occurred during the reporting period, the report must include the number, duration, and a brief description for each type of malfunction which occurred during the reporting period and which caused or may have caused any applicable emission limitation to be exceeded. The report must also include a description of actions taken by you during a malfunction of a boiler, process heater, or associated air pollution control

device or CMS to minimize emissions in accordance with [§ 63.7500\(a\)\(3\)](#), including actions taken to correct the malfunction.

(xiv) Include the date of the most recent tune-up for each unit subject to only the requirement to conduct an annual, biennial, or 5-year tune-up according to [§ 63.7540\(a\)\(10\)](#), [\(11\)](#), or [\(12\)](#) respectively. Include the date of the most recent burner inspection if it was not done annually, biennially, or on a 5-year period and was delayed until the next scheduled or unscheduled unit shutdown.

(xv) If you plan to demonstrate compliance by emission averaging, certify the emission level achieved or the control technology employed is no less stringent than the level or control technology contained in the notification of compliance status in [§ 63.7545\(e\)\(5\)\(i\)](#).

(xvi) For each reporting period, the compliance reports must include all of the calculated 30 day rolling average values for CEMS (CO, HCl, SO₂, and mercury), 10 day rolling average values for CO CEMS when the limit is expressed as a 10 day instead of 30 day rolling average, and the PM CPMS data.

(xvii) Statement by a responsible official with that official's name, title, and signature, certifying the truth, accuracy, and completeness of the content of the report.

(xviii) For each instance of startup or shutdown include the information required to be monitored, collected, or recorded according to the requirements of [§ 63.7555\(d\)](#).

(d) For each deviation from an emission limit or operating limit in this subpart that occurs at an individual boiler or process heater where you are not using a CMS to comply with that emission limit or operating limit, or from the work practice standards for periods of startup and shutdown, the compliance report must additionally contain the information required in [paragraphs \(d\)\(1\)](#) through [\(3\)](#) of this section.

(1) A description of the deviation and which emission limit, operating limit, or work practice standard from which you deviated.

(2) Information on the number, duration, and cause of deviations (including unknown cause), as applicable, and the corrective action taken.

(3) If the deviation occurred during an annual performance test, provide the date the annual performance test was completed.

(e) For each deviation from an emission limit, operating limit, and monitoring requirement in this subpart occurring at an individual boiler or process heater where you are using a CMS to comply with that emission limit or operating limit, the compliance report must additionally contain the information required in [paragraphs \(e\)\(1\)](#) through [\(9\)](#) of this section. This includes any deviations from your site-specific monitoring plan as required in [§ 63.7505\(d\)](#).

(1) The date and time that each deviation started and stopped and description of the nature of the deviation (i.e., what you deviated from).

(2) The date and time that each CMS was inoperative, except for zero (low-level) and high-level checks.

(3) The date, time, and duration that each CMS was out of control, including the information in [§ 63.8\(c\)\(8\)](#).

(4) The date and time that each deviation started and stopped.

(5) A summary of the total duration of the deviation during the reporting period and the total duration as a percent of the total source operating time during that reporting period.

(6) A characterization of the total duration of the deviations during the reporting period into those that are due to control equipment problems, process problems, other known causes, and other unknown causes.

(7) A summary of the total duration of CMS's downtime during the reporting period and the total duration of CMS downtime as a percent of the total source operating time during that reporting period.

(8) A brief description of the source for which there was a deviation.

(9) A description of any changes in CMSs, processes, or controls since the last reporting period for the source for which there was a deviation.

(f-g) [Reserved]

(h) You must submit the reports according to the procedures specified in [paragraphs \(h\)\(1\)](#) through [\(3\)](#) of this section.

(1) Within 60 days after the date of completing each performance test (as defined in [§ 63.2](#)) required by this subpart, you must submit the results of the performance tests, including any fuel analyses, following the procedure specified in either [paragraph \(h\)\(1\)\(i\)](#) or [\(ii\)](#) of this section.

(i) For data collected using test methods supported by the EPA's Electronic Reporting Tool (ERT) as listed on the EPA's ERT Web site (<http://www.epa.gov/ttn/chief/ert/index.html>), you must submit the results of the performance test to the EPA via the Compliance and Emissions Data Reporting Interface (CEDRI). (CEDRI can be accessed through the EPA's Central Data Exchange (CDX) (<https://cdx.epa.gov/>.) Performance test data must be submitted in a file format generated through use of the EPA's ERT or an electronic file format consistent with the extensible markup language (XML) schema listed on the EPA's ERT Web site. If you claim that some of the performance test information being submitted is confidential business information (CBI), you must submit a complete file generated

through the use of the EPA's ERT or an alternate electronic file consistent with the XML schema listed on the EPA's ERT Web site, including information claimed to be CBI, on a compact disc, flash drive, or other commonly used electronic storage media to the EPA. The electronic media must be clearly marked as CBI and mailed to U.S. EPA/OAPQS/CORE CBI Office, Attention: Group Leader, Measurement Policy Group, MD C404-02, 4930 Old Page Rd., Durham, NC 27703. The same ERT or alternate file with the CBI omitted must be submitted to the EPA via the EPA's CDX as described earlier in this paragraph.

(ii) For data collected using test methods that are not supported by the EPA's ERT as listed on the EPA's ERT Web site at the time of the test, you must submit the results of the performance test to the Administrator at the appropriate address listed in [§ 63.13](#).

(2) Within 60 days after the date of completing each CEMS performance evaluation (as defined in 63.2), you must submit the results of the performance evaluation following the procedure specified in either [paragraph \(h\)\(2\)\(i\)](#) or [\(ii\)](#) of this section.

(i) For performance evaluations of continuous monitoring systems measuring relative accuracy test audit (RATA) pollutants that are supported by the EPA's ERT as listed on the EPA's ERT Web site at the time of the evaluation, you must submit the results of the performance evaluation to the EPA via the CEDRI. (CEDRI can be accessed through the EPA's CDX.) Performance evaluation data must be submitted in a file format generated through the use of the EPA's ERT or an alternate file format consistent with the XML schema listed on the EPA's ERT Web site. If you claim that some of the performance evaluation information being transmitted is CBI, you must submit a complete file generated through the use of the EPA's ERT or an alternate electronic file consistent with the XML schema listed on the EPA's ERT Web site, including information claimed to be CBI, on a compact disc, flash drive, or other commonly used electronic storage media to the EPA. The electronic media must be clearly marked as CBI and mailed to U.S. EPA/OAPQS/CORE CBI Office, Attention: Group Leader, Measurement Policy Group, MD C404-02, 4930 Old Page Rd., Durham, NC 27703. The same ERT or alternate file with the CBI omitted must be submitted to the EPA via the EPA's CDX as described earlier in this paragraph.

(ii) For any performance evaluations of continuous monitoring systems measuring RATA pollutants that are not supported by the EPA's ERT as listed on the ERT Web site at the time of the evaluation, you must submit the results of the performance evaluation to the Administrator at the appropriate address listed in [§ 63.13](#).

(3) You must submit all reports required by Table 9 of this subpart electronically to the EPA via the CEDRI. (CEDRI can be accessed through the EPA's CDX.) You must use the appropriate electronic report in CEDRI for this subpart. Instead of using the electronic report in CEDRI for this subpart, you may submit an alternate electronic file consistent with the XML schema listed on the CEDRI Web site (<http://www.epa.gov/ttn/chief/cedri/index.html>), once the XML schema is available. If the reporting form specific to this subpart is not available in CEDRI at the time that the report is due, you must submit the report to the

Administrator at the appropriate address listed in [§ 63.13](#). You must begin submitting reports via CEDRI no later than 90 days after the form becomes available in CEDRI.

[[78 FR 7183](#), Jan. 31, 2013, as amended at [80 FR 72814](#), Nov. 20, 2015]

§ 63.7555 What records must I keep?

(a) You must keep records according to [paragraphs \(a\)\(1\)](#) and [\(2\)](#) of this section.

(1) A copy of each notification and report that you submitted to comply with this subpart, including all documentation supporting any Initial Notification or Notification of Compliance Status or semiannual compliance report that you submitted, according to the requirements in [§ 63.10\(b\)\(2\)\(xiv\)](#).

(2) Records of performance tests, fuel analyses, or other compliance demonstrations and performance evaluations as required in [§ 63.10\(b\)\(2\)\(viii\)](#).

(3) For units in the limited use subcategory, you must keep a copy of the federally enforceable permit that limits the annual capacity factor to less than or equal to 10 percent and fuel use records for the days the boiler or process heater was operating.

(b) For each CEMS, COMS, and continuous monitoring system you must keep records according to [paragraphs \(b\)\(1\)](#) through [\(5\)](#) of this section.

(1) Records described in [§ 63.10\(b\)\(2\)\(vii\)](#) through [\(xi\)](#).

(2) Monitoring data for continuous opacity monitoring system during a performance evaluation as required in [§ 63.6\(h\)\(7\)\(i\)](#) and [\(ii\)](#).

(3) Previous (*i.e.*, superseded) versions of the performance evaluation plan as required in [§ 63.8\(d\)\(3\)](#).

(4) Request for alternatives to relative accuracy test for CEMS as required in [§ 63.8\(f\)\(6\)\(i\)](#).

(5) Records of the date and time that each deviation started and stopped.

(c) You must keep the records required in Table 8 to this subpart including records of all monitoring data and calculated averages for applicable operating limits, such as opacity, pressure drop, pH, and operating load, to show continuous compliance with each emission limit and operating limit that applies to you.

(d) For each boiler or process heater subject to an emission limit in Tables 1, 2, or 11 through 13 to this subpart, you must also keep the applicable records in [paragraphs \(d\)\(1\)](#) through [\(11\)](#) of this section.

(1) You must keep records of monthly fuel use by each boiler or process heater, including the type(s) of fuel and amount(s) used.

(2) If you combust non-hazardous secondary materials that have been determined not to be solid waste pursuant to [§ 241.3\(b\)\(1\)](#) and [\(2\) of this chapter](#), you must keep a record that documents how the secondary material meets each of the legitimacy criteria under [§ 241.3\(d\)\(1\) of this chapter](#). If you combust a fuel that has been processed from a discarded non-hazardous secondary material pursuant to [§ 241.3\(b\)\(4\) of this chapter](#), you must keep records as to how the operations that produced the fuel satisfy the definition of processing in [§ 241.2 of this chapter](#). If the fuel received a non-waste determination pursuant to the petition process submitted under [§ 241.3\(c\) of this chapter](#), you must keep a record that documents how the fuel satisfies the requirements of the petition process. For operating units that combust non-hazardous secondary materials as fuel per [§ 241.4 of this chapter](#), you must keep records documenting that the material is listed as a non-waste under [§ 241.4\(a\) of this chapter](#). Units exempt from the incinerator standards under section 129(g)(1) of the Clean Air Act because they are qualifying facilities burning a homogeneous waste stream do not need to maintain the records described in this [paragraph \(d\)\(2\)](#).

(3) A copy of all calculations and supporting documentation of maximum chlorine fuel input, using Equation 7 of [§ 63.7530](#), that were done to demonstrate continuous compliance with the HCl emission limit, for sources that demonstrate compliance through performance testing. For sources that demonstrate compliance through fuel analysis, a copy of all calculations and supporting documentation of HCl emission rates, using Equation 16 of [§ 63.7530](#), that were done to demonstrate compliance with the HCl emission limit. Supporting documentation should include results of any fuel analyses and basis for the estimates of maximum chlorine fuel input or HCl emission rates. You can use the results from one fuel analysis for multiple boilers and process heaters provided they are all burning the same fuel type. However, you must calculate chlorine fuel input, or HCl emission rate, for each boiler and process heater.

(4) A copy of all calculations and supporting documentation of maximum mercury fuel input, using Equation 8 of [§ 63.7530](#), that were done to demonstrate continuous compliance with the mercury emission limit for sources that demonstrate compliance through performance testing. For sources that demonstrate compliance through fuel analysis, a copy of all calculations and supporting documentation of mercury emission rates, using Equation 17 of [§ 63.7530](#), that were done to demonstrate compliance with the mercury emission limit. Supporting documentation should include results of any fuel analyses and basis for the estimates of maximum mercury fuel input or mercury emission rates. You can use the results from one fuel analysis for multiple boilers and process heaters provided they are all burning the same fuel type. However, you must calculate mercury fuel input, or mercury emission rates, for each boiler and process heater.

(5) If, consistent with [§ 63.7515\(b\)](#), you choose to stack test less frequently than annually, you must keep a record that documents that your emissions in the previous stack test(s) were less than 75 percent of the applicable emission limit (or, in specific instances noted in Tables 1 and 2 or 11 through 13 to this subpart, less than the applicable emission limit), and

document that there was no change in source operations including fuel composition and operation of air pollution control equipment that would cause emissions of the relevant pollutant to increase within the past year.

(6) Records of the occurrence and duration of each malfunction of the boiler or process heater, or of the associated air pollution control and monitoring equipment.

(7) Records of actions taken during periods of malfunction to minimize emissions in accordance with the general duty to minimize emissions in [§ 63.7500\(a\)\(3\)](#), including corrective actions to restore the malfunctioning boiler or process heater, air pollution control, or monitoring equipment to its normal or usual manner of operation.

(8) A copy of all calculations and supporting documentation of maximum TSM fuel input, using Equation 9 of [§ 63.7530](#), that were done to demonstrate continuous compliance with the TSM emission limit for sources that demonstrate compliance through performance testing. For sources that demonstrate compliance through fuel analysis, a copy of all calculations and supporting documentation of TSM emission rates, using Equation 18 of [§ 63.7530](#), that were done to demonstrate compliance with the TSM emission limit. Supporting documentation should include results of any fuel analyses and basis for the estimates of maximum TSM fuel input or TSM emission rates. You can use the results from one fuel analysis for multiple boilers and process heaters provided they are all burning the same fuel type. However, you must calculate TSM fuel input, or TSM emission rates, for each boiler and process heater.

(9) You must maintain records of the calendar date, time, occurrence and duration of each startup and shutdown.

(10) You must maintain records of the type(s) and amount(s) of fuels used during each startup and shutdown.

(11) For each startup period, for units selecting paragraph (2) of the definition of “startup” in [§ 63.7575](#) you must maintain records of the time that clean fuel combustion begins; the time when you start feeding fuels that are not clean fuels; the time when useful thermal energy is first supplied; and the time when the PM controls are engaged.

(12) If you choose to rely on paragraph (2) of the definition of “startup” in [§ 63.7575](#), for each startup period, you must maintain records of the hourly steam temperature, hourly steam pressure, hourly steam flow, hourly flue gas temperature, and all hourly average CMS data (*e.g.*, CEMS, PM CPMS, COMS, ESP total secondary electric power input, scrubber pressure drop, scrubber liquid flow rate) collected during each startup period to confirm that the control devices are engaged. In addition, if compliance with the PM emission limit is demonstrated using a PM control device, you must maintain records as specified in [paragraphs \(d\)\(12\)\(i\) through \(iii\)](#) of this section.

(i) For a boiler or process heater with an electrostatic precipitator, record the number of fields in service, as well as each field's secondary voltage and secondary current during each hour of startup.

(ii) For a boiler or process heater with a fabric filter, record the number of compartments in service, as well as the differential pressure across the baghouse during each hour of startup.

(iii) For a boiler or process heater with a wet scrubber needed for filterable PM control, record the scrubber's liquid flow rate and the pressure drop during each hour of startup.

(13) If you choose to use paragraph (2) of the definition of “startup” in [§ 63.7575](#) and you find that you are unable to safely engage and operate your PM control(s) within 1 hour of first firing of non-clean fuels, you may choose to rely on paragraph (1) of definition of “startup” in [§ 63.7575](#) or you may submit to the delegated permitting authority a request for a variance with the PM controls requirement, as described below.

(i) The request shall provide evidence of a documented manufacturer-identified safety issue.

(ii) The request shall provide information to document that the PM control device is adequately designed and sized to meet the applicable PM emission limit.

(iii) In addition, the request shall contain documentation that:

(A) The unit is using clean fuels to the maximum extent possible to bring the unit and PM control device up to the temperature necessary to alleviate or prevent the identified safety issues prior to the combustion of primary fuel;

(B) The unit has explicitly followed the manufacturer's procedures to alleviate or prevent the identified safety issue; and

(C) Identifies with specificity the details of the manufacturer's statement of concern.

(iv) You must comply with all other work practice requirements, including but not limited to data collection, recordkeeping, and reporting requirements.

(e) If you elect to average emissions consistent with [§ 63.7522](#), you must additionally keep a copy of the emission averaging implementation plan required in [§ 63.7522\(g\)](#), all calculations required under [§ 63.7522](#), including monthly records of heat input or steam generation, as applicable, and monitoring records consistent with [§ 63.7541](#).

(f) If you elect to use efficiency credits from energy conservation measures to demonstrate compliance according to [§ 63.7533](#), you must keep a copy of the Implementation Plan required in [§ 63.7533\(d\)](#) and copies of all data and calculations used to establish credits according to [§ 63.7533\(b\)](#), [\(c\)](#), and [\(f\)](#).

(g) If you elected to demonstrate that the unit meets the specification for mercury for the unit designed to burn gas 1 subcategory, you must maintain monthly records (or at the frequency required by [§ 63.7540\(c\)](#)) of the calculations and results of the fuel specification for mercury in Table 6.

(h) If you operate a unit in the unit designed to burn gas 1 subcategory that is subject to this subpart, and you use an alternative fuel other than natural gas, refinery gas, gaseous fuel subject to another subpart under this part, other gas 1 fuel, or gaseous fuel subject to another subpart of this part or part 60, 61, or 65, you must keep records of the total hours per calendar year that alternative fuel is burned and the total hours per calendar year that the unit operated during periods of gas curtailment or gas supply emergencies.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7185](#), Jan. 31, 2013; [80 FR 72816](#), Nov. 20, 2015]

§ 63.7560 In what form and how long must I keep my records?

(a) Your records must be in a form suitable and readily available for expeditious review, according to [§ 63.10\(b\)\(1\)](#).

(b) As specified in [§ 63.10\(b\)\(1\)](#), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record.

(c) You must keep each record on site, or they must be accessible from on site (for example, through a computer network), for at least 2 years after the date of each occurrence, measurement, maintenance, corrective action, report, or record, according to [§ 63.10\(b\)\(1\)](#). You can keep the records off site for the remaining 3 years.

Other Requirements and Information

§ 63.7565 What parts of the General Provisions apply to me?

Table 10 to this subpart shows which parts of the General Provisions in [§§ 63.1](#) through [63.15](#) apply to you.

§ 63.7570 Who implements and enforces this subpart?

(a) This subpart can be implemented and enforced by the EPA, or an Administrator such as your state, local, or tribal agency. If the EPA Administrator has delegated authority to your state, local, or tribal agency, then that agency (as well as the EPA) has the authority to implement and enforce this subpart. You should contact your EPA Regional Office to find out if this subpart is delegated to your state, local, or tribal agency.

(b) In delegating implementation and enforcement authority of this subpart to a state, local, or tribal agency under [40 CFR part 63, subpart E](#), the authorities listed in [paragraphs \(b\)\(1\) through \(4\)](#) of this section are retained by the EPA Administrator and are not transferred to the state, local, or tribal agency, however, the EPA retains oversight of this subpart and can take enforcement actions, as appropriate.

(1) Approval of alternatives to the emission limits and work practice standards in [§ 63.7500\(a\)](#) and [\(b\)](#) under [§ 63.6\(g\)](#), except as specified in [§ 63.7555\(d\)\(13\)](#).

(2) Approval of major change to test methods in Table 5 to this subpart under [§ 63.7\(e\)\(2\)\(ii\)](#) and [\(f\)](#) and as defined in [§ 63.90](#), and alternative analytical methods requested under [§ 63.7521\(b\)\(2\)](#).

(3) Approval of major change to monitoring under [§ 63.8\(f\)](#) and as defined in [§ 63.90](#), and approval of alternative operating parameters under [§§ 63.7500\(a\)\(2\)](#) and [63.7522\(g\)\(2\)](#).

(4) Approval of major change to recordkeeping and reporting under [§ 63.10\(e\)](#) and as defined in [§ 63.90](#).

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7186](#), Jan. 31, 2013; [80 FR 72817](#), Nov. 20, 2015]

§ 63.7575 What definitions apply to this subpart?

Terms used in this subpart are defined in the Clean Air Act, in [§ 63.2](#) (the General Provisions), and in this section as follows:

10-day rolling average means the arithmetic mean of the previous 240 hours of valid operating data. Valid data excludes hours during startup and shutdown, data collected during periods when the monitoring system is out of control as specified in your site-specific monitoring plan, while conducting repairs associated with periods when the monitoring system is out of control, or while conducting required monitoring system quality assurance or quality control activities, and periods when this unit is not operating. The 240 hours should be consecutive, but not necessarily continuous if operations were intermittent.

30-day rolling average means the arithmetic mean of the previous 720 hours of valid CO CEMS data. The 720 hours should be consecutive, but not necessarily continuous if operations were intermittent. For parameters other than CO, 30-day rolling average means either the arithmetic mean of all valid hours of data from 30 successive operating days or the arithmetic mean of the previous 720 hours of valid operating data. Valid data excludes hours during startup and shutdown, data collected during periods when the monitoring system is out of control as specified in your site-specific monitoring plan, while conducting repairs associated with periods when the monitoring system is out of control, or while conducting required monitoring system quality assurance or quality control activities, and periods when this unit is not operating.

Annual capacity factor means the ratio between the actual heat input to a boiler or process heater from the fuels burned during a calendar year and the potential heat input to the boiler or process heater had it been operated for 8,760 hours during a year at the maximum steady state design heat input capacity.

Annual heat input means the heat input for the 12 months preceding the compliance demonstration.

Average annual heat input rate means total heat input divided by the hours of operation for the 12 months preceding the compliance demonstration.

Bag leak detection system means a group of instruments that are capable of monitoring particulate matter loadings in the exhaust of a fabric filter (*i.e.*, baghouse) in order to detect bag failures. A bag leak detection system includes, but is not limited to, an instrument that operates on electrodynamic, triboelectric, light scattering, light transmittance, or other principle to monitor relative particulate matter loadings.

Benchmark means the fuel heat input for a boiler or process heater for the one-year period before the date that an energy demand reduction occurs, unless it can be demonstrated that a different time period is more representative of historical operations.

Biodiesel means a mono-alkyl ester derived from biomass and conforming to ASTM D6751-11b, Standard Specification for Biodiesel Fuel Blend Stock (B100) for Middle Distillate Fuels (incorporated by reference, see [§ 63.14](#)).

Biomass or bio-based solid fuel means any biomass-based solid fuel that is not a solid waste. This includes, but is not limited to, wood residue; wood products (*e.g.*, trees, tree stumps, tree limbs, bark, lumber, sawdust, sander dust, chips, scraps, slabs, millings, and shavings); animal manure, including litter and other bedding materials; vegetative agricultural and silvicultural materials, such as logging residues (slash), nut and grain hulls and chaff (*e.g.*, almond, walnut, peanut, rice, and wheat), bagasse, orchard prunings, corn stalks, coffee bean hulls and grounds. This definition of biomass is not intended to suggest that these materials are or are not solid waste.

Blast furnace gas fuel-fired boiler or process heater means an industrial/commercial/institutional boiler or process heater that receives 90 percent or more of its total annual gas volume from blast furnace gas.

Boiler means an enclosed device using controlled flame combustion and having the primary purpose of recovering thermal energy in the form of steam or hot water. Controlled flame combustion refers to a steady-state, or near steady-state, process wherein fuel and/or oxidizer feed rates are controlled. A device combusting solid waste, as defined in [§ 241.3 of this chapter](#), is not a boiler unless the device is exempt from the definition of a solid waste incineration unit as provided in section 129(g)(1) of the Clean Air Act. Waste heat boilers are excluded from this definition.

Boiler system means the boiler and associated components, such as, the feed water system, the combustion air system, the fuel system (including burners), blowdown system, combustion control systems, steam systems, and condensate return systems.

Calendar year means the period between January 1 and December 31, inclusive, for a given year.

Clean dry biomass means any biomass-based solid fuel that have not been painted, pigment-stained, or pressure treated, does not contain contaminants at concentrations not normally associated with virgin biomass materials and has a moisture content of less than 20 percent and is not a solid waste.

Coal means all solid fuels classifiable as anthracite, bituminous, sub-bituminous, or lignite by ASTM D388 (incorporated by reference, see [§ 63.14](#)), coal refuse, and petroleum coke. For the purposes of this subpart, this definition of “coal” includes synthetic fuels derived from coal, including but not limited to, solvent-refined coal, coal-oil mixtures, and coal-water mixtures. Coal derived gases are excluded from this definition.

Coal refuse means any by-product of coal mining or coal cleaning operations with an ash content greater than 50 percent (by weight) and a heating value less than 13,900 kilojoules per kilogram (6,000 Btu per pound) on a dry basis.

Commercial/institutional boiler means a boiler used in commercial establishments or institutional establishments such as medical centers, nursing homes, research centers, institutions of higher education, elementary and secondary schools, libraries, religious establishments, governmental buildings, hotels, restaurants, and laundries to provide electricity, steam, and/or hot water.

Common stack means the exhaust of emissions from two or more affected units through a single flue. Affected units with a common stack may each have separate air pollution control systems located before the common stack, or may have a single air pollution control system located after the exhausts come together in a single flue.

Cost-effective energy conservation measure means a measure that is implemented to improve the energy efficiency of the boiler or facility that has a payback (return of investment) period of 2 years or less.

Daily block average means the arithmetic mean of all valid emission concentrations or parameter levels recorded when a unit is operating measured over the 24-hour period from 12 a.m. (midnight) to 12 a.m. (midnight), except for periods of startup and shutdown or downtime.

Deviation.

(1) **Deviation** means any instance in which an affected source subject to this subpart, or an owner or operator of such a source:

(i) Fails to meet any applicable requirement or obligation established by this subpart including, but not limited to, any emission limit, operating limit, or work practice standard; or

(ii) Fails to meet any term or condition that is adopted to implement an applicable requirement in this subpart and that is included in the operating permit for any affected source required to obtain such a permit.

(2) A deviation is not always a violation.

Dioxins/furans means tetra- through octa-chlorinated dibenzo-p-dioxins and dibenzofurans.

Distillate oil means fuel oils that contain 0.05 weight percent nitrogen or less and comply with the specifications for fuel oil numbers 1 and 2, as defined by the American Society of Testing and Materials in ASTM D396 (incorporated by reference, see [§ 63.14](#)) or diesel fuel oil numbers 1 and 2, as defined by the American Society for Testing and Materials in ASTM D975 (incorporated by reference, see [§ 63.14](#)), kerosene, and biodiesel as defined by the American Society of Testing and Materials in ASTM D6751-11b (incorporated by reference, see [§ 60.14](#)).

Dry scrubber means an add-on air pollution control system that injects dry alkaline sorbent (dry injection) or sprays an alkaline sorbent (spray dryer) to react with and neutralize acid gas in the exhaust stream forming a dry powder material. Sorbent injection systems used as control devices in fluidized bed boilers and process heaters are included in this definition. A dry scrubber is a dry control system.

Dutch oven means a unit having a refractory-walled cell connected to a conventional boiler setting. Fuel materials are introduced through an opening in the roof of the dutch oven and burn in a pile on its floor. Fluidized bed boilers are not part of the dutch oven design category.

Efficiency credit means emission reductions above those required by this subpart. Efficiency credits generated may be used to comply with the emissions limits. Credits may come from pollution prevention projects that result in reduced fuel use by affected units. Boilers that are shut down cannot be used to generate credits unless the facility provides documentation linking the permanent shutdown to implementation of the energy conservation measures identified in the energy assessment.

Electric utility steam generating unit (EGU) means a fossil fuel-fired combustion unit of more than 25 megawatts electric (MWe) that serves a generator that produces electricity for sale. A fossil fuel-fired unit that cogenerates steam and electricity and supplies more than one-third of its potential electric output capacity and more than 25 MWe output to any utility power distribution system for sale is considered an electric utility steam generating unit. To be “capable of combusting” fossil fuels, an EGU would need to have these fuels allowed in their operating permits and have the appropriate fuel handling facilities on-site or otherwise available (e.g., coal handling equipment, including coal storage area, belts and conveyers, pulverizers, etc.; oil storage facilities). In addition, fossil fuel-fired EGU means any EGU that fired fossil fuel for more than 10.0 percent of the average annual heat input in any 3 consecutive calendar years or

for more than 15.0 percent of the annual heat input during any one calendar year after April 16, 2012.

Electrostatic precipitator (ESP) means an add-on air pollution control device used to capture particulate matter by charging the particles using an electrostatic field, collecting the particles using a grounded collecting surface, and transporting the particles into a hopper. An electrostatic precipitator is usually a dry control system.

Energy assessment means the following for the emission units covered by this subpart:

(1) The energy assessment for facilities with affected boilers and process heaters with a combined heat input capacity of less than 0.3 trillion Btu (TBtu) per year will be 8 on-site technical labor hours in length maximum, but may be longer at the discretion of the owner or operator of the affected source. The boiler system(s), process heater(s), and any on-site energy use system(s) accounting for at least 50 percent of the affected boiler(s) energy (*e.g.*, steam, hot water, process heat, or electricity) production, as applicable, will be evaluated to identify energy savings opportunities, within the limit of performing an 8-hour on-site energy assessment.

(2) The energy assessment for facilities with affected boilers and process heaters with a combined heat input capacity of 0.3 to 1.0 TBtu/year will be 24 on-site technical labor hours in length maximum, but may be longer at the discretion of the owner or operator of the affected source. The boiler system(s), process heater(s), and any on-site energy use system(s) accounting for at least 33 percent of the energy (*e.g.*, steam, hot water, process heat, or electricity) production, as applicable, will be evaluated to identify energy savings opportunities, within the limit of performing a 24-hour on-site energy assessment.

(3) The energy assessment for facilities with affected boilers and process heaters with a combined heat input capacity greater than 1.0 TBtu/year will be up to 24 on-site technical labor hours in length for the first TBtu/yr plus 8 on-site technical labor hours for every additional 1.0 TBtu/yr not to exceed 160 on-site technical hours, but may be longer at the discretion of the owner or operator of the affected source. The boiler system(s), process heater(s), and any on-site energy use system(s) accounting for at least 20 percent of the energy (*e.g.*, steam, process heat, hot water, or electricity) production, as applicable, will be evaluated to identify energy savings opportunities.

(4) The on-site energy use systems serving as the basis for the percent of affected boiler(s) and process heater(s) energy production in paragraphs (1), (2), and (3) of this definition may be segmented by production area or energy use area as most logical and applicable to the specific facility being assessed (*e.g.*, product X manufacturing area; product Y drying area; Building Z).

Energy management practices means the set of practices and procedures designed to manage energy use that are demonstrated by the facility's energy policies, a facility energy manager and other staffing responsibilities, energy performance measurement and tracking methods, an

energy saving goal, action plans, operating procedures, internal reporting requirements, and periodic review intervals used at the facility.

Energy management program means a program that includes a set of practices and procedures designed to manage energy use that are demonstrated by the facility's energy policies, a facility energy manager and other staffing responsibilities, energy performance measurement and tracking methods, an energy saving goal, action plans, operating procedures, internal reporting requirements, and periodic review intervals used at the facility. Facilities may establish their program through energy management systems compatible with ISO 50001.

Energy use system includes the following systems located on-site that use energy (steam, hot water, or electricity) provided by the affected boiler or process heater: process heating; compressed air systems; machine drive (motors, pumps, fans); process cooling; facility heating, ventilation, and air-conditioning systems; hot water systems; building envelop; and lighting; or other systems that use steam, hot water, process heat, or electricity provided by the affected boiler or process heater. Energy use systems are only those systems using energy clearly produced by affected boilers and process heaters.

Equivalent means the following only as this term is used in Table 6 to this subpart:

- (1) An equivalent sample collection procedure means a published voluntary consensus standard or practice (VCS) or EPA method that includes collection of a minimum of three composite fuel samples, with each composite consisting of a minimum of three increments collected at approximately equal intervals over the test period.
- (2) An equivalent sample compositing procedure means a published VCS or EPA method to systematically mix and obtain a representative subsample (part) of the composite sample.
- (3) An equivalent sample preparation procedure means a published VCS or EPA method that: Clearly states that the standard, practice or method is appropriate for the pollutant and the fuel matrix; or is cited as an appropriate sample preparation standard, practice or method for the pollutant in the chosen VCS or EPA determinative or analytical method.
- (4) An equivalent procedure for determining heat content means a published VCS or EPA method to obtain gross calorific (or higher heating) value.
- (5) An equivalent procedure for determining fuel moisture content means a published VCS or EPA method to obtain moisture content. If the sample analysis plan calls for determining metals (especially the mercury, selenium, or arsenic) using an aliquot of the dried sample, then the drying temperature must be modified to prevent vaporizing these metals. On the other hand, if metals analysis is done on an "as received" basis, a separate aliquot can be dried to determine moisture content and the metals concentration mathematically adjusted to a dry basis.
- (6) An equivalent pollutant (mercury, HCl) determinative or analytical procedure means a published VCS or EPA method that clearly states that the standard, practice, or method is

appropriate for the pollutant and the fuel matrix and has a published detection limit equal or lower than the methods listed in Table 6 to this subpart for the same purpose.

Fabric filter means an add-on air pollution control device used to capture particulate matter by filtering gas streams through filter media, also known as a baghouse. A fabric filter is a dry control system.

Federally enforceable means all limitations and conditions that are enforceable by the EPA Administrator, including, but not limited to, the requirements of [40 CFR parts 60, 61, 63, and 65](#), requirements within any applicable state implementation plan, and any permit requirements established under [40 CFR 52.21](#) or under [40 CFR 51.18](#) and [40 CFR 51.24](#).

Fluidized bed boiler means a boiler utilizing a fluidized bed combustion process that is not a pulverized coal boiler.

Fluidized bed boiler with an integrated fluidized bed heat exchanger means a boiler utilizing a fluidized bed combustion where the entire tube surface area is located outside of the furnace section at the exit of the cyclone section and exposed to the flue gas stream for conductive heat transfer. This design applies only to boilers in the unit designed to burn coal/solid fossil fuel subcategory that fire coal refuse.

Fluidized bed combustion means a process where a fuel is burned in a bed of granulated particles, which are maintained in a mobile suspension by the forward flow of air and combustion products.

Fossil fuel means natural gas, oil, coal, and any form of solid, liquid, or gaseous fuel derived from such material.

Fuel cell means a boiler type in which the fuel is dropped onto suspended fixed grates and is fired in a pile. The refractory-lined fuel cell uses combustion air preheating and positioning of secondary and tertiary air injection ports to improve boiler efficiency. Fluidized bed, dutch oven, pile burner, hybrid suspension grate, and suspension burners are not part of the fuel cell subcategory.

Fuel type means each category of fuels that share a common name or classification. Examples include, but are not limited to, bituminous coal, sub-bituminous coal, lignite, anthracite, biomass, distillate oil, residual oil. Individual fuel types received from different suppliers are not considered new fuel types.

Gaseous fuel includes, but is not limited to, natural gas, process gas, landfill gas, coal derived gas, refinery gas, and biogas. Blast furnace gas and process gases that are regulated under another subpart of this [part](#), or [part 60](#), [part 61](#), or [part 65 of this chapter](#), are exempted from this definition.

Heat input means heat derived from combustion of fuel in a boiler or process heater and does not include the heat input from preheated combustion air, recirculated flue gases, returned

condensate, or exhaust gases from other sources such as gas turbines, internal combustion engines, kilns, etc.

Heavy liquid includes residual oil and any other liquid fuel not classified as a light liquid.

Hourly average means the arithmetic average of at least four CMS data values representing the four 15-minute periods in an hour, or at least two 15-minute data values during an hour when CMS calibration, quality assurance, or maintenance activities are being performed.

Hot water heater means a closed vessel with a capacity of no more than 120 U.S. gallons in which water is heated by combustion of gaseous, liquid, or biomass/bio-based solid fuel and is withdrawn for use external to the vessel. Hot water boilers (i.e., not generating steam) combusting gaseous, liquid, or biomass fuel with a heat input capacity of less than 1.6 million Btu per hour are included in this definition. The 120 U.S. gallon capacity threshold to be considered a hot water heater is independent of the 1.6 MMBtu/hr heat input capacity threshold for hot water boilers. Hot water heater also means a tankless unit that provides on demand hot water.

Hybrid suspension grate boiler means a boiler designed with air distributors to spread the fuel material over the entire width and depth of the boiler combustion zone. The biomass fuel combusted in these units exceeds a moisture content of 40 percent on an as-fired annual heat input basis as demonstrated by monthly fuel analysis. The drying and much of the combustion of the fuel takes place in suspension, and the combustion is completed on the grate or floor of the boiler. Fluidized bed, dutch oven, and pile burner designs are not part of the hybrid suspension grate boiler design category.

Industrial boiler means a boiler used in manufacturing, processing, mining, and refining or any other industry to provide steam, hot water, and/or electricity.

Light liquid includes distillate oil, biodiesel, or vegetable oil.

Limited-use boiler or process heater means any boiler or process heater that burns any amount of solid, liquid, or gaseous fuels and has a federally enforceable annual capacity factor of no more than 10 percent.

Liquid fuel includes, but is not limited to, light liquid, heavy liquid, any form of liquid fuel derived from petroleum, used oil, liquid biofuels, biodiesel, and vegetable oil.

Load fraction means the actual heat input of a boiler or process heater divided by heat input during the performance test that established the minimum sorbent injection rate or minimum activated carbon injection rate, expressed as a fraction (*e.g.*, for 50 percent load the load fraction is 0.5). For boilers and process heaters that co-fire natural gas or refinery gas with a solid or liquid fuel, the load fraction is determined by the actual heat input of the solid or liquid fuel divided by heat input of the solid or liquid fuel fired during the performance test (*e.g.*, if the performance test was conducted at 100 percent solid fuel firing, for 100 percent load firing 50 percent solid fuel and 50 percent natural gas the load fraction is 0.5).

Major source for oil and natural gas production facilities, as used in this subpart, shall have the same meaning as in [§ 63.2](#), except that:

- (1) Emissions from any oil or gas exploration or production well (with its associated equipment, as defined in this section), and emissions from any pipeline compressor station or pump station shall not be aggregated with emissions from other similar units to determine whether such emission points or stations are major sources, even when emission points are in a contiguous area or under common control;
- (2) Emissions from processes, operations, or equipment that are not part of the same facility, as defined in this section, shall not be aggregated; and
- (3) For facilities that are production field facilities, only HAP emissions from glycol dehydration units and storage vessels with the potential for flash emissions shall be aggregated for a major source determination. For facilities that are not production field facilities, HAP emissions from all HAP emission units shall be aggregated for a major source determination.

Metal process furnaces are a subcategory of process heaters, as defined in this subpart, which include natural gas-fired annealing furnaces, preheat furnaces, reheat furnaces, aging furnaces, heat treat furnaces, and homogenizing furnaces.

Million Btu (MMBtu) means one million British thermal units.

Minimum activated carbon injection rate means load fraction multiplied by the lowest hourly average activated carbon injection rate measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limit.

Minimum oxygen level means the lowest hourly average oxygen level measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limit.

Minimum pressure drop means the lowest hourly average pressure drop measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limit.

Minimum scrubber effluent pH means the lowest hourly average sorbent liquid pH measured at the inlet to the wet scrubber according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable hydrogen chloride emission limit.

Minimum scrubber liquid flow rate means the lowest hourly average liquid flow rate (e.g., to the PM scrubber or to the acid gas scrubber) measured according to Table 7 to this subpart during the most recent performance stack test demonstrating compliance with the applicable emission limit.

Minimum scrubber pressure drop means the lowest hourly average scrubber pressure drop measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limit.

Minimum sorbent injection rate means:

- (1) The load fraction multiplied by the lowest hourly average sorbent injection rate for each sorbent measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limits; or
- (2) For fluidized bed combustion not using an acid gas wet scrubber or dry sorbent injection control technology to comply with the HCl emission limit, the lowest average ratio of sorbent to sulfur measured during the most recent performance test.

Minimum total secondary electric power means the lowest hourly average total secondary electric power determined from the values of secondary voltage and secondary current to the electrostatic precipitator measured according to Table 7 to this subpart during the most recent performance test demonstrating compliance with the applicable emission limits.

Natural gas means:

- (1) A naturally occurring mixture of hydrocarbon and nonhydrocarbon gases found in geologic formations beneath the earth's surface, of which the principal constituent is methane; or
- (2) Liquefied petroleum gas, as defined in ASTM D1835 (incorporated by reference, see [§ 63.14](#)); or
- (3) A mixture of hydrocarbons that maintains a gaseous state at ISO conditions. Additionally, natural gas must either be composed of at least 70 percent methane by volume or have a gross calorific value between 35 and 41 megajoules (MJ) per dry standard cubic meter (950 and 1,100 Btu per dry standard cubic foot); or
- (4) Propane or propane derived synthetic natural gas. Propane means a colorless gas derived from petroleum and natural gas, with the molecular structure C_3H_8 .

Opacity means the degree to which emissions reduce the transmission of light and obscure the view of an object in the background.

Operating day means a 24-hour period between 12 midnight and the following midnight during which any fuel is combusted at any time in the boiler or process heater unit. It is not necessary for fuel to be combusted for the entire 24-hour period. For calculating rolling average emissions, an operating day does not include the hours of operation during startup or shutdown.

Other combustor means a unit designed to burn solid fuel that is not classified as a dutch oven, fluidized bed, fuel cell, hybrid suspension grate boiler, pulverized coal boiler, stoker, sloped grate, or suspension boiler as defined in this subpart.

Other gas 1 fuel means a gaseous fuel that is not natural gas or refinery gas and does not exceed a maximum concentration of 40 micrograms/cubic meters of mercury.

Oxygen analyzer system means all equipment required to determine the oxygen content of a gas stream and used to monitor oxygen in the boiler or process heater flue gas, boiler or process heater, firebox, or other appropriate location. This definition includes oxygen trim systems. The source owner or operator must install, calibrate, maintain, and operate the oxygen analyzer system in accordance with the manufacturer's recommendations.

Oxygen trim system means a system of monitors that is used to maintain excess air at the desired level in a combustion device over its operating load range. A typical system consists of a flue gas oxygen and/or CO monitor that automatically provides a feedback signal to the combustion air controller or draft controller.

Particulate matter (PM) means any finely divided solid or liquid material, other than uncombined water, as measured by the test methods specified under this subpart, or an approved alternative method.

Period of gas curtailment or supply interruption means a period of time during which the supply of gaseous fuel to an affected boiler or process heater is restricted or halted for reasons beyond the control of the facility. The act of entering into a contractual agreement with a supplier of natural gas established for curtailment purposes does not constitute a reason that is under the control of a facility for the purposes of this definition. An increase in the cost or unit price of natural gas due to normal market fluctuations not during periods of supplier delivery restriction does not constitute a period of natural gas curtailment or supply interruption. On-site gaseous fuel system emergencies or equipment failures qualify as periods of supply interruption when the emergency or failure is beyond the control of the facility.

Pile burner means a boiler design incorporating a design where the anticipated biomass fuel has a high relative moisture content. Grates serve to support the fuel, and underfire air flowing up through the grates provides oxygen for combustion, cools the grates, promotes turbulence in the fuel bed, and fires the fuel. The most common form of pile burning is the dutch oven.

Process heater means an enclosed device using controlled flame, and the unit's primary purpose is to transfer heat indirectly to a process material (liquid, gas, or solid) or to a heat transfer material (e.g., glycol or a mixture of glycol and water) for use in a process unit, instead of generating steam. Process heaters are devices in which the combustion gases do not come into direct contact with process materials. A device combusting solid waste, as defined in [§ 241.3 of this chapter](#), is not a process heater unless the device is exempt from the definition of a solid waste incineration unit as provided in section 129(g)(1) of the Clean Air Act. Process heaters do not include units used for comfort heat or space heat, food preparation for on-site consumption, or autoclaves. Waste heat process heaters are excluded from this definition.

Pulverized coal boiler means a boiler in which pulverized coal or other solid fossil fuel is introduced into an air stream that carries the coal to the combustion chamber of the boiler where it is fired in suspension.

Qualified energy assessor means:

(1) Someone who has demonstrated capabilities to evaluate energy savings opportunities for steam generation and major energy using systems, including, but not limited to:

- (i) Boiler combustion management.
- (ii) Boiler thermal energy recovery, including
 - (A) Conventional feed water economizer,
 - (B) Conventional combustion air preheater, and
 - (C) Condensing economizer.
- (iii) Boiler blowdown thermal energy recovery.
- (iv) Primary energy resource selection, including
 - (A) Fuel (primary energy source) switching, and
 - (B) Applied steam energy versus direct-fired energy versus electricity.
- (v) Insulation issues.
- (vi) Steam trap and steam leak management.
- (vi) Condensate recovery.
- (viii) Steam end-use management.

(2) Capabilities and knowledge includes, but is not limited to:

- (i) Background, experience, and recognized abilities to perform the assessment activities, data analysis, and report preparation.
- (ii) Familiarity with operating and maintenance practices for steam or process heating systems.
- (iii) Additional potential steam system improvement opportunities including improving steam turbine operations and reducing steam demand.
- (iv) Additional process heating system opportunities including effective utilization of waste heat and use of proper process heating methods.
- (v) Boiler-steam turbine cogeneration systems.

(vi) Industry specific steam end-use systems.

Refinery gas means any gas that is generated at a petroleum refinery and is combusted. Refinery gas includes natural gas when the natural gas is combined and combusted in any proportion with a gas generated at a refinery. Refinery gas includes gases generated from other facilities when that gas is combined and combusted in any proportion with gas generated at a refinery.

Regulated gas stream means an offgas stream that is routed to a boiler or process heater for the purpose of achieving compliance with a standard under another subpart of this [part](#) or [part 60](#), [part 61](#), or [part 65 of this chapter](#).

Residential boiler means a boiler used to provide heat and/or hot water and/or as part of a residential combined heat and power system. This definition includes boilers located at an institutional facility (e.g., university campus, military base, church grounds) or commercial/industrial facility (e.g., farm) used primarily to provide heat and/or hot water for:

- (1) A dwelling containing four or fewer families; or
- (2) A single unit residence dwelling that has since been converted or subdivided into condominiums or apartments.

Residual oil means crude oil, fuel oil that does not comply with the specifications under the definition of distillate oil, and all fuel oil numbers 4, 5, and 6, as defined by the American Society of Testing and Materials in ASTM D396-10 (incorporated by reference, *see* [§ 63.14\(b\)](#)).

Responsible official means responsible official as defined in [§ 70.2](#).

Rolling average means the average of all data collected during the applicable averaging period. For demonstration of compliance with a CO CEMS-based emission limit based on CO concentration a 30-day (10-day) rolling average is comprised of the average of all the hourly average concentrations over the previous 720 (240) operating hours calculated each operating day. To demonstrate compliance on a 30-day rolling average basis for parameters other than CO, you must indicate the basis of the 30-day rolling average period you are using for compliance, as discussed in [§ 63.7545\(e\)\(2\)\(iii\)](#). If you indicate the 30 operating day basis, you must calculate a new average value each operating day and shall include the measured hourly values for the preceding 30 operating days. If you select the 720 operating hours basis, you must average of all the hourly average concentrations over the previous 720 operating hours calculated each operating day.

Secondary material means the material as defined in [§ 241.2 of this chapter](#).

Shutdown means the period in which cessation of operation of a boiler or process heater is initiated for any purpose. Shutdown begins when the boiler or process heater no longer supplies useful thermal energy (such as heat or steam) for heating, cooling, or process purposes and/or generates electricity or when no fuel is being fed to the boiler or process heater, whichever is earlier. Shutdown ends when the boiler or process heater no longer supplies useful thermal

energy (such as steam or heat) for heating, cooling, or process purposes and/or generates electricity, and no fuel is being combusted in the boiler or process heater.

Sloped grate means a unit where the solid fuel is fed to the top of the grate from where it slides downwards; while sliding the fuel first dries and then ignites and burns. The ash is deposited at the bottom of the grate. Fluidized bed, dutch oven, pile burner, hybrid suspension grate, suspension burners, and fuel cells are not considered to be a sloped grate design.

Solid fossil fuel includes, but is not limited to, coal, coke, petroleum coke, and tire derived fuel.

Solid fuel means any solid fossil fuel or biomass or bio-based solid fuel.

Startup means:

(1) Either the first-ever firing of fuel in a boiler or process heater for the purpose of supplying useful thermal energy for heating and/or producing electricity, or for any other purpose, or the firing of fuel in a boiler after a shutdown event for any purpose. Startup ends when any of the useful thermal energy from the boiler or process heater is supplied for heating, and/or producing electricity, or for any other purpose, or

(2) The period in which operation of a boiler or process heater is initiated for any purpose. Startup begins with either the first-ever firing of fuel in a boiler or process heater for the purpose of supplying useful thermal energy (such as steam or heat) for heating, cooling or process purposes, or producing electricity, or the firing of fuel in a boiler or process heater for any purpose after a shutdown event. Startup ends four hours after when the boiler or process heater supplies useful thermal energy (such as heat or steam) for heating, cooling, or process purposes, or generates electricity, whichever is earlier.

Steam output means:

(1) For a boiler that produces steam for process or heating only (no power generation), the energy content in terms of MMBtu of the boiler steam output,

(2) For a boiler that cogenerates process steam and electricity (also known as combined heat and power), the total energy output, which is the sum of the energy content of the steam exiting the turbine and sent to process in MMBtu and the energy of the electricity generated converted to MMBtu at a rate of 10,000 Btu per kilowatt-hour generated (10 MMBtu per megawatt-hour), and

(3) For a boiler that generates only electricity, the alternate output-based emission limits would be the appropriate emission limit from Table 1 or 2 of this subpart in units of pounds per million Btu heat input (lb per MWh).

(4) For a boiler that performs multiple functions and produces steam to be used for any combination of paragraphs (1), (2), and (3) of this definition that includes electricity generation of paragraph (3) of this definition, the total energy output, in terms of MMBtu of steam output,

is the sum of the energy content of steam sent directly to the process and/or used for heating (S_1), the energy content of turbine steam sent to process plus energy in electricity according to paragraph (2) of this definition (S_2), and the energy content of electricity generated by a electricity only turbine as paragraph (3) of this definition ($MW_{(3)}$) and would be calculated using Equation 21 of this section. In the case of boilers supplying steam to one or more common heaters, S_1 , S_2 , and $MW_{(3)}$ for each boiler would be calculated based on the its (steam energy) contribution (fraction of total steam energy) to the common heater.

$$SO_M = S_1 + S_2 + (MW_{(3)} \times CFn) \quad (\text{Eq. 21})$$

Where:

SO_M = Total steam output for multi-function boiler, MMBtu

S_1 = Energy content of steam sent directly to the process and/or used for heating, MMBtu

S_2 = Energy content of turbine steam sent to the process plus energy in electricity according to (2) above, MMBtu

$MW_{(3)}$ = Electricity generated according to paragraph (3) of this definition, MWh

CFn = Conversion factor for the appropriate subcategory for converting electricity generated according to paragraph (3) of this definition to equivalent steam energy, MMBtu/MWh

CFn for emission limits for boilers in the unit designed to burn solid fuel subcategory = 10.8

CFn PM and CO emission limits for boilers in one of the subcategories of units designed to burn coal = 11.7

CFn PM and CO emission limits for boilers in one of the subcategories of units designed to burn biomass = 12.1

CFn for emission limits for boilers in one of the subcategories of units designed to burn liquid fuel = 11.2

CFn for emission limits for boilers in the unit designed to burn gas 2 (other) subcategory = 6.2

Stoker means a unit consisting of a mechanically operated fuel feeding mechanism, a stationary or moving grate to support the burning of fuel and admit under-grate air to the fuel, an overfire air system to complete combustion, and an ash discharge system. This definition of stoker includes air swept stokers. There are two general types of stokers: Underfeed and overfeed. Overfeed stokers include mass feed and spreader stokers. Fluidized bed, dutch oven, pile burner, hybrid suspension grate, suspension burners, and fuel cells are not considered to be a stoker design.

Stoker/sloped grate/other unit designed to burn kiln dried biomass means the unit is in the units designed to burn biomass/bio-based solid subcategory that is either a stoker, sloped grate, or other combustor design and is not in the stoker/sloped grate/other units designed to burn wet biomass subcategory.

Stoker/sloped grate/other unit designed to burn wet biomass means the unit is in the units designed to burn biomass/bio-based solid subcategory that is either a stoker, sloped grate, or other combustor design and any of the biomass/bio-based solid fuel combusted in the unit exceeds 20 percent moisture on an annual heat input basis.

Suspension burner means a unit designed to fire dry biomass/biobased solid particles in suspension that are conveyed in an airstream to the furnace like pulverized coal. The combustion of the fuel material is completed on a grate or floor below. The biomass/biobased fuel combusted in the unit shall not exceed 20 percent moisture on an annual heat input basis. Fluidized bed, dutch oven, pile burner, and hybrid suspension grate units are not part of the suspension burner subcategory.

Temporary boiler means any gaseous or liquid fuel boiler or process heater that is designed to, and is capable of, being carried or moved from one location to another by means of, for example, wheels, skids, carrying handles, dollies, trailers, or platforms. A boiler or process heater is not a temporary boiler or process heater if any one of the following conditions exists:

- (1) The equipment is attached to a foundation.
- (2) The boiler or process heater or a replacement remains at a location within the facility and performs the same or similar function for more than 12 consecutive months, unless the regulatory agency approves an extension. An extension may be granted by the regulating agency upon petition by the owner or operator of a unit specifying the basis for such a request. Any temporary boiler or process heater that replaces a temporary boiler or process heater at a location and performs the same or similar function will be included in calculating the consecutive time period.
- (3) The equipment is located at a seasonal facility and operates during the full annual operating period of the seasonal facility, remains at the facility for at least 2 years, and operates at that facility for at least 3 months each year.
- (4) The equipment is moved from one location to another within the facility but continues to perform the same or similar function and serve the same electricity, process heat, steam, and/or hot water system in an attempt to circumvent the residence time requirements of this definition.

Total selected metals (TSM) means the sum of the following metallic hazardous air pollutants: arsenic, beryllium, cadmium, chromium, lead, manganese, nickel and selenium.

Traditional fuel means the fuel as defined in [§ 241.2 of this chapter](#).

Tune-up means adjustments made to a boiler or process heater in accordance with the procedures outlined in [§ 63.7540\(a\)\(10\)](#).

Ultra low sulfur liquid fuel means a distillate oil that has less than or equal to 15 ppm sulfur.

Unit designed to burn biomass/bio-based solid subcategory includes any boiler or process heater that burns at least 10 percent biomass or bio-based solids on an annual heat input basis in combination with solid fossil fuels, liquid fuels, or gaseous fuels.

Unit designed to burn coal/solid fossil fuel subcategory includes any boiler or process heater that burns any coal or other solid fossil fuel alone or at least 10 percent coal or other solid fossil fuel on an annual heat input basis in combination with liquid fuels, gaseous fuels, or less than 10 percent biomass and bio-based solids on an annual heat input basis.

Unit designed to burn gas 1 subcategory includes any boiler or process heater that burns only natural gas, refinery gas, and/or other gas 1 fuels. Gaseous fuel boilers and process heaters that burn liquid fuel for periodic testing of liquid fuel, maintenance, or operator training, not to exceed a combined total of 48 hours during any calendar year, are included in this definition. Gaseous fuel boilers and process heaters that burn liquid fuel during periods of gas curtailment or gas supply interruptions of any duration are also included in this definition.

Unit designed to burn gas 2 (other) subcategory includes any boiler or process heater that is not in the unit designed to burn gas 1 subcategory and burns any gaseous fuels either alone or in combination with less than 10 percent coal/solid fossil fuel, and less than 10 percent biomass/bio-based solid fuel on an annual heat input basis, and no liquid fuels. Gaseous fuel boilers and process heaters that are not in the unit designed to burn gas 1 subcategory and that burn liquid fuel for periodic testing of liquid fuel, maintenance, or operator training, not to exceed a combined total of 48 hours during any calendar year, are included in this definition. Gaseous fuel boilers and process heaters that are not in the unit designed to burn gas 1 subcategory and that burn liquid fuel during periods of gas curtailment or gas supply interruption of any duration are also included in this definition.

Unit designed to burn heavy liquid subcategory means a unit in the unit designed to burn liquid subcategory where at least 10 percent of the heat input from liquid fuels on an annual heat input basis comes from heavy liquids.

Unit designed to burn light liquid subcategory means a unit in the unit designed to burn liquid subcategory that is not part of the unit designed to burn heavy liquid subcategory.

Unit designed to burn liquid subcategory includes any boiler or process heater that burns any liquid fuel, but less than 10 percent coal/solid fossil fuel and less than 10 percent biomass/bio-based solid fuel on an annual heat input basis, either alone or in combination with gaseous fuels. Units in the unit design to burn gas 1 or unit designed to burn gas 2 (other) subcategories that burn liquid fuel for periodic testing of liquid fuel, maintenance, or operator training, not to exceed a combined total of 48 hours during any calendar year are not included in this definition. Units in the unit design to burn gas 1 or unit designed to burn gas 2 (other) subcategories during

periods of gas curtailment or gas supply interruption of any duration are also not included in this definition.

Unit designed to burn liquid fuel that is a non-continental unit means an industrial, commercial, or institutional boiler or process heater meeting the definition of the unit designed to burn liquid subcategory located in the State of Hawaii, the Virgin Islands, Guam, American Samoa, the Commonwealth of Puerto Rico, or the Northern Mariana Islands.

Unit designed to burn solid fuel subcategory means any boiler or process heater that burns only solid fuels or at least 10 percent solid fuel on an annual heat input basis in combination with liquid fuels or gaseous fuels.

Useful thermal energy means energy (*i.e.*, steam, hot water, or process heat) that meets the minimum operating temperature, flow, and/or pressure required by any energy use system that uses energy provided by the affected boiler or process heater.

Vegetable oil means oils extracted from vegetation.

Voluntary Consensus Standards or VCS mean technical standards (*e.g.*, materials specifications, test methods, sampling procedures, business practices) developed or adopted by one or more voluntary consensus bodies. EPA/Office of Air Quality Planning and Standards, by precedent, has only used VCS that are written in English. Examples of VCS bodies are: American Society of Testing and Materials (ASTM 100 Barr Harbor Drive, P.O. Box CB700, West Conshohocken, Pennsylvania 19428-B2959, (800) 262-1373, <http://www.astm.org>), American Society of Mechanical Engineers (ASME ASME, Three Park Avenue, New York, NY 10016-5990, (800) 843-2763, <http://www.asme.org>), International Standards Organization (ISO 1, ch. de la Voie-Creuse, Case postale 56, CH-1211 Geneva 20, Switzerland, + 41 22 749 01 11, <http://www.iso.org/iso/home.htm>), Standards Australia (AS Level 10, The Exchange Centre, 20 Bridge Street, Sydney, GPO Box 476, Sydney NSW 2001, + 61 2 9237 6171 <http://www.stadards.org.au>), British Standards Institution (BSI, 389 Chiswick High Road, London, W4 4AL, United Kingdom, + 44 (0)20 8996 9001, <http://www.bsigroup.com>), Canadian Standards Association (CSA 5060 Spectrum Way, Suite 100, Mississauga, Ontario L4W 5N6, Canada, 800-463-6727, <http://www.csa.ca>), European Committee for Standardization (CEN CENELEC Management Centre Avenue Marnix 17 B-1000 Brussels, Belgium + 32 2 550 08 11, <http://www.cen.eu/cen>), and German Engineering Standards (VDI VDI Guidelines Department, P.O. Box 10 11 39 40002, Duesseldorf, Germany, + 49 211 6214-230, <http://www.vdi.eu>). The types of standards that are not considered VCS are standards developed by: The United States, *e.g.*, California (CARB) and Texas (TCEQ); industry groups, such as American Petroleum Institute (API), Gas Processors Association (GPA), and Gas Research Institute (GRI); and other branches of the U.S. government, *e.g.*, Department of Defense (DOD) and Department of Transportation (DOT). This does not preclude EPA from using standards developed by groups that are not VCS bodies within their rule. When this occurs, EPA has done searches and reviews for VCS equivalent to these non-EPA methods.

Waste heat boiler means a device that recovers normally unused energy (*i.e.*, hot exhaust gas) and converts it to usable heat. Waste heat boilers are also referred to as heat recovery steam

generators. Waste heat boilers are heat exchangers generating steam from incoming hot exhaust gas from an industrial (e.g., thermal oxidizer, kiln, furnace) or power (e.g., combustion turbine, engine) equipment. Duct burners are sometimes used to increase the temperature of the incoming hot exhaust gas.

Waste heat process heater means an enclosed device that recovers normally unused energy (i.e., hot exhaust gas) and converts it to usable heat. Waste heat process heaters are also referred to as recuperative process heaters. This definition includes both fired and unfired waste heat process heaters.

Wet scrubber means any add-on air pollution control device that mixes an aqueous stream or slurry with the exhaust gases from a boiler or process heater to control emissions of particulate matter or to absorb and neutralize acid gases, such as hydrogen chloride. A wet scrubber creates an aqueous stream or slurry as a byproduct of the emissions control process.

Work practice standard means any design, equipment, work practice, or operational standard, or combination thereof, that is promulgated pursuant to section 112(h) of the Clean Air Act.

[[78 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7163](#), Jan. 31, 2013; [80 FR 72817](#), Nov. 20, 2015]

Table 1 to Subpart DDDDD of Part 63 - Emission Limits for New or Reconstructed Boilers and Process Heaters

As stated in [§ 63.7500](#), you must comply with the following applicable emission limits:

[Units with heat input capacity of 10 million Btu per hour or greater]

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	Or the emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
1. Units in all subcategories designed to burn solid fuel.	a. HCl	2.2E-02 lb per MMBtu of heat input	2.5E-02 lb per MMBtu of steam output or 0.28 lb per MWh	For M26A, collect a minimum of 1 dscm per run; for M26 collect a minimum

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	Or the emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
	b. Mercury	8.0E-07 ^a lb per MMBtu of heat input	8.7E-07 ^a lb per MMBtu of steam output or 1.1E-05 ^a lb per MWh	of 120 liters per run. For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 4 dscm.
2. Units designed to burn coal/solid fossil fuel	a. Filterable PM (or TSM)	1.1E-03 lb per MMBtu of heat input; or (2.3E-05 lb per MMBtu of heat input)	1.1E-03 lb per MMBtu of steam output or 1.4E-02 lb per MWh; or (2.7E-05 lb per MMBtu of steam output or 2.9E-04 lb per MWh)	Collect a minimum of 3 dscm per run.
3. Pulverized coal boilers designed to burn coal/solid fossil fuel	a. Carbon monoxide (CO) (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (320 ppm by volume on a dry basis corrected to 3 percent oxygen, ^d 30-	0.11 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	Or the emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
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4. Stokers/others designed to burn coal/solid fossil fuel	a. CO (or CEMS)	<p>day rolling average)</p> <p>130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (340 ppm by volume on a dry basis corrected to 3 percent oxygen,^d 30-day rolling average)</p>	<p>0.12 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average</p>	<p>1 hr minimum sampling time.</p>
5. Fluidized bed units designed to burn coal/solid fossil fuel	a. CO (or CEMS)	<p>130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (230 ppm by volume on a dry basis corrected to 3 percent oxygen,^d 30-day rolling average)</p>	<p>0.11 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average</p>	<p>1 hr minimum sampling time.</p>
6. Fluidized bed units with an integrated heat exchanger designed to burn coal/solid fossil fuel	a. CO (or CEMS)	<p>140 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (150 ppm by volume on a dry basis corrected to 3 percent oxygen,^d 30-</p>	<p>1.2E-01 lb per MMBtu of steam output or 1.5 lb per MWh; 3-run average</p>	<p>1 hr minimum sampling time.</p>

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	Or the emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
7. Stokers/sloped grate/others designed to burn wet biomass fuel	a. CO (or CEMS)	<p>day rolling average)</p> <p>620 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (390 ppm by volume on a dry basis corrected to 3 percent oxygen,^d 30-day rolling average)</p>	<p>5.8E-01 lb per MMBtu of steam output or 6.8 lb per MWh; 3-run average</p>	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	<p>3.0E-02 lb per MMBtu of heat input; or (2.6E-05 lb per MMBtu of heat input)</p>	<p>3.5E-02 lb per MMBtu of steam output or 4.2E-01 lb per MWh; or (2.7E-05 lb per MMBtu of steam output or 3.7E-04 lb per MWh)</p>	Collect a minimum of 2 dscm per run.
8. Stokers/sloped grate/others designed to burn kiln-dried biomass fuel	a. CO	<p>460 ppm by volume on a dry basis corrected to 3 percent oxygen</p>	<p>4.2E-01 lb per MMBtu of steam output or 5.1 lb per MWh</p>	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	<p>3.0E-02 lb per MMBtu of heat input; or (4.0E-03 lb per MMBtu of heat</p>	<p>3.5E-02 lb per MMBtu of steam output or 4.2E-01 lb per MWh; or</p>	Collect a minimum of 2 dscm per run.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	Or the emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
		input)	(4.2E-03 lb per MMBtu of steam output or 5.6E-02 lb per MWh)	
9. Fluidized bed units designed to burn biomass/bio-based solids	a. CO (or CEMS)	230 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (310 ppm by volume on a dry basis corrected to 3 percent oxygen, ^d 30-day rolling average)	2.2E-01 lb per MMBtu of steam output or 2.6 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	9.8E-03 lb per MMBtu of heat input; or (8.3E-05 ^a lb per MMBtu of heat input)	1.2E-02 lb per MMBtu of steam output or 0.14 lb per MWh; or (1.1E-04 ^a lb per MMBtu of steam output or 1.2E-03 ^a lb per MWh)	Collect a minimum of 3 dscm per run.
10. Suspension burners designed to burn biomass/bio-based solids	a. CO (or CEMS)	2,400 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (2,000 ppm by volume on a dry	1.9 lb per MMBtu of steam output or 27 lb per MWh; 3-run average	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	Or the emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
		basis corrected to 3 percent oxygen, ^d 10-day rolling average)		
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (6.5E-03 lb per MMBtu of heat input)	3.1E-02 lb per MMBtu of steam output or 4.2E-01 lb per MWh; or (6.6E-03 lb per MMBtu of steam output or 9.1E-02 lb per MWh)	Collect a minimum of 2 dscm per run.
11. Dutch Ovens/Pile burners designed to burn biomass/bio-based solids	a. CO (or CEMS)	330 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (520 ppm by volume on a dry basis corrected to 3 percent oxygen, ^d 10-day rolling average)	3.5E-01 lb per MMBtu of steam output or 3.6 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.2E-03 lb per MMBtu of heat input; or (3.9E-05 lb per MMBtu of heat input)	4.3E-03 lb per MMBtu of steam output or 4.5E-02 lb per MWh; or (5.2E-05 lb per MMBtu of steam output or 5.5E-04	Collect a minimum of 3 dscm per run.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	Or the emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
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12. Fuel cell units designed to burn biomass/bio-based solids	a. CO	910 ppm by volume on a dry basis corrected to 3 percent oxygen	1.1 lb per MMBtu of steam output or 1.0E + 01 lb per MWh	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.0E-02 lb per MMBtu of heat input; or (2.9E-05 ^a lb per MMBtu of heat input)	3.0E-02 lb per MMBtu of steam output or 2.8E-01 lb per MWh; or (5.1E-05 lb per MMBtu of steam output or 4.1E-04 lb per MWh)	Collect a minimum of 2 dscm per run.
13. Hybrid suspension grate boiler designed to burn biomass/bio-based solids	a. CO (or CEMS)	1,100 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (900 ppm by volume on a dry basis corrected to 3 percent oxygen, ^d 30-day rolling average)	1.4 lb per MMBtu of steam output or 12 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.6E-02 lb per MMBtu of heat input; or (4.4E-04 lb per MMBtu of heat	3.3E-02 lb per MMBtu of steam output or 3.7E-01 lb per MWh; or	Collect a minimum of 3 dscm per run.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	Or the emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
		input)	(5.5E-04 lb per MMBtu of steam output or 6.2E-03 lb per MWh)	
14. Units designed to burn liquid fuel	a. HCl	4.4E-04 lb per MMBtu of heat input	4.8E-04 lb per MMBtu of steam output or 6.1E-03 lb per MWh	For M26A: Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	b. Mercury	4.8E-07 ^a lb per MMBtu of heat input	5.3E-07 ^a lb per MMBtu of steam output or 6.7E-06 ^a lb per MWh	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 4 dscm.
15. Units designed to burn heavy liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average	0.13 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or	1.3E-02 lb per MMBtu of heat	1.5E-02 lb per MMBtu of steam	Collect a minimum

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	Or the emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
	TSM)	input; or (7.5E-05 lb per MMBtu of heat input)	output or 1.8E-01 lb per MWh; or (8.2E-05 lb per MMBtu of steam output or 1.1E-03 lb per MWh)	of 3 dscm per run.
16. Units designed to burn light liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen	0.13 lb per MMBtu of steam output or 1.4 lb per MWh	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.1E-03 ^a lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	1.2E-03 ^a lb per MMBtu of steam output or 1.6E-02 ^a lb per MWh; or (3.2E-05 lb per MMBtu of steam output or 4.0E-04 lb per MWh)	Collect a minimum of 3 dscm per run.
17. Units designed to burn liquid fuel that are non-continental units	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average based on stack test	0.13 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or	2.3E-02 lb per MMBtu of heat input; or (8.6E-04 lb	2.5E-02 lb per MMBtu of steam output or 3.2E-01	Collect a minimum of 4 dscm per run.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	Or the emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
	TSM)	per MMBtu of heat input)	lb per MWh; or (9.4E-04 lb per MMBtu of steam output or 1.2E-02 lb per MWh)	
18. Units designed to burn gas 2 (other) gases	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen	0.16 lb per MMBtu of steam output or 1.0 lb per MWh	1 hr minimum sampling time.
	b. HCl	1.7E-03 lb per MMBtu of heat input	2.9E-03 lb per MMBtu of steam output or 1.8E-02 lb per MWh	For M26A, Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	c. Mercury	7.9E-06 lb per MMBtu of heat input	1.4E-05 lb per MMBtu of steam output or 8.3E-05 lb per MWh	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 3 dscm.
	d. Filterable PM (or	6.7E-03 lb per MMBtu of heat	1.2E-02 lb per MMBtu of steam	Collect a minimum

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	Or the emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
	TSM)	input; or (2.1E-04 lb per MMBtu of heat input)	output or 7.0E-02 lb per MWh; or (3.5E-04 lb per MMBtu of steam output or 2.2E-03 lb per MWh)	of 3 dscm per run.

^a If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit, you can skip testing according to [§ 63.7515](#) if all of the other provisions of [§ 63.7515](#) are met. For all other pollutants that do not contain a footnote “a”, your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

^b Incorporated by reference, see [§ 63.14](#).

^c If your affected source is a new or reconstructed affected source that commenced construction or reconstruction after June 4, 2010, and before April 1, 2013, you may comply with the emission limits in Tables 11, 12 or 13 to this subpart until January 31, 2016. On and after January 31, 2016, you must comply with the emission limits in Table 1 to this subpart.

^d An owner or operator may request an alternative test method under [§ 63.7 of this chapter](#), in order that compliance with the carbon monoxide emissions limit be determined using carbon dioxide as a diluent correction in place of oxygen at 3%. EPA Method 19 F-factors and EPA Method 19 equations must be used to generate the appropriate CO₂ correction percentage for the fuel type burned in the unit, and must also take into account that the 3% oxygen correction is to be done on a dry basis. The alternative test method request must account for any CO₂ being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc.

[[78 FR 7193](#), Jan. 31, 2013, as amended at [80 FR 72819](#), Nov. 20, 2015]

Table 2 to Subpart DDDDD of Part 63 - Emission Limits for Existing Boilers and Process Heaters

As stated in [§ 63.7500](#), you must comply with the following applicable emission limits:

[Units with heat input capacity of 10 million Btu per hour or greater]

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during startup and shutdown . . .	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
1. Units in all subcategories designed to burn solid fuel	a. HCl	2.2E-02 lb per MMBtu of heat input	2.5E-02 lb per MMBtu of steam output or 0.27 lb per MWh	For M26A, Collect a minimum of 1 dscm per run; for M26, collect a minimum of 120 liters per run.
	b. Mercury	5.7E-06 lb per MMBtu of heat input	6.4E-06 lb per MMBtu of steam output or 7.3E-05 lb per MWh	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 3 dscm.
2. Units design to burn coal/solid fossil fuel	a. Filterable PM (or TSM)	4.0E-02 lb per MMBtu of heat input; or (5.3E-05 lb per MMBtu of heat input)	4.2E-02 lb per MMBtu of steam output or 4.9E-01 lb per MWh; or (5.6E-05 lb per MMBtu of steam output or 6.5E-04	Collect a minimum of 2 dscm per run.

If your boiler or process heater is in this subcategory ...	For the following pollutants ...	The emissions must not exceed the following emission limits, except during startup and shutdown ...	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown ...	Using this specified sampling volume or test run duration ...
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lb per MWh)

3. Pulverized coal boilers designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (320 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	0.11 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.
4. Stokers/others designed to burn coal/solid fossil fuel	a. CO (or CEMS)	160 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (340 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	0.14 lb per MMBtu of steam output or 1.7 lb per MWh; 3-run average	1 hr minimum sampling time.
5. Fluidized bed units designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (230 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-	0.12 lb per MMBtu of steam output or 1.4 lb per MWh; 3-run average	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory ...	For the following pollutants ...	The emissions must not exceed the following emission limits, except during startup and shutdown ...	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown ...	Using this specified sampling volume or test run duration ...
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6. Fluidized bed units with an integrated heat exchanger designed to burn coal/solid fossil fuel	a. CO (or CEMS)	140 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (150 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1.3E-01 lb per MMBtu of steam output or 1.5 lb per MWh; 3-run average	1 hr minimum sampling time.
7. Stokers/sloped grate/others designed to burn wet biomass fuel	a. CO (or CEMS)	1,500 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (720 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1.4 lb per MMBtu of steam output or 17 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.7E-02 lb per MMBtu of heat input; or (2.4E-04 lb per MMBtu of heat input)	4.3E-02 lb per MMBtu of steam output or 5.2E-01 lb per MWh; or (2.8E-04 lb per MMBtu of steam output or 3.4E-04 lb per MWh)	Collect a minimum of 2 dscm per run.

If your boiler or process heater is in this subcategory ...	For the following pollutants ...	The emissions must not exceed the following emission limits, except during startup and shutdown ...	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown ...	Using this specified sampling volume or test run duration ...
8. Stokers/sloped grate/others designed to burn kiln-dried biomass fuel	a. CO	460 ppm by volume on a dry basis corrected to 3 percent oxygen	4.2E-01 lb per MMBtu of steam output or 5.1 lb per MWh	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.2E-01 lb per MMBtu of heat input; or (4.0E-03 lb per MMBtu of heat input)	3.7E-01 lb per MMBtu of steam output or 4.5 lb per MWh; or (4.6E-03 lb per MMBtu of steam output or 5.6E-02 lb per MWh)	Collect a minimum of 1 dscm per run.
9. Fluidized bed units designed to burn biomass/bio-based solid	a. CO (or CEMS)	470 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (310 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	4.6E-01 lb per MMBtu of steam output or 5.2 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.1E-01 lb per MMBtu of heat input; or (1.2E-03 lb per MMBtu of heat input)	1.4E-01 lb per MMBtu of steam output or 1.6 lb per MWh; or (1.5E-03 lb per MMBtu of steam output or	Collect a minimum of 1 dscm per run.

If your boiler or process heater is in this subcategory ...	For the following pollutants ...	The emissions must not exceed the following emission limits, except during startup and shutdown ...	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown ...	Using this specified sampling volume or test run duration ...
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10. Suspension burners designed to burn biomass/bio-based solid	a. CO (or CEMS)	2,400 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (2,000 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 10-day rolling average)	1.7E-02 lb per MWh) 1.9 lb per MMBtu of steam output or 27 lb per MWh; 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	5.1E-02 lb per MMBtu of heat input; or (6.5E-03 lb per MMBtu of heat input)	5.2E-02 lb per MMBtu of steam output or 7.1E-01 lb per MWh; or (6.6E-03 lb per MMBtu of steam output or 9.1E-02 lb per MWh)	Collect a minimum of 2 dscm per run.
11. Dutch Ovens/Pile burners designed to burn biomass/bio-based solid	a. CO (or CEMS)	770 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (520 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 10-	8.4E-01 lb per MMBtu of steam output or 8.4 lb per MWh; 3-run average	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory ...	For the following pollutants ...	The emissions must not exceed the following emission limits, except during startup and shutdown ...	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown ...	Using this specified sampling volume or test run duration ...
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day rolling average)

	b. Filterable PM (or TSM)	2.8E-01 lb per MMBtu of heat input; or (2.0E-03 lb per MMBtu of heat input)	3.9E-01 lb per MMBtu of steam output or 3.9 lb per MWh; or (2.8E-03 lb per MMBtu of steam output or 2.8E-02 lb per MWh)	Collect a minimum of 1 dscm per run.
12. Fuel cell units designed to burn biomass/bio-based solid	a. CO	1,100 ppm by volume on a dry basis corrected to 3 percent oxygen	2.4 lb per MMBtu of steam output or 12 lb per MWh	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.0E-02 lb per MMBtu of heat input; or (5.8E-03 lb per MMBtu of heat input)	5.5E-02 lb per MMBtu of steam output or 2.8E-01 lb per MWh; or (1.6E-02 lb per MMBtu of steam output or 8.1E-02 lb per MWh)	Collect a minimum of 2 dscm per run.
13. Hybrid suspension grate units designed to burn biomass/bio-based solid	a. CO (or CEMS)	3,500 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (900 ppm by volume on a dry	3.5 lb per MMBtu of steam output or 39 lb per MWh; 3-run average	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory ...	For the following pollutants ...	The emissions must not exceed the following emission limits, except during startup and shutdown ...	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown ...	Using this specified sampling volume or test run duration ...
		basis corrected to 3 percent oxygen, ^c 30-day rolling average)		
	b. Filterable PM (or TSM)	4.4E-01 lb per MMBtu of heat input; or (4.5E-04 lb per MMBtu of heat input)	5.5E-01 lb per MMBtu of steam output or 6.2 lb per MWh; or (5.7E-04 lb per MMBtu of steam output or 6.3E-03 lb per MWh)	Collect a minimum of 1 dscm per run.
14. Units designed to burn liquid fuel	a. HCl	1.1E-03 lb per MMBtu of heat input	1.4E-03 lb per MMBtu of steam output or 1.6E-02 lb per MWh	For M26A, collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	b. Mercury	2.0E-06 ^a lb per MMBtu of heat input	2.5E-06 ^a lb per MMBtu of steam output or 2.8E-05 lb per MWh	For M29, collect a minimum of 3 dscm per run; for M30A or M30B collect a minimum sample as specified in the method, for ASTM D6784, ^b collect a minimum of 2 dscm.
15. Units designed to burn heavy liquid	a. CO	130 ppm by volume on a dry basis	0.13 lb per MMBtu of steam output or	1 hr minimum

If your boiler or process heater is in this subcategory ...	For the following pollutants ...	The emissions must not exceed the following emission limits, except during startup and shutdown ...	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown ...	Using this specified sampling volume or test run duration ...
fuel		corrected to 3 percent oxygen, 3-run average	1.4 lb per MWh; 3-run average	sampling time.
	b. Filterable PM (or TSM)	6.2E-02 lb per MMBtu of heat input; or (2.0E-04 lb per MMBtu of heat input)	7.5E-02 lb per MMBtu of steam output or 8.6E-01 lb per MWh; or (2.5E-04 lb per MMBtu of steam output or 2.8E-03 lb per MWh)	Collect a minimum of 1 dscm per run.
16. Units designed to burn light liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen	0.13 lb per MMBtu of steam output or 1.4 lb per MWh	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	7.9E-03 ^a lb per MMBtu of heat input; or (6.2E-05 lb per MMBtu of heat input)	9.6E-03 ^a lb per MMBtu of steam output or 1.1E-01 ^a lb per MWh; or (7.5E-05 lb per MMBtu of steam output or 8.6E-04 lb per MWh)	Collect a minimum of 3 dscm per run.
17. Units designed to burn liquid fuel that are non-	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run	0.13 lb per MMBtu of steam output or 1.4 lb per MWh; 3-	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory ...	For the following pollutants ...	The emissions must not exceed the following emission limits, except during startup and shutdown ...	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown ...	Using this specified sampling volume or test run duration ...
continental units		average based on stack test	run average	
18. Units designed to burn gas 2 (other) gases	<p>b. Filterable PM (or TSM)</p> <p>a. CO</p> <p>b. HCl</p> <p>c. Mercury</p>	<p>2.7E-01 lb per MMBtu of heat input; or (8.6E-04 lb per MMBtu of heat input)</p> <p>130 ppm by volume on a dry basis corrected to 3 percent oxygen</p> <p>1.7E-03 lb per MMBtu of heat input</p> <p>7.9E-06 lb per MMBtu of heat input</p>	<p>3.3E-01 lb per MMBtu of steam output or 3.8 lb per MWh; or (1.1E-03 lb per MMBtu of steam output or 1.2E-02 lb per MWh)</p> <p>0.16 lb per MMBtu of steam output or 1.0 lb per MWh</p> <p>2.9E-03 lb per MMBtu of steam output or 1.8E-02 lb per MWh</p> <p>1.4E-05 lb per MMBtu of steam output or 8.3E-05 lb per MWh</p>	<p>Collect a minimum of 2 dscm per run.</p> <p>1 hr minimum sampling time.</p> <p>For M26A, collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.</p> <p>For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784^b collect a</p>

If your boiler or process heater is in this subcategory ...	For the following pollutants ...	The emissions must not exceed the following emission limits, except during startup and shutdown ...	The emissions must not exceed the following alternative output-based limits, except during startup and shutdown ...	Using this specified sampling volume or test run duration ...
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minimum of 2 dscm.

d. Filterable PM (or TSM)	6.7E-03 lb per MMBtu of heat input or (2.1E-04 lb per MMBtu of heat input)	1.2E-02 lb per MMBtu of steam output or 7.0E-02 lb per MWh; or (3.5E-04 lb per MMBtu of steam output or 2.2E-03 lb per MWh)	Collect a minimum of 3 dscm per run.
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^a If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit, you can skip testing according to [§ 63.7515](#) if all of the other provisions of [§ 63.7515](#) are met. For all other pollutants that do not contain a footnote a, your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

^b Incorporated by reference, see [§ 63.14](#).

^c An owner or operator may request an alternative test method under [§ 63.7 of this chapter](#), in order that compliance with the carbon monoxide emissions limit be determined using carbon dioxide as a diluent correction in place of oxygen at 3%. EPA Method 19 F-factors and EPA Method 19 equations must be used to generate the appropriate CO₂ correction percentage for the fuel type burned in the unit, and must also take into account that the 3% oxygen correction is to be done on a dry basis. The alternative test method request must account for any CO₂ being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc.

[[78 FR 7195](#), Jan. 31, 2013, as amended at [80 FR 72821](#), Nov. 20, 2015]

Table 3 to Subpart DDDDD of Part 63 - Work Practice Standards

As stated in [§ 63.7500](#), you must comply with the following applicable work practice standards:

If your unit is . . .	You must meet the following . . .
<p>1. A new or existing boiler or process heater with a continuous oxygen trim system that maintains an optimum air to fuel ratio, or a heat input capacity of less than or equal to 5 million Btu per hour in any of the following subcategories: unit designed to burn gas 1; unit designed to burn gas 2 (other); or unit designed to burn light liquid, or a limited use boiler or process heater</p>	<p>Conduct a tune-up of the boiler or process heater every 5 years as specified in § 63.7540.</p>
<p>2. A new or existing boiler or process heater without a continuous oxygen trim system and with heat input capacity of less than 10 million Btu per hour in the unit designed to burn heavy liquid or unit designed to burn solid fuel subcategories; or a new or existing boiler or process heater with heat input capacity of less than 10 million Btu per hour, but greater than 5 million Btu per hour, in any of the following subcategories: unit designed to burn gas 1; unit designed to burn gas 2 (other); or unit designed to burn light liquid</p>	<p>Conduct a tune-up of the boiler or process heater biennially as specified in § 63.7540.</p>
<p>3. A new or existing boiler or process heater without a continuous oxygen trim system and with heat input capacity of 10 million Btu per hour or greater</p>	<p>Conduct a tune-up of the boiler or process heater annually as specified in § 63.7540. Units in either the Gas 1 or Metal Process Furnace subcategories will conduct this tune-up as a work practice for all regulated emissions under this subpart. Units in all other subcategories will conduct this tune-up as a work practice for dioxins/furans.</p>
<p>4. An existing boiler or process heater located at a major source facility, not including</p>	<p>Must have a one-time energy assessment performed by a qualified energy assessor. An energy assessment completed on or after January</p>

If your unit is . . .	You must meet the following . . .
limited use units	<p>1, 2008, that meets or is amended to meet the energy assessment requirements in this table, satisfies the energy assessment requirement. A facility that operated under an energy management program developed according to the ENERGY STAR guidelines for energy management or compatible with ISO 50001 for at least one year between January 1, 2008 and the compliance date specified in § 63.7495 that includes the affected units also satisfies the energy assessment requirement. The energy assessment must include the following with extent of the evaluation for items a. to e. appropriate for the on-site technical hours listed in § 63.7575:</p> <ul style="list-style-type: none"> a. A visual inspection of the boiler or process heater system. b. An evaluation of operating characteristics of the boiler or process heater systems, specifications of energy using systems, operating and maintenance procedures, and unusual operating constraints. c. An inventory of major energy use systems consuming energy from affected boilers and process heaters and which are under the control of the boiler/process heater owner/operator. d. A review of available architectural and engineering plans, facility operation and maintenance procedures and logs, and fuel usage. e. A review of the facility's energy management program and provide recommendations for improvements consistent with the definition of energy management program, if identified.

If your unit is . . .	You must meet the following . . .
<p>5. An existing or new boiler or process heater subject to emission limits in Table 1 or 2 or 11 through 13 to this subpart during startup</p>	<p>f. A list of cost-effective energy conservation measures that are within the facility's control.</p> <p>g. A list of the energy savings potential of the energy conservation measures identified.</p> <p>h. A comprehensive report detailing the ways to improve efficiency, the cost of specific improvements, benefits, and the time frame for recouping those investments.</p> <p>a. You must operate all CMS during startup.</p> <p>b. For startup of a boiler or process heater, you must use one or a combination of the following clean fuels: Natural gas, synthetic natural gas, propane, other Gas 1 fuels, distillate oil, syngas, ultra-low sulfur diesel, fuel oil-soaked rags, kerosene, hydrogen, paper, cardboard, refinery gas, liquefied petroleum gas, clean dry biomass, and any fuels meeting the appropriate HCl, mercury and TSM emission standards by fuel analysis.</p> <p>c. You have the option of complying using either of the following work practice standards.</p> <p>(1) If you choose to comply using definition (1) of “startup” in § 63.7575, once you start firing fuels that are not clean fuels, you must vent emissions to the main stack(s) and engage all of the applicable control devices except limestone injection in fluidized bed combustion (FBC) boilers, dry scrubber, fabric filter, and selective catalytic reduction (SCR). You must start your limestone injection in FBC boilers, dry scrubber, fabric filter, and SCR systems as expeditiously as possible. Startup ends when steam or heat is supplied for any purpose, OR</p> <p>(2) If you choose to comply using definition (2) of “startup” in § 63.7575, once you start to feed fuels that are not clean fuels, you must vent</p>

If your unit is . . .	You must meet the following . . .
<p>6. An existing or new boiler or process heater subject to emission limits in Tables 1 or 2 or 11 through 13 to this subpart during shutdown</p>	<p>emissions to the main stack(s) and engage all of the applicable control devices so as to comply with the emission limits within 4 hours of start of supplying useful thermal energy. You must engage and operate PM control within one hour of first feeding fuels that are not clean fuels^a. You must start all applicable control devices as expeditiously as possible, but, in any case, when necessary to comply with other standards applicable to the source by a permit limit or a rule other than this subpart that require operation of the control devices. You must develop and implement a written startup and shutdown plan, as specified in § 63.7505(e).</p> <p>d. You must comply with all applicable emission limits at all times except during startup and shutdown periods at which time you must meet this work practice. You must collect monitoring data during periods of startup, as specified in § 63.7535(b). You must keep records during periods of startup. You must provide reports concerning activities and periods of startup, as specified in § 63.7555.</p> <p>You must operate all CMS during shutdown. While firing fuels that are not clean fuels during shutdown, you must vent emissions to the main stack(s) and operate all applicable control devices, except limestone injection in FBC boilers, dry scrubber, fabric filter, and SCR but, in any case, when necessary to comply with other standards applicable to the source that require operation of the control device.</p> <p>If, in addition to the fuel used prior to initiation of shutdown, another fuel must be used to support the shutdown process, that additional fuel must be one or a combination of the following clean fuels: Natural gas, synthetic natural gas,</p>

If your unit is . . .	You must meet the following . . .
	<p>propane, other Gas 1 fuels, distillate oil, syngas, ultra-low sulfur diesel, refinery gas, and liquefied petroleum gas.</p> <p>You must comply with all applicable emissions limits at all times except for startup or shutdown periods conforming with this work practice. You must collect monitoring data during periods of shutdown, as specified in § 63.7535(b). You must keep records during periods of shutdown. You must provide reports concerning activities and periods of shutdown, as specified in § 63.7555.</p>

^a As specified in [§ 63.7555\(d\)\(13\)](#), the source may request an alternative timeframe with the PM controls requirement to the permitting authority (state, local, or tribal agency) that has been delegated authority for this subpart by EPA. The source must provide evidence that (1) it is unable to safely engage and operate the PM control(s) to meet the “fuel firing + 1 hour” requirement and (2) the PM control device is appropriately designed and sized to meet the filterable PM emission limit. It is acknowledged that there may be another control device that has been installed other than ESP that provides additional PM control (e.g., scrubber).

[[78 FR 7198](#), Jan. 31, 2013, as amended at [80 FR 72823](#), Nov. 20, 2015]

Table 4 to Subpart DDDDD of Part 63 - Operating Limits for Boilers and Process Heaters

As stated in [§ 63.7500](#), you must comply with the applicable operating limits:

Table 4 to Subpart DDDDD of Part 63 - Operating Limits for Boilers and Process Heaters

When complying with a Table 1, 2, 11, 12, or 13 numerical emission limit using . . .	You must meet these operating limits . . .
1. Wet PM scrubber control on a boiler or process heater not using a PM CPMS	Maintain the 30-day rolling average pressure drop and the 30-day rolling average liquid flow rate at or above the lowest one-hour average pressure drop and the lowest one-hour average liquid flow rate, respectively, measured during the performance test demonstrating compliance with the PM emission limitation

When complying with a Table 1, 2, 11, 12, or 13 numerical emission limit using . . .

You must meet these operating limits . . .

according to [§ 63.7530\(b\)](#) and Table 7 to this subpart.

2. Wet acid gas (HCl) scrubber^a control on a boiler or process heater not using a HCl CEMS

Maintain the 30-day rolling average effluent pH at or above the lowest one-hour average pH and the 30-day rolling average liquid flow rate at or above the lowest one-hour average liquid flow rate measured during the performance test demonstrating compliance with the HCl emission limitation according to [§ 63.7530\(b\)](#) and Table 7 to this subpart.

3. Fabric filter control on a boiler or process heater not using a PM CPMS

a. Maintain opacity to less than or equal to 10 percent opacity or the highest hourly average opacity reading measured during the performance test run demonstrating compliance with the PM (or TSM) emission limitation (daily block average); or

b. Install and operate a bag leak detection system according to [§ 63.7525](#) and operate the fabric filter such that the bag leak detection system alert is not activated more than 5 percent of the operating time during each 6-month period.

4. Electrostatic precipitator control on a boiler or process heater not using a PM CPMS

a. This option is for boilers and process heaters that operate dry control systems (*i.e.*, an ESP without a wet scrubber). Existing and new boilers and process heaters must maintain opacity to less than or equal to 10 percent opacity or the highest hourly average opacity reading measured during the performance test run demonstrating compliance with the PM (or TSM) emission limitation (daily block average).

b. This option is only for boilers and process heaters not subject to PM CPMS or continuous compliance with an opacity limit (*i.e.*, dry ESP). Maintain the 30-day rolling average total secondary electric power input of the electrostatic precipitator at or above the operating limits established during the performance test according to [§ 63.7530\(b\)](#) and Table 7 to this subpart.

5. Dry scrubber or carbon injection control on a boiler

Maintain the minimum sorbent or carbon injection rate as defined in [§ 63.7575 of this subpart](#).

When complying with a Table 1, 2, 11, 12, or 13 numerical emission limit using . . .

You must meet these operating limits . . .

or process heater not using a mercury CEMS

6. Any other add-on air pollution control type on a boiler or process heater not using a PM CPMS

This option is for boilers and process heaters that operate dry control systems. Existing and new boilers and process heaters must maintain opacity to less than or equal to 10 percent opacity or the highest hourly average opacity reading measured during the performance test run demonstrating compliance with the PM (or TSM) emission limitation (daily block average).

7. Performance testing

For boilers and process heaters that demonstrate compliance with a performance test, maintain the 30-day rolling average operating load of each unit such that it does not exceed 110 percent of the highest hourly average operating load recorded during the performance test.

8. Oxygen analyzer system

For boilers and process heaters subject to a CO emission limit that demonstrate compliance with an O₂ analyzer system as specified in [§ 63.7525\(a\)](#), maintain the 30-day rolling average oxygen content at or above the lowest hourly average oxygen concentration measured during the CO performance test, as specified in Table 8. This requirement does not apply to units that install an oxygen trim system since these units will set the trim system to the level specified in [§ 63.7525\(a\)](#).

9. SO₂ CEMS

For boilers or process heaters subject to an HCl emission limit that demonstrate compliance with an SO₂ CEMS, maintain the 30-day rolling average SO₂ emission rate at or below the highest hourly average SO₂ concentration measured during the HCl performance test, as specified in Table 8.

^a A wet acid gas scrubber is a control device that removes acid gases by contacting the combustion gas with an alkaline slurry or solution. Alkaline reagents include, but not limited to, lime, limestone and sodium.

[[80 FR 72874](#), Nov. 20, 2015]

Table 5 to Subpart DDDDD of Part 63 - Performance Testing Requirements

As stated in [§ 63.7520](#), you must comply with the following requirements for performance testing for existing, new or reconstructed affected sources:

To conduct a performance test for the following pollutant . . .	You must . . .	Using, as appropriate . . .
1. Filterable PM	<p>a. Select sampling ports location and the number of traverse points</p> <p>b. Determine velocity and volumetric flow-rate of the stack gas</p> <p>c. Determine oxygen or carbon dioxide concentration of the stack gas</p> <p>d. Measure the moisture content of the stack gas</p> <p>e. Measure the PM emission concentration</p> <p>f. Convert emissions concentration to lb per MMBtu emission rates</p>	<p>Method 1 at 40 CFR part 60, appendix A-1 of this chapter.</p> <p>Method 2, 2F, or 2G at 40 CFR part 60, appendix A-1 or A-2 to part 60 of this chapter.</p> <p>Method 3A or 3B at 40 CFR part 60, appendix A-2 to part 60 of this chapter, or ANSI/ASME PTC 19.10-1981.^a</p> <p>Method 4 at 40 CFR part 60, appendix A-3 of this chapter.</p> <p>Method 5 or 17 (positive pressure fabric filters must use Method 5D) at 40 CFR part 60, appendix A-3 or A-6 of this chapter.</p> <p>Method 19 F-factor methodology at 40 CFR part 60, appendix A-7 of this chapter.</p>
2. TSM	<p>a. Select sampling ports location and the number of traverse points</p> <p>b. Determine velocity and volumetric flow-</p>	<p>Method 1 at 40 CFR part 60, appendix A-1 of this chapter.</p> <p>Method 2, 2F, or 2G at 40 CFR part 60, appendix A-1 or A-2 of this chapter.</p>

To conduct a performance test for the following pollutant . . .	You must. . .	Using, as appropriate . . .
	<p>rate of the stack gas</p> <p>c. Determine oxygen or carbon dioxide concentration of the stack gas</p> <p>d. Measure the moisture content of the stack gas</p> <p>e. Measure the TSM emission concentration</p> <p>f. Convert emissions concentration to lb per MMBtu emission rates</p>	<p>Method 3A or 3B at 40 CFR part 60, appendix A-1 of this chapter, or ANSI/ASME PTC 19.10-1981.^a</p> <p>Method 4 at 40 CFR part 60, appendix A-3 of this chapter.</p> <p>Method 29 at 40 CFR part 60, appendix A-8 of this chapter</p> <p>Method 19 F-factor methodology at 40 CFR part 60, appendix A-7 of this chapter.</p>
3. Hydrogen chloride	<p>a. Select sampling ports location and the number of traverse points</p> <p>b. Determine velocity and volumetric flow-rate of the stack gas</p> <p>c. Determine oxygen or carbon dioxide concentration of the stack gas</p> <p>d. Measure the moisture content of the stack gas</p> <p>e. Measure the hydrogen chloride emission concentration</p>	<p>Method 1 at 40 CFR part 60, appendix A-1 of this chapter.</p> <p>Method 2, 2F, or 2G at 40 CFR part 60, appendix A-2 of this chapter.</p> <p>Method 3A or 3B at 40 CFR part 60, appendix A-2 of this chapter, or ANSI/ASME PTC 19.10-1981.^a</p> <p>Method 4 at 40 CFR part 60, appendix A-3 of this chapter.</p> <p>Method 26 or 26A (M26 or M26A) at 40 CFR part 60, appendix A-8 of this chapter.</p>

To conduct a performance test for the following pollutant . . .	You must. . .	Using, as appropriate . . .
4. Mercury	<p>f. Convert emissions concentration to lb per MMBtu emission rates</p> <p>a. Select sampling ports location and the number of traverse points</p> <p>b. Determine velocity and volumetric flow-rate of the stack gas</p> <p>c. Determine oxygen or carbon dioxide concentration of the stack gas</p> <p>d. Measure the moisture content of the stack gas</p> <p>e. Measure the mercury emission concentration</p> <p>f. Convert emissions concentration to lb per MMBtu emission rates</p>	<p>Method 19 F-factor methodology at 40 CFR part 60, appendix A-7 of this chapter.</p> <p>Method 1 at 40 CFR part 60, appendix A-1 of this chapter.</p> <p>Method 2, 2F, or 2G at 40 CFR part 60, appendix A-1 or A-2 of this chapter.</p> <p>Method 3A or 3B at 40 CFR part 60, appendix A-1 of this chapter, or ANSI/ASME PTC 19.10-1981.^a</p> <p>Method 4 at 40 CFR part 60, appendix A-3 of this chapter.</p> <p>Method 29, 30A, or 30B (M29, M30A, or M30B) at 40 CFR part 60, appendix A-8 of this chapter or Method 101A at 40 CFR part 61, appendix B of this chapter, or ASTM Method D6784.^a</p> <p>Method 19 F-factor methodology at 40 CFR part 60, appendix A-7 of this chapter.</p>
5. CO	<p>a. Select the sampling ports location and the number of traverse points</p> <p>b. Determine oxygen concentration of the</p>	<p>Method 1 at 40 CFR part 60, appendix A-1 of this chapter.</p> <p>Method 3A or 3B at 40 CFR part 60, appendix A-3 of this chapter, or ASTM D6522-00</p>

To conduct a performance test for the following pollutant . . .	You must . . .	Using, as appropriate . . .
	stack gas	(Reapproved 2005), or ANSI/ASME PTC 19.10-1981. ^a
	c. Measure the moisture content of the stack gas	Method 4 at 40 CFR part 60, appendix A-3 of this chapter.
	d. Measure the CO emission concentration	Method 10 at 40 CFR part 60, appendix A-4 of this chapter. Use a measurement span value of 2 times the concentration of the applicable emission limit.

^a Incorporated by reference, see [§ 63.14](#).

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7200](#), Jan. 31, 2013; [80 FR 72825](#), Nov. 20, 2015]

Table 6 to Subpart DDDDD of Part 63 - Fuel Analysis Requirements

As stated in [§ 63.7521](#), you must comply with the following requirements for fuel analysis testing for existing, new or reconstructed affected sources. However, equivalent methods (as defined in [§ 63.7575](#)) may be used in lieu of the prescribed methods at the discretion of the source owner or operator:

To conduct a fuel analysis for the following pollutant . . .	You must . . .	Using . . .
1. Mercury	a. Collect fuel samples	Procedure in § 63.7521(c) or ASTM D5192 ^a , or ASTM D7430 ^a , or ASTM D6883 ^a , or ASTM D2234/D2234M ^a (for coal) or EPA 1631 or EPA 1631E or ASTM D6323 ^a (for solid), or EPA 821-R-01-013 (for liquid or solid), or ASTM D4177 ^a (for liquid), or ASTM D4057 ^a (for liquid), or

To conduct a fuel analysis for the following pollutant . . .	You must . . .	Using . . .
		equivalent.
	b. Composite fuel samples	Procedure in § 63.7521(d) or equivalent.
	c. Prepare composited fuel samples	EPA SW-846-3050B ^a (for solid samples), ASTM D2013/D2013M ^a (for coal), ASTM D5198 ^a (for biomass), or EPA 3050 ^a (for solid fuel), or EPA 821-R-01-013 ^a (for liquid or solid), or equivalent.
	d. Determine heat content of the fuel type	ASTM D5865 ^a (for coal) or ASTM E711 ^a (for biomass), or ASTM D5864 ^a for liquids and other solids, or ASTM D240 ^a or equivalent.
	e. Determine moisture content of the fuel type	ASTM D3173 ^a , ASTM E871 ^a , or ASTM D5864 ^a , or ASTM D240 ^a , or ASTM D95 ^a (for liquid fuels), or ASTM D4006 ^a (for liquid fuels), or equivalent.
	f. Measure mercury concentration in fuel sample	ASTM D6722 ^a (for coal), EPA SW-846-7471B ^a or EPA 1631 or EPA 1631E ^a (for solid samples), or EPA SW-846-7470A ^a or EPA SW-846-7471B ^a (for liquid samples), or EPA 821-R-01-013 ^a (for liquid or solid), or equivalent.
	g. Convert concentration into units of pounds of mercury per MMBtu of heat content	For fuel mixtures use Equation 8 in § 63.7530 .
2. HCl	a. Collect fuel samples	Procedure in § 63.7521(c) or ASTM D5192 ^a , or ASTM D7430 ^a , or ASTM D6883 ^a , or ASTM D2234/D2234M ^a (for coal) or ASTM D6323 ^a (for coal or biomass), ASTM D4177 ^a (for liquid fuels) or ASTM D4057 ^a (for liquid fuels), or equivalent.

To conduct a fuel analysis for the following pollutant . . .	You must . . .	Using . . .
	b. Composite fuel samples	Procedure in § 63.7521(d) or equivalent.
	c. Prepare composited fuel samples	EPA SW-846-3050B ^a (for solid samples), ASTM D2013/D2013M ^a (for coal), or ASTM D5198 ^a (for biomass), or EPA 3050 ^a or equivalent.
	d. Determine heat content of the fuel type	ASTM D5865 ^a (for coal) or ASTM E711 ^a (for biomass), ASTM D5864 ^a , ASTM D240 ^a or equivalent.
	e. Determine moisture content of the fuel type	ASTM D3173 ^a or ASTM E871 ^a , or D5864 ^a , or ASTM D240 ^a , or ASTM D95 ^a (for liquid fuels), or ASTM D4006 ^a (for liquid fuels), or equivalent.
	f. Measure chlorine concentration in fuel sample	EPA SW-846-9250 ^a , ASTM D6721 ^a , ASTM D4208 ^a (for coal), or EPA SW-846-5050 ^a or ASTM E776 ^a (for solid fuel), or EPA SW-846-9056 ^a or SW-846-9076 ^a (for solids or liquids) or equivalent.
	g. Convert concentrations into units of pounds of HCl per MMBtu of heat content	For fuel mixtures use Equation 7 in § 63.7530 and convert from chlorine to HCl by multiplying by 1.028.
3. Mercury Fuel Specification for other gas 1 fuels	a. Measure mercury concentration in the fuel sample and convert to units of micrograms per cubic meter, or	Method 30B (M30B) at 40 CFR part 60, appendix A-8 of this chapter or ASTM D5954 ^a , ASTM D6350 ^a , ISO 6978-1:2003(E) ^a , or ISO 6978-2:2003(E) ^a , or EPA-1631 ^a or equivalent.
	b. Measure mercury concentration in the exhaust gas when firing only the other gas 1 fuel is fired in the boiler or	Method 29, 30A, or 30B (M29, M30A, or M30B) at 40 CFR part 60, appendix A-8 of this chapter or Method 101A or Method 102 at 40 CFR part 61, appendix B of this chapter, or ASTM Method D6784 ^a or equivalent.

To conduct a fuel analysis for the following pollutant . . .	You must . . .	Using . . .
	process heater	
4. TSM	a. Collect fuel samples	Procedure in § 63.7521(c) or ASTM D5192 ^a , or ASTM D7430 ^a , or ASTM D6883 ^a , or ASTM D2234/D2234M ^a (for coal) or ASTM D6323 ^a (for coal or biomass), or ASTM D4177 ^a , (for liquid fuels), or ASTM D4057 ^a (for liquid fuels), or equivalent.
	b. Composite fuel samples	Procedure in § 63.7521(d) or equivalent.
	c. Prepare composited fuel samples	EPA SW-846-3050B ^a (for solid samples), ASTM D2013/D2013M ^a (for coal), ASTM D5198 ^a or TAPPI T266 ^a (for biomass), or EPA 3050 ^a or equivalent.
	d. Determine heat content of the fuel type	ASTM D5865 ^a (for coal) or ASTM E711 ^a (for biomass), or ASTM D5864 ^a for liquids and other solids, or ASTM D240 ^a or equivalent.
	e. Determine moisture content of the fuel type	ASTM D3173 ^a or ASTM E871 ^a , or D5864 ^a , or ASTM D240 ^a , or ASTM D95 ^a (for liquid fuels), or ASTM D4006 ^a (for liquid fuels), or ASTM D4177 ^a (for liquid fuels) or ASTM D4057 ^a (for liquid fuels), or equivalent.
	f. Measure TSM concentration in fuel sample	ASTM D3683 ^a , or ASTM D4606 ^a , or ASTM D6357 ^a or EPA 200.8 ^a or EPA SW-846-6020 ^a , or EPA SW-846-6020A ^a , or EPA SW-846-6010C ^a , EPA 7060 ^a or EPA 7060A ^a (for arsenic only), or EPA SW-846-7740 ^a (for selenium only).
	g. Convert concentrations into units of pounds of TSM per MMBtu of heat content	For fuel mixtures use Equation 9 in § 63.7530 .

^a Incorporated by reference, see [§ 63.14](#).

[[83 FR 56725](#), Nov. 14, 2018]

Table 7 to Subpart DDDDD of Part 63 - Establishing Operating Limits^{a b}

As stated in [§ 63.7520](#), you must comply with the following requirements for establishing operating limits:

Table 7 to Subpart DDDDD of Part 63 - Establishing Operating Limits^{a b}

If you have an applicable emission limit for . . .	And your operating limits are based on . . .	You must . . .	Using . . .	According to the following requirements
1. PM, TSM, or mercury	a. Wet scrubber operating parameters	i. Establish a site-specific minimum scrubber pressure drop and minimum flow rate operating limit according to § 63.7530(b)	(1) Data from the scrubber pressure drop and liquid flow rate monitors and the PM, TSM, or mercury performance test	(a) You must collect scrubber pressure drop and liquid flow rate data every 15 minutes during the entire period of the performance tests. (b) Determine the lowest hourly average scrubber pressure drop and liquid flow rate by computing the hourly averages using all of the 15-minute readings taken during each performance test.
	b. Electrostatic precipitator operating parameters (option only for units that operate wet	i. Establish a site-specific minimum total secondary electric power input according to § 63.7530(b)	(1) Data from the voltage and secondary amperage monitors during the PM or mercury	(a) You must collect secondary voltage and secondary amperage for each ESP cell and calculate total secondary electric power input data every

If you have an applicable emission limit for . . .	And your operating limits are based on . . .	You must . . .	Using . . .	According to the following requirements
	scrubbers)		performance test	<p>15 minutes during the entire period of the performance tests.</p> <p>(b) Determine the average total secondary electric power input by computing the hourly averages using all of the 15-minute readings taken during each performance test.</p> <p>(a) You must collect opacity readings every 15 minutes during the entire period of the performance tests.</p> <p>(b) Determine the average hourly opacity reading for each performance test run by computing the hourly averages using all of the 15-minute readings taken during each performance test run.</p> <p>(c) Determine the highest hourly average opacity reading measured during the test run demonstrating compliance with the PM (or TSM) emission limitation.</p>
	c. Opacity	i. Establish a site-specific maximum opacity level	(1) Data from the opacity monitoring system during the PM performance test	

If you have an applicable emission limit for . . .	And your operating limits are based on . . .	You must . . .	Using . . .	According to the following requirements
2. HCl	a. Wet scrubber operating parameters	i. Establish site-specific minimum effluent pH and flow rate operating limits according to § 63.7530(b)	(1) Data from the pH and liquid flow-rate monitors and the HCl performance test	(a) You must collect pH and liquid flow-rate data every 15 minutes during the entire period of the performance tests. (b) Determine the hourly average pH and liquid flow rate by computing the hourly averages using all of the 15-minute readings taken during each performance test.
	b. Dry scrubber operating parameters	i. Establish a site-specific minimum sorbent injection rate operating limit according to § 63.7530(b) . If different acid gas sorbents are used during the HCl performance test, the average value for each sorbent becomes the site-specific operating limit for that sorbent	(1) Data from the sorbent injection rate monitors and HCl or mercury performance test	(a) You must collect sorbent injection rate data every 15 minutes during the entire period of the performance tests. (b) Determine the hourly average sorbent injection rate by computing the hourly averages using all of the 15-minute readings taken during each performance test. (c) Determine the lowest hourly average of the three test run averages established during the performance test as your operating

If you have an applicable emission limit for . . .	And your operating limits are based on . . .	You must . . .	Using . . .	According to the following requirements
	c. Alternative Maximum SO ₂ emission rate	i. Establish a site-specific maximum SO ₂ emission rate operating limit according to § 63.7530(b)	(1) Data from SO ₂ CEMS and the HCl performance test	<p>limit. When your unit operates at lower loads, multiply your sorbent injection rate by the load fraction, as defined in § 63.7575, to determine the required injection rate.</p> <p>(a) You must collect the SO₂ emissions data according to § 63.7525(m) during the most recent HCl performance tests.</p> <p>(b) The maximum SO₂ emission rate is equal to the highest hourly average SO₂ emission rate measured during the most recent HCl performance tests.</p>
3. Mercury	a. Activated carbon injection	i. Establish a site-specific minimum activated carbon injection rate operating limit according to § 63.7530(b)	(1) Data from the activated carbon rate monitors and mercury performance test	<p>(a) You must collect activated carbon injection rate data every 15 minutes during the entire period of the performance tests.</p> <p>(b) Determine the hourly average activated carbon injection rate by computing the hourly averages using all of the</p>

If you have an applicable emission limit for . . .	And your operating limits are based on . . .	You must . . .	Using . . .	According to the following requirements
<p>4. Carbon monoxide for which compliance is demonstrated by a performance test</p>	<p>a. Oxygen</p>	<p>i. Establish a unit-specific limit for minimum oxygen level according to § 63.7530(b)</p>	<p>(1) Data from the oxygen analyzer system specified in § 63.7525(a)</p>	<p>15-minute readings taken during each performance test. (c) Determine the lowest hourly average established during the performance test as your operating limit. When your unit operates at lower loads, multiply your activated carbon injection rate by the load fraction, as defined in § 63.7575, to determine the required injection rate.</p> <p>(a) You must collect oxygen data every 15 minutes during the entire period of the performance tests. (b) Determine the hourly average oxygen concentration by computing the hourly averages using all of the 15-minute readings taken during each performance test. (c) Determine the lowest hourly average established during the performance test as your minimum</p>

If you have an applicable emission limit for . . .	And your operating limits are based on . . .	You must . . .	Using . . .	According to the following requirements
5. Any pollutant for which compliance is demonstrated by a performance test	a. Boiler or process heater operating load	i. Establish a unit specific limit for maximum operating load according to § 63.7520(c)	(1) Data from the operating load monitors or from steam generation monitors	operating limit. (a) You must collect operating load or steam generation data every 15 minutes during the entire period of the performance test. (b) Determine the average operating load by computing the hourly averages using all of the 15-minute readings taken during each performance test. (c) Determine the highest hourly average of the three test run averages during the performance test, and multiply this by 1.1 (110 percent) as your operating limit.

^a Operating limits must be confirmed or reestablished during performance tests.

^b If you conduct multiple performance tests, you must set the minimum liquid flow rate and pressure drop operating limits at the higher of the minimum values established during the performance tests. For a minimum oxygen level, if you conduct multiple performance tests, you must set the minimum oxygen level at the lower of the minimum values established during the performance tests.

[[80 FR 72827](#), Nov. 20, 2015]

Table 8 to Subpart DDDDD of Part 63 - Demonstrating Continuous Compliance

As stated in [§ 63.7540](#), you must show continuous compliance with the emission limitations for each boiler or process heater according to the following:

<p>If you must meet the following operating limits or work practice standards . . .</p>	<p>You must demonstrate continuous compliance by . . .</p>
<p>1. Opacity</p>	<p>a. Collecting the opacity monitoring system data according to § 63.7525(c) and § 63.7535; and</p> <p>b. Reducing the opacity monitoring data to 6-minute averages; and</p> <p>c. Maintaining daily block average opacity to less than or equal to 10 percent or the highest hourly average opacity reading measured during the performance test run demonstrating compliance with the PM (or TSM) emission limitation.</p>
<p>2. PM CPMS</p>	<p>a. Collecting the PM CPMS output data according to § 63.7525;</p> <p>b. Reducing the data to 30-day rolling averages; and</p> <p>c. Maintaining the 30-day rolling average PM CPMS output data to less than the operating limit established during the performance test according to § 63.7530(b)(4).</p>
<p>3. Fabric Filter Bag Leak Detection Operation</p>	<p>Installing and operating a bag leak detection system according to § 63.7525 and operating the fabric filter such that the requirements in § 63.7540(a)(7) are met.</p>
<p>4. Wet Scrubber Pressure Drop and Liquid Flow-rate</p>	<p>a. Collecting the pressure drop and liquid flow rate monitoring system data according to §§ 63.7525 and 63.7535; and</p> <p>b. Reducing the data to 30-day rolling averages; and</p> <p>c. Maintaining the 30-day rolling average pressure drop and liquid flow-rate at or above the operating limits established during the performance test according to § 63.7530(b).</p>
<p>5. Wet Scrubber pH</p>	<p>a. Collecting the pH monitoring system data according to §§ 63.7525 and 63.7535; and</p>

If you must meet the following operating limits or work practice standards . . .	You must demonstrate continuous compliance by . . .
	<ul style="list-style-type: none"> b. Reducing the data to 30-day rolling averages; and c. Maintaining the 30-day rolling average pH at or above the operating limit established during the performance test according to § 63.7530(b).
6. Dry Scrubber Sorbent or Carbon Injection Rate	<ul style="list-style-type: none"> a. Collecting the sorbent or carbon injection rate monitoring system data for the dry scrubber according to §§ 63.7525 and 63.7535; and b. Reducing the data to 30-day rolling averages; and c. Maintaining the 30-day rolling average sorbent or carbon injection rate at or above the minimum sorbent or carbon injection rate as defined in § 63.7575.
7. Electrostatic Precipitator Total Secondary Electric Power Input	<ul style="list-style-type: none"> a. Collecting the total secondary electric power input monitoring system data for the electrostatic precipitator according to §§ 63.7525 and 63.7535; and b. Reducing the data to 30-day rolling averages; and c. Maintaining the 30-day rolling average total secondary electric power input at or above the operating limits established during the performance test according to § 63.7530(b).
8. Emission limits using fuel analysis	<ul style="list-style-type: none"> a. Conduct monthly fuel analysis for HCl or mercury or TSM according to Table 6 to this subpart; and b. Reduce the data to 12-month rolling averages; and c. Maintain the 12-month rolling average at or below the applicable emission limit for HCl or mercury or TSM in Tables 1 and 2 or 11 through 13 to this subpart. d. Calculate the HCl, mercury, and/or TSM emission rate from the boiler or process heater in units of lb/MMBtu using Equation 15 and Equations 17, 18, and/or 19 in § 63.7530.

If you must meet the following operating limits or work practice standards . . .	You must demonstrate continuous compliance by . . .
9. Oxygen content	<p>a. Continuously monitor the oxygen content using an oxygen analyzer system according to § 63.7525(a). This requirement does not apply to units that install an oxygen trim system since these units will set the trim system to the level specified in § 63.7525(a)(7).</p> <p>b. Reducing the data to 30-day rolling averages; and</p> <p>c. Maintain the 30-day rolling average oxygen content at or above the lowest hourly average oxygen level measured during the CO performance test.</p>
10. Boiler or process heater operating load	<p>a. Collecting operating load data or steam generation data every 15 minutes.</p> <p>b. Reducing the data to 30-day rolling averages; and</p> <p>c. Maintaining the 30-day rolling average operating load such that it does not exceed 110 percent of the highest hourly average operating load recorded during the performance test according to § 63.7520(c).</p>
11. SO ₂ emissions using SO ₂ CEMS	<p>a. Collecting the SO₂ CEMS output data according to § 63.7525;</p> <p>b. Reducing the data to 30-day rolling averages; and</p> <p>c. Maintaining the 30-day rolling average SO₂ CEMS emission rate to a level at or below the highest hourly SO₂ rate measured during the HCl performance test according to § 63.7530.</p>

[[78 FR 7204](#), Jan. 31, 2013, as amended at [80 FR 72829](#), Nov. 20, 2015]

Table 9 to Subpart DDDDD of Part 63 - Reporting Requirements

As stated in [§ 63.7550](#), you must comply with the following requirements for reports:

You must submit a(n)	The report must contain . . .	You must submit the report . . .
1. Compliance report	<p>a. Information required in § 63.7550(c)(1) through (5); and</p> <p>b. If there are no deviations from any emission limitation (emission limit and operating limit) that applies to you and there are no deviations from the requirements for work practice standards for periods of startup and shutdown in Table 3 to this subpart that apply to you, a statement that there were no deviations from the emission limitations and work practice standards during the reporting period. If there were no periods during which the CMSs, including continuous emissions monitoring system, continuous opacity monitoring system, and operating parameter monitoring systems, were out-of-control as specified in § 63.8(c)(7), a statement that there were no periods during which the CMSs were out-of-control during the reporting period; and</p> <p>c. If you have a deviation from any emission limitation (emission limit and operating limit) where you are not using a CMS to comply with that emission limit or operating limit, or a deviation from a work practice standard for periods of startup and shutdown, during the reporting period, the report must contain the information in § 63.7550(d); and</p> <p>d. If there were periods during which the CMSs, including continuous emissions monitoring system, continuous opacity monitoring system, and operating parameter monitoring systems, were out-of-control as specified in § 63.8(c)(7), or otherwise not operating, the report must contain the information in § 63.7550(e)</p>	Semiannually, annually, biennially, or every 5 years according to the requirements in § 63.7550(b) .

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7205](#), Jan. 31, 2013; [80 FR 72830](#), Nov. 20, 2015]

Table 10 to Subpart DDDDD of Part 63 - Applicability of General Provisions to Subpart DDDDD

As stated in [§ 63.7565](#), you must comply with the applicable General Provisions according to the following:

Citation	Subject	Applies to subpart DDDDD
§ 63.1	Applicability	Yes.
§ 63.2	Definitions	Yes. Additional terms defined in § 63.7575
§ 63.3	Units and Abbreviations	Yes.
§ 63.4	Prohibited Activities and Circumvention	Yes.
§ 63.5	Preconstruction Review and Notification Requirements	Yes.
§ 63.6(a), (b)(1)-(b)(5), (b)(7), (c)	Compliance with Standards and Maintenance Requirements	Yes.
§ 63.6(e)(1)(i)	General duty to minimize emissions.	No. See § 63.7500(a)(3) for the general duty requirement.
§ 63.6(e)(1)(ii)	Requirement to correct malfunctions as soon as practicable.	No.
§ 63.6(e)(3)	Startup, shutdown, and malfunction plan requirements.	No.
§ 63.6(f)(1)	Startup, shutdown, and	No.

Citation	Subject	Applies to subpart DDDDD
	malfunction exemptions for compliance with non-opacity emission standards.	
§ 63.6(f)(2) and (3)	Compliance with non-opacity emission standards.	Yes.
§ 63.6(g)	Use of alternative standards	Yes, except § 63.7555(d)(13) specifies the procedure for application and approval of an alternative timeframe with the PM controls requirement in the startup work practice (2).
§ 63.6(h)(1)	Startup, shutdown, and malfunction exemptions to opacity standards.	No. See § 63.7500(a) .
§ 63.6(h)(2) to (h)(9)	Determining compliance with opacity emission standards	No. Subpart DDDDD specifies opacity as an operating limit not an emission standard.
§ 63.6(i)	Extension of compliance	Yes. Note: Facilities may also request extensions of compliance for the installation of combined heat and power, waste heat recovery, or gas pipeline or fuel feeding infrastructure as a means of complying with this subpart.
§ 63.6(j)	Presidential exemption.	Yes.
§ 63.7(a), (b), (c), and (d)	Performance Testing Requirements	Yes.
§ 63.7(e)(1)	Conditions for conducting performance	No. Subpart DDDDD specifies conditions for conducting performance tests at § 63.7520(a) to

Citation	Subject	Applies to subpart DDDDD
	tests	(c).
§ 63.7(e)(2)-(e)(9), (f), (g), and (h)	Performance Testing Requirements	Yes.
§ 63.8(a) and (b)	Applicability and Conduct of Monitoring	Yes.
§ 63.8(c)(1)	Operation and maintenance of CMS	Yes.
§ 63.8(c)(1)(i)	General duty to minimize emissions and CMS operation	No. See § 63.7500(a)(3) .
§ 63.8(c)(1)(ii)	Operation and maintenance of CMS	Yes.
§ 63.8(c)(1)(iii)	Startup, shutdown, and malfunction plans for CMS	No.
§ 63.8(c)(2) to (c)(9)	Operation and maintenance of CMS	Yes.
§ 63.8(d)(1) and (2)	Monitoring Requirements, Quality Control Program	Yes.
§ 63.8(d)(3)	Written procedures for CMS	Yes, except for the last sentence, which refers to a startup, shutdown, and malfunction plan. Startup, shutdown, and malfunction plans are not required.
§ 63.8(e)	Performance evaluation of a CMS	Yes.
§ 63.8(f)	Use of an alternative monitoring method.	Yes.

Citation	Subject	Applies to subpart DDDDD
§ 63.8(g)	Reduction of monitoring data	Yes.
§ 63.9	Notification Requirements	Yes.
§ 63.10(a), (b)(1)	Recordkeeping and Reporting Requirements	Yes.
§ 63.10(b)(2)(i)	Recordkeeping of occurrence and duration of startups or shutdowns	Yes.
§ 63.10(b)(2)(ii)	Recordkeeping of malfunctions	No. See § 63.7555(d)(7) for recordkeeping of occurrence and duration and § 63.7555(d)(8) for actions taken during malfunctions.
§ 63.10(b)(2)(iii)	Maintenance records	Yes.
§ 63.10(b)(2)(iv) and (v)	Actions taken to minimize emissions during startup, shutdown, or malfunction	No.
§ 63.10(b)(2)(vi)	Recordkeeping for CMS malfunctions	Yes.
§ 63.10(b)(2)(vii) to (xiv)	Other CMS requirements	Yes.
§ 63.10(b)(3)	Recordkeeping requirements for applicability determinations	No.
§ 63.10(c)(1) to (9)	Recordkeeping for sources with CMS	Yes.

Citation	Subject	Applies to subpart DDDDD
§ 63.10(c)(10) and (11)	Recording nature and cause of malfunctions, and corrective actions	No. See § 63.7555(d)(7) for recordkeeping of occurrence and duration and § 63.7555(d)(8) for actions taken during malfunctions.
§ 63.10(c)(12) and (13)	Recordkeeping for sources with CMS	Yes.
§ 63.10(c)(15)	Use of startup, shutdown, and malfunction plan	No.
§ 63.10(d)(1) and (2)	General reporting requirements	Yes.
§ 63.10(d)(3)	Reporting opacity or visible emission observation results	No.
§ 63.10(d)(4)	Progress reports under an extension of compliance	Yes.
§ 63.10(d)(5)	Startup, shutdown, and malfunction reports	No. See § 63.7550(c)(11) for malfunction reporting requirements.
§ 63.10(e)	Additional reporting requirements for sources with CMS	Yes.
§ 63.10(f)	Waiver of recordkeeping or reporting requirements	Yes.
§ 63.11	Control Device Requirements	No.
§ 63.12	State Authority and Delegation	Yes.

Citation	Subject	Applies to subpart DDDDD
§ 63.13-63.16	Addresses, Incorporation by Reference, Availability of Information, Performance Track Provisions	Yes.
§ 63.1(a)(5),(a)(7)-(a)(9), (b)(2), (c)(3)-(4), (d), 63.6(b)(6), (c)(3), (c)(4), (d), (e)(2), (e)(3)(ii), (h)(3), (h)(5)(iv), 63.8(a)(3), 63.9(b)(3), (h)(4), 63.10(c)(2)-(4), (c)(9).	Reserved	No.

[[76 FR 15664](#), Mar. 21, 2011, as amended at [78 FR 7205](#), Jan. 31, 2013; [80 FR 72830](#), Nov. 20, 2015]

Table 11 to Subpart DDDDD of Part 63 - Alternative Emission Limits for New or Reconstructed Boilers and Process Heaters That Commenced Construction or Reconstruction After June 4, 2010, and Before May 20, 2011

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
1. Units in all subcategories designed to burn solid fuel	a. HCl	0.022 lb per MMBtu of heat input	For M26A, collect a minimum of 1 dscm per run; for M26 collect a minimum of 120 liters per run.
2. Units in all subcategories designed to burn solid fuel that	a. Mercury	8.0E-07 ^a lb per MMBtu of heat input	For M29, collect a minimum of 4 dscm per

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
combust at least 10 percent biomass/bio-based solids on an annual heat input basis and less than 10 percent coal/solid fossil fuels on an annual heat input basis			run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 4 dscm.
3. Units in all subcategories designed to burn solid fuel that combust at least 10 percent coal/solid fossil fuels on an annual heat input basis and less than 10 percent biomass/bio-based solids on an annual heat input basis	a. Mercury	2.0E-06 lb per MMBtu of heat input	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 4 dscm.
4. Units design to burn coal/solid fossil fuel	a. Filterable PM (or TSM)	1.1E-03 lb per MMBtu of heat input; or (2.3E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
5. Pulverized coal boilers designed to burn coal/solid fossil fuel	a. Carbon monoxide (CO) (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (320 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.
6. Stokers designed to burn	a. CO (or	130 ppm by volume on a dry basis corrected to 3	1 hr minimum sampling

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
coal/solid fossil fuel	CEMS)	percent oxygen, 3-run average; or (340 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 10-day rolling average)	time.
7. Fluidized bed units designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (230 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.
8. Fluidized bed units with an integrated heat exchanger designed to burn coal/solid fossil fuel	a. CO (or CEMS)	140 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (150 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.
9. Stokers/sloped grate/others designed to burn wet biomass fuel	a. CO (or CEMS)	620 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (390 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (2.6E-05 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
10. Stokers/sloped grate/others designed to burn kiln-dried biomass fuel	a. CO	560 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (4.0E-03 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
11. Fluidized bed units designed to burn biomass/bio-based solids	a. CO (or CEMS)	230 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (310 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	9.8E-03 lb per MMBtu of heat input; or (8.3E-05 ^a lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
12. Suspension burners designed to burn biomass/bio-based solids	a. CO (or CEMS)	2,400 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (2,000 ppm by volume on a dry basis	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
		corrected to 3 percent oxygen, ^c 10-day rolling average)	
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (6.5E-03 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
13. Dutch Ovens/Pile burners designed to burn biomass/bio-based solids	a. CO (or CEMS)	1,010 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (520 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 10-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	8.0E-03 lb per MMBtu of heat input; or (3.9E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
14. Fuel cell units designed to burn biomass/bio-based solids	a. CO	910 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.0E-02 lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
15. Hybrid suspension grate	a. CO (or	1,100 ppm by volume on	1 hr minimum sampling

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
boiler designed to burn biomass/bio-based solids	CEMS)	a dry basis corrected to 3 percent oxygen, 3-run average; or (900 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	time.
16. Units designed to burn liquid fuel	b. Filterable PM (or TSM)	2.6E-02 lb per MMBtu of heat input; or (4.4E-04 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
	a. HCl	4.4E-04 lb per MMBtu of heat input	For M26A: Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	b. Mercury	4.8E-07 ^a lb per MMBtu of heat input	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 4 dscm.
17. Units designed to burn heavy liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
18. Units designed to burn light liquid fuel	b. Filterable PM (or TSM)	1.3E-02 lb per MMBtu of heat input; or (7.5E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.0E-03 ^a lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
19. Units designed to burn liquid fuel that are non-continental units	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average based on stack test	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.3E-02 lb per MMBtu of heat input; or (8.6E-04 lb per MMBtu of heat input)	Collect a minimum of 4 dscm per run.
20. Units designed to burn gas 2 (other) gases	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average	1 hr minimum sampling time.
	b. HCl	1.7E-03 lb per MMBtu of heat input	For M26A, Collect a minimum of 2 dscm per run; for M26, collect a

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
	c. Mercury	7.9E-06 lb per MMBtu of heat input	<p>minimum of 240 liters per run.</p> <p>For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784^b collect a minimum of 3 dscm.</p>
	d. Filterable PM (or TSM)	6.7E-03 lb per MMBtu of heat input; or (2.1E-04 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.

^a If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit, you can skip testing according to [§ 63.7515](#) if all of the other provision of [§ 63.7515](#) are met. For all other pollutants that do not contain a footnote “a”, your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

^b Incorporated by reference, see [§ 63.14](#).

^c An owner or operator may request an alternative test method under [§ 63.7 of this chapter](#), in order that compliance with the carbon monoxide emissions limit be determined using carbon dioxide as a diluent correction in place of oxygen at 3%. EPA Method 19 F-factors and EPA Method 19 equations must be used to generate the appropriate CO₂ correction percentage for the fuel type burned in the unit, and must also take into account that the 3% oxygen correction is to be done on a dry basis. The alternative test method request must account for any CO₂ being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc.

Table 12 to Subpart DDDDD of Part 63 - Alternative Emission Limits for New or Reconstructed Boilers and Process Heaters That Commenced Construction or Reconstruction After May 20, 2011, and Before December 23, 2011

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
1. Units in all subcategories designed to burn solid fuel	a. HCl	0.022 lb per MMBtu of heat input	For M26A, collect a minimum of 1 dscm per run; for M26 collect a minimum of 120 liters per run.
	b. Mercury	3.5E-06 ^a lb per MMBtu of heat input	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 3 dscm.
2. Units design to burn coal/solid fossil fuel	a. Filterable PM (or TSM)	1.1E-03 lb per MMBtu of heat input; or (2.3E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
3. Pulverized coal boilers designed to burn coal/solid fossil fuel	a. Carbon monoxide (CO) (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (320 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
4. Stokers designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (340 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 10-day rolling average)	1 hr minimum sampling time.
5. Fluidized bed units designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (230 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.
6. Fluidized bed units with an integrated heat exchanger designed to burn coal/solid fossil fuel	a. CO (or CEMS)	140 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (150 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.
7. Stokers/sloped grate/others designed to burn wet biomass fuel	a. CO (or CEMS)	620 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (390 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	3.0E-02 lb per MMBtu of heat input; or (2.6E-05 lb per	Collect a minimum of 2 dscm per run.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
		MMBtu of heat input)	
8. Stokers/sloped grate/others designed to burn kiln-dried biomass fuel	a. CO b. Filterable PM (or TSM)	460 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average 3.0E-02 lb per MMBtu of heat input; or (4.0E-03 lb per MMBtu of heat input)	1 hr minimum sampling time. Collect a minimum of 2 dscm per run.
9. Fluidized bed units designed to burn biomass/bio-based solids	a. CO (or CEMS) b. Filterable PM (or TSM)	260 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (310 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average) 9.8E-03 lb per MMBtu of heat input; or (8.3E-05 ^a lb per MMBtu of heat input)	1 hr minimum sampling time. Collect a minimum of 3 dscm per run.
10. Suspension burners designed to burn biomass/bio-based solids	a. CO (or CEMS) b. Filterable PM (or TSM)	2,400 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (2,000 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 10-day rolling average) 3.0E-02 lb per MMBtu of heat input; or (6.5E-03 lb per MMBtu of heat input)	1 hr minimum sampling time. Collect a minimum of 2 dscm per run.
11. Dutch Ovens/Pile	a. CO (or	470 ppm by volume on a dry	1 hr minimum sampling

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
burners designed to burn biomass/bio-based solids	CEMS)	basis corrected to 3 percent oxygen, 3-run average; or (520 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 10-day rolling average)	time.
12. Fuel cell units designed to burn biomass/bio-based solids	b. Filterable PM (or TSM)	3.2E-03 lb per MMBtu of heat input; or (3.9E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
	a. CO b. Filterable PM (or TSM)	910 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average 2.0E-02 lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	1 hr minimum sampling time. Collect a minimum of 2 dscm per run.
13. Hybrid suspension grate boiler designed to burn biomass/bio-based solids	a. CO (or CEMS)	1,500 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (900 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.
14. Units designed to burn liquid fuel	a. HCl	4.4E-04 lb per MMBtu of heat input	For M26A: Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
	b. Mercury	4.8E-07 ^a lb per MMBtu of heat input	run. For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 4 dscm.
15. Units designed to burn heavy liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.3E-02 lb per MMBtu of heat input; or (7.5E-05 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
16. Units designed to burn light liquid fuel	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.3E-03 ^a lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
17. Units designed to burn liquid fuel that are non-continental units	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average based on stack test	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.3E-02 lb per MMBtu of heat input; or (8.6E-04 lb per MMBtu of heat input)	Collect a minimum of 4 dscm per run.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
18. Units designed to burn gas 2 (other) gases	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average	1 hr minimum sampling time.
	b. HCl	1.7E-03 lb per MMBtu of heat input	For M26A, Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	c. Mercury	7.9E-06 lb per MMBtu of heat input	For M29, collect a minimum of 3 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 3 dscm.
	d. Filterable PM (or TSM)	6.7E-03 lb per MMBtu of heat input; or (2.1E-04 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.

^a If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit, you can skip testing according to [§ 63.7515](#) if all of the other provision of [§ 63.7515](#) are met. For all other pollutants that do not contain a footnote “a”, your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

^b Incorporated by reference, see [§ 63.14](#).

^c An owner or operator may request an alternative test method under [§ 63.7 of this chapter](#), in order that compliance with the carbon monoxide emissions limit be determined using carbon dioxide as a diluent correction in place of oxygen at 3%. EPA Method 19 F-factors and EPA Method 19 equations must be used to generate the appropriate CO₂ correction percentage for the fuel type burned in the unit, and must also take into account that the 3% oxygen correction is to

be done on a dry basis. The alternative test method request must account for any CO₂ being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc.

[80 FR 72834, Nov. 20, 2015]

Table 13 to Subpart DDDDD of Part 63 - Alternative Emission Limits for New or Reconstructed Boilers and Process Heaters That Commenced Construction or Reconstruction After December 23, 2011, and Before April 1, 2013

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
1. Units in all subcategories designed to burn solid fuel	a. HCl	0.022 lb per MMBtu of heat input	For M26A, collect a minimum of 1 dscm per run; for M26 collect a minimum of 120 liters per run.
	b. Mercury	8.6E-07 ^a lb per MMBtu of heat input	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 4 dscm.
2. Pulverized coal boilers designed to burn coal/solid fossil fuel	a. Carbon monoxide (CO) (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (320 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
	b. Filterable PM (or TSM)	1.1E-03 lb per MMBtu of heat input; or (2.8E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
3. Stokers designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (340 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 10-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.8E-02 lb per MMBtu of heat input; or (2.3E-05 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
4. Fluidized bed units designed to burn coal/solid fossil fuel	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (230 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	1.1E-03 lb per MMBtu of heat input; or (2.3E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
5. Fluidized bed units with an integrated heat exchanger designed to burn coal/solid fossil fuel	a. CO (or CEMS)	140 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (150 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
6. Stokers/sloped grate/others designed to burn wet biomass fuel	<p>b. Filterable PM (or TSM)</p> <p>a. CO (or CEMS)</p>	<p>1.1E-03 lb per MMBtu of heat input; or (2.3E-05 lb per MMBtu of heat input)</p> <p>620 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (410 ppm by volume on a dry basis corrected to 3 percent oxygen,^c 10-day rolling average)</p>	<p>Collect a minimum of 3 dscm per run.</p> <p>1 hr minimum sampling time.</p>
7. Stokers/sloped grate/others designed to burn kiln-dried biomass fuel	<p>b. Filterable PM (or TSM)</p> <p>a. CO</p>	<p>3.0E-02 lb per MMBtu of heat input; or (2.6E-05 lb per MMBtu of heat input)</p> <p>460 ppm by volume on a dry basis corrected to 3 percent oxygen</p>	<p>Collect a minimum of 2 dscm per run.</p> <p>1 hr minimum sampling time.</p>
8. Fluidized bed units designed to burn biomass/bio-based solids	<p>b. Filterable PM (or TSM)</p> <p>a. CO (or CEMS)</p>	<p>3.2E-01 lb per MMBtu of heat input; or (4.0E-03 lb per MMBtu of heat input)</p> <p>230 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (310 ppm by volume on a dry basis corrected to 3 percent oxygen,^c 30-day rolling average)</p>	<p>Collect a minimum of 2 dscm per run.</p> <p>1 hr minimum sampling time.</p>
	b. Filterable PM (or	9.8E-03 lb per MMBtu of heat input; or (8.3E-05 ^a lb per	Collect a minimum of 3 dscm per run.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
9. Suspension burners designed to burn biomass/bio-based solids	TSM) a. CO (or CEMS)	MMBtu of heat input) 2,400 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (2,000 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 10-day rolling average)	1 hr minimum sampling time.
10. Dutch Ovens/Pile burners designed to burn biomass/bio-based solids	b. Filterable PM (or TSM) a. CO (or CEMS)	5.1E-02 lb per MMBtu of heat input; or (6.5E-03 lb per MMBtu of heat input) 810 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (520 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 10-day rolling average)	Collect a minimum of 2 dscm per run.
11. Fuel cell units designed to burn biomass/bio-based solids	b. Filterable PM (or TSM) a. CO	3.6E-02 lb per MMBtu of heat input; or (3.9E-05 lb per MMBtu of heat input) 910 ppm by volume on a dry basis corrected to 3 percent oxygen	1 hr minimum sampling time.
	b. Filterable PM (or TSM)	2.0E-02 lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
12. Hybrid suspension grate boiler designed to burn biomass/bio-based solids	a. CO (or CEMS)	1,500 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (900 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 30-day rolling average)	1 hr minimum sampling time.
13. Units designed to burn liquid fuel	b. Filterable PM (or TSM)	2.6E-02 lb per MMBtu of heat input; or (4.4E-04 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run. For M26A: Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
14. Units designed to burn heavy liquid fuel	a. HCl	1.2E-03 lb per MMBtu of heat input	For M29, collect a minimum of 4 dscm per run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784 ^b collect a minimum of 4 dscm.
	b. Mercury	4.9E-07 ^a lb per MMBtu of heat input	
	a. CO (or CEMS)	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average; or (18 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 10-day rolling average)	1 hr minimum sampling time.

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
15. Units designed to burn light liquid fuel	a. CO (or CEMS)	130 ^a ppm by volume on a dry basis corrected to 3 percent oxygen; or (60 ppm by volume on a dry basis corrected to 3 percent oxygen, ^c 1-day block average)	1 hr minimum sampling time.
16. Units designed to burn liquid fuel that are non-continental units	b. Filterable PM (or TSM)	1.1E-03 ^a lb per MMBtu of heat input; or (2.9E-05 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
16. Units designed to burn liquid fuel that are non-continental units	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-run average based on stack test; or (91 ppm by volume on a dry basis corrected to 3 percent oxygen, 3-hour rolling average)	1 hr minimum sampling time.
16. Units designed to burn liquid fuel that are non-continental units	b. Filterable PM (or TSM)	2.3E-02 lb per MMBtu of heat input; or (8.6E-04 lb per MMBtu of heat input)	Collect a minimum of 2 dscm per run.
17. Units designed to burn gas 2 (other) gases	a. CO	130 ppm by volume on a dry basis corrected to 3 percent oxygen	1 hr minimum sampling time.
	b. HCl	1.7E-03 lb per MMBtu of heat input	For M26A, Collect a minimum of 2 dscm per run; for M26, collect a minimum of 240 liters per run.
	c. Mercury	7.9E-06 lb per MMBtu of heat input	For M29, collect a minimum of 3 dscm per

If your boiler or process heater is in this subcategory . . .	For the following pollutants . . .	The emissions must not exceed the following emission limits, except during periods of startup and shutdown . . .	Using this specified sampling volume or test run duration . . .
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run; for M30A or M30B, collect a minimum sample as specified in the method; for ASTM D6784^b collect a minimum of 3 dscm.

d. Filterable PM (or TSM)	6.7E-03 lb per MMBtu of heat input; or (2.1E-04 lb per MMBtu of heat input)	Collect a minimum of 3 dscm per run.
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^a If you are conducting stack tests to demonstrate compliance and your performance tests for this pollutant for at least 2 consecutive years show that your emissions are at or below this limit and you are not required to conduct testing for CEMS or CPMS monitor certification, you can skip testing according to [§ 63.7515](#) if all of the other provision of [§ 63.7515](#) are met. For all other pollutants that do not contain a footnote “a”, your performance tests for this pollutant for at least 2 consecutive years must show that your emissions are at or below 75 percent of this limit in order to qualify for skip testing.

^b Incorporated by reference, see [§ 63.14](#).

^c An owner or operator may request an alternative test method under [§ 63.7 of this chapter](#), in order that compliance with the carbon monoxide emissions limit be determined using carbon dioxide as a diluent correction in place of oxygen at 3%. EPA Method 19 F-factors and EPA Method 19 equations must be used to generate the appropriate CO₂ correction percentage for the fuel type burned in the unit, and must also take into account that the 3% oxygen correction is to be done on a dry basis. The alternative test method request must account for any CO₂ being added to, or removed from, the emissions gas stream as a result of limestone injection, scrubber media, etc.

[[78 FR 7210](#), Jan. 31, 2013, as amended at [80 FR 72836](#), Nov. 20, 2015]

Appendix G

40 C.F.R. Part 63 Subpart SSSS

National Emission Standards for Hazardous Air Pollutants: Surface Coating of Metal Coil

Subpart SSSS - National Emission Standards for Hazardous Air Pollutants: Surface Coating of Metal Coil

Source: [67 FR 39812](#), June 10, 2002, unless otherwise noted.

What This Subpart Covers

§ 63.5080 What is in this subpart?

This subpart describes the actions you must take to reduce emissions of hazardous air pollutants (HAP) if you own or operate a facility that performs metal coil surface coating operations and is a major source of HAP. This subpart establishes emission standards and states what you must do to comply. Certain requirements apply to all who must comply with the subpart; others depend on the means you use to comply with an emission standard.

§ 63.5090 Does this subpart apply to me?

(a) The provisions of this subpart apply to each facility that is a major source of HAP, as defined in [§ 63.2](#), at which a coil coating line is operated, except as provided in [paragraphs \(b\) and \(e\)](#) of this section.

(b) This subpart does not apply to any coil coating line that meets the criteria of [paragraph \(b\)\(1\)](#) or [\(2\)](#) of this section.

(1) A coil coating line that is part of research or laboratory equipment.

(2) A coil coating line on which at least 85 percent of the metal coil coated, based on surface area, is less than 0.15 millimeter (0.006 inch) thick, except as provided in [paragraph \(c\)](#) of this section.

(c) If you operate a coating line subject to [subpart JJJJ of this part](#) that also meets the criteria in either [paragraph \(c\)\(1\)](#) or [\(2\)](#) of this section, and you choose to comply with the requirements of this subpart, then such compliance constitutes compliance with subpart JJJJ. The coating line for which you choose this option is, therefore, included in the affected source for this subpart as defined in [§ 63.5110](#) and shall not be included in the affected source for subpart JJJJ as defined in [§ 63.3300](#).

(1) The coating line is used to coat metal coil of thicknesses both less than and greater than or equal to 0.15 millimeter (0.006 inch) thick, regardless of the percentage of surface area of each thickness coated.

(2) The coating line is used to coat only metal coil that is less than 0.15 millimeter (0.006 inch) thick and the coating line is controlled by a common control device that also receives organic HAP emissions from a coil coating line that is subject to the requirements of this subpart.

(d) Each coil coating line that does not comply with the provisions of this subpart because it meets the criteria in [paragraph \(b\)\(2\)](#) of this section, that for any rolling 12-month period fails to meet the criteria in [paragraph \(b\)\(2\)](#) would from that point forward become subject to the provisions of this subpart. After becoming subject to the provisions of this subpart, the coil coating line would no longer be eligible to use the criteria of [paragraph \(b\)\(2\)](#) of this section, even if in subsequent 12-month periods at least 85 percent of the metal coil coated, based on surface area, is less than 0.15 millimeter (0.006 inch) thick.

(e) This subpart does not apply to the application of incidental markings (including letters, numbers, or symbols) that are added to bare metal coils and that are used for only product identification or for product inventory control. The application of letters, numbers, or symbols to a coated metal coil is considered a coil coating process and part of the coil coating affected source.

[[67 FR 39812](#), June 10, 2002, as amended at [85 FR 10861](#), Feb. 25, 2020]

§ 63.5100 Which of my emissions sources are affected by this subpart?

The affected source subject to this subpart is the collection of all of the coil coating lines at your facility.

§ 63.5110 What special definitions are used in this subpart?

All terms used in this subpart that are not defined in this section have the meaning given to them in the Clean Air Act (CAA) and in [subpart A of this part](#).

Always-controlled work station means a work station associated with a curing oven from which the curing oven exhaust is delivered to a control device with no provision for the oven exhaust to bypass the control device. Sampling lines for analyzers and relief valves needed for safety purposes are not considered bypass lines.

Capture efficiency means the fraction of all organic HAP emissions generated by a process that is delivered to a control device, expressed as a percentage.

Capture system means a hood, enclosed room, or other means of collecting organic HAP emissions and conveying them to a control device.

Car-seal means a seal that is placed on a device that is used to change the position of a valve or damper (e.g., from open to closed) in such a way that the position of the valve or damper cannot be changed without breaking the seal.

Coating means material applied onto or impregnated into a substrate for decorative, protective, or functional purposes. Such materials include, but are not limited to, paints, varnishes, sealants, inks, adhesives, maskants, and temporary coatings. Decorative, protective, or functional

materials that consist only of solvents, protective oils, acids, bases, or any combination of these substances are not considered coatings for the purposes of this subpart.

Coating material means the coating and other products (e.g., a catalyst and resin in multi-component coatings) combined to make a single material at the coating facility that is applied to metal coil. For the purposes of this subpart, an organic solvent that is used to thin a coating prior to application to the metal coil is considered a coating material.

Coil coating line means a process and the collection of equipment used to apply an organic coating to the surface of metal coil. A coil coating line includes a web unwind or feed section, a series of one or more work stations, any associated curing oven, wet section, and quench station. A coil coating line does not include ancillary operations such as mixing/thinning, cleaning, wastewater treatment, and storage of coating material.

Control device means a device such as a solvent recovery device or oxidizer which reduces the organic HAP in an exhaust gas by recovery or by destruction.

Control device efficiency means the ratio of organic HAP emissions recovered or destroyed by a control device to the total organic HAP emissions that are introduced into the control device, expressed as a percentage.

Curing oven means the device that uses heat or radiation to dry or cure the coating material applied to the metal coil.

Day means a 24-consecutive-hour period.

Deviation, before August 24, 2020, means any instance in which an affected source, subject to this subpart, or an owner or operator of such a source:

- (1) Fails to meet any requirement or obligation established by this subpart including, but not limited to, any emission limitation (including any operating limit) or work practice standard; or
- (2) Fails to meet any term or condition that is adopted to implement an applicable requirement in this subpart and that is included in the operating permit for any affected source required to obtain such a permit; or
- (3) Fails to meet any emission limitation (including any operating limit) or work practice standard in this subpart during start-up, shutdown, or malfunction, regardless of whether or not such failure is permitted by this subpart.

Deviation, on and after August 24, 2020, means any instance in which an affected source, subject to this subpart, or an owner or operator of such a source:

- (1) Fails to meet any requirement or obligation established by this subpart including, but not limited to, any emission limitation (including any operating limit) or work practice standard; or

(2) Fails to meet any term or condition that is adopted to implement an applicable requirement in this subpart and that is included in the operating permit for any affected source required to obtain such a permit.

Existing affected source means an affected source the construction of which commenced on or before July 18, 2000, and it has not subsequently undergone reconstruction as defined in [§ 63.2](#).

Facility means all contiguous or adjoining property that is under common ownership or control, including properties that are separated only by a road or other public right-of-way.

Flexible packaging means any package or part of a package the shape of which can be readily changed. Flexible packaging includes but is not limited to bags, pouches, labels, liners and wraps utilizing paper, plastic, film, aluminum foil, metalized or coated paper or film, or any combination of these materials.

HAP applied means the organic HAP content of all coating materials applied to a substrate by a coil coating line.

Intermittently-controllable work station means a work station associated with a curing oven with provisions for the curing oven exhaust to be delivered to a control device or diverted from a control device through a bypass line, depending on the position of a valve or damper. Sampling lines for analyzers and relief valves needed for safety purposes are not considered bypass lines.

Metal coil means a continuous metal strip that is at least 0.15 millimeter (0.006 inch) thick, which is packaged in a roll or coil prior to coating. After coating, it may or may not be rewound into a roll or coil. Metal coil does not include metal webs that are coated for use in flexible packaging.

Month means a calendar month or a pre-specified period of 28 days to 35 days to allow for flexibility in recordkeeping when data are based on a business accounting period.

Never-controlled work station means a work station which is not equipped with provisions by which any emissions, including those in the exhaust from any associated curing oven, may be delivered to a control device.

New affected source means an affected source the construction or reconstruction of which commenced after July 18, 2000.

Overall organic HAP control efficiency means the total efficiency of a control system, determined either by:

- (1) The product of the capture efficiency as determined in accordance with the requirements of [§ 63.5160\(e\)](#) and the control device efficiency as determined in accordance with the requirements of [§ 63.5160\(a\)\(1\)\(i\)](#) and [\(ii\)](#) or [§ 63.5160\(d\)](#); or
- (2) A liquid-liquid material balance in accordance with the requirements of [§ 63.5170\(e\)\(1\)](#).

Permanent total enclosure (PTE) means a permanently installed enclosure that meets the criteria of Method 204 of appendix M, [40 CFR part 51](#) for a PTE, and that directs all the exhaust gases from the enclosure to a control device.

Protective oil means an organic material that is applied to metal for the purpose of providing lubrication or protection from corrosion without forming a solid film. This definition of protective oil includes but is not limited to lubricating oils, evaporative oils (including those that evaporate completely), and extrusion oils.

Research or laboratory equipment means any equipment for which the primary purpose is to conduct research and development into new processes and products, where such equipment is operated under the close supervision of technically trained personnel and is not engaged in the manufacture of products for commercial sale in commerce, except in a de minimis manner.

Temporary total enclosure (TTE) means an enclosure constructed for the purpose of measuring the capture efficiency of pollutants emitted from a given source, as defined in Method 204 of [40 CFR part 51, appendix M](#).

Work station means a unit on a coil coating line where coating material is deposited onto the metal coil substrate.

[[67 FR 39812](#), June 10, 2002, as amended at [85 FR 10861](#), Feb. 25, 2020]

Emission Standards and Compliance Dates

§ 63.5120 What emission standards must I meet?

(a) Each coil coating affected source must limit organic HAP emissions to the level specified in [paragraph \(a\)\(1\)](#), [\(2\)](#), or [\(3\)](#) of this section:

(1) No more than 2 percent of the organic HAP applied for each month during each 12-month compliance period (98 percent reduction); or

(2) No more than 0.046 kilogram (kg) of organic HAP per liter of solids applied during each 12-month compliance period; or

(3) If you use an oxidizer to control organic HAP emissions, operate the oxidizer such that an outlet organic HAP concentration of no greater than 20 parts per million by volume (ppmv) on a dry basis is achieved and the efficiency of the capture system is 100 percent.

(b) You must demonstrate compliance with one of these standards by following the applicable procedures in [§ 63.5170](#).

§ 63.5121 What operating limits must I meet?

(a) Except as provided in [paragraph \(b\)](#) of this section, for any coil coating line for which you use an add-on control device, unless you use a solvent recovery system and conduct a liquid-liquid material balance according to [§ 63.5170\(e\)\(1\)](#), you must meet the applicable operating limits specified in Table 1 to this subpart. You must establish the operating limits during performance tests according to the requirements in [§ 63.5160\(d\)\(3\)](#) and Table 1 to [§ 63.5160](#). You must meet the operating limits established during the most recent performance test required in [§ 63.5160](#) at all times after you establish them.

(b) If you use an add-on control device other than those listed in Table 1 to this subpart, or wish to monitor an alternative parameter and comply with a different operating limit, you must apply to the Administrator for approval of alternative monitoring under [§ 63.8\(f\)](#).

[[67 FR 39812](#), June 10, 2002, as amended at [85 FR 10862](#), Feb. 25, 2020]

§ 63.5130 When must I comply?

(a) For an existing affected source, the compliance date is June 10, 2005.

(b) If you own or operate a new affected source subject to the provisions of this subpart, you must comply immediately upon start-up of the affected source, or by June 10, 2002, whichever is later.

(c) Affected sources which have undergone reconstruction are subject to the requirements for new affected sources.

(d) The initial compliance period begins on the applicable compliance date specified in [paragraph \(a\)](#) or [\(b\)](#) of this section and ends on the last day of the 12th month following the compliance date. If the compliance date falls on any day other than the first day of a month, then the initial compliance period extends through that month plus the next 12 months.

(e) For the purpose of demonstrating continuous compliance, a compliance period consists of 12 months. Each month after the end of the initial compliance period described in [paragraph \(d\)](#) of this section is the end of a compliance period consisting of that month and the preceding 11 months.

[[67 FR 39812](#), June 10, 2002, as amended at [85 FR 10862](#), Feb. 25, 2020]

General Requirements for Compliance with the Emission Standards and for Monitoring and Performance Tests

§ 63.5140 What general requirements must I meet to comply with the standards?

(a) Before August 24, 2020, you must be in compliance with the applicable emission standards in [§ 63.5120](#) and the operating limits in Table 1 to this subpart at all times, except during periods of start-up, shutdown, and malfunction of any capture system and control device used to comply with this subpart. On and after August 24, 2020 you must be in compliance with the applicable emission standards in [§ 63.5120](#) and the operating limits in Table 1 to this subpart at all times. If you are complying with the emission standards of this subpart without the use of a capture system and control device, you must be in compliance with the standards at all times.

(b) Before August 24, 2020, you must always operate and maintain your affected source, including air pollution control and monitoring equipment, according to the provisions in [§ 63.6\(e\)\(1\)](#). On and after August 24, 2020, at all times, you must operate and maintain your affected source, including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions. The general duty to minimize emissions does not require the owner or operator to make any further efforts to reduce emissions if levels required by the applicable standard have been achieved. Determination of whether a source is operating in compliance with operation and maintenance requirements will be based on information available to the Administrator that may include, but is not limited to, monitoring results, review of operation and maintenance procedures, review of operation and maintenance records, and inspection of the affected source.

(c) Table 2 of this subpart provides cross references to [subpart A of this part](#), indicating the applicability of the General Provisions requirements to this subpart.

[[67 FR 39812](#), June 10, 2002, as amended at [85 FR 10862](#), Feb. 25, 2020]

§ 63.5150 If I use a control device to comply with the emission standards, what monitoring must I do?

Table 1 to [§ 63.5150](#) - Control Device Monitoring Requirements Index

If you operate a coil coating line and have the following:	Then you must:
1. Control device	Monitor control device operating parameters (§ 63.5150(a)(3)).
2. Capture system	Monitor capture system operating parameters (§ 63.5150(a)(4)).
3. Intermittently controllable work station	Monitor parameters related to possible exhaust flow through any bypass to a control device (§ 63.5150(a)(1)).

If you operate a coil coating line and have the following:

Then you must:

4. Continuous emission monitors

Operate continuous emission monitors and perform a quarterly audit ([§ 63.5150\(a\)\(2\)](#)).

(a) To demonstrate continuing compliance with the standards, you must monitor and inspect each capture system and each control device required to comply with [§ 63.5120](#) following the date on which the initial performance test of the capture system and control device is completed. You must install and operate the monitoring equipment as specified in [paragraphs \(a\)\(1\) through \(4\)](#) of this section. On and after August 24, 2020, you must also maintain the monitoring equipment at all times in accordance with [§ 63.5140\(b\)](#) and keep the necessary parts readily available for routine repairs of the monitoring equipment.

(1) ***Bypass monitoring.*** If you operate coil coating lines with intermittently-controllable work stations, you must follow at least one of the procedures in [paragraphs \(a\)\(1\)\(i\) through \(iv\)](#) of this section for each curing oven associated with these work stations to monitor for potential bypass of the control device:

(i) ***Flow control position indicator.*** Install, calibrate, maintain, and operate according to the manufacturer's specifications a flow control position indicator that provides a record indicating whether the exhaust stream from the curing oven is directed to the control device or is diverted from the control device. The time and flow control position must be recorded at least once per hour, as well as every time the flow direction is changed. The flow control position indicator must be installed at the entrance to any bypass line that could divert the exhaust stream away from the control device to the atmosphere.

(ii) ***Car-seal or lock-and-key valve closures.*** Secure any bypass line valve in the closed position with a car-seal or a lock-and-key type configuration when the control device is in operation; a visual inspection of the seal or closure mechanism will be performed at least once every month to ensure that the valve or damper is maintained in the closed position, and the exhaust stream is not diverted through the bypass line.

(iii) ***Valve closure continuous monitoring.*** Ensure that any bypass line valve or damper is in the closed position through continuous monitoring of valve position when the control device is in operation. The monitoring system must be inspected at least once every month to verify that the monitor will indicate valve position.

(iv) ***Automatic shutdown system.*** Use an automatic shutdown system in which the coil coating line is stopped when flow is diverted away from the control device to any bypass line when the control device is in operation. The automatic shutdown system must be inspected at least once every month to verify that it will detect diversions of flow and shutdown operations.

(2) **Continuous emission monitoring system (CEMS).** If you are demonstrating continuous compliance with the standards in [§ 63.5120\(a\)\(1\)](#) or [\(2\)](#) through continuous emission monitoring of a control device, you must install, calibrate, operate, and maintain continuous emission monitors to measure the total organic volatile matter concentration at both the control device inlet and outlet, and you must continuously monitor flow rate. If you are demonstrating continuous compliance with the outlet organic HAP concentration limit in [§ 63.5120\(a\)\(3\)](#), you must install, calibrate, operate, and maintain a continuous emission monitor to measure the total organic volatile matter concentration at the control device outlet.

(i) All CEMS must comply with performance specification 8 or 9 of [40 CFR part 60, appendix B](#), as appropriate for the detection principle you choose. The requirements of [40 CFR part 60](#), procedure 1, appendix F must also be followed. In conducting the quarterly audits of the monitors as required by procedure 1, appendix F, you must use compounds representative of the gaseous emission stream being controlled.

(ii) As specified in [§ 63.8\(c\)\(4\)\(ii\)](#), each CEMS and each flow rate monitor must complete a minimum of one cycle of operation (sampling, analyzing, and data recording) for each successive 15-minute period. Information which must be determined for recordkeeping purposes, as required by [§ 63.5190\(a\)\(1\)\(i\)](#) includes:

(A) The hourly average of all recorded readings;

(B) The daily average of all recorded readings for each operating day; and

(C) The monthly average for each month during the semiannual reporting period.

(3) **Temperature monitoring of oxidizers.** If you are complying with the requirements of the standards in [§ 63.5120](#) through the use of an oxidizer and demonstrating continuous compliance through monitoring of an oxidizer operating parameter, you must comply with [paragraphs \(a\)\(3\)\(i\)](#) through [\(iii\)](#) of this section.

(i) Install, calibrate, maintain, and operate temperature monitoring equipment according to manufacturer's specifications. The calibration of the chart recorder, data logger, or temperature indicator must be verified every 3 months; or the chart recorder, data logger, or temperature indicator must be replaced. You must replace the equipment either if you choose not to perform the calibration, or if the equipment cannot be calibrated properly. Each temperature monitoring device must be equipped with a continuous recorder. The device must have an accuracy of ± 1 percent of the temperature being monitored in degrees Celsius, or ± 1 °Celsius, whichever is greater.

(ii) For an oxidizer other than a catalytic oxidizer, to demonstrate continuous compliance with the operating limit established according to [§ 63.5160\(d\)\(3\)\(i\)](#), you must install the thermocouple or temperature sensor in the combustion chamber at a location in the combustion zone.

(iii) For a catalytic oxidizer, if you are demonstrating continuous compliance with the operating limit established according to [§ 63.5160\(d\)\(3\)\(ii\)\(A\)](#) and [\(B\)](#), then you must install the thermocouples or temperature sensors in the vent stream at the nearest feasible point to the inlet and outlet of the catalyst bed. Calculate the temperature difference across the catalyst. If you are demonstrating continuous compliance with the operating limit established according to [§ 63.5160\(d\)\(3\)\(ii\)\(C\)](#) and [\(D\)](#), then you must install the thermocouple or temperature sensor in the vent stream at the nearest feasible point to the inlet of the catalyst bed.

(4) **Capture system monitoring.** If you are complying with the requirements of the standards in [§ 63.5120](#) through the use of a capture system and control device, you must develop a capture system monitoring plan containing the information specified in [paragraphs \(a\)\(4\)\(i\)](#) and [\(ii\)](#) of this section. You must monitor the capture system in accordance with [paragraph \(a\)\(4\)\(iii\)](#) of this section. You must make the monitoring plan available for inspection by the permitting authority upon request.

(i) The monitoring plan must identify the operating parameter to be monitored to ensure that the capture efficiency measured during compliance tests is maintained, explain why this parameter is appropriate for demonstrating ongoing compliance, and identify the specific monitoring procedures.

(ii) The plan also must specify operating limits at the capture system operating parameter value, or range of values, that demonstrates compliance with the standards in [§ 63.5120](#). The operating limits must represent the conditions indicative of proper operation and maintenance of the capture system.

(iii) You must conduct monitoring in accordance with the plan.

(b) If an operating parameter monitored in accordance with [paragraphs \(a\)\(3\)](#) and [\(4\)](#) of this section is out of the allowed range specified in Table 1 to this subpart it will be considered a deviation from the operating limit.

[[67 FR 39812](#), June 10, 2002, as amended at [85 FR 10862](#), Feb. 25, 2020]

§ 63.5160 What performance tests must I complete?

Table 1 to [§ 63.5160](#) - Required Performance Testing Summary

If you control HAP on your coil coating line by:	You must:
1. Limiting HAP or Volatile matter	Determine the HAP or volatile matter and solids content of coating materials

If you control HAP on your coil coating line by:

You must:

content of coatings

according to the procedures in [§ 63.5160\(b\)](#) and [\(c\)](#).

2. Using a capture system and add-on control device

Except as specified in [paragraph \(a\)](#) of this section, conduct an initial performance test within 180 days of the applicable compliance date in [§ 63.5130](#), and conduct periodic performance tests within 5 years following the previous performance test, as follows: If you are not required to complete periodic performance tests as a requirement of renewing your facility's operating permit under [40 CFR part 70](#) or [40 CFR part 71](#), you must conduct the first periodic performance test before March 25, 2023, unless you already have conducted a performance test on or after March 25, 2018; thereafter, you must conduct a performance test no later than 5 years following the previous performance test. Operating limits must be confirmed or reestablished during each performance test. If you are required to complete periodic performance tests as a requirement of renewing your facility's operating permit under [40 CFR part 70](#) or [40 CFR part 71](#), you must conduct the periodic testing in accordance with the terms and schedule required by your permit conditions. For each performance test: (1) For each capture and control system, determine the destruction or removal efficiency of each control device according to [§ 63.5160\(d\)](#) and the capture efficiency of each capture system according to [§ 63.5160\(e\)](#), and (2) confirm or re-establish the operating limits.

(a) If you use a control device to comply with the requirements of [§ 63.5120](#), you are not required to conduct a performance test to demonstrate compliance if one or more of the criteria in [paragraphs \(a\)\(1\)](#) through [\(3\)](#) of this section are met:

(1) The control device is equipped with continuous emission monitors for determining total organic volatile matter concentration, and capture efficiency has been determined in accordance with the requirements of this subpart; and the continuous emission monitors are used to demonstrate continuous compliance in accordance with [§ 63.5150\(a\)\(2\)](#); or

(2) You have received a waiver of performance testing under [§ 63.7\(h\)](#); or

(3) The control device is a solvent recovery system and you choose to comply by means of a monthly liquid-liquid material balance.

(b) **Organic HAP content.** You must determine the organic HAP weight fraction of each coating material applied by following one of the procedures in [paragraphs \(b\)\(1\)](#) through [\(4\)](#) of this section:

(1) **Method 311.** You may test the material in accordance with Method 311 of [appendix A of this part](#). The Method 311 determination may be performed by the manufacturer of the material and the results provided to you. The organic HAP content must be calculated according to the criteria and procedures in [paragraphs \(b\)\(1\)\(i\)](#) through [\(iii\)](#) of this section.

(i) Count only those organic HAP in Table 3 to this subpart that are measured to be present at greater than or equal to 0.1 weight percent and greater than or equal to 1.0 weight percent for other organic HAP compounds.

(ii) Express the weight fraction of each organic HAP you count according to [paragraph \(b\)\(1\)\(i\)](#) of this section as a value truncated to four places after the decimal point (for example, 0.3791).

(iii) Calculate the total weight fraction of organic HAP in the tested material by summing the counted individual organic HAP weight fractions and truncating the result to three places after the decimal point (for example, 0.763).

(2) **Method 24 in appendix A-7 of part 60.** For coatings, you may determine the total volatile matter content as weight fraction of nonaqueous volatile matter and use it as a substitute for organic HAP, using Method 24 in appendix A-7 of part 60. As an alternative to using Method 24, you may use ASTM D2369-10 (2015), “Test Method for Volatile Content of Coatings” (incorporated by reference, see [§ 63.14](#)). The determination of total volatile matter content using a method specified in this [paragraph \(b\)\(2\)](#) or as provided in [paragraph \(b\)\(3\)](#) of this section may be performed by the manufacturer of the coating and the results provided to you.

(3) **Alternative method.** You may use an alternative test method for determining the organic HAP weight fraction once the Administrator has approved it. You must follow the procedure in [§ 63.7\(f\)](#) to submit an alternative test method for approval.

(4) **Formulation data.** You may use formulation data provided that the information represents each organic HAP in Table 3 to this subpart that is present at a level equal to or greater than 0.1 percent and equal to or greater than 1.0 percent for other organic HAP compounds in any raw material used, weighted by the mass fraction of each raw material used in the material. Formulation data may be provided to you by the manufacturer of the coating material. In the event of any inconsistency between test data obtained with the test methods specified in [paragraphs \(b\)\(1\)](#) through [\(3\)](#) of this section and formulation data, the test data will govern.

(c) **Solids content and density.** You must determine the solids content and the density of each coating material applied. You may determine the volume solids content using ASTM D2697-03(2014) Standard Test Method for Volume Nonvolatile Matter in Clear or Pigmented Coatings (incorporated by reference, see [§ 63.14](#)) or ASTM D6093-97 (2016) Standard Test

Method for Percent Volume Nonvolatile Matter in Clear or Pigmented Coatings Using a Helium Gas Pycnometer (incorporated by reference, see [§ 63.14](#)), or an EPA approved alternative method. You must determine the density of each coating using ASTM D1475-13 “Standard Test Method for Density of Liquid Coatings, Inks, and Related Products” (incorporated by reference, see [§ 63.14](#)) or ASTM D2111-10 (2015) “Standard Test Methods for Specific Gravity and Density of Halogenated Organic Solvents and Their Admixtures” (incorporated by reference, see [§ 63.14](#)). The solids determination using ASTM D2697-03(2014) or ASTM D6093-97 (2016) and the density determination using ASTM D1475-13 or ASTM 2111-10 (2015) may be performed by the manufacturer of the material and the results provided to you. Alternatively, you may rely on formulation data provided by material providers to determine the volume solids. In the event of any inconsistency between test data obtained with the ASTM test methods specified in this section and formulation data, the test data will govern.

(d) ***Control device destruction or removal efficiency.*** If you are using an add-on control device, such as an oxidizer, to comply with the standard in [§ 63.5120](#), you must conduct performance tests according to Table 1 to [§ 63.5160](#) to establish the destruction or removal efficiency of the control device or the outlet HAP concentration achieved by the oxidizer, according to the methods and procedures in [paragraphs \(d\)\(1\)](#) and [\(2\)](#) of this section. During performance tests, you must establish the operating limits required by [§ 63.5121](#) according to [paragraph \(d\)\(3\)](#) of this section.

(1) Performance tests conducted to determine the destruction or removal efficiency of the control device must be performed such that control device inlet and outlet testing is conducted simultaneously. To determine the outlet organic HAP concentration achieved by the oxidizer, only oxidizer outlet testing must be conducted. The data must be reduced in accordance with the test methods and procedures in paragraphs (d)(1)(i) through (ix).

(i) Method 1 or 1A of [40 CFR part 60, appendix A](#), is used for sample and velocity traverses to determine sampling locations.

(ii) Method 2, 2A, 2C, 2D, 2F, or 2G of [40 CFR part 60, appendix A](#), is used to determine gas volumetric flow rate.

(iii) Method 3, 3A, or 3B of [40 CFR part 60, appendix A](#), used for gas analysis to determine dry molecular weight. You may also use as an alternative to Method 3B, the manual method for measuring the oxygen, carbon dioxide, and carbon monoxide content of exhaust gas, ANSI/ASME PTC 19.10-1981, “Flue and Exhaust Gas Analyses” (incorporated by reference, see [§ 63.14](#)).

(iv) Method 4 of [40 CFR part 60, appendix A](#), is used to determine stack gas moisture.

(v) Methods for determining gas volumetric flow rate, dry molecular weight, and stack gas moisture must be performed, as applicable, during each test run, as specified in [paragraph \(d\)\(1\)\(vii\)](#) of this section.

(vi) Method 25 or 25A in appendix A-7 of part 60 is used to determine total gaseous non-methane organic matter concentration. You may use Method 18 in appendix A-6 of part 60 to subtract methane emissions from measured total gaseous organic mass emissions as carbon. Use the same test method for both the inlet and outlet measurements, which must be conducted simultaneously. You must submit notification of the intended test method to the Administrator for approval along with notification of the performance test required under [§ 63.7 \(b\)](#). You must use Method 25A if any of the conditions described in [paragraphs \(d\)\(1\)\(vi\)\(A\)](#) through [\(D\)](#) of this section apply to the control device.

(A) The control device is not an oxidizer.

(B) The control device is an oxidizer, but an exhaust gas volatile organic matter concentration of 50 ppmv or less is required to comply with the standards in [§ 63.5120](#); or

(C) The control device is an oxidizer, but the volatile organic matter concentration at the inlet to the control system and the required level of control are such that they result in exhaust gas volatile organic matter concentrations of 50 ppmv or less; or

(D) The control device is an oxidizer, but because of the high efficiency of the control device, the anticipated volatile organic matter concentration at the control device exhaust is 50 ppmv or less, regardless of inlet concentration.

(vii) Each performance test must consist of three separate runs, except as provided by [§ 63.7\(e\)\(3\)](#); each run must be conducted for at least 1 hour under the conditions that exist when the affected source is operating under normal operating conditions. For the purpose of determining volatile organic matter concentrations and mass flow rates, the average of the results of all runs will apply. If you are demonstrating compliance with the outlet organic HAP concentration limit in [§ 63.5120\(a\)\(3\)](#), only the average outlet volatile organic matter concentration must be determined.

(viii) If you are determining the control device destruction or removal efficiency, for each run, determine the volatile organic matter mass flow rates using Equation 1 of this section:

$$M_f = Q_{sd} C_C (12)(0.0416)(10^{-6}) \quad (\text{Eq. 1})$$

Where:

M_f = total organic volatile matter mass flow rate, kg/per hour (h).

C_c = concentration of organic compounds as carbon in the vent gas, as determined by Method 25 or Method 25A, ppmv, dry basis.

Q_{sd} = volumetric flow rate of gases entering or exiting the control device, as determined by Method 2, 2A, 2C, 2D, 2F, or 2G, dry standard cubic meters (dscm)/h.

0.0416 = conversion factor for molar volume, kg-moles per cubic meter (mol/m³) (@ 293 Kelvin (K) and 760 millimeters of mercury (mmHg)).

(ix) For each run, determine the control device destruction or removal efficiency, DRE, using Equation 2 of this section:

$$DRE = \frac{M_{fi} - M_{fo}}{M_{fi}} \times 100 \quad (\text{Eq. 2})$$

Where:

DRE = organic emissions destruction or removal efficiency of the add-on control device, percent.

M_{fi} = organic volatile matter mass flow rate at the inlet to the control device, kg/h.

M_{fo} = organic volatile matter mass flow rate at the outlet of the control device, kg/h.

(x) The control device destruction or removal efficiency is determined as the average of the efficiencies determined in the three test runs and calculated in Equation 2 of this section.

(2) You must record such process information as may be necessary to determine the conditions in existence at the time of the performance test. Before August 24, 2020, operations during periods of start-up, shutdown, and malfunction will not constitute representative conditions for the purpose of a performance test. On and after August 24, 2020, you must conduct the performance test under representative operating conditions for the coating operation. Operations during periods of start-up, shutdown, or nonoperation do not constitute representative conditions for the purpose of a performance test. The owner or operator may not conduct performance tests during periods of malfunction. You must record the process information that is necessary to document operating conditions during the test and explain why the conditions represent normal operation. Upon request, you must make available to the Administrator such records as may be necessary to determine the conditions of performance tests.

(3) **Operating limits.** If you are using a capture system and add-on control device other than a solvent recovery system for which you conduct a liquid-liquid material balance to comply with the requirements in [§ 63.5120](#), you must establish the applicable operating limits required by [§ 63.5121](#). These operating limits apply to each capture system and to each add-on emission control device that is not monitored by CEMS, and you must establish the operating limits during performance tests required by [paragraph \(d\)](#) of this section according to the requirements in [paragraphs \(d\)\(3\)\(i\) through \(iii\)](#) of this section.

(i) **Thermal oxidizer.** If your add-on control device is a thermal oxidizer, establish the operating limits according to [paragraphs \(d\)\(3\)\(i\)\(A\) and \(B\)](#) of this section.

(A) During performance tests, you must monitor and record the combustion temperature at least once every 15 minutes during each of the three test runs. You must monitor the temperature in the firebox of the thermal oxidizer or immediately downstream of the firebox before any substantial heat exchange occurs.

(B) Use the data collected during the performance test to calculate and record the average combustion temperature maintained during the performance test. This average combustion temperature is the minimum operating limit for your thermal oxidizer.

(ii) **Catalytic oxidizer.** If your add-on control device is a catalytic oxidizer, establish the operating limits according to either paragraphs (d)(3)(ii)(A) and (B) or [paragraphs \(d\)\(3\)\(ii\)\(C\) and \(D\)](#) of this section.

(A) During the performance test, you must monitor and record the temperature just before the catalyst bed and the temperature difference across the catalyst bed at least once every 15 minutes during each of the three test runs.

(B) Use the data collected during the performance test to calculate and record the average temperature just before the catalyst bed and the average temperature difference across the catalyst bed maintained during the performance test. These are the minimum operating limits for your catalytic oxidizer.

(C) As an alternative to monitoring the temperature difference across the catalyst bed, you may monitor the temperature at the inlet to the catalyst bed and implement a site-specific inspection and maintenance plan for your catalytic oxidizer as specified in [paragraph \(d\)\(3\)\(ii\)\(D\)](#) of this section. During the performance test, you must monitor and record the temperature just before the catalyst bed at least once every 15 minutes during each of the three test runs. Use the data collected during the performance test to calculate and record the average temperature just before the catalyst bed during the performance test. This is the minimum operating limit for your catalytic oxidizer.

(D) You must develop and implement an inspection and maintenance plan for your catalytic oxidizer(s) for which you elect to monitor according to [paragraph \(d\)\(3\)\(ii\)\(C\)](#) of this section. The plan must address, at a minimum, the elements specified in paragraphs (d)(3)(ii)(D) (1) through (3) of this section.

(1) Annual sampling and analysis of the catalyst activity (*i.e.*, conversion efficiency) following the manufacturer's or catalyst supplier's recommended procedures.

(2) Monthly inspection of the oxidizer system including the burner assembly and fuel supply lines for problems and,

(3) Annual internal and monthly external visual inspection of the catalyst bed to check for channeling, abrasion, and settling. If problems are found, you must take corrective action consistent with the manufacturer's recommendations and conduct a new performance test to determine destruction efficiency according to [§ 63.5160](#).

(iii) **Other types of control devices.** If you use a control device other than an oxidizer or a solvent recovery system for which you choose to comply by means of a monthly liquid-liquid material balance, or wish to monitor an alternative parameter and comply with a different operating limit, you must apply to the Administrator for approval of alternative monitoring under [§ 63.8\(f\)](#).

(e) **Capture efficiency.** If you are required to determine capture efficiency to meet the requirements of [§ 63.5170\(e\)\(2\)](#), [\(f\)\(1\)](#) and [\(2\)](#), [\(g\)\(2\)](#) through [\(4\)](#), or [\(i\)\(2\)](#) and [\(3\)](#), you must determine capture efficiency using the procedures in [paragraph \(e\)\(1\)](#), [\(2\)](#), or [\(3\)](#) of this section, as applicable.

(1) For an enclosure that meets the criteria for a PTE, you may assume it achieves 100 percent capture efficiency. You must confirm that your capture system is a PTE by demonstrating that it meets the requirements of section 6 of EPA Method 204 of [40 CFR part 51, appendix M](#) (or an EPA approved alternative method), and that all exhaust gases from the enclosure are delivered to a control device.

(2) You may determine capture efficiency, CE, according to the protocols for testing with temporary total enclosures that are specified in Method 204A through F of [40 CFR part 51, appendix M](#). You may exclude never-controlled work stations from such capture efficiency determinations.

(3) As an alternative to the procedures specified in [paragraphs \(e\)\(1\)](#) and [\(2\)](#) of this section, if you are required to conduct a capture efficiency test, you may use any capture efficiency protocol and test methods that satisfy the criteria of either the Data Quality Objective or the Lower Confidence Limit approach as described in appendix A to [subpart KK of this part](#). You may exclude never-controlled work stations from such capture efficiency determinations.

[[67 FR 39812](#), June 10, 2002, as amended at [85 FR 10862](#), Feb. 25, 2020]

Requirements for Showing Compliance

§ 63.5170 How do I demonstrate compliance with the standards?

You must include all coating materials (as defined in [§ 63.5110](#)) used in the affected source when determining compliance with the applicable emission limit in [§ 63.5120](#). To make this determination, you must use at least one of the four compliance options listed in Table 1 of this section. You may apply any of the compliance options to an individual coil coating line, or to multiple lines as a group, or to the entire affected source. You may use different compliance options for different coil coating lines, or at different times on the same line. However, you may not use different compliance options at the same time on the same coil coating line. If you switch between compliance options for any coil coating line or group of lines, you must document this

switch as required by [§ 63.5190\(a\)](#), and you must report it in the next semiannual compliance report required in [§ 63.5180](#).

Table 1 to [§ 63.5170](#) - Compliance Demonstration Requirements Index

If you choose to demonstrate compliance by:	Then you must demonstrate that:
1. Use of “as purchased” compliant coatings	a. Each coating material used during the 12-month compliance period does not exceed 0.046 kg HAP per liter solids, as purchased. Paragraph (a) of this section.
2. Use of “as applied” compliant coatings	<p>a. Each coating material used does not exceed 0.046 kg HAP per liter solids on a rolling 12-month average as applied basis, determined monthly. Paragraphs (b)(1) of this section; or</p> <p>b. Average of all coating materials used does not exceed 0.046 kg HAP per liter solids on a rolling 12-month average as applied basis, determined monthly. Paragraph (b)(2) of this section.</p> <p>Overall organic HAP control efficiency is at least 98 percent on a monthly basis for individual or groups of coil coating lines; or overall organic HAP control efficiency is at least 98 percent during performance tests conducted according to Table 1 to § 63.5170 and operating limits are achieved continuously for individual coil coating lines; or oxidizer outlet HAP concentration is no greater than 20 ppmv and there is 100-percent capture efficiency during performance tests conducted according to Table 1 to § 63.5170 and operating limits are achieved continuously for individual coil coating lines. Paragraph (c) of this section.</p>
3. Use of a capture system and control device	Overall organic HAP control efficiency is at least 98 percent on a monthly basis for individual or groups of coil coating lines; or overall organic HAP control efficiency is at least 98 percent during performance tests conducted according to Table 1 to § 63.5170 and operating limits are achieved continuously for individual coil coating lines; or oxidizer outlet HAP concentration is no greater than 20 ppmv and there is 100-percent capture efficiency during performance tests conducted according to Table 1 to § 63.5170 and operating limits are achieved continuously for individual coil coating lines. Paragraph (c) of this section.
4. Use of a combination of compliant coatings and control devices and maintaining an acceptable equivalent emission rate	Average equivalent emission rate does not exceed 0.046 kg HAP per liter solids on a rolling 12-month average as applied basis, determined monthly. Paragraph (d) of this section.

(a) *As-purchased compliant coatings.* If you elect to use coatings that individually meet the organic HAP emission limit in [§ 63.5120\(a\)\(2\)](#) as-purchased, to which you will not add HAP during distribution or application, you must demonstrate that each coating material applied

during the 12-month compliance period contains no more than 0.046 kg HAP per liter of solids on an as-purchased basis.

(1) Determine the organic HAP content for each coating material in accordance with [§ 63.5160\(b\)](#) and the volume solids content in accordance with [§ 63.5160\(c\)](#).

(2) Combine these results using Equation 1 of this section and compare the result to the organic HAP emission limit in [§ 63.5120\(a\)\(2\)](#) to demonstrate that each coating material contains no more organic HAP than the limit.

$$H_{\text{siap}} = \frac{C_{\text{hi}} D_i}{V_{\text{si}}} \quad (\text{Eq. 1})$$

Where:

H_{siap} = as-purchased, organic HAP to solids ratio of coating material, i, kg organic HAP/liter solids applied.

C_{hi} = organic HAP content of coating material, i, expressed as a weight-fraction, kg/kg.

D_i = density of coating material, i, kg/l.

V_{si} = volume fraction of solids in coating, i, l/l.

(b) ***As-applied compliant coatings.*** If you choose to use “as-applied” compliant coatings, you must demonstrate that the average of each coating material applied during the 12-month compliance period contains no more than 0.046 kg of organic HAP per liter of solids applied in accordance with (b)(1) of this section, or demonstrate that the average of all coating materials applied during the 12-month compliance period contain no more than 0.046 kg of organic HAP per liter of solids applied in accordance with [paragraph \(b\)\(2\)](#) of this section.

(1) To demonstrate that the average organic HAP content on the basis of solids applied for each coating material applied, $H_{\text{Si yr}}$, is less than 0.046 kg HAP per liter solids applied for the 12-month compliance period, use Equation 2 of this section:

$$H_{\text{Si yr}} = \frac{\sum_{y=1}^{12} \left[V_i D_i C_{\text{ahi}} + \sum_{i=1}^q V_j D_j C_{\text{hij}} \right]}{\sum_{y=1}^{12} V_i V_{\text{si}}} \quad (\text{Eq. 2})$$

Where:

$H_{si\ yr}$ = average for the 12-month compliance period, as-applied, organic HAP to solids ratio of material, i, kg organic HAP/liter solids applied.

V_i = volume of coating material, i, l.

D_i = density of coating material, i, kg/l.

C_{ahi} = monthly average, as-applied, organic HAP content of solids-containing coating material, i, expressed as a weight fraction, kilogram (kg)/kg.

V_j = volume of solvent, j, l.

D_j = density of solvent, j, kg/l.

C_{hij} = organic HAP content of solvent, j, added to coating material, i, expressed as a weight fraction, kg/kg.

V_{si} = volume fraction of solids in coating, i, l/l.

y = identifier for months.

q = number of different solvents, thinners, reducers, diluents, or other non-solids-containing coating materials applied in a month.

(2) To demonstrate that the average organic HAP content on the basis of solids applied, $H_{S\ yr}$, of all coating materials applied is less than 0.046 kg HAP per liter solids applied for the 12-month compliance period, use Equation 3 of this section:

$$H_{S\ yr} = \frac{\sum_{y=1}^{12} \left[\sum_{i=1}^p V_i D_i C_{ahi} + \sum_{j=1}^q V_j D_j C_{hij} \right]}{\sum_{y=1}^{12} \left[\sum_{i=1}^p V_i V_{si} \right]} \quad (\text{Eq. 3})$$

Where:

$H_{S\ yr}$ = average for the 12-month compliance period, as-applied, organic HAP to solids ratio of all materials applied, kg organic HAP/liter solids applied.

V_i = volume of coating material, i, l.

D_i = density of coating material, i, kg/l.

C_{ahi} = monthly average, as-applied, organic HAP content of solids-containing coating material, i, expressed as a weight fraction, kilogram (kg)/kg.

V_j = volume of solvent, j, l.

D_j = density of solvent, j, kg/l.

C_{hij} = organic HAP content of solvent, j, added to coating material, i, expressed as a weight fraction, kg/kg.

V_{si} = volume fraction of solids in coating, i, l/l.

p = number of different coating materials applied in a month.

q = number of different solvents, thinners, reducers, diluents, or other non-solids-containing coating materials applied in a month.

y = identifier for months.

(c) **Capture and control to reduce emissions to no more than the allowable limit.** If you use one or more capture systems and one or more control devices and demonstrate an average overall organic HAP control efficiency of at least 98 percent for each month to comply with [§ 63.5120\(a\)\(1\)](#); or operate a capture system and oxidizer so that the capture efficiency is 100 percent and the oxidizer outlet HAP concentration is no greater than 20 ppmv on a dry basis to comply with [§ 63.5120\(a\)\(3\)](#), you must follow one of the procedures in [paragraphs \(c\)\(1\)](#) through [\(4\)](#) of this section. Alternatively, you may demonstrate compliance for an individual coil coating line by operating its capture system and control device and continuous parameter monitoring system according to the procedures in [paragraph \(i\)](#) of this section.

(1) If the affected source uses one compliance procedure to limit organic HAP emissions to the level specified in [§ 63.5120\(a\)\(1\)](#) or [\(3\)](#) and has only always-controlled work stations, then you must demonstrate compliance with the provisions of [paragraph \(e\)](#) of this section when emissions from the affected source are controlled by one or more solvent recovery devices.

(2) If the affected source uses one compliance procedure to limit organic HAP emissions to the level specified in [§ 63.5120\(a\)\(1\)](#) or [\(3\)](#) and has only always-controlled work stations, then you must demonstrate compliance with the provisions of [paragraph \(f\)](#) of this section when emissions are controlled by one or more oxidizers.

(3) If the affected source operates both solvent recovery and oxidizer control devices, one or more never-controlled work stations, or one or more intermittently-controllable work stations, or uses more than one compliance procedure, then you must demonstrate compliance with the provisions of [paragraph \(g\)](#) of this section.

(4) The method of limiting organic HAP emissions to the level specified in [§ 63.5120\(a\)\(3\)](#) is the installation and operation of a PTE around each work station and associated curing oven in the coating line and the ventilation of all organic HAP emissions from each PTE to an oxidizer with an outlet organic HAP concentration of no greater than 20 ppmv on a dry basis. An enclosure that meets the requirements in [§ 63.5160\(e\)\(1\)](#) is considered a PTE. Compliance of the oxidizer with the outlet organic HAP concentration limit is demonstrated either through continuous emission monitoring according to [paragraph \(c\)\(4\)\(ii\)](#) of this section or through performance tests according to the requirements of [§ 63.5160\(d\)](#) and Table 1 to [§ 63.5160](#). If this method is selected, you must meet the requirements of [paragraph \(c\)\(4\)\(i\)](#) of this section to demonstrate continuing achievement of 100 percent capture of organic HAP emissions and either [paragraph \(c\)\(4\)\(ii\)](#) or [paragraph \(c\)\(4\)\(iii\)](#) of this section, respectively, to demonstrate continuous compliance with the oxidizer outlet organic HAP concentration limit through continuous emission monitoring or continuous operating parameter monitoring:

(i) Whenever a work station is operated, continuously monitor the capture system operating parameter established in accordance with [§ 63.5150\(a\)\(4\)](#).

(ii) To demonstrate that the value of the exhaust gas organic HAP concentration at the outlet of the oxidizer is no greater than 20 ppmv, on a dry basis, install, calibrate, operate, and maintain CEMS according to the requirements of [§ 63.5150\(a\)\(2\)](#).

(iii) To demonstrate continuous compliance with operating limits established in accordance with [§ 63.5150\(a\)\(3\)](#), whenever a work station is operated, continuously monitor the applicable oxidizer operating parameter.

(d) **Capture and control to achieve the emission rate limit.** If you use one or more capture systems and one or more control devices and limit the organic HAP emission rate to no more than 0.046 kg organic HAP emitted per liter of solids applied on a 12-month average as-applied basis, then you must follow one of the procedures in [paragraphs \(d\)\(1\)](#) through [\(3\)](#) of this section.

(1) If you use one or more solvent recovery devices, you must demonstrate compliance with the provisions in [paragraph \(e\)](#) of this section.

(2) If you use one or more oxidizers, you must demonstrate compliance with the provisions in [paragraph \(f\)](#) of this section.

(3) If you use both solvent recovery devices and oxidizers, or operate one or more never-controlled work stations or one or more intermittently controllable work stations, you must demonstrate compliance with the provisions in [paragraph \(g\)](#) of this section.

(e) **Use of solvent recovery to demonstrate compliance.** If you use one or more solvent recovery devices to control emissions from always-controlled work stations, you must show compliance by following the procedures in either [paragraph \(e\)\(1\)](#) or [\(2\)](#) of this section:

(1) **Liquid-liquid material balance.** Perform a liquid-liquid material balance for each month as specified in [paragraphs \(e\)\(1\)\(i\)](#) through [\(vi\)](#) of this section and use Equations 4 through 6 of this section to convert the data to units of this standard. All determinations of quantity of coating and composition of coating must be made at a time and location in the process after all ingredients (including any dilution solvent) have been added to the coating, or appropriate adjustments must be made to account for any ingredients added after the amount of coating has been determined.

(i) Measure the mass of each coating material applied on the work station or group of work stations controlled by one or more solvent recovery devices during the month.

(ii) If demonstrating compliance with the organic HAP emission rate based on solids applied, determine the organic HAP content of each coating material applied during the month following the procedure in [§ 63.5160\(b\)](#).

(iii) Determine the volatile matter content of each coating material applied during the month following the procedure in [§ 63.5160\(c\)](#).

(iv) If demonstrating compliance with the organic HAP emission rate based on solids applied, determine the solids content of each coating material applied during the month following the procedure in [§ 63.5160\(c\)](#).

(v) For each solvent recovery device used to comply with [§ 63.5120\(a\)](#), install, calibrate, maintain, and operate according to the manufacturer's specifications, a device that indicates the cumulative amount of volatile matter recovered by the solvent recovery device on a monthly basis. The device must be initially certified by the manufacturer to be accurate to within ± 2.0 percent.

(vi) For each solvent recovery device used to comply with [§ 63.5120\(a\)](#), measure the amount of volatile matter recovered for the month.

(vii) **Recovery efficiency, R_v .** Calculate the volatile organic matter collection and recovery efficiency, R_v , using Equation 4 of this section:

$$R_v = 100 \frac{\sum_{k=1}^s M_{kvr}}{\sum_{i=1}^p M_i C_{vi} + \sum_{j=1}^q M_j} \quad (\text{Eq. 4})$$

Where:

R_v = organic volatile matter collection and recovery efficiency, percent.

M_{kvr} = mass of volatile matter recovered in a month by solvent recovery device, k, kg.

M_i = mass of coating material, i, applied in a month, kg.

C_{vi} = volatile matter content of coating material, i, expressed as a weight fraction, kg/kg.

M_j = mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material (excluding H_2O), j, applied in a month, kg.

p = number of different coating materials applied in a month.

q = number of different solvents, thinners, reducers, diluents, or other non-solids-containing coating materials applied in a month.

s = number of solvent recovery devices used to comply with the standard of [§ 63.5120 of this subpart](#), in the facility.

(viii) **Organic HAP emitted, H_e** . Calculate the mass of organic HAP emitted during the month, H_e , using Equation 5 of this section:

$$H_e = \left[1 - \frac{R_v}{100} \right] \left[\sum_{i=1}^p \left(C_{hi} M_i + \sum_{j=1}^q C_{hij} M_{ij} \right) \right] \quad (\text{Eq. 5})$$

Where:

H_e = total monthly organic HAP emitted, kg.

R_v = organic volatile matter collection and recovery efficiency, percent.

C_{hi} = organic HAP content of coating material, i, expressed as a weight-fraction, kg/kg.

M_i = mass of coating material, i, applied in a month, kg.

C_{hij} = organic HAP content of solvent, j, added to coating material, i, expressed as a weight fraction, kg/kg.

M_{ij} = mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material, j, added to solids-containing coating material, i, in a month, kg.

p = number of different coating materials applied in a month.

q = number of different solvents, thinners, reducers, diluents, or other non-solids-containing coating materials applied in a month.

(ix) **Organic HAP emission rate based on solids applied for the 12-month compliance period, L_{ANNUAL} .** Calculate the organic HAP emission rate based on solids applied for the 12-month compliance period, L_{ANNUAL} , using Equation 6 of this section:

$$L_{\text{ANNUAL}} = \frac{\sum_{y=1}^{12} H_e}{\sum_{y=1}^{12} \left[\sum_{i=1}^p C_{si} M_i \right]} \quad (\text{Eq. 6})$$

Where:

L_{ANNUAL} = mass organic HAP emitted per volume of solids applied for the 12-month compliance period, kg/liter.

H_e = total monthly organic HAP emitted, kg.

C_{si} = solids content of coating material, i , expressed as liter of solids/kg of material.

M_i = mass of coating material, i , applied in a month, kg.

y = identifier for months.

p = number of different coating materials applied in a month.

(x) **Compare actual performance to performance required by compliance option.** The affected source is in compliance with [§ 63.5120\(a\)](#) if it meets the requirement in either [paragraph \(e\)\(1\)\(x\)\(A\)](#) or [\(B\)](#) of this section:

(A) The average volatile organic matter collection and recovery efficiency, R_v , is 98 percent or greater each month of the 12-month compliance period; or

(B) The organic HAP emission rate based on solids applied for the 12-month compliance period, L_{ANNUAL} , is 0.046 kg organic HAP per liter solids applied or less.

(2) **Continuous emission monitoring of control device performance.** Use continuous emission monitors to demonstrate recovery efficiency, conduct performance tests of capture efficiency and volumetric flow rate, and continuously monitor a site specific operating parameter to ensure that capture efficiency and volumetric flow rate are maintained following the procedures in [paragraphs \(e\)\(2\)\(i\)](#) through [\(xi\)](#) of this section:

(i) **Control device destruction or removal efficiency, DRE.** For each control device used to comply with [§ 63.5120\(a\)](#), continuously monitor the gas stream entering and exiting the

control device to determine the total volatile organic matter mass flow rate (e.g., by determining the concentration of the vent gas in grams per cubic meter and the volumetric flow rate in cubic meters per second, such that the total volatile organic matter mass flow rate in grams per second can be calculated using Equation 1 of [§ 63.5160](#), and the percent destruction or removal efficiency, DRE, of the control device can be calculated for each month using Equation 2 of [§ 63.5160](#).

(ii) Determine the percent capture efficiency, CE, for each work station in accordance with [§ 63.5160\(e\)](#).

(iii) **Capture efficiency monitoring.** Whenever a work station is operated, continuously monitor the operating parameter established in accordance with [§ 63.5150\(a\)\(4\)](#).

(iv) **Control efficiency, R.** Calculate the overall organic HAP control efficiency, R, achieved for each month using Equation 7 of this section:

$$R = 100 \frac{\sum_{A=1}^w \left[(\text{DRE}_K \text{CE}_A) \left(\sum_{i=1}^p M_{Ai} C_{vi} + \sum_{j=1}^q M_{Aj} \right) \right]}{\sum_{i=1}^p M_i C_{vi} + \sum_{j=1}^q M_j} \quad (\text{Eq. 7})$$

Where:

R = overall organic HAP control efficiency, percent.

DRE_k = organic volatile matter destruction or removal efficiency of control device, k, percent.

CE_A = organic volatile matter capture efficiency of the capture system for work station, A, percent.

M_{Ai} = mass of coating material, i, applied on work station, A, in a month, kg.

C_{vi} = volatile matter content of coating material, i, expressed as a weight fraction, kg/kg.

M_{Aj} = mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material (including H_2O), j, applied on work station, A, in a month, kg.

M_i = mass of coating material, i, applied in a month, kg.

M_j = mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material (excluding H_2O), j, applied in a month, kg.

w = number of always-controlled work stations in the facility.

p = number of different coating materials applied in a month.

q = number of different solvents, thinners, reducers, diluents, or other non-solids-containing coating materials applied in a month.

(v) If demonstrating compliance with the organic HAP emission rate based on solids applied, measure the mass of each coating material applied on each work station during the month.

(vi) If demonstrating compliance with the organic HAP emission rate based on solids applied, determine the organic HAP content of each coating material applied during the month in accordance with [§ 63.5160\(b\)](#).

(vii) If demonstrating compliance with the organic HAP emission rate based on solids applied, determine the solids content of each coating material applied during the month in accordance with [§ 63.5160\(c\)](#).

(viii) If demonstrating compliance with the organic HAP emission rate based on solids applied, calculate the organic HAP emitted during the month, H_e , for each month using Equation 8 of this section:

$$H_e = \sum_{A=1}^w \left[\left(1 - (\text{DRE}_k \text{CE}_A) \left(\sum_{i=1}^p \left(C_{hi} M_{Ai} + \sum_{j=1}^q C_{hij} M_{Aij} \right) \right) \right) \right] \quad (\text{Eq. 8})$$

Where:

H_e = total monthly organic HAP emitted, kg.

DRE_k = organic volatile matter destruction or removal efficiency of control device, k, percent.

CE_A = organic volatile matter capture efficiency of the capture system for work station, A, percent.

C_{hi} = organic HAP content of coating material, i, expressed as a weight-fraction, kg/kg.

M_{Ai} = mass of coating material, i, applied on work station, A, in a month, kg.

C_{hij} = organic HAP content of solvent, j, added to coating material, i, expressed as a weight fraction, kg/kg.

M_{Aij} = mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material, j, added to solids-containing coating material, i, applied on work station, A, in a month, kg.

w = number of always-controlled work stations in the facility.

p = number of different coating materials applied in a month.

q = number of different solvents, thinners, reducers, diluents, or other non-solids-containing coating materials applied in a month.

(ix) **Organic HAP emission rate based on solids applied for the 12-month compliance period, L_{ANNUAL} .** Calculate the organic HAP emission rate based on solids applied for the 12-month compliance period, L_{ANNUAL} , using Equation 6 of this section.

(x) **Compare actual performance to performance required by compliance option.** The affected source is in compliance with [§ 63.5120\(a\)](#) if each capture system operating parameter is operated at an average value greater than or less than (as appropriate) the operating parameter value established in accordance with [§ 63.5150](#) for each 3-hour period; and

(A) The overall organic HAP control efficiency, R, is 98 percent or greater for each; or

(B) The organic HAP emission rate based on solids applied for the 12-month compliance period, L_{ANNUAL} , is 0.046 kg organic HAP per liter solids applied or less.

(f) **Use of oxidation to demonstrate compliance.** If you use one or more oxidizers to control emissions from always controlled work stations, you must follow the procedures in either [paragraph \(f\)\(1\)](#) or [\(2\)](#) of this section:

(1) **Continuous monitoring of capture system and control device operating parameters.** Demonstrate compliance through performance tests of capture efficiency and control device efficiency and continuous monitoring of capture system and control device operating parameters as specified in [paragraphs \(f\)\(1\)\(i\)](#) through [\(xi\)](#) of this section:

(i) For each oxidizer used to comply with [§ 63.5120\(a\)](#), determine the oxidizer destruction or removal efficiency, DRE, using the procedure in [§ 63.5160\(d\)](#).

(ii) Whenever a work station is operated, continuously monitor the operating parameter established in accordance with [§ 63.5150\(a\)\(3\)](#).

(iii) Determine the capture system capture efficiency, CE, for each work station in accordance with [§ 63.5160\(e\)](#).

(iv) Whenever a work station is operated, continuously monitor the operating parameter established in accordance with [§ 63.5150\(a\)\(4\)](#).

(v) Calculate the overall organic HAP control efficiency, R , achieved using Equation 7 of this section.

(vi) If demonstrating compliance with the organic HAP emission rate based on solids applied, measure the mass of each coating material applied on each work station during the month.

(vii) If demonstrating compliance with the organic HAP emission rate based on solids applied, determine the organic HAP content of each coating material applied during the month following the procedure in [§ 63.5160\(b\)](#).

(viii) If demonstrating compliance with the organic HAP emission rate based on solids applied, determine the solids content of each coating material applied during the month following the procedure in [§ 63.5160\(c\)](#).

(ix) Calculate the organic HAP emitted during the month, H_e , for each month:

(A) For each work station and its associated oxidizer, use Equation 8 of this section.

(B) For periods when the oxidizer has not operated within its established operating limit, the control device efficiency is determined to be zero.

(x) ***Organic HAP emission rate based on solids applied for the 12-month compliance period, L_{ANNUAL}*** . If demonstrating compliance with the organic HAP emission rate based on solids applied for the 12-month compliance period, calculate the organic HAP emission rate based on solids applied, L_{ANNUAL} , for the 12-month compliance period using Equation 6 of this section.

(xi) ***Compare actual performance to performance required by compliance option***. The affected source is in compliance with [§ 63.5120\(a\)](#) if each oxidizer is operated such that the average operating parameter value is greater than the operating parameter value established in [§ 63.5150\(a\)\(3\)](#) for each 3-hour period, and each capture system operating parameter average value is greater than or less than (as appropriate) the operating parameter value established in [§ 63.5150\(a\)\(4\)](#) for each 3-hour period; and the requirement in either [paragraph \(f\)\(1\)\(xi\)\(A\)](#) or [\(B\)](#) of this section is met.

(A) The overall organic HAP control efficiency, R , is 98 percent or greater for each; or

(B) The organic HAP emission rate based on solids applied, L_{ANNUAL} , is 0.046 kg organic HAP per liter solids applied or less for the 12-month compliance period.

(2) ***Continuous emission monitoring of control device performance***. Use continuous emission monitors, conduct performance tests of capture efficiency, and continuously monitor a site specific operating parameter to ensure that capture efficiency is maintained. Compliance must be demonstrated in accordance with [paragraph \(e\)\(2\)](#) of this section.

(g) **Combination of capture and control.** You must demonstrate compliance according to the procedures in [paragraphs \(g\)\(1\)](#) through [\(8\)](#) of this section if both solvent recovery and oxidizer control devices, one or more never controlled coil coating stations, or one or more intermittently controllable coil coating stations are operated; or more than one compliance procedure is used.

(1) Solvent recovery system using liquid/liquid material balance compliance

demonstration. For each solvent recovery system used to control one or more work stations for which you choose to comply by means of a liquid-liquid material balance, you must determine the organic HAP emissions each month of the 12-month compliance period for those work stations controlled by that solvent recovery system according to either [paragraph \(g\)\(1\)\(i\)](#) or [\(ii\)](#) of this section:

(i) In accordance with [paragraphs \(e\)\(1\)\(i\)](#) through [\(iii\)](#) and [\(e\)\(1\)\(v\)](#) through [\(viii\)](#) of this section if the work stations controlled by that solvent recovery system are only always-controlled work stations; or

(ii) In accordance with [paragraphs \(e\)\(1\)\(ii\)](#) through [\(iii\)](#), [\(e\)\(1\)\(v\)](#) through [\(vi\)](#), and [\(h\)](#) of this section if the work stations controlled by that solvent recovery system include one or more never-controlled or intermittently-controllable work stations.

(2) Solvent recovery system using performance test and continuous monitoring compliance

demonstration. For each solvent recovery system used to control one or more coil coating stations for which you choose to comply by means of performance testing of capture efficiency, continuous emission monitoring of the control device, and continuous monitoring of a capture system operating parameter, each month of the 12-month compliance period you must meet the requirements of [paragraphs \(g\)\(2\)\(i\)](#) and [\(ii\)](#) of this section:

(i) For each capture system delivering emissions to that solvent recovery system, monitor an operating parameter established in [§ 63.5150\(a\)\(4\)](#) to ensure that capture system efficiency is maintained; and

(ii) Determine the organic HAP emissions for those work stations served by each capture system delivering emissions to that solvent recovery system according to either [paragraph \(g\)\(2\)\(ii\)\(A\)](#) or [\(B\)](#) of this section:

(A) In accordance with [paragraphs \(e\)\(2\)\(i\)](#) through [\(iii\)](#) and [\(e\)\(2\)\(v\)](#) through [\(viii\)](#) of this section if the work stations served by that capture system are only always-controlled coil coating stations; or

(B) In accordance with [paragraphs \(e\)\(2\)\(i\)](#) through [\(iii\)](#), [\(e\)\(2\)\(v\)](#) through [\(vii\)](#), and [\(h\)](#) of this section if the work stations served by that capture system include one or more never-controlled or intermittently-controllable work stations.

(3) Oxidizer using performance tests and continuous monitoring of operating parameters compliance demonstration. For each oxidizer used to control emissions from one or more

work stations for which you choose to demonstrate compliance through performance tests of capture efficiency, control device efficiency, and continuous monitoring of capture system and control device operating parameters, each month of the 12-month compliance period you must meet the requirements of [paragraphs \(g\)\(3\)\(i\)](#) through [\(iii\)](#) of this section:

(i) Monitor an operating parameter established in [§ 63.5150\(a\)\(3\)](#) to ensure that control device destruction or removal efficiency is maintained; and

(ii) For each capture system delivering emissions to that oxidizer, monitor an operating parameter established in [§ 63.5150\(a\)\(4\)](#) to ensure capture efficiency; and

(iii) Determine the organic HAP emissions for those work stations served by each capture system delivering emissions to that oxidizer according to either [paragraph \(g\)\(3\)\(iii\)\(A\)](#) or [\(B\)](#) of this section:

(A) In accordance with [paragraphs \(f\)\(1\)\(i\)](#) through [\(v\)](#) and [\(ix\)](#) of this section if the work stations served by that capture system are only always-controlled work stations; or

(B) In accordance with [paragraphs \(f\)\(1\)\(i\)](#) through [\(v\)](#), [\(ix\)](#), and [\(h\)](#) of this section if the work stations served by that capture system include one or more never-controlled or intermittently-controllable work stations.

(4) ***Oxidizer using continuous emission monitoring compliance demonstration.*** For each oxidizer used to control emissions from one or more work stations for which you choose to demonstrate compliance through capture efficiency testing, continuous emission monitoring of the control device, and continuous monitoring of a capture system operating parameter, each month of the 12-month compliance period you must meet the requirements in [paragraphs \(g\)\(4\)\(i\)](#) and [\(ii\)](#) of this section:

(i) For each capture system delivering emissions to that oxidizer, monitor an operating parameter established in [§ 63.5150\(a\)\(4\)](#) to ensure capture efficiency; and

(ii) Determine the organic HAP emissions for those work stations served by each capture system delivering emissions to that oxidizer according to either [paragraph \(g\)\(4\)\(ii\)\(A\)](#) or [\(B\)](#) of this section:

(A) In accordance with [paragraphs \(e\)\(2\)\(i\)](#) through [\(iii\)](#) and [\(e\)\(2\)\(v\)](#) through [\(viii\)](#) of this section if the work stations served by that capture system are only always-controlled work stations; or

(B) In accordance with [paragraphs \(e\)\(2\)\(i\)](#) through [\(iii\)](#), [\(e\)\(2\)\(v\)](#) through [\(vii\)](#), and [\(h\)](#) of this section if the work stations served by that capture system include one or more never-controlled or intermittently-controllable work stations.

(5) ***Uncontrolled work stations.*** For uncontrolled work stations, each month of the 12-month compliance period you must determine the organic HAP applied on those work stations using

Equation 9 of this section. The organic HAP emitted from an uncontrolled work station is equal to the organic HAP applied on that work station:

$$H_m = \sum_{A=1}^x \left(\sum_{i=1}^p C_{hi} M_{Ai} + \sum_{j=1}^q C_{hij} M_{Aij} \right) \quad (\text{Eq. 9})$$

Where:

H_m = facility total monthly organic HAP applied on uncontrolled coil coating stations, kg.

C_{hi} = organic HAP content of coating material, i, expressed as a weight-fraction, kg/kg.

M_{Ai} = mass of coating material, i, applied on work station, A, in a month, kg.

C_{hij} = organic HAP content of solvent, j, added to coating material, i, expressed as a weight fraction, kg/kg.

M_{Aij} = mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material, j, added to solids-containing coating material, i, applied on work station, A, in a month, kg.

x = number of uncontrolled work stations in the facility.

p = number of different coating materials applied in a month.

q = number of different solvents, thinners, reducers, diluents, or other non-solids-containing coating materials applied in a month.

(6) If demonstrating compliance with the organic HAP emission rate based on solids applied, each month of the 12-month compliance period you must determine the solids content of each coating material applied during the month following the procedure in [§ 63.5160\(c\)](#).

(7) **Organic HAP emitted.** You must determine the organic HAP emissions for the affected source for each 12-month compliance period by summing all monthly organic HAP emissions calculated according to [paragraphs \(g\)\(1\), \(g\)\(2\)\(ii\), \(g\)\(3\)\(iii\), \(g\)\(4\)\(ii\), and \(g\)\(5\)](#) of this section.

(8) **Compare actual performance to performance required by compliance option.** The affected source is in compliance with [§ 63.5120\(a\)](#) for the 12-month compliance period if all operating parameters required to be monitored under [paragraphs \(g\)\(2\) through \(4\)](#) of this section were maintained at the values established in [§ 63.5150](#); and it meets the requirement in either [paragraph \(g\)\(8\)\(i\)](#) or [\(ii\)](#) of this section.

(i) The total mass of organic HAP emitted by the affected source was not more than 0.046 kg HAP per liter of solids applied for the 12-month compliance period; or

(ii) The total mass of organic HAP emitted by the affected source was not more than 2 percent of the total mass of organic HAP applied by the affected source each month. You must determine the total mass of organic HAP applied by the affected source in each month of the 12-month compliance period using Equation 9 of this section.

(h) **Organic HAP emissions from intermittently-controllable or never-controlled coil coating stations.** If you have been expressly referenced to this paragraph by [paragraphs \(g\)\(1\)\(ii\), \(g\)\(2\)\(ii\)\(B\), \(g\)\(3\)\(iii\)\(B\), or \(g\)\(4\)\(ii\)\(B\)](#) of this section for calculation procedures to determine organic HAP emissions, you must for your intermittently-controllable or never-controlled work stations meet the requirements of [paragraphs \(h\)\(1\) through \(6\)](#) of this section:

(1) Determine the sum of the mass of all solids-containing coating materials which are applied on intermittently-controllable work stations in bypass mode, and the mass of all solids-containing coating materials which are applied on never-controlled coil coating stations during each month of the 12-month compliance period, M_{Bi} .

(2) Determine the sum of the mass of all solvents, thinners, reducers, diluents, and other nonsolids-containing coating materials which are applied on intermittently-controllable work stations in bypass mode, and the mass of all solvents, thinners, reducers, diluents and other nonsolids-containing coating materials which are applied on never-controlled work stations during each month of the 12-month compliance period, M_{Bj} .

(3) Determine the sum of the mass of all solids-containing coating materials which are applied on intermittently-controllable work stations in controlled mode, and the mass of all solids-containing coating materials which are applied on always-controlled work stations during each month of the 12-month compliance period, M_{Ci} .

(4) Determine the sum of the mass of all solvents, thinners, reducers, diluents, and other nonsolids-containing coating materials which are applied on intermittently-controllable work stations in controlled mode, and the mass of all solvents, thinners, reducers, diluents, and other nonsolids-containing coating materials which are applied on always-controlled work stations during each month of the 12-month compliance period, M_{Cj} .

(5) **Liquid-liquid material balance calculation of HAP emitted.** For each work station or group of work stations for which you use the provisions of [paragraph \(g\)\(1\)\(ii\)](#) of this section, you must calculate the organic HAP emitted during the month using Equation 10 of this section:

$$H_e = \left[\sum_{i=1}^p M_{Ci} C_{hi} + \sum_{j=1}^q M_{Cj} C_{hj} \right] \left[1 - \frac{\sum_{k=1}^s M_{kvr}}{\sum_{i=1}^p M_{Ci} C_{vi} + \sum_{j=1}^q M_{Cj}} \right] + \left[\sum_{i=1}^p M_{Bi} C_{hi} + \sum_{j=1}^q M_{Bj} C_{hj} \right]$$

Where:

H_e = total monthly organic HAP emitted, kg.

M_{ci} = sum of the mass of solids-containing coating material, i, applied on intermittently-controllable work stations operating in controlled mode and the mass of solids-containing coating material, i, applied on always-controlled work stations, in a month, kg.

C_{hi} = organic HAP content of coating material, i, expressed as a weight-fraction, kg/kg.

M_{cj} = sum of the mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material, j, applied on intermittently-controllable work stations operating in controlled mode and the mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material, j, applied on always-controlled work stations in a month, kg.

C_{hj} = organic HAP content of solvent, j, expressed as a weight fraction, kg/kg.

M_{kvr} = mass of volatile matter recovered in a month by solvent recovery device, k, kg.

C_{vi} = volatile matter content of coating material, i, expressed as a weight fraction, kg/kg.

M_{Bi} = sum of the mass of solids-containing coating material, i, applied on intermittently-controllable work stations operating in bypass mode and the mass of solids-containing coating material, i, applied on never-controlled work stations, in a month, kg.

M_{Bj} = sum of the mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material, j, applied on intermittently-controllable work stations operating in bypass mode and the mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material, j, applied on never-controlled work stations, in a month, kg.

p = number of different coating materials applied in a month.

q = number of different solvents, thinners, reducers, diluents, or other non-solids-containing coating materials applied in a month.

s = number of solvent recovery devices used to comply with the standard of [§ 63.5120 of this subpart](#), in the facility.

(6) Control efficiency calculation of HAP emitted. For each work station or group of work stations for which you use the provisions of [paragraphs \(g\)\(2\)\(ii\)\(B\), \(g\)\(3\)\(iii\)\(B\), or \(g\)\(4\)\(ii\)\(B\)](#) of this section, you must calculate the organic HAP emitted during the month, H_e , using Equation 11 of this section:

$$He = \sum_{A=1}^{w_i} \left[\left(\sum_{i=1}^p M_{ci} C_{hi} + \sum_{j=1}^q M_{cj} C_{hj} \right) (1 - DRE_k CE_A) \right] + \left[\sum_{i=1}^p M_{Bi} C_{hi} + \sum_{j=1}^q M_{Bj} C_{hj} \right]$$

Where:

H_e = total monthly organic HAP emitted, kg.

M_{ci} = sum of the mass of solids-containing coating material, i, applied on intermittently-controllable work stations operating in controlled mode and the mass of solids-containing coating material, i, applied on always-controlled work stations, in a month, kg.

C_{hi} = organic HAP content of coating material, i, expressed as a weight-fraction, kg/kg.

M_{cj} = sum of the mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material, j, applied on intermittently-controllable work stations operating in controlled mode and the mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material, j, applied on always-controlled work stations in a month, kg.

C_{hj} = organic HAP content of solvent, j, expressed as a weight fraction, kg/kg.

DRE_k = organic volatile matter destruction or removal efficiency of control device, k, percent.

CE_A = organic volatile matter capture efficiency of the capture system for work station, A, percent.

M_{Bi} = sum of the mass of solids-containing coating material, i, applied on intermittently-controllable work stations operating in bypass mode and the mass of solids-containing coating material, i, applied on never-controlled work stations, in a month, kg.

M_{Bj} = sum of the mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material, j, applied on intermittently-controllable work stations operating in bypass mode and the mass of solvent, thinner, reducer, diluent, or other non-solids-containing coating material, j, applied on never-controlled work stations, in a month, kg.

w_i = number of intermittently-controllable work stations in the facility.

p = number of different coating materials applied in a month.

q = number of different solvents, thinners, reducers, diluents, or other non-solids-containing coating materials applied in a month.

(i) **Capture and control system compliance demonstration procedures using a CPMS for a coil coating line.** If you use an add-on control device, to demonstrate compliance for each capture system and each control device through performance tests and continuous monitoring

of capture system and control device operating parameters, you must meet the requirements in [paragraphs \(i\)\(1\)](#) through [\(3\)](#) of this section.

(1) Conduct performance tests according to the schedule in Table 1 to [§ 63.5160](#) to determine the control device destruction or removal efficiency, DRE, according to [§ 63.5160\(d\)](#) and Table 1 to [§ 63.5160](#).

(2) Determine the emission capture efficiency, CE, in accordance with [§ 63.5160\(e\)](#).

(3) Whenever a coil coating line is operated, continuously monitor the operating parameters established according to [§ 63.5150\(a\)\(3\)](#) and

(4) to ensure capture and control efficiency.

[[67 FR 39812](#), June 10, 2002, as amended at [85 FR 10864](#), Feb. 25, 2020]

Reporting and Recordkeeping

§ 63.5180 What reports must I submit?

(a) Submit the reports specified in [paragraphs \(b\)](#) through [\(i\)](#) of this section to the EPA Regional Office that serves the State or territory in which the affected source is located and to the delegated State agency:

(b) You must submit an initial notification required in [§ 63.9\(b\)](#).

(1) Submit an initial notification for an existing source no later than 2 years after June 10, 2002, or no later than 120 days after the source becomes subject to this subpart, whichever is later.

(2) Submit an initial notification for a new or reconstructed source as required by [§ 63.9\(b\)](#).

(3) For the purpose of this subpart, a title V permit application may be used in lieu of the initial notification required under [§ 63.9\(b\)](#), provided the same information is contained in the permit application as required by [§ 63.9\(b\)](#), and the State to which the permit application has been submitted has an approved operating permit program under [part 70 of this chapter](#) and has received delegation of authority from the EPA.

(4) Submit a title V permit application used in lieu of the initial notification required under [§ 63.9\(b\)](#) by the same due dates as those specified in [paragraphs \(b\)\(1\)](#) and [\(2\)](#) of this section for the initial notifications.

(c) You must submit a Notification of Performance Test as specified in [§§ 63.7](#) and [63.9\(e\)](#) if you are complying with the emission standard using a control device. This notification and the site-specific test plan required under [§ 63.7\(c\)\(2\)](#) must identify the operating parameter to be monitored to ensure that the capture efficiency measured during the performance test is

maintained. You may consider the operating parameter identified in the site-specific test plan to be approved unless explicitly disapproved, or unless comments received from the Administrator require monitoring of an alternate parameter.

(d) You must submit a Notification of Compliance Status as specified in [§ 63.9\(h\)](#). You must submit the Notification of Compliance Status no later than 30 calendar days following the end of the initial 12-month compliance period described in [§ 63.5130](#).

(e) You must submit performance test reports as specified in [§ 63.10\(d\)\(2\)](#) if you are using a control device to comply with the emission standards and you have not obtained a waiver from the performance test requirement.

(f) Before August 24, 2020, you must submit start-up, shutdown, and malfunction reports as specified in [§ 63.10\(d\)\(5\)](#) if you use a control device to comply with this subpart.

(1) Before August 24, 2020, if your actions during a start-up, shutdown, or malfunction of an affected source (including actions taken to correct a malfunction) are not completely consistent with the procedures specified in the source's start-up, shutdown, and malfunction plan specified in [§ 63.6\(e\)\(3\)](#) and required before August 24, 2020, you must state such information in the report. The start-up, shutdown, or malfunction report will consist of a letter containing the name, title, and signature of the responsible official who is certifying its accuracy, that will be submitted to the Administrator. Separate start-up, shutdown, or malfunction reports are not required if the information is included in the report specified in [paragraph \(g\)](#) of this section. The start-up, shutdown, and malfunction plan and start-up, shutdown, and malfunction report are no longer required on and after August 24, 2020.

(2) [Reserved]

(g) You must submit semi-annual compliance reports containing the information specified in [paragraphs \(g\)\(1\)](#) and [\(2\)](#) of this section.

(1) Compliance report dates.

(i) The first semiannual reporting period begins 1 day after the end of the initial compliance period described in [§ 63.5130\(d\)](#) that applies to your affected source and ends 6 months later.

(ii) The first semiannual compliance report must cover the first semiannual reporting period and be postmarked or delivered no later than 30 days after the reporting period ends.

(iii) Each subsequent compliance report must cover the semiannual reporting period from January 1 through June 30 or the semiannual reporting period from July 1 through December 31.

(iv) Each subsequent compliance report must be postmarked or delivered no later than July 31 or January 31, whichever date is the first date following the end of the semiannual reporting period.

(v) For each affected source that is subject to permitting regulations pursuant to [40 CFR part 70](#) or part 71, and the permitting authority has established dates for submitting semiannual reports pursuant to [40 CFR 70.6\(a\)\(3\)\(iii\)\(A\)](#) or [40 CFR 71.6\(a\)\(3\)\(iii\)\(A\)](#), you may submit the first and subsequent compliance reports according to the dates the permitting authority has established instead of according to the dates in [paragraphs \(g\)\(1\)\(i\) through \(iv\)](#) of this section.

(2) The semi-annual compliance report must contain the following information:

(i) Company name and address.

(ii) Statement by a responsible official with that official's name, title, and signature, certifying the accuracy of the content of the report.

(iii) Date of report and beginning and ending dates of the reporting period. The reporting period is the 6-month period ending on June 30 or December 31. Note that the information reported for each of the 6 months in the reporting period will be based on the last 12 months of data prior to the date of each monthly calculation.

(iv) Identification of the compliance option or options specified in Table 1 to [§ 63.5170](#) that you used on each coating operation during the reporting period. If you switched between compliance options during the reporting period, you must report the beginning dates you used each option.

(v) A statement that there were no deviations from the applicable emission limit in [§ 63.5120](#) or the applicable operating limit(s) established according to [§ 63.5121](#) during the reporting period, and that no CEMS were inoperative, inactive, malfunctioning, out-of-control, repaired, or adjusted.

(h) You must submit, for each deviation occurring at an affected source where you are not using CEMS to comply with the standards in this subpart, the semi-annual compliance report containing the information in [paragraphs \(g\)\(2\)\(i\) through \(iv\)](#) of this section and the information in [paragraphs \(h\)\(1\) through \(4\)](#) of this section:

(1) The total operating time of each affected source during the reporting period.

(2) Before August 24, 2020, you must provide information on the number, duration, and cause of deviations (including unknown cause, if applicable) as applicable, and the corrective action taken. On and after August 24, 2020, you must provide information on the number, date, time, duration, and cause of deviations from an emission limit in [§ 63.5120](#) or any applicable operating limit established according to [§ 63.5121](#) (including unknown cause, if applicable) as applicable, and the corrective action taken.

(3) Before August 24, 2020, you must provide information on the number, duration, and cause for continuous parameter monitoring system downtime incidents (including unknown cause other than downtime associated with zero and span and other daily calibration checks, if applicable). On and after August 24, 2020, you must provide the information specified in [paragraphs \(h\)\(3\)\(i\)](#) and [\(ii\)](#) of this section.

(i) Number, date, time, duration, cause (including unknown cause), and descriptions of corrective actions taken for continuous parameter monitoring systems that are inoperative (except for zero (low-level) and high-level checks).

(ii) Number, date, time, duration, cause (including unknown cause), and descriptions of corrective actions taken for continuous parameter monitoring systems that are out of control as specified in [§ 63.8\(c\)\(7\)](#).

(4) On and after August 24, 2020, for each deviation from an emission limit in [§ 63.5120](#) or any applicable operating limit established according to [§ 63.5121](#), you must provide a list of the affected source or equipment, an estimate of the quantity of each regulated pollutant emitted over any emission limit in [§ 63.5120](#), a description of the method used to estimate the emissions, and the actions you took to minimize emissions in accordance with [§ 63.5140\(b\)](#).

(i) You must submit, for each deviation from the applicable emission limit in [§ 63.5120](#) or the applicable operation limit(s) established according to [§ 63.5121](#) occurring at an affected source where you are using CEMS to comply with the standards in this subpart, the semi-annual compliance report containing the information in [paragraphs \(g\)\(2\)\(i\)](#) through [\(iv\)](#) of this section, and the information in [paragraphs \(i\)\(1\)](#) through [\(12\)](#) of this section:

(1) The date and time that each malfunction of the capture system or add-on control devices started and stopped.

(2) Before August 24, 2020, the date and time that each CEMS was inoperative, except for zero (low-level) and high-level checks. On and after August 24, 2020, for each instance that the CEMS was inoperative, except for zero (low-level) and high-level checks, the date, time, and duration that the CEMS was inoperative; the cause (including unknown cause) for the CEMS being inoperative; and a description of corrective actions taken.

(3) Before August 24, 2020, the date and time that each CEMS was out-of-control, including the information in [§ 63.8\(c\)\(8\)](#). On and after August 24, 2020, for each instance that the CEMS was out-of-control, as specified in [§ 63.8\(c\)\(7\)](#), the date, time, and duration that the CEMS was out-of-control; the cause (including unknown cause) for the CEMS being out-of-control; and descriptions of corrective actions taken.

(4) Before August 24, 2020, the date and time that each deviation started and stopped, and whether each deviation occurred during a period of start-up, shutdown, or malfunction or during another period. On and after August 24, 2020, the date, time, and duration of each deviation from an emission limit in [§ 63.5120](#). For each deviation, an estimate of the quantity

of each regulated pollutant emitted over any emission limit in [§ 63.5120](#) to this subpart, and a description of the method used to estimate the emissions.

(5) A summary of the total duration of the deviation during the reporting period, and the total duration as a percent of the total source operating time during that reporting period.

(6) Before August 24, 2020, a breakdown of the total duration of the deviations during the reporting period into those that are due to start-up, shutdown, control equipment problems, process problems, other known causes, and other unknown causes. On and after August 24, 2020, a breakdown of the total duration of the deviations during the reporting period into those that are due to control equipment problems, process problems, other known causes, and other unknown causes.

(7) A summary of the total duration of CEMS downtime during the reporting period, and the total duration of CEMS downtime as a percent of the total source operating time during that reporting period.

(8) A breakdown of the total duration of CEMS downtime during the reporting period into periods that are due to monitoring equipment malfunctions, nonmonitoring equipment malfunctions, quality assurance/quality control calibrations, other known causes, and other unknown causes.

(9) Before August 24, 2020, a brief description of the metal coil coating line. On and after August 24, 2020, a list of the affected source or equipment, including a brief description of the metal coil coating line.

(10) The monitoring equipment manufacturer(s) and model number(s).

(11) The date of the latest CEMS certification or audit.

(12) A description of any changes in CEMS, processes, or controls since the last reporting period.

[[67 FR 39812](#), June 10, 2002, as amended at [68 FR 12592](#), Mar. 17, 2003; [85 FR 10865](#), Feb. 25, 2020; [85 FR 73908](#), Nov. 19, 2020]

§ 63.5181 What are my electronic reporting requirements?

(a) Beginning no later than August 24, 2020, you must submit the results of each performance test as required in [§ 63.5180\(e\)](#) following the procedure specified in [paragraphs \(a\)\(1\)](#) through [\(3\)](#) of this section.

(1) For data collected using test methods supported by the EPA's Electronic Reporting Tool (ERT) as listed on the EPA's ERT website (<https://www.epa.gov/electronic-reporting-air-emissions/electronic-reporting-tool-ert>) at the time of the test, you must submit the results of the performance test to the EPA via the Compliance and Emissions Data Reporting Interface

(CEDRI). The CEDRI interface can be accessed through the EPA's Central Data Exchange (CDX) (<https://cdx.epa.gov/>). Performance test data must be submitted in a file format generated through the use of the EPA's ERT or an alternate electronic file format consistent with the extensible markup language (XML) schema listed on the EPA's ERT website.

(2) For data collected using test methods that are not supported by the EPA's ERT as listed on the EPA's ERT website at the time of the test, you must submit the results of the performance test in portable document format (PDF) using the attachment module of the ERT.

(3) If you claim that some of the performance test information being submitted under [paragraph \(a\)\(1\)](#) of this section is confidential business information (CBI), you must submit a complete file generated through the use of the EPA's ERT or an alternate electronic file consistent with the XML schema listed on the EPA's ERT website, including information claimed to be CBI, on a compact disc, flash drive or other commonly used electronic storage medium to the EPA. The electronic medium must be clearly marked as CBI and mailed to U.S. EPA/OAQPS/CORE CBI Office, Attention: Group Leader, Measurement Policy Group, MD C404-02, 4930 Old Page Rd., Durham, NC 27703. The same ERT or alternate file with the CBI omitted must be submitted to the EPA via the EPA's CDX as described in [paragraph \(a\)\(1\)](#) of this section.

(b) Beginning on August 24, 2020, the owner or operator shall submit the initial notifications required in [§ 63.9\(b\)](#) and the notification of compliance status required in [§§ 63.9\(h\)](#) and [63.5180\(d\)](#) to the EPA via the CEDRI. The CEDRI interface can be accessed through the EPA's CDX (<https://cdx.epa.gov/>). The owner or operator must upload to CEDRI an electronic copy of each applicable notification in PDF. The applicable notification must be submitted by the deadline specified in this subpart, regardless of the method in which the reports are submitted. Owners or operators who claim that some of the information required to be submitted via CEDRI is CBI shall submit a complete report generated using the appropriate form in CEDRI or an alternate electronic file consistent with the XML schema listed on the EPA's CEDRI website, including information claimed to be CBI, on a compact disc, flash drive, or other commonly used electronic storage medium to the EPA. The electronic medium shall be clearly marked as CBI and mailed to U.S. EPA/OAQPS/CORE CBI Office, Attention: Group Leader, Measurement Policy Group, MD C404-02, 4930 Old Page Rd., Durham, NC 27703. The same file with the CBI omitted shall be submitted to the EPA via the EPA's CDX as described earlier in this paragraph.

(c) Beginning on March 25, 2021, or once the reporting template has been available on the CEDRI website for 1 year, whichever date is later, the owner or operator shall submit the semiannual compliance report required in [§ 63.5180\(g\)](#) through [\(i\)](#), as applicable, to the EPA via the CEDRI. The CEDRI interface can be accessed through the EPA's CDX (<https://cdx.epa.gov/>). The owner or operator must use the appropriate electronic template on the CEDRI website for this subpart (<https://www.epa.gov/electronic-reporting-air-emissions/compliance-and-emissions-data-reporting-interface-cedri>). The date on which the report templates become available will be listed on the CEDRI website. If the reporting form for the semiannual compliance report specific to this subpart is not available in CEDRI at the

time that the report is due, you must submit the report to the Administrator at the appropriate addresses listed in [§ 63.13](#). Once the form has been available in CEDRI for 1 year, you must begin submitting all subsequent reports via CEDRI. The reports must be submitted by the deadlines specified in this subpart, regardless of the method in which the reports are submitted. Owners or operators who claim that some of the information required to be submitted via CEDRI is CBI shall submit a complete report generated using the appropriate form in CEDRI, including information claimed to be CBI, on a compact disc, flash drive, or other commonly used electronic storage medium to the EPA. The electronic medium shall be clearly marked as CBI and mailed to U.S. EPA/OAQPS/CORE CBI Office, Attention: Group Leader, Measurement Policy Group, MD C404-02, 4930 Old Page Rd., Durham, NC 27703. The same file with the CBI omitted shall be submitted to the EPA via the EPA's CDX as described earlier in this paragraph.

(d) If you are required to electronically submit a report through the CEDRI in the EPA's CDX, you may assert a claim of EPA system outage for failure to timely comply with the reporting requirement. To assert a claim of EPA system outage, you must meet the requirements outlined in [paragraphs \(g\)\(1\) through \(7\)](#) of this section.

(1) You must have been or will be precluded from accessing CEDRI and submitting a required report within the time prescribed due to an outage of either the EPA's CEDRI or CDX systems.

(2) The outage must have occurred within the period of time beginning five business days prior to the date that the submission is due.

(3) The outage may be planned or unplanned.

(4) You must submit notification to the Administrator in writing as soon as possible following the date you first knew, or through due diligence should have known, that the event may cause or caused a delay in reporting.

(5) You must provide to the Administrator a written description identifying:

(i) The date(s) and time(s) when CDX or CEDRI was accessed and the system was unavailable;

(ii) A rationale for attributing the delay in reporting beyond the regulatory deadline to the EPA system outage;

(iii) Measures taken or to be taken to minimize the delay in reporting; and

(iv) The date by which you propose to report, or if you have already met the reporting requirement at the time of the notification, the date you reported.

(6) The decision to accept the claim of EPA system outage and allow an extension to the reporting deadline is solely within the discretion of the Administrator.

(7) In any circumstance, the report must be submitted electronically as soon as possible after the outage is resolved.

(e) If you are required to electronically submit a report through CEDRI in the EPA's CDX, you may assert a claim of force majeure for failure to timely comply with the reporting requirement. To assert a claim of force majeure, you must meet the requirements outlined in [paragraphs \(h\)\(1\)](#) through [\(5\)](#) of this section.

(1) You may submit a claim if a force majeure event is about to occur, occurs, or has occurred or there are lingering effects from such an event within the period of time beginning five business days prior to the date the submission is due. For the purposes of this section, a force majeure event is defined as an event that will be or has been caused by circumstances beyond the control of the affected facility, its contractors, or any entity controlled by the affected facility that prevents you from complying with the requirement to submit a report electronically within the time period prescribed. Examples of such events are acts of nature (*e.g.*, hurricanes, earthquakes, or floods), acts of war or terrorism, or equipment failure or safety hazard beyond the control of the affected facility (*e.g.*, large scale power outage).

(2) You must submit notification to the Administrator in writing as soon as possible following the date you first knew, or through due diligence should have known, that the event may cause or has caused a delay in reporting.

(3) You must provide to the Administrator:

(i) A written description of the force majeure event;

(ii) A rationale for attributing the delay in reporting beyond the regulatory deadline to the force majeure event;

(iii) Measures taken or to be taken to minimize the delay in reporting; and

(iv) The date by which you propose to report, or if you have already met the reporting requirement at the time of the notification, the date you reported.

(4) The decision to accept the claim of force majeure and allow an extension to the reporting deadline is solely within the discretion of the Administrator.

(5) In any circumstance, the reporting must occur as soon as possible after the force majeure event occurs.

[\[85 FR 10866, Feb. 25, 2020\]](#)

§ 63.5190 What records must I maintain?

(a) You must maintain the records specified in [paragraphs \(a\)](#) and [\(b\)](#) of this section in accordance with [§ 63.10\(b\)\(1\)](#):

- (1) Records of the coating lines on which you used each compliance option and the time periods (beginning and ending dates and times) you used each option.
- (2) Records specified in [§ 63.10\(b\)\(2\)](#) of all measurements needed to demonstrate compliance with this subpart, including:
 - (i) Continuous emission monitor data in accordance with [§ 63.5150\(a\)\(2\)](#);
 - (ii) Control device and capture system operating parameter data in accordance with [§ 63.5150\(a\)\(1\)](#), [\(3\)](#), and [\(4\)](#);
 - (iii) Organic HAP content data for the purpose of demonstrating compliance in accordance with [§ 63.5160\(b\)](#);
 - (iv) Volatile matter and solids content data for the purpose of demonstrating compliance in accordance with [§ 63.5160\(c\)](#);
 - (v) Overall control efficiency determination or alternative outlet HAP concentration using capture efficiency tests and control device destruction or removal efficiency tests in accordance with [§ 63.5160\(d\)](#), [\(e\)](#), and [\(f\)](#); and
 - (vi) Material usage, HAP usage, volatile matter usage, and solids usage and compliance demonstrations using these data in accordance with [§ 63.5170\(a\)](#), [\(b\)](#), and [\(d\)](#);
- (3) Records specified in [§ 63.10\(b\)\(3\)](#); and
- (4) Additional records specified in [§ 63.10\(c\)](#) for each continuous monitoring system operated by the owner or operator in accordance with [§ 63.5150\(a\)\(2\)](#).
- (5) On and after August 24, 2020, for each deviation from an emission limitation reported under [§ 63.5180\(h\)](#) or [\(i\)](#), a record of the information specified in [paragraphs \(a\)\(5\)\(i\)](#) through [\(iv\)](#) of this section, as applicable.
 - (i) The date, time, and duration of the deviation, as reported under [§ 63.5180\(h\)](#) and [\(i\)](#).
 - (ii) A list of the affected sources or equipment for which the deviation occurred and the cause of the deviation, as reported under [§ 63.5180\(h\)](#) and [\(i\)](#).
 - (iii) An estimate of the quantity of each regulated pollutant emitted over any applicable emission limit in [§ 63.5120](#) to this subpart or any applicable operating limit established according to [§ 63.5121](#) to this subpart, and a description of the method used to calculate the estimate, as reported under [§ 63.5180\(h\)](#) and [\(i\)](#).
 - (iv) A record of actions taken to minimize emissions in accordance with [§ 63.5140\(b\)](#) and any corrective actions taken to return the affected unit to its normal or usual manner of operation.

(b) Maintain records of all liquid-liquid material balances that are performed in accordance with the requirements of [§ 63.5170](#).

(c) Any records required to be maintained by this subpart that are in reports that were submitted electronically via the EPA's CEDRI may be maintained in electronic format. This ability to maintain electronic copies does not affect the requirement for facilities to make records, data, and reports available upon request to a delegated air agency or the EPA as part of an on-site compliance evaluation.

[[67 FR 39812](#), June 10, 2002, as amended at [85 FR 10867](#), Feb. 25, 2020]

Delegation of Authority

§ 63.5200 What authorities may be delegated to the States?

(a) This subpart can be implemented and enforced by us, the EPA, or a delegated authority such as your State, local, or tribal agency. If the EPA Administrator has delegated authority to your State, local, or tribal agency, then that agency has the authority to implement and enforce this subpart. You should contact your EPA Regional Office to find out if this subpart is delegated to your State, local, or tribal agency.

(b) In delegating implementation and enforcement authority of this subpart to a State, local, or tribal agency under section [40 CFR part 63, subpart E](#), the authorities contained in [paragraph \(c\)](#) of this section are retained by the EPA Administrator and not transferred to the State, local, or tribal agency.

(c) Authority which will not be delegated to States, local, or tribal agencies:

(1) Approval of alternatives to the emission limitations in [§ 63.5120](#);

(2) Approval of major alternatives to test methods under [§ 63.7\(e\)\(2\)\(ii\)](#) and [\(f\)](#) and as defined in [§ 63.5160](#);

(3) Approval of major alternatives to monitoring under [§ 63.8\(f\)](#) and as defined in [§ 63.5150](#);
and

(4) Approval of major alternatives to recordkeeping and reporting under [§ 63.10\(f\)](#) and as defined in [§§ 63.5180](#) and [63.5190](#).

§§ 63.5201-63.5209 [Reserved]

Table 1 to Subpart SSSS of Part 63 - Operating Limits if Using Add-on Control Devices and Capture System

If you are required to comply with operating limits by [§ 63.5121](#), you must comply with the applicable operating limits in the following table:

For the following device . . .	You must meet the following operating limit . . .	And you must demonstrate continuous compliance with the operating limit by . . .
1. thermal oxidizer	a. the average combustion temperature in any 3-hour period must not fall below the combustion temperature limit established according to § 63.5160(d)(3)(i)	i. collecting the combustion temperature data according to § 63.5150(a)(3) ; ii. reducing the data to 3-hour block averages; and iii. maintaining the 3-hour average combustion temperature at or above the temperature limit.
2. catalytic oxidizer	a. the average temperature measured just before the catalyst bed in any 3-hour period must not fall below the limit established according to § 63.5160(d)(3)(ii) ; and either	i. collecting the temperature data according to § 63.5150(a)(3) ; ii. reducing the data to 3-hour block averages; and iii. maintaining the 3-hour average temperature before the catalyst bed at or above the temperature limit.
	b. ensure that the average temperature difference across the catalyst bed in any 3-hour period does not fall below the temperature difference limit established according to § 63.5160(d)(3)(ii) ; or	i. collecting the temperature data according to § 63.5150(a)(3) ; ii. reducing the data to 3-hour block averages; and iii. maintaining the 3-hour average temperature difference at or above the temperature difference limit.
	c. develop and implement an inspection and maintenance plan according to § 63.5160(d)(3)(ii)	maintaining an up-to-date inspection and maintenance plan, records of annual catalyst activity checks, records of monthly inspections of the oxidizer system, and records of the annual internal inspections of the catalyst bed. If a problem is discovered during a monthly or annual inspection required by § 63.5160(d)(3)(ii) , you must take corrective action as soon as practicable consistent with the manufacturer's recommendations.

For the following device . . .	You must meet the following operating limit . . .	And you must demonstrate continuous compliance with the operating limit by . . .
3. emission capture system	develop a monitoring plan that identifies operating parameter to be monitored and specifies operating limits according to § 63.5150(a)(4)	conducting monitoring according to the plan § 63.5150(a)(4) .

Table 2 to Subpart SSSS of Part 63 - Applicability of General Provisions to Subpart SSSS

You must comply with the applicable General Provisions requirements according to the following table:

General provisions reference	Subject	Applicable to subpart SSSS	Explanation
§ 63.1(a)(1)-(4)	General Applicability	Yes	
§ 63.1(a)(6)	Source Category Listing	Yes	
§ 63.1(a)(10)-(12)	Timing and Overlap Clarifications	Yes	
§ 63.1(b)(1)	Initial Applicability Determination	Yes	Applicability to Subpart SSSS is also specified in § 63.5090 .
§ 63.1(b)(3)	Applicability Determination Recordkeeping	Yes	
§ 63.1(c)(1)	Applicability after Standard Established	Yes	
§ 63.1(c)(2)	Applicability of Permit Program for Area Sources	Yes	
§ 63.1(c)(5)	Extensions and Notifications	Yes	

General provisions reference	Subject	Applicable to subpart SSSS	Explanation
§ 63.1(c)(6)	Yes		
§ 63.1(e)	Applicability of Permit Program Before Relevant Standard is Set	Yes	
§ 63.2	Definitions	Yes	Additional definitions are specified in § 63.5110 .
§ 63.3	Units and Abbreviations	Yes	
§ 63.4(a)(1)-(2)	Prohibited Activities	Yes	
§ 63.4(b)-(c)	Circumvention/Fragmentation	Yes	
§ 63.5(a)	Construction/Reconstruction	Yes	
§ 63.5(b)(1), (3), (4), (6)	Requirements for Existing, Newly Constructed, and Reconstructed Sources	Yes	
§ 63.5(d)(1)(i)-(ii)(F), (d)(1)(ii)(H), (d)(1)(ii)(J), (d)(1)(iii), (d)(2)-(4)	Application for Approval of Construction/Reconstruction	Yes	Only total HAP emissions in terms of tons per year are required for § 63.5(d)(1)(ii)(H) .
§ 63.5(e)	Approval of Construction/Reconstruction	Yes	
§ 63.5(f)	Approval of Construction/Reconstruction Based on Prior State Review	Yes	
§ 63.6(a)	Compliance with Standards and Maintenance Requirements- Applicability	Yes	

General provisions reference	Subject	Applicable to subpart SSSS	Explanation
§ 63.6(b)(1)-(5), (b)(7)	Compliance Dates for New and Reconstructed Sources	Yes	Section 63.5130 specifies the compliance dates.
§ 63.6(c)(1), (2), (5)	Compliance Dates for Existing Sources	Yes	Section 63.5130 specifies the compliance dates.
§ 63.6(e)(1)(i)-(ii)	General Duty to Minimize Emissions and Requirement to Correct Malfunctions As Soon As Possible	Yes before August 24, 2020, No on and after August 24, 2020	See § 63.5140(b) for general duty requirement.
§ 63.6(e)(1)(iii)	Operation and Maintenance Requirements	Yes	
§ 63.6(e)(3)(i), (e)(3)(iii)-(ix)	SSMP Requirements	Yes before August 24, 2020, No on and after August 24, 2020	
§ 63.6(f)(1)	SSM Exemption	Yes before August 24, 2020, No on and after August 24, 2020	See § 63.5140(b) for general duty requirement.
§ 63.6(f)(2)-(3)	Compliance with Non-Opacity Emission Standards	Yes	
§ 63.6(g)	Alternative Non-Opacity Emission Standard	Yes	
§ 63.6(h)	Compliance with Opacity/Visible	No	Subpart SSSS does not establish opacity

General provisions reference	Subject	Applicable to subpart SSSS	Explanation
	Emission Standards		standards or visible emission standards.
§ 63.6(i)(1)-(14), (i)(16)	Extension of Compliance and Administrator's Authority	Yes	
§ 63.6(j)	Presidential Compliance Exemption	Yes	
§ 63.7(a)-(d) except (a)(2)(i)-(viii)	Performance Test Requirements	Yes	
§ 63.7(e)(1)	Performance Testing	Yes before August 24, 2020, No on and after August 24, 2020	See § 63.5160(d)(2) .
§ 63.7(e)(2)-(4)	Conduct of Performance Tests	Yes	
§ 63.7(f)	Alternative Test Method	Yes	EPA retains approval authority.
§ 63.7(g)-(h)	Data Analysis and Waiver of Tests	Yes	
§ 63.8(a)(1)-(2)	Monitoring Requirements - Applicability	Yes	Additional requirements for monitoring are specified in § 63.5150(a) .
§ 63.8(a)(4)	Additional Monitoring Requirements	No	Subpart SSSS does not have monitoring requirements for flares.
§ 63.8(b)	Conduct of Monitoring	Yes	
§ 63.8(c)(1)	Operation and Maintenance of	Yes before	Section 63.5150(a)

General provisions reference	Subject	Applicable to subpart SSSS	Explanation
	Continuous Monitoring System (CMS)	August 24, 2020, No on and after August 24, 2020	specifies the requirements for the operation of CMS for capture systems and add-on control devices at sources using these to comply. Applies only to monitoring of capture system and add-on control device efficiency at sources using these to comply with the standards. Additional requirements for CMS operations and maintenance are specified in § 63.5170 .
§ 63.8(c)(2)-(3)	CMS Operation and Maintenance	Yes	
§ 63.8(c)(4)-(5)	CMS Continuous Operation Procedures	No	Subpart SSSS does not require COMS.
§ 63.8(c)(6)-(8)	CMS Requirements	Yes	Provisions only apply if CEMS are used.
§ 63.8(d)-(e)	CMS Quality Control, Written Procedures, and Performance Evaluation	Yes	Provisions only apply if CEMS are used.
§ 63.8(f)(1)-(5)	Use of an Alternative Monitoring Method	Yes	EPA retains approval authority.
§ 63.8(f)(6)	Alternative to Relative Accuracy Test	No	Section 63.8(f)(6) provisions are not applicable because subpart SSSS does not

General provisions reference	Subject	Applicable to subpart SSSS	Explanation
			require CEMS.
§ 63.8(g)	Data Reduction	No	Sections 63.5170, 63.5140, 63.5150, and 63.5150 specify monitoring data reduction.
§ 63.9(a)	Notification of Applicability	Yes	
§ 63.9(b)(1)	Initial Notifications	Yes	
§ 63.9(b)(2)	Initial Notifications	Yes	With the exception that § 63.5180(b)(1) provides 2 years after the proposal date for submittal of the initial notification for existing sources.
§ 63.9(b)(4)(i), (b)(4)(v), (b)(5)	Application for Approval of Construction or Reconstruction	Yes	
§ 63.9(c)-(e)	Request for Extension of Compliance, New Source Notification for Special Compliance Requirements, and Notification of Performance Test	Yes	Notification of performance test requirement applies only to capture system and add-on control device performance tests at sources using these to comply with the standards.
§ 63.9(f)	Notification of Visible Emissions/Opacity Test	No	Subpart SSSS does not require opacity and visible emissions observations.

General provisions reference	Subject	Applicable to subpart SSSS	Explanation
§ 63.9(g)	Additional Notifications When Using CMS	No	Provisions for COMS are not applicable.
§ 63.9(h)(1)-(3)	Notification of Compliance Status	Yes	Section 63.5130 specifies the dates for submitting the notification of compliance status.
§ 63.9(h)(5)-(6)	Clarifications	Yes	
§ 63.9(i)	Adjustment of Submittal Deadlines	Yes	
§ 63.9(j)	Change in Previous Information	Yes	
§ 63.9(k)	Yes	Only as specified in § 63.9(j)	
§ 63.10(a)	Recordkeeping/Reporting - Applicability and General Information	Yes	
§ 63.10(b)(1)	General Recordkeeping Requirements	Yes	Additional requirements are specified in § 63.5190 .
§ 63.10(b)(2)(i)-(ii)	Recordkeeping of Occurrence and Duration of Startups and Shutdowns and Recordkeeping of Failures to Meet Standards	Yes before August 24, 2020, No on and after August 24, 2020	See § 63.5190(a)(5) .
§ 63.10(b)(2)(iii)	Maintenance Records	Yes	
§ 63.10(b)(2)(iv)-	Actions Taken to Minimize Emissions During Startup,	Yes before August 24,	See § 63.5190(a)(5) .

General provisions reference	Subject	Applicable to subpart SSSS	Explanation
(v)	Shutdown, and Malfunction	2020, No on and after August 24, 2020	
§ 63.10(b)(2)(vi)	Recordkeeping for CMS Malfunctions	Yes before August 24, 2020, No on and after August 24, 2020	See § 63.5190(a)(5) .
§ 63.10(b)(2)(vii)-(xiv)	Other CMS Requirements	Yes	
§ 63.10(b)(3)	Recordkeeping Requirements for Applicability Determinations	Yes	
§ 63.10(c)	Additional CMS Recordkeeping Requirements	No	See § 63.5190(a)(5) .
§ 63.10(d)(1)-(2)	General Reporting Requirements and Report of Performance Test Results	Yes	Additional requirements are specified in § 63.5180(e) .
§ 63.10(d)(3)	Reporting Opacity or Visible Emissions Observations	No	Subpart SSSS does not require opacity and visible emissions observations.
§ 63.10(d)(4)	Progress Reports for Sources with Compliance Extensions	Yes	
§ 63.10(d)(5)	Startup, Shutdown, Malfunction Reports	Yes before August 24, 2020, No on and after August 24,	

General provisions reference	Subject	Applicable to subpart SSSS	Explanation
		2020	
§ 63.10(e)	Additional Reporting Requirements for Sources with CMS	No	
§ 63.10(f)	Recordkeeping/Reporting Waiver	Yes	
§ 63.11	Control Device Requirements/Flares	No	Subpart SSSS does not specify use of flares for compliance.
§ 63.12	State Authority and Delegations	Yes	
§ 63.13(a)	Addresses	Yes before August 24, 2020, No on and after August 24, 2020	
§ 63.13(b)	Submittal to State Agencies	Yes	
§ 63.13(c)	Submittal to State Agencies	Yes before August 24, 2020, No unless the state requires the submittal via CEDRI, on and after August 24, 2020	
§ 63.14	Incorporation by Reference	Yes	Subpart SSSS includes provisions for alternative ASTM and ASME test methods that are incorporated by

General provisions reference	Subject	Applicable to subpart SSSS	Explanation
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reference.

§ 63.15	Availability of Information/Confidentiality	Yes	
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[[85 FR 10868](#), Feb. 25, 2020, as amended at [85 FR 73908](#), Nov. 19, 2020]

Table 3 to Subpart SSSS of Part 63 - List of Hazardous Air Pollutants That Must Be Counted Toward Total Organic HAP Content if Present at 0.1 Percent or More by Mass

Chemical name	CAS No.
1,1,2,2-Tetrachloroethane	79-34-5
1,1,2-Trichloroethane	79-00-5
1,1-Dimethylhydrazine	57-14-7
1,2-Dibromo-3-chloropropane	96-12-8
1,2-Diphenylhydrazine	122-66-7
1,3-Butadiene	106-99-0
1,3-Dichloropropene	542-75-6
1,4-Dioxane	123-91-1
2,4,6-Trichlorophenol	88-06-2
2,4/2,6-Dinitrotoluene (mixture)	25321-14-6
2,4-Dinitrotoluene	121-14-2
2,4-Toluene diamine	95-80-7

Chemical name	CAS No.
2-Nitropropane	79-46-9
3,3'-Dichlorobenzidine	91-94-1
3,3'-Dimethoxybenzidine	119-90-4
3,3'-Dimethylbenzidine	119-93-7
4,4'-Methylene bis(2-chloroaniline)	101-14-4
Acetaldehyde	75-07-0
Acrylamide	79-06-1
Acrylonitrile	107-13-1
Allyl chloride	107-05-1
alpha-Hexachlorocyclohexane (a-HCH)	319-84-6
Aniline	62-53-3
Benzene	71-43-2
Benzidine	92-87-5
Benzotrichloride	98-07-7
Benzyl chloride	100-44-7
beta-Hexachlorocyclohexane (b-HCH)	319-85-7
Bis(2-ethylhexyl)phthalate	117-81-7
Bis(chloromethyl)ether	542-88-1
Bromoform	75-25-2
Captan	133-06-2
Carbon tetrachloride	56-23-5

Chemical name	CAS No.
Chlordane	57-74-9
Chlorobenzilate	510-15-6
Chloroform	67-66-3
Chloroprene	126-99-8
Cresols (mixed)	1319-77-3
DDE	3547-04-4
Dichloroethyl ether	111-44-4
Dichlorvos	62-73-7
Epichlorohydrin	106-89-8
Ethyl acrylate	140-88-5
Ethylene dibromide	106-93-4
Ethylene dichloride	107-06-2
Ethylene oxide	75-21-8
Ethylene thiourea	96-45-7
Ethylidene dichloride (1,1-Dichloroethane)	75-34-3
Formaldehyde	50-00-0
Heptachlor	76-44-8
Hexachlorobenzene	118-74-1
Hexachlorobutadiene	87-68-3
Hexachloroethane	67-72-1
Hydrazine	302-01-2

Chemical name	CAS No.
Isophorone	78-59-1
Lindane (hexachlorocyclohexane, all isomers)	58-89-9
m-Cresol	108-39-4
Methylene chloride	75-09-2
Naphthalene	91-20-3
Nitrobenzene	98-95-3
Nitrosodimethylamine	62-75-9
o-Cresol	95-48-7
o-Toluidine	95-53-4
Parathion	56-38-2
p-Cresol	106-44-5
p-Dichlorobenzene	106-46-7
Pentachloronitrobenzene	82-68-8
Pentachlorophenol	87-86-5
Propoxur	114-26-1
Propylene dichloride	78-87-5
Propylene oxide	75-56-9
Quinoline	91-22-5
Tetrachloroethene	127-18-4
Toxaphene	8001-35-2
Trichloroethylene	79-01-6

Chemical name	CAS No.
Trifluralin	1582-09-8
Vinyl bromide	593-60-2
Vinyl chloride	75-01-4
Vinylidene chloride	75-35-4

[[85 FR 10870](#), Feb. 25, 2020]

Appendix H

40 C.F.R. Part 63 Subpart CCC

***National Emission Standards for Hazardous Air Pollutants for Steel Pickling – HCl Process
Facilities and Hydrochloric Acid Regeneration Plants***

Subpart CCC - National Emission Standards for Hazardous Air Pollutants for Steel Pickling - HCl Process Facilities and Hydrochloric Acid Regeneration Plants

Source: [64 FR 33218](#), June 22, 1999, unless otherwise noted.

§ 63.1155 Applicability.

(a) The provisions of this subpart apply to the following facilities and plants that are major sources for hazardous air pollutants (HAP) or are parts of facilities that are major sources for HAP:

(1) All new and existing steel pickling facilities that pickle carbon steel using hydrochloric acid solution that contains 6 percent or more by weight HCl and is at a temperature of 100 °F or higher; and

(2) All new and existing hydrochloric acid regeneration plants.

(3) The provisions of this subpart do not apply to facilities that pickle carbon steel without using hydrochloric acid, to facilities that pickle only specialty steel, or to acid regeneration plants that regenerate only acids other than hydrochloric acid.

(b) For the purposes of implementing this subpart, the affected sources at a facility or plant subject to this subpart are as follows: Continuous and batch pickling lines, hydrochloric acid regeneration plants, and hydrochloric acid storage vessels.

(c) Table 1 to this subpart specifies the provisions of this part 63, subpart A that apply and those that do not apply to owners and operators of steel pickling facilities and hydrochloric acid regeneration plants subject to this subpart.

(d) In response to an action to enforce the standards set forth in this subpart, the owner or operator may assert an affirmative defense to a claim for civil penalties for violations of such standards that are caused by a malfunction, as defined in [§ 63.2](#). Appropriate penalties may be assessed, however, if the owner or operator fails to meet the burden of proving all the requirements in the affirmative defense. The affirmative defense shall not be available for claims for injunctive relief.

(1) To establish the affirmative defense in any action to enforce such a standard, the owner or operator must timely meet the reporting requirements of [paragraph \(d\)\(2\)](#) of this section, and must prove by a preponderance of evidence that:

(i) The violation was caused by a sudden, infrequent, and unavoidable failure of air pollution control equipment, process equipment, or a process to operate in a normal and usual manner; and could not have been prevented through careful planning, proper design, or better operation and maintenance practices; and did not stem from any activity or event that could have been foreseen and avoided, or planned for; and was not part of a recurring pattern indicative of inadequate design, operation, or maintenance; and

- (ii) Repairs were made as expeditiously as possible when exceeded violation occurred. Off-shift and overtime labor were used, to the extent practicable to make these repairs; and
- (iii) The frequency, amount, and duration of the violation (including any bypass) were minimized to the maximum extent practicable; and
- (iv) If the violation resulted from a bypass of control equipment or a process, then the bypass was unavoidable to prevent loss of life, personal injury, or severe property damage; and
- (v) All possible steps were taken to minimize the impact of the violation on ambient air quality, the environment, and human health; and
- (vi) All emissions monitoring and control systems were kept in operation if at all possible, consistent with safety and good air pollution control practices; and
- (vii) All of the actions in response to the violation were documented by properly signed, contemporaneous operating logs; and
- (viii) At all times, the affected source was operated in a manner consistent with good practices for minimizing emissions; and
- (ix) A written root cause analysis has been prepared, the purpose of which is to determine, correct, and eliminate the primary causes of the malfunction and the violation resulting from the malfunction event at issue. The analysis shall also specify, using the best monitoring methods and engineering judgment, the amount of excess emissions that were the result of the malfunction.

(2) **Report.** The owner of operator seeking to assert an affirmative defense shall submit a written report to the Administrator with all necessary supporting documentation, that it has met the requirements set forth in [paragraph \(d\)\(1\)](#) of this section. This affirmative defense report shall be included in the first periodic compliance, deviation report or excess emission report otherwise required after the initial occurrence of the violation of the relevant standard (which may be the end of any applicable averaging period). If such compliance, deviation report or excess emission report is due less than 45 days after the initial occurrence of the violation, the affirmation defense report may be included in the second compliance, deviation report or excess emission report due after the initial occurrence of the violation of the relevant standard.

[[64 FR 33218](#), June 22, 1999, as amended at [77 FR 58250](#), Sept. 19, 2012]

§ 63.1156 Definitions.

Terms used in this subpart are defined in the Clean Air Act, in [subpart A of this part](#), or in this section as follows:

Affirmative defense means, in the context of an enforcement proceeding, a response or a defense put forward by a defendant, regarding which the defendant has the burden of proof, and the merits of which are independently and objectively evaluated in a judicial or administrative proceeding.

Batch pickling line means the collection of equipment and tanks configured for pickling metal in any form but usually in discrete shapes where the material is lowered in batches into a bath of acid solution, allowed to remain until the scale is dissolved, then removed from the solution, drained, and rinsed by spraying or immersion in one or more rinse tanks to remove residual acid.

Carbon steel means steel that contains approximately 2 percent or less carbon, 1.65 percent or less manganese, 0.6 percent or less silicon, and 0.6 percent or less copper.

Closed-vent system means a system that is not open to the atmosphere and that is composed of piping, ductwork, connections, and, if necessary, flow-inducing devices that transport emissions from a process unit or piece of equipment (e.g., pumps, pressure relief devices, sampling connections, open-ended valves or lines, connectors, and instrumentation systems) back into a closed system or into any device that is capable of reducing or collecting emissions.

Continuous pickling line means the collection of equipment and tanks configured for pickling metal strip, rod, wire, tube, or pipe that is passed through an acid solution in a continuous or nearly continuous manner and rinsed in another tank or series of tanks to remove residual acid. This definition includes continuous spray towers.

Hydrochloric acid regeneration plant means the collection of equipment and processes configured to reconstitute fresh hydrochloric acid pickling solution from spent pickle liquor using a thermal treatment process.

Hydrochloric acid regeneration plant production mode means operation under conditions that result in production of usable regenerated acid or iron oxide.

Hydrochloric acid storage vessel means a stationary vessel used for the bulk containment of virgin or regenerated hydrochloric acid.

Responsible maintenance official means a person designated by the owner or operator as having the knowledge and the authority to sign records and reports required under this rule.

Specialty steel means a category of steel that includes silicon electrical, alloy, tool, and stainless steels.

Spray tower means an enclosed vertical tower in which acid pickling solution is sprayed onto moving steel strip in multiple vertical passes.

Steel pickling means the chemical removal of iron oxide mill scale that is formed on steel surfaces during hot rolling or hot forming of semi-finished steel products through contact with an aqueous solution of acid where such contact occurs prior to shaping or coating of the finished

steel product. This definition does not include removal of light rust or scale from finished steel products or activation of the metal surface prior to plating or coating.

Steel pickling facility means any facility that operates one or more batch or continuous steel pickling lines.

[[64 FR 33218](#), June 22, 1999, as amended at [77 FR 58250](#), Sept. 19, 2012]

§ 63.1157 Emission standards for existing sources.

(a) **Pickling lines.** No owner or operator of an existing affected continuous or batch pickling line at a steel pickling facility shall cause or allow to be discharged into the atmosphere from the affected pickling line:

- (1) Any gases that contain HCl in a concentration in excess of 18 parts per million by volume (ppmv); or
- (2) HCl at a mass emission rate that corresponds to a collection efficiency of less than 97 percent.

(b) **Hydrochloric acid regeneration plants.**

- (1) No owner or operator of an existing affected plant shall cause or allow to be discharged into the atmosphere from the affected plant any gases that contain HCl in a concentration greater than 25 ppmv.
- (2) In addition to the requirement of [paragraph \(b\)\(1\)](#) of this section, no owner or operator of an existing plant shall cause or allow to be discharged into the atmosphere from the affected plant any gases that contain chlorine (Cl₂) in a concentration in excess of 6 ppmv.

[[64 FR 33218](#), June 22, 1999, as amended at [77 FR 58250](#), Sept. 19, 2012]

§ 63.1158 Emission standards for new or reconstructed sources.

(a) **Pickling lines -**

(1) **Continuous pickling lines.** No owner or operator of a new or reconstructed affected continuous pickling line at a steel pickling facility shall cause or allow to be discharged into the atmosphere from the affected pickling line:

- (i) Any gases that contain HCl in a concentration in excess of 6 ppmv; or
- (ii) HCl at a mass emission rate that corresponds to a collection efficiency of less than 99 percent.

(2) **Batch pickling lines.** No owner or operator of a new or reconstructed affected batch pickling line at a steel pickling facility shall cause or allow to be discharged into the atmosphere from the affected pickling line:

(i) Any gases that contain HCl in a concentration in excess of 18 ppmv; or

(ii) HCl at a mass emission rate that corresponds to a collection efficiency of less than 97 percent.

(b) **Hydrochloric acid regeneration plants.**

(1) No owner or operator of a new or reconstructed affected plant shall cause or allow to be discharged into the atmosphere from the affected plant any gases that contain HCl in a concentration greater than 12 ppmv.

(2) In addition to the requirement of [paragraph \(b\)\(1\)](#) of this section, no owner or operator of a new or reconstructed affected plant shall cause or allow to be discharged into the atmosphere from the affected plant any gases that contain Cl₂ in a concentration in excess of 6 ppmv.

§ 63.1159 Operational and equipment standards for existing, new, or reconstructed sources.

(a) **Hydrochloric acid regeneration plant.** The owner or operator of an affected plant must operate the affected plant at all times while in production mode in a manner that minimizes the proportion of excess air fed to the process and maximizes the process offgas temperature consistent with producing usable regenerated acid or iron oxide.

(b) **Hydrochloric acid storage vessels.** The owner or operator of an affected vessel shall provide and operate, except during loading and unloading of acid, a closed-vent system for each vessel. Loading and unloading shall be conducted either through enclosed lines or each point where the acid is exposed to the atmosphere shall be equipped with a local fume capture system, ventilated through an air pollution control device.

(c) **General duty to minimize emissions.** At all times, each owner or operator must operate and maintain any affected source subject to the requirements of this subpart, including associated air pollution control equipment and monitoring equipment in a manner consistent with safety and good air pollution control practices for minimizing emissions. The general duty to minimize emissions does not require the owner or operator to make any further efforts to reduce emissions if levels required by this standard have been achieved. Determination of whether such operation and maintenance procedures are being used will be based on information available to the Administrator which may include, but is not limited to, monitoring results, review of operation and maintenance procedures, review of operation and maintenance records, and inspection of the source.

§ 63.1160 Compliance dates and maintenance requirements.

(a) *Compliance dates.*

(1) The owner or operator of an affected existing steel pickling facility and/or hydrochloric acid regeneration plant subject to this subpart shall achieve initial compliance with the requirements of this subpart no later than June 22, 2001.

(2) The owner or operator of a new or reconstructed steel pickling facility and/or hydrochloric acid regeneration plant subject to this subpart that commences construction or reconstruction after September 18, 1997, shall achieve compliance with the requirements of this subpart immediately upon startup of operations or by June 22, 1999, whichever is later.

(b) *Maintenance requirements.*

(1) The owner or operator shall prepare an operation and maintenance plan for each emission control device to be implemented no later than the compliance date. The plan shall be incorporated by reference into the source's title V permit. All such plans must be consistent with good maintenance practices, and, for a scrubber emission control device, must at a minimum:

(i) Require monitoring and recording the pressure drop across the scrubber once per shift while the scrubber is operating in order to identify changes that may indicate a need for maintenance;

(ii) Require the manufacturer's recommended maintenance at the recommended intervals on fresh solvent pumps, recirculating pumps, discharge pumps, and other liquid pumps, in addition to exhaust system and scrubber fans and motors associated with those pumps and fans;

(iii) Require cleaning of the scrubber internals and mist eliminators at intervals sufficient to prevent buildup of solids or other fouling;

(iv) Require an inspection of each scrubber at intervals of no less than 3 months with:

(A) Cleaning or replacement of any plugged spray nozzles or other liquid delivery devices;

(B) Repair or replacement of missing, misaligned, or damaged baffles, trays, or other internal components;

(C) Repair or replacement of droplet eliminator elements as needed;

(D) Repair or replacement of heat exchanger elements used to control the temperature of fluids entering or leaving the scrubber; and

(E) Adjustment of damper settings for consistency with the required air flow.

(v) If the scrubber is not equipped with a viewport or access hatch allowing visual inspection, alternate means of inspection approved by the Administrator may be used.

(vi) The owner or operator shall initiate procedures for corrective action within 1 working day of detection of an operating problem and complete all corrective actions as soon as practicable. Procedures to be initiated are the applicable actions that are specified in the maintenance plan. Failure to initiate or provide appropriate repair, replacement, or other corrective action is a violation of the maintenance requirement of this subpart.

(vii) The owner or operator shall maintain a record of each inspection, including each item identified in [paragraph \(b\)\(2\)\(iv\)](#) of this section, that is signed by the responsible maintenance official and that shows the date of each inspection, the problem identified, a description of the repair, replacement, or other corrective action taken, and the date of the repair, replacement, or other corrective action taken.

(2) The owner or operator of each hydrochloric acid regeneration plant shall develop and implement a written maintenance program. The program shall require:

(i) Performance of the manufacturer's recommended maintenance at the recommended intervals on all required systems and components;

(ii) Initiation of procedures for appropriate and timely repair, replacement, or other corrective action within 1 working day of detection; and

(iii) Maintenance of a daily record, signed by a responsible maintenance official, showing the date of each inspection for each requirement, the problems found, a description of the repair, replacement, or other action taken, and the date of repair or replacement.

[[64 FR 33218](#), June 22, 1999, as amended at [77 FR 58250](#), Sept. 19, 2012]

§ 63.1161 Performance testing and test methods.

(a) ***Demonstration of compliance.*** The owner or operator shall conduct an initial performance test for each process or emission control device to determine and demonstrate compliance with the applicable emission limitation according to the requirements in [§ 63.7](#) of [subpart A of this part](#) and in this section. Performance tests shall be conducted under such conditions as the Administrator specifies to the owner or operator based on representative performance of the affected source for the period being tested. Upon request, the owner or operator shall make available to the Administrator such records as may be necessary to determine the conditions of performance tests.

(b) ***Establishment of scrubber operating parameters.*** During the performance test for each emission control device, the owner or operator using a wet scrubber to achieve compliance shall establish site-specific operating parameter values for the minimum scrubber makeup water flow rate and, for scrubbers that operate with recirculation, the minimum recirculation water flow rate. During the emission test, each operating parameter must be monitored continuously and recorded with sufficient frequency to establish a representative average value for that parameter, but no less frequently than once every 15 minutes. The owner or operator shall determine the operating parameter monitoring values as the averages of the values recorded during any of the runs for which results are used to establish the emission concentration or collection efficiency per [paragraph \(a\)\(2\)](#) of this section. An owner or operator may conduct multiple performance tests to establish alternative compliant operating parameter values. Also, an owner or operator may reestablish compliant operating parameter values as part of any performance test that is conducted subsequent to the initial test or tests.

(c) ***Establishment of hydrochloric acid regeneration plant operating parameters.***

(1) During the performance test for hydrochloric acid regeneration plants, the owner or operator shall establish site-specific operating parameter values for the minimum process offgas temperature and the maximum proportion of excess air fed to the process as described in [§ 63.1162\(b\)\(1\) of this subpart](#). During the emission test, each operating parameter must be monitored and recorded with sufficient frequency to establish a representative average value for that parameter, but no less frequently than once every 15 minutes for parameters that are monitored continuously. Amount of iron in the spent pickle liquor shall be determined for each run by sampling the liquor every 15 minutes and analyzing a composite of the samples. The owner or operator shall determine the compliant monitoring values as the averages of the values recorded during any of the runs for which results are used to establish the emission concentration per [paragraph \(a\)\(2\)](#) of this section. An owner or operator may conduct multiple performance tests to establish alternative compliant operating parameter values. Also, an owner or operator may reestablish compliant operating parameter values as part of any performance test that is conducted subsequent to the initial test or tests.

(2) [Reserved]

(d) ***Test methods.***

(1) The following test methods in appendix A of [40 CFR part 60](#) shall be used to determine compliance under [§§ 63.1157\(a\)](#), [63.1157\(b\)](#), [63.1158\(a\)](#), and [63.1158\(b\) of this subpart](#):

(i) Method 1, to determine the number and location of sampling points, with the exception that no traverse point shall be within one inch of the stack or duct wall;

(ii) Method 2, to determine gas velocity and volumetric flow rate;

(iii) Method 3, to determine the molecular weight of the stack gas;

(iv) Method 4, to determine the moisture content of the stack gas; and

(v) Method 26A, "Determination of Hydrogen Halide and Halogen Emissions from Stationary Sources - Isokinetic Method," to determine the HCl mass flows at the inlet and outlet of a control device or the concentration of HCl discharged to the atmosphere, and also to determine the concentration of Cl₂ discharged to the atmosphere from acid regeneration plants. If compliance with a collection efficiency standard is being demonstrated, inlet and outlet measurements shall be performed simultaneously. The minimum sampling time for each run shall be 60 minutes and the minimum sample volume 0.85 dry standard cubic meters (30 dry standard cubic feet). The concentrations of HCl and Cl₂ shall be calculated for each run as follows:

$$C_{\text{HCl}} (\text{ppmv}) = 0.659 C_{\text{HCl}} (\text{mg/dscm}),$$

$$\text{and } C_{\text{Cl}_2} (\text{ppmv}) = 0.339 C_{\text{Cl}_2} (\text{mg/dscm}),$$

where C(ppmv) is concentration in ppmv and C(mg/dscm) is concentration in milligrams per dry standard cubic meter as calculated by the procedure given in Method 26A.

(2) The owner or operator may use equivalent alternative measurement methods approved by the Administrator.

[[64 FR 33218](#), June 22, 1999, as amended at [77 FR 58251](#), Sept. 19, 2012]

§ 63.1162 Monitoring requirements.

(a) The owner or operator of a new, reconstructed, or existing steel pickling facility or acid regeneration plant subject to this subpart shall:

(1) Conduct performance tests to measure the HCl mass flows at the control device inlet and outlet or the concentration of HCl exiting the control device according to the procedures described in [§ 63.1161 of this subpart](#). Performance tests shall be conducted either annually or according to an alternative schedule that is approved by the applicable permitting authority, but no less frequently than every 2 1/2 years or twice per title V permit term. If any performance test shows that the HCl emission limitation is being exceeded, then the owner or operator is in violation of the emission limit.

(2) In addition to conducting performance tests, if a wet scrubber is used as the emission control device, install, operate, and maintain systems for the measurement and recording of the scrubber makeup water flow rate and, if required, recirculation water flow rate. These flow rates must be monitored continuously and recorded at least once per shift while the scrubber is operating. Operation of the wet scrubber with excursions of scrubber makeup water flow rate and recirculation water flow rate less than the minimum values established during the performance test or tests will require initiation of corrective action as specified by the maintenance requirements in [§ 63.1160\(b\)\(2\) of this subpart](#).

(3) If an emission control device other than a wet scrubber is used, install, operate, and maintain systems for the measurement and recording of the appropriate operating parameters.

(4) Failure to record each of the operating parameters listed in [paragraph \(a\)\(2\)](#) of this section is a violation of the monitoring requirements of this subpart.

(5) Each monitoring device shall be certified by the manufacturer to be accurate to within 5 percent and shall be calibrated in accordance with the manufacturer's instructions but not less frequently than once per year.

(6) The owner or operator may develop and implement alternative monitoring requirements subject to approval by the Administrator.

(b) The owner or operator of a new, reconstructed, or existing acid regeneration plant subject to this subpart shall also install, operate, and maintain systems for the measurement and recording of the:

(1) Process offgas temperature, which shall be monitored continuously and recorded at least once every shift while the facility is operating in production mode; and

(2) Parameters from which proportion of excess air is determined. Proportion of excess air shall be determined by a combination of total air flow rate, fuel flow rate, spent pickle liquor addition rate, and amount of iron in the spent pickle liquor, or by any other combination of parameters approved by the Administrator in accordance with [§ 63.8\(f\)](#) of [subpart A of this part](#). Proportion of excess air shall be determined and recorded at least once every shift while the plant is operating in production mode.

(3) Each monitoring device must be certified by the manufacturer to be accurate to within 5 percent and must be calibrated in accordance with the manufacturer's instructions but not less frequently than once per year.

(4) Operation of the plant with the process offgas temperature lower than the value established during performance testing or with the proportion of excess air greater than the value established during performance testing is a violation of the operational standard specified in [§ 63.1159\(a\)](#) of [this subpart](#).

(c) The owner or operator of an affected hydrochloric acid storage vessel shall inspect each vessel semiannually to determine that the closed-vent system and either the air pollution control device or the enclosed loading and unloading line, whichever is applicable, are installed and operating when required.

§ 63.1163 Notification requirements.

(a) *Initial notifications.* As required by [§ 63.9\(b\)](#) of [subpart A of this part](#), the owner or operator shall submit the following written notifications to the Administrator:

(1) The owner or operator of an area source that subsequently becomes subject to the requirements of the standard shall provide notification to the applicable permitting authority as required by [§ 63.9\(b\)\(1\)](#) of [subpart A of this part](#).

(2) As required by [§ 63.9\(b\)\(2\)](#) of [subpart A of this part](#), the owner or operator of an affected source that has an initial startup before June 22, 1999, shall notify the Administrator that the source is subject to the requirements of the standard. The notification shall be submitted not later than October 20, 1999 (or within 120 calendar days after the source becomes subject to this standard), and shall contain the information specified in [§§ 63.9\(b\)\(2\)\(i\)](#) through [63.9\(b\)\(2\)\(v\)](#) of [subpart A of this part](#).

(3) As required by [§ 63.9\(b\)\(3\)](#) of [subpart A of this part](#), the owner or operator of a new or reconstructed affected source, or a source that has been reconstructed such that it is an affected source, that has an initial startup after the effective date and for which an application for approval of construction or reconstruction is not required under [§ 63.5\(d\)](#) of [subpart A of this part](#), shall notify the Administrator in writing that the source is subject to the standards no later than 120 days after initial startup, or no later than 120 days after the source becomes subject to this subpart, whichever is later. The notification shall contain the information specified in [§§ 63.9\(b\)\(2\)\(i\)](#) through [\(v\)](#) of [subpart A of this part](#), delivered or postmarked with the notification required in [§ 63.9\(b\)\(5\)](#) of [subpart A of this part](#).

(4) As required by [§ 63.9\(b\)\(4\)](#) of [subpart A of this part](#), the owner or operator of a new or reconstructed major affected source that has an initial startup after June 22, 1999, and for which an application for approval of construction or reconstruction is required under [§ 63.5\(d\)](#) of [subpart A of this part](#) shall provide the information specified in [§§ 63.9\(b\)\(4\)\(i\)](#) through [63.9\(b\)\(4\)\(v\)](#) of [subpart A of this part](#).

(5) As required by [§ 63.9\(b\)\(5\)](#) of [subpart A of this part](#), the owner or operator who, after June 22, 1999, intends to construct a new affected source or reconstruct an affected source subject to this standard, or reconstruct a source such that it becomes an affected source subject to this standard, shall notify the Administrator, in writing, of the intended construction or reconstruction.

(b) ***Request for extension of compliance.*** As required by [§ 63.9\(c\)](#) of [subpart A of this part](#), if the owner or operator of an affected source cannot comply with this standard by the applicable compliance date for that source, or if the owner or operator has installed BACT or technology to meet LAER consistent with [§ 63.6\(i\)\(5\)](#) of [subpart A of this part](#), he/she may submit to the Administrator (or the State with an approved permit program) a request for an extension of compliance as specified in [§§ 63.6\(i\)\(4\)](#) through [63.6\(i\)\(6\)](#) of [subpart A of this part](#).

(c) ***Notification that source is subject to special compliance requirements.*** As required by [§ 63.9\(d\)](#) of [subpart A of this part](#), an owner or operator of a new source that is subject to special compliance requirements as specified in [§§ 63.6\(b\)\(3\)](#) and [63.6\(b\)\(4\)](#) of [subpart A of this part](#) shall notify the Administrator of his/her compliance obligations not later than the notification dates established in [§ 63.9\(b\)](#) of [subpart A of this part](#) for new sources that are not subject to the special provisions.

(d) ***Notification of performance test.*** As required by [§ 63.9\(e\)](#) of [subpart A of this part](#), the owner or operator of an affected source shall notify the Administrator in writing of his or her intention to conduct a performance test at least 60 calendar days before the performance test is

scheduled to begin, to allow the Administrator to review and approve the site-specific test plan required under [§ 63.7\(c\)](#) of [subpart A of this part](#) and, if requested by the Administrator, to have an observer present during the test.

(e) **Notification of compliance status.** The owner or operator of an affected source shall submit a notification of compliance status as required by [§ 63.9\(h\)](#) of [subpart A of this part](#) when the source becomes subject to this standard.

[[64 FR 33218](#), June 22, 1999, as amended at [85 FR 73897](#), Nov. 19, 2020]

§ 63.1164 Reporting requirements.

(a) **Reporting results of performance tests.** Within 60 days after the date of completing each performance test (defined in [§ 63.2](#)), as required by this subpart you must submit the results of the performance tests, including any associated fuel analyses, required by this subpart to the EPA's WebFIRE database by using the Compliance and Emissions Data Reporting Interface (CEDRI) that is accessed through the EPA's Central Data Exchange (CDX) (www.epa.gov/cdx). Performance test data must be submitted in the file format generated through use of the EPA's Electronic Reporting Tool (ERT) (see <http://www.epa.gov/ttn/chief/ert/index.html>). Only data collected using test methods on the ERT Web site are subject to this requirement for submitting reports electronically to WebFIRE. Owners or operators who claim that some of the information being submitted for performance tests is confidential business information (CBI) must submit a complete ERT file including information claimed to be CBI on a compact disk, flash drive or other commonly used electronic storage media to the EPA. The electronic media must be clearly marked as CBI and mailed to U.S. EPA/OAPQS/CORE CBI Office, Attention: WebFIRE Administrator, MD C404-02, 4930 Old Page Rd., Durham, NC 27703. The same ERT file with the CBI omitted must be submitted to the EPA via CDX as described earlier in this paragraph. At the discretion of the delegated authority, you must also submit these reports, including the confidential business information, to the delegated authority in the format specified by the delegated authority. For any performance test conducted using test methods that are not listed on the ERT Web site, the owner or operator shall submit the results of the performance test to the Administrator at the appropriate address listed in [§ 63.13](#).

(b) **Progress reports.** The owner or operator of an affected source who is required to submit progress reports under [§ 63.6\(i\)](#) of [subpart A of this part](#) shall submit such reports to the Administrator (or the State with an approved permit program) by the dates specified in the written extension of compliance.

(c) **Reporting malfunctions.** The number, duration, and a brief description for each type of malfunction which occurred during the reporting period and which caused or may have caused any applicable emission limitation to be exceeded shall be stated in a semiannual report. The report must also include a description of actions taken by an owner or operator during a malfunction of an affected source to minimize emissions in accordance with [§ 63.1159\(c\)](#), including actions taken to correct a malfunction. The report, to be certified by the owner or

operator or other responsible official, shall be submitted semiannually and delivered or postmarked by the 30th day following the end of each calendar half.

[[64 FR 33218](#), June 22, 1999, as amended at [71 FR 20458](#), Apr. 20, 2006; [77 FR 58251](#), Sept. 19, 2012]

§ 63.1165 Recordkeeping requirements.

(a) *General recordkeeping requirements.* As required by [§ 63.10\(b\)\(2\)](#) of [subpart A of this part](#), the owner or operator shall maintain records for 5 years from the date of each record of:

- (1) The occurrence and duration of each malfunction of operation (*i.e.*, process equipment);
- (2) The occurrence and duration of each malfunction of the air pollution control equipment;
- (3) All maintenance performed on the air pollution control equipment;
- (4) Actions taken during periods of malfunction to minimize emissions in accordance with [§ 63.1259\(c\)](#) and the dates of such actions (including corrective actions to restore malfunctioning process and air pollution control equipment to its normal or usual manner of operation);
- (5) All required measurements needed to demonstrate compliance with the standard and to support data that the source is required to report, including, but not limited to, performance test measurements (including initial and any subsequent performance tests) and measurements as may be necessary to determine the conditions of the initial test or subsequent tests;
- (6) All results of initial or subsequent performance tests;
- (7) If the owner or operator has been granted a waiver from recordkeeping or reporting requirements under [§ 63.10\(f\)](#) of [subpart A of this part](#), any information demonstrating whether a source is meeting the requirements for a waiver of recordkeeping or reporting requirements;
- (8) If the owner or operator has been granted a waiver from the initial performance test under [§ 63.7\(h\)](#) of [subpart A of this part](#), a copy of the full request and the Administrator's approval or disapproval;
- (9) All documentation supporting initial notifications and notifications of compliance status required by [§ 63.9](#) of [subpart A of this part](#); and
- (10) Records of any applicability determination, including supporting analyses.

(b) *Subpart CCC records.*

(1) In addition to the general records required by [paragraph \(a\)](#) of this section, the owner or operator shall maintain records for 5 years from the date of each record of:

(i) Scrubber makeup water flow rate and recirculation water flow rate if a wet scrubber is used;

(ii) Calibration and manufacturer certification that monitoring devices are accurate to within 5 percent; and

(iii) Each maintenance inspection and repair, replacement, or other corrective action.

(2) The owner or operator of an acid regeneration plant shall also maintain records for 5 years from the date of each record of process offgas temperature and parameters that determine proportion of excess air.

(3) The owner or operator shall keep the written operation and maintenance plan on record after it is developed to be made available for inspection, upon request, by the Administrator for the life of the affected source or until the source is no longer subject to the provisions of this subpart. In addition, if the operation and maintenance plan is revised, the owner or operator shall keep previous (i.e., superseded) versions of the plan on record to be made available for inspection by the Administrator for a period of 5 years after each revision to the plan.

(c) **Recent records.** General records and subpart CCC records for the most recent 2 years of operation must be maintained on site. Records for the previous 3 years may be maintained off site.

[[64 FR 33218](#), June 22, 1999, as amended at [77 FR 58251](#), Sept. 19, 2012]

§ 63.1166 Implementation and enforcement.

(a) This subpart can be implemented and enforced by the U.S. EPA, or a delegated authority such as the applicable State, local, or Tribal agency. If the U.S. EPA Administrator has delegated authority to a State, local, or Tribal agency, then that agency, in addition to the U.S. EPA, has the authority to implement and enforce this subpart. Contact the applicable U.S. EPA Regional Office to find out if implementation and enforcement of this subpart is delegated to a State, local, or Tribal agency.

(b) In delegating implementation and enforcement authority of this subpart to a State, local, or Tribal agency under [subpart E of this part](#), the authorities contained in [paragraph \(c\)](#) of this section are retained by the Administrator of U.S. EPA and cannot be transferred to the State, local, or Tribal agency.

(c) The authorities that cannot be delegated to State, local, or Tribal agencies are as specified in [paragraphs \(c\)\(1\)](#) through [\(8\)](#) of this section.

- (1) Approval of alternatives to the requirements in §§ [63.1155](#), [63.1157](#) through [63.1159](#), and [63.1160\(a\)](#).
- (2) Approval of major alternatives to test methods under [§ 63.7\(e\)\(2\)\(ii\)](#) and [\(f\)](#), as defined in [§ 63.90](#), and as required in this subpart.
- (3) Approval of any alternative measurement methods for HCl and CL₂ to those specified in [§ 63.1161\(d\)\(1\)](#).
- (4) Approval of major alternatives to monitoring under [§ 63.8\(f\)](#), as defined in [§ 63.90](#), and as required in this subpart.
- (5) Approval of any alternative monitoring requirements to those specified in §§ [63.1162\(a\)\(2\)](#) through [\(5\)](#) and [63.1162\(b\)\(1\)](#) through [\(3\)](#).
- (6) Approval of major alternatives to recordkeeping and reporting under [§ 63.10\(f\)](#), as defined in [§ 63.90](#), and as required in this subpart.
- (7) Waiver of recordkeeping requirements specified in [§ 63.1165](#).
- (8) Approval of an alternative schedule for conducting performance tests to the requirement specified in [§ 63.1162\(a\)\(1\)](#).

[[68 FR 37356](#), June 23, 2003]

§§ 63.1167-63.1174 [Reserved]

Table 1 to Subpart CCC of Part 63 - Applicability of General Provisions ([40 CFR Part 63, Subpart A](#)) to Subpart CCC

Reference	Applies to Subpart CCC	Explanation
63.1-63.5	Yes.	
63.6 (a)-(d)	Yes	
63.6(e)(1)(i)	No	See § 63.1259(c) for general duty requirement. Any cross-reference to § 63.6(e)(1)(i) in any other general provision incorporated by reference shall be treated as a cross-reference to §

Reference	Applies to Subpart CCC	Explanation
		63.1259(c) .
63.6(e)(1)(ii)	No	
63.6(e)(1)(iii)	Yes	
63.6(e)(2)	No	Section reserved.
63.6(e)(3)	No	
63.6(f)(1)	No	
63.6(f)(2)-(3)	Yes	
63.6(g)	Yes	
63.6(h)	No	Subpart CCC does not contain an opacity or visible emission standard.
63.6 (i)-(j)	Yes.	
63.7	Yes	
63.8(a)-(c)	Yes	
63.8(d)(1)-(2)	Yes	
63.8(d)(3)	Yes, except for last sentence	
63.8(e)-(f)	Yes	
63.9(j)	Yes	
63.9(k)	Yes	Only as specified in § 63.9(j) .
63.10(a)	Yes	

Reference	Applies to Subpart CCC	Explanation
63.10(b)(1)	Yes	
63.10(b)(2)(i)	No	
63.10(b)(2)(ii)	No	See § 63.1265(a)(1) for recordkeeping of occurrence and duration of malfunctions. See § 63.1265(a)(4) for recordkeeping of actions taken during malfunction. Any cross-reference to § 63.10(b)(2)(ii) in any other general provision incorporated by reference shall be treated as a cross-reference to § 63.1265(a)(1) .
63.10(b)(2)(iii)	Yes	
63.10(b)(2)(iv)-(b)(2)(v)	No	
63.10(b)(2)(vi)-(b)(2)(xiv)	Yes	
63.10(b)(3)	Yes	
63.10(c)(1)-(9)	Yes	
63.10(c)(10)	No	See § 63.1164(c) for reporting malfunctions. Any cross-reference to § 63.10(c)(10) in any other general provision incorporated by reference shall be treated as a cross-reference to § 63.1164(c) .
63.10(c)(11)	No	See § 63.1164(c) for reporting malfunctions. Any cross-reference to § 63.10(c)(11) in any other general provision incorporated by reference shall be treated as a cross-reference to § 63.1164(c) .
63.10(c)(12)-(c)(14)	Yes	
63.10(c)(15)	No	
63.10(d)(1)-(2)	Yes.	
63.10(d)(3)	No	Subpart CCC does not contain an opacity or visible emission

Reference	Applies to Subpart CCC	Explanation
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standard.

63.10(d)(4) Yes

63.10(d)(5) No

63.10(e)-(f) Yes.

63.11 No Subpart CCC does not require the use of flares.

63.12-63.15 Yes

[[64 FR 33218](#), June 22, 1999, as amended at [77 FR 58252](#), Sept. 19, 2012; [85 FR 73897](#), Nov. 19, 2020]

Appendix I

Case by Case Basis Analysis for the Electric Arc Furnaces (SN-01 and SN-02)

December 10, 2021

Mr. Thomas Rheaume
Senior Operations Manager / Air Permits
Arkansas Department of Energy and Environment, Division of Environmental Quality (AEEDEQ)
Air Quality Division
5301 Northshore Drive
North Little Rock, AR 72118

Re: ePortal Electronic Submission
Proposed Steel Mill Project - Air Permit Application
Supplement #1: Case-By-Case MACT Review – Proposed Electric Arc Furnaces (EAFs)
Big River Steel LLC
Osceola, Arkansas Scrap to Steel Mill

Dear Mr. Rheaume:

On September 20, 2021, Big River Steel LLC (BRS) submitted an air permit application for a Prevention of Significant Deterioration (PSD) Major Modification to the BRS Osceola, Arkansas Scrap to Steel Mill. The application represented a request from BRS to the Arkansas Department of Energy and Environment, Division of Environmental Quality (AEEDEQ) to issue a construction / operating permit which would allow BRS to construct / operate a new scrap to steel mill project at the Osceola, Arkansas mill site, referred to as the “Proposed Steel Mill Project”. This document hereby represents a supplement to that air permit application, referred to as Supplement #1. The purpose of this supplement is to clarify, to the AEEDEQ, the applicability of the Environmental Protection Agency’s (EPA’s) National Emission Standards for Hazardous Air Pollutants (NESHAP) provisions for the control of regulated Hazardous Air Pollutants (HAPs) as they pertain to installation / operation of two Electric Arc Furnaces (EAFs) that are part of the Proposed Steel Mill Project.

This supplement hereby addresses two (2) key items related to the applicability of EPA’s NESHAP provisions to the Proposed Steel Mill Project’s EAFs: (1) amendment of the September 20, 2021 air permit application to clarify that 40 CFR Part 63, Subpart EEEEE (NESHAP for Iron and Steel Foundries) is not applicable to the Proposed Steel Mill Project; and (2) establish case-by-case Maximum Achievable Control Technology (MACT) limitations for the two EAFs associated with the Proposed Steel Mill Project.

Included in this supplement, is an overview of EPA’s NESHAP provisions as defined in 40 CFR Part 63, review of EPA’s NESHAP provisions related to the Steel Industry, the non-applicability of NESHAP Subpart EEEEE to the Proposed Steel Mill Project, non-applicability determination of other promulgated NESHAP provisions, and a Case-by-Case MACT determination for the EAFs associated with the Proposed Steel Mill Project.

General Overview of EPA’s NESHAP Provisions

The 1990 amendments to the Clean Air Act (CAA) mandated significant new air quality programs, including the National Emissions Standards for Hazardous Air Pollutants (NESHAP) program.

42 U.S.C.A § 7412 (referred to as CAA Section 112) addresses the reduction of emissions of HAPs. Section 112 includes provisions for the promulgation of NESHAP, or maximum achievable control technology (MACT) standards. The subsections of § 112 that are relevant to the construction of new stationary sources with the potential to emit regulated Hazardous Air Pollutants (as defined under Section 112 (b)), are summarized below:

- List of Source Categories: Requires that the EPA publish and regularly update (at least every 8 years) a listing of all categories and subcategories of major and area sources that emit HAPs as well as requirements

associated with delisting categories and subcategories. 42 U.S.C. § 7412(c). The list of source categories itself is not contained in the CAA; it was initially published in the Federal Register on July 16, 1992 (56 FR 31576).

- **Emission Standards:** States that the EPA must promulgate regulations establishing emission standards (NESHAP) for each category or subcategory of major sources and area sources of HAPs [listed pursuant to Section 112(c)]. The standards must require the maximum degree of emission reduction that the EPA determines to be achievable by each particular source category. Different criteria for maximum achievable control technology (MACT) apply for new and existing sources. Less stringent standards, known as generally available control technology (GACT) standards, are allowed at the Administrator's discretion for area sources. 42 U.S.C. § 7412(d)
- **Modifications, Construction and Reconstruction:** Requires owners or operators of newly constructed, reconstructed, and modified major sources of HAPs to apply MACT if emission increases are above certain levels. For purposes of Section 112(g) sources must submit a pre-construction permit application proposing source-specific MACT. 42 U.S.C. § 7412(g).
- **Work Practice Standards and Other Requirements:** Allows the EPA, in cases where it is not feasible to prescribe or enforce an emission standard [under Section 112(d) or (f)], to promulgate a design, equipment, work practice, or operational standard. Also allows an owner or operator to use an alternative means of emission reduction if it can be proven that an equal reduction in emissions of any HAP will be achieved. 42 U.S.C. § 7412(h).
- **Equivalent Emission Limitation by Permit:** Ensures control of HAP emissions even if the EPA should miss a scheduled NESHAP promulgation date. If the EPA misses a scheduled promulgation date by 18 months, major sources in that category must submit to their respective State (or local) agencies a permit application proposing source-specific MACT. Conditions of the MACT determination must be incorporated into the Title V operating permit. Section 112(j) is commonly referred to as the "MACT hammer." 42 U.S.C. § 7412(j).

Review of EPA's NESHAP Provisions - Steel Industry

Pursuant to the various specific listing requirements in § 112(c), on July 16, 1992 EPA finalized its initial list of 174 categories of major and area sources that would be subject to emission standards. 57 Fed. Reg. 31576 (July 16, 1992). The following categories were included on EPA's list that used the term "Steel":

- Integrated Iron and Steel Manufacturing;
- Non-stainless-Steel Manufacturing - Electric Arc Furnace (EAF) Operation;
- Stainless-Steel Manufacturing - Electric Arc Furnace (EAF) Operation;
- Steel Foundries; and
- Steel Pickling - HCL Process.

EPA's original list included only "major sources" of HAPs within these categories. *Id.* at 31591 - 31592. On December 3, 1993, EPA published a schedule for promulgations of emissions standards for the following steel categories:

- Integrated Iron and Steel Manufacturing - November 15, 2000;
- Non-stainless-Steel Manufacturing - Electric Arc Furnace (EAF) Operation - November 15, 1997;
- Stainless-Steel Manufacturing - Electric Arc Furnace (EAF) Operation - November 15, 1997;

- Steel Foundries - November 15, 2000; and
- Steel Pickling – HCL Process – November 15, 1997.

58 Fed. Reg. 63941 (December 3, 1993). On June 4, 1996 EPA revised the list of categories and deleted the Non-Stainless-Steel Manufacturing – Electric Arc Furnace (EAF) Operation and the Stainless-Steel Manufacturing – Electric Arc Furnace (EAF) Operation categories. 61 Fed. Reg. 28197 (June 4, 1996). In doing so, EPA stated that these categories were being removed since (1) there were no existing facilities which qualified as major sources; (2) arsenic, antimony, beryllium, cadmium, chromium, cobalt, lead, manganese, mercury, nickel and selenium are believed to be the only HAPs emitted from the EAF source categories; (3) EPA determined that “worse case” total facility HAP emissions from the EAFs operating at the time would emit about “one half of the amount of HAP which would classify them as major sources”; and (4) existing facilities were already subject to the NSPS for EAF operations (specifically, 40 C.F.R. Subpart AAa) which regulates the air pollution control device outlet concentration and visible emissions from the EAF Melt Shop and any new facilities would likewise be subject to the NSPS. Id. at 28201.

On June 26, 2002, EPA added “Stainless and Nonstainless Steel Manufacturing Electric Arc Furnaces” and “Steel Foundries” to its source category list for “area sources” of HAPs. 67 Fed. Reg. 43112. Subsequently, on December 28, 2007 EPA finalized its NESHAP applicable to “Electric Arc Furnace Steelmaking Facilities”¹ at “area sources” of HAPs. 72 Fed. Reg. 74087. This subpart is referred to as NESHAP Subpart YYYYY and applies to EAFs at steelmaking facilities. In connection with its proposed rule to adopt Subpart YYYYY, USEPA noted that it had identified two EAF facilities co-located at integrated iron and steel plants that are major sources. 72 Fed. Reg. 53814, 53819 (Sept. 20, 2007). While stating that the existence of these two EAF facilities did not preclude it from adopting Subpart YYYYY, EPA stated that it intended to add “EAF steelmaking facilities” at major sources of HAPs to its list under CAA § 112(c) and to develop a NESHAP for such facilities. Id. at 53816. EPA has not yet added this major source category to its list or conducted rulemaking to adopt a NESHAP for EAF steelmaking facilities at major sources of HAPs.

Applicability of NESHAP Subparts to the Proposed Steel Mill Project EAFs

As discussed in the September 20, 2021 PSD air permit application, for the Proposed Steel Mill Project, BRS conducted a review of EPA’s promulgated NESHAP provisions to determine the applicability of these provisions to the Proposed Steel Mill Project. A discussion of BRS’s initial review of these provisions is provided below, as well as a discussion on BRS’s review of EPA’s history of promulgated NESHAPs as they pertain to emission sources associated with the Steel Industry.

Initial Review of NESHAP Subpart EEEEE

In section 3.0 of the application, a review of applicable state and federal air regulations was presented, as it pertains to the new emission units of regulated New Source Review (NSR) air pollutants associated with the Proposed Steel Mill Project. In subsection 3.3.4.5 a discussion was provided on the applicability of the National Emission Standards for Hazardous Air Pollutants (NESHAP) Subpart EEEEE “National Emission Standards for Hazardous Air Pollutants for Iron and Steel Foundries”. This Subpart is codified under Section 40 of the Code of Federal Regulations (CFR), Part 63, Subpart EEEEE.

¹ Note that EPA changed the name of this source category from “Stainless and Nonstainless Steel Manufacturing Electric Arc Furnaces” to “Electric Arc Furnace Steelmaking Facilities” in connection with its final rule adopting Subpart YYYYY. 72 Fed. Reg. 53814, 53817. It did so to clarify that all types of steel made in an EAF, such as stainless steel, carbon steel, specialty steel, and other grades and alloys of steel would be included in this subcategory.

During the initial review of applicable federal air regulations, a review of Subpart EEEEE was conducted. That review included §§ 63.7680 and 63.7681 of Subpart EEEEE, which discuss the purpose of Subpart EEEEE and identify processes/production units at foundries subject to Subpart EEEEE. These sections do not include a reference to the NAICS Codes, however, Subpart EEEEE does include the following definition of “Iron and Steel Foundry”:

- A facility or portion of a facility that melts scrap, ingot, and /or other forms of iron and / or steel and pours the resulting molten metal into molds to produce final or near final shape products for introduction into commerce.
- Metal melting furnace means a cupola, electric arc furnace, or electric induction furnace that converts scrap, foundry returns, and / or other solid forms of iron and / or steel to a liquid state.

40 C.F.R. § 63.7765. During the initial review of these definitions, it was determined that this Subpart may be applicable to the EAFs associated with the Proposed Steel Mill Project, but there was an area of potential confusion concerning whether the casting process to be used at the Proposed Steel Mill Project would be considered a molding process. As such, this Subpart was listed as an applicable requirement in the September 20, 2021 application with the understanding that further evaluation could be conducted after discussions with the AEEDEQ.

NESHAP Subpart EEEEE Is Not Applicable to the Proposed Steel Mill Project

BRS has further assessed the applicability of Subpart EEEEE to the EAFs associated with the Proposed Steel Mill Project from a technical and legal perspective. Based upon this review, BRS has concluded that Subpart EEEEE is not applicable to the EAFs at the Proposed Steel Mill Project for the reasons stated below.

In connection with the final rule adopting Subpart EEEEE, EPA included a table that identified three Industry NAICS Codes as “Regulated Entities.” Specifically:

“Categories and entities potentially regulated by this action include:

331511 | Iron foundries, Iron and Steel plants. Automotive and large equipment manufacturers.

331512 | Steel investment foundries.

331513 | Steel foundries (except investment).”

69 Fed. Reg. 21906 (April 22, 2004). As stated in the September 20, 2021 application, the Proposed Steel Mill Project is classified under NAICS Code 331110 which pertains to Iron and Steel Mills and Ferroalloy Manufacturing (i.e., Electric Arc Furnace Steelmaking Facilities).² NAICS Code 331110 is not included in the list of industry categories being regulated by EPA under Subpart EEEEE. Conversely, NAICS Code 331110 is identified in the final rule adopting Subpart YYYYY (NESHAP for Area Sources: Electric Arc Steelmaking Facilities).³ Based on the inclusion

² NAICS Code 331110 (2017) provides the following description for the Iron and Steel Mills and Ferroalloy Manufacturing classification: This industry comprises establishments primarily engaged in one or more of the following: (1) direct reduction of iron ore; (2) manufacturing pig iron in molten or solid form; (3) converting pig iron into steel; (4) making steel; (5) making steel and manufacturing shapes (e.g., bar, plate, rod, sheet, strip, wire); (6) making steel and forming pipe and tube; and (7) manufacturing electrometallurgical ferroalloys. Ferroalloys add critical elements, such as silicon and manganese for carbon steel and chromium, vanadium, tungsten, titanium, and molybdenum for low- and high-alloy metals. Ferroalloys include iron-rich alloys and more pure forms of elements added during the steel manufacturing process that alter or improve the characteristics of the metal.

³ Note that USEPA’s final rule adopting Subpart YYYYY refers to NAICS code 331111, which was the NAICS code classification for Iron and Steel Mills and Ferroalloy Manufacturing at the time of that rulemaking (i.e., 2007). 72 Fed. Reg. 53814 (September 20, 2007). In 2012, the NAICS code classification for Iron and Steel Mills and

of specific references to NAICS codes 331511, 331512 and 33153 and the specific omission of NAICS Code 331110 (or NAICS Code 331111 (see footnote 3)) in connection with the final rule adopting Subpart EEEEE BRS believes that EPA intended for Subpart EEEEE to apply to EAFs at an “Iron and Steel Foundry” and not to EAFs at an Electric Arc Furnace Steelmaking Facility.

Moreover, the Proposed Steel Mill Project does not meet the definition of an iron and steel foundry provided in the final rule adopting Subpart EEEEE nor does it have the operations or manufacture the type of steel products contemplated by the NAICS Codes referenced in this rulemaking (i.e., 331511, 331512 and 331513). In discussing the type of facilities that would be subject to Subpart EEEEE, EPA provided the following definition for Iron and Steel Foundry:

“A facility that melts scrap, ingot and / or other forms of Iron and / or steel and pour the resulting molten metal into molds to produce final or near final shape products for introduction into commerce.”

78 Fed. 21906, 21907. The NAICS codes referenced by EPA in the final rule (i.e., 331511, 331512 and 331513) are consistent with this definition and contemplate pouring molten iron and steel into specifically designed molds typically consisting of wax covered with ceramic or sand to cast the final or near final shape of products. The NAICS code descriptions note that most of the facilities within these codes do not produce their own steel.

The Proposed Steel Mill Project will melt metal scrap using two (2) EAFs and will then pour the resulting molten metal into a casting process. The casting process forms a continuous steel coil. The steel coil is cut and rolled at the end of that casting process. The steel coils produced by BRS may then be further processed to meet customer specification. However, the steel coils to be produced by the Proposed Steel Mill Project will not represent a final or near final shape of the product that ultimately will be produced by BRS’s customers.

Finally, it is important to note that EPA, in connection with its rulemaking efforts related to the iron and steel industry, has already addressed Electric Arc Furnace Steelmaking Facilities (i.e., EAFs used to melt scrap steel and hot briquetted iron to produce coiled steel products) and Iron and Steel Foundries in separate rulemaking proceedings. In EPA’s initial list of categories of major and area sources of HAPS under CAA § 112(c)(1), EPA identified Non-Stainless and Stainless-Steel Manufacturing---Electric Arc Furnace Operations and Iron/Steel Foundries as unique and separate source categories for the purposes of the development of NESHAPs. 57 Fed. Reg. 31576, 31591. This distinction has continued and is clearly demonstrated by the definition used for the term “Electric arc furnace (EAF) steelmaking facility” used in the area source NESHAP (Subpart YYYYY).

40 CFR Part 63, Subpart YYYYY defines the term “Electric arc furnace (EAF) steelmaking facility” as “a steel plant that produces carbon, alloy, or specialty steels using an EAF. This definition excludes EAF steelmaking facilities at steel foundries and EAF facilities used to produce nonferrous metals.” 40 CFR § 63.106692; see also 72 Fed. Reg. 53814, 53835 (September 20, 2007) (proposing to exclude “EAF Steelmaking facilities at steel foundries” from Subpart YYYYY) and 72 Fed. Reg. 74087, 740108 (December 28, 2007) (retaining exclusion of “EAF Steelmaking facilities at steel foundries” from Subpart YYYYY and, in response to comment, adding additional exclusion for “EAF facilities used to produce nonferrous metals.”). The EAFs to be installed in connection with the Proposed Steel Mill Project are similar to those currently in operation at the BRS location. In short, it is clear from the definition of “Electric Arc Furnace (EAF) steelmaking facility” in Subpart YYYYY that USEPA did not intend to regulate under Subpart EEEEE EAFs that melt scrap steel to make coiled steel products such as the Proposed Steel Mill Project.

Ferroalloy Manufacturing changed to 331110 and this classification was retained by NAICS in connection with its most current update. No substantive changes to the description of the Iron and Steel Mills and Ferroalloy Manufacturing classification were made in connection with the transition from NAICS code 331111 to 331110 in 2012.

Accordingly, based upon the foregoing regulatory and technical analysis, BRS has concluded that Subpart EEEEE does not apply to the EAFs and related equipment and operations at the Proposed Steel Mill Project.

Review of other Applicable NESHAP Provision to the Proposed Steel Mill Project (Electric Arc Furnaces)

Consequently, since Subpart EEEEE has been determined to not apply to the Proposed Steel Mill Project, a review of other promulgated NESHAP Subparts was performed by BRS to determine applicability to the Two (2) EAFs associated with the Proposed Steel Mill Project. The four steps followed by BRS to determine applicable MACT provisions are provided below:

First Step – Review of Current Promulgated NESHAP Provisions for Electric Arc Furnaces at Steelmaking Facilities

The first step was to review the source categories, developed by EPA, that would be subject to emission reductions of regulated hazardous air pollutants (HAPs). On February 12, 2002, EPA published a revision to the source category list under Section 112 of the Clean Air Act. 67 Fed. Reg. 6521. In this notice, EPA stated it was providing a revision to the list of categories of major and area sources of HAP emissions.

Specifically, EPA listed specific source categories. The category developed for the steel industry was defined as: “Ferrous Metals Processing.” EPA did establish NESHAP provisions for several manufacturing categories that pertained to the steel industry. Provided below is a listing of current NESHAP provisions promulgated by EPA for manufacturing categories as they pertain to the steel industry:

- Integrated Iron and Steel Manufacturing (Subpart FFFFF);
- Steel Foundries (Subpart EEEEE); and
- Steel Pickling – HCL process Facilities and Hydrochloric Acid Regeneration Plants (Subpart CCC). Please note that this Subpart was listed by BRS as an applicable NESHAP provision and will apply to the HCL process associated with the Proposed Steel Mill Project. This supplement will not further discuss the requirements of this Subpart. Refer to the initial application, dated September 20, 2021.

As discussed above, the following source categories were deleted by EPA under the NESHAP provisions for the steel industry:

- Non-Stainless-Steel Manufacturing – Electric Arc Furnace (EAF) operation (Removed from Section 112 source category list by EPA – see discussion above); and
- Stainless Steel Manufacturing – Electric Arc Furnaces (EAF) operations (Removed from Section 112 source category list by EPA – see discussion above).

As of December 2021, EPA has not established a NESHAP provision for EAFs at steelmaking facilities producing stainless and non-stainless steel at a major source of regulated HAPs.

Second Step – Review of Current Promulgated NESHAP Provisions for Applicability to the Proposed Steel Mill Project’s Electric Arc Furnaces

In connection with this review, we evaluated the potential applicability of other NESHAP adopted for the steel industry to determine whether they would be applicable to the EAFs at the Proposed Steel Mill Project. Based upon this review, and for the reasons set forth in more detail below, we have determined that these NESHAP are not applicable:

- Subpart FFFFF “National Emission Standards for Hazardous Air Pollutants for Integrated Iron and Steel Manufacturing Facilities” was reviewed and determined to not apply to the Proposed Steel Mill Project since its applicability was for only Integrated Iron and Steel manufacturing facilities at a major source of regulated HAPs. An Integrated Iron and Steel Facility was defined as an establishment engaged in the production of steel from iron ore. The Proposed Steel Mill Project will be engaged in the production of steel from scrap steel. This particular Subpart identifies the affected sources for each new sister plant, blast furnace and basic oxygen process furnace (BOPF) shop at an integrated Iron and Steel manufacturing facility. These types of process operations will not be performed or associated with the new mill. As such Subpart FFFFF is not applicable to the Proposed Steel Mill Project;
- As discussed in more detail above, Subpart EEEEE “National Emission Standards for Hazardous Air Pollutants for Iron and Steel Foundries” was reviewed and determined to not apply to the Proposed Steel Mill Project; and
- Subpart YYYYY is not applicable because the Proposed Steel Mill Project will be classified as a major source of regulated HAPs.

Third Step – Review of EPA Requirements for Non-Regulated Source Categories of HAPs -Electric Arc Furnaces at Steelmaking Facilities – Major Sources Of Regulated HAPs

The third step was to review EPA requirements for proposed projects that involve new emission units with the potential to emit regulated HAPs at major and non-major (area source) stationary emission sources. Section 112(g) of the 1990 CAA amendments, and its implementing regulations at 40 CFR Part 63 Subpart B (known as the case-by-case MACT) apply to any new stationary source that would be major for HAPs or any addition to an existing major source where the addition itself entails HAP emissions above major source thresholds.⁴ Subpart B under Section 63 of Title 40 of the Code of Federal Regulations identifies the requirements for control technology determinations in accordance with Clean Air Act sections 112(g) and 112(j) for such major sources which do not fall under a Section 112 listed source category. 40 CFR Part 63.42(c) states that no person may begin actual construction of a major source of HAP in such State or local jurisdiction unless:

- The major source in question has been specifically regulated or exempted from regulation under a standard issued pursuant to section 112(d) , section 112(h) or section 112(j) in part 63, and the owner and operator has fully complied with all procedures and requirements for preconstruction review established by that standard, including any applicable requirements set forth in Subpart A of this Part 63; or
- The permitting authority has made a final and effective case-by-case determination pursuant to the provisions of § 63.43 such that emissions from the constructed or reconstructed major

⁴ See 40 CFR §63.41: “Construct a major source means: (1) To fabricate, erect, or install at any greenfield site a stationary source or group of stationary sources which is located within a contiguous area and under common control and which emits or has the potential to emit 10 tons per year of any HAP's or 25 tons per year of any combination of HAP, or (2) To fabricate, erect, or install at any developed site a new process or production unit which in and of itself emits or has the potential to emit 10 tons per year of any HAP or 25 tons per year of any combination of HAP, unless the process or production unit satisfies criteria in paragraphs (2) (i) through (vi) of this definition.”

source will be controlled to a level no less stringent than the maximum achievable control technology emission limitation for new sources.

The Proposed Steel Mill Project presumably would meet this definition and thus would be required to go through a case-by-case MACT determination.

Notwithstanding, EPA's regulations implementing CAA § 112(g) includes the following exception from such requirements:

“Exclusion for stationary sources in deleted source categories. The requirements of this subpart do not apply to stationary sources that are within a source category that has been deleted from the source category list pursuant to section 112(c)(9) of the Act.”

40 CFR §63.40(e). Notably, this exemption for delisted source categories specifically references CAA Section 112(c)(9), which allows the EPA to delist a source category, if, e.g., “emissions from no source in the category or subcategory concerned (or group of sources in the case of area sources) exceed a level which is adequate to protect public health with an ample margin of safety” 42 USC §7412(c)(9).

As noted above, on June 4, 1996, EPA revised the list of source categories by deleting the Non-Stainless-Steel Manufacturing – Electric Arc Furnace (EAF) Operation and the Stainless-Steel Manufacturing – Electric Arc Furnace (EAF) Operation source categories. 61 Fed. Reg. 28197 (June 5, 1996). However, in doing so, the EPA specifically said that it was NOT being delisted pursuant to the agency's delisting power under Section 112(c)(9) of the CAA. *Id.* at 28200 (“The Agency is not invoking the authority within Section 112(c)(9) for deleting source categories. . . . Instead, in today's notice, the Agency is simply contending that the data originally used for listing were erroneous, and that, based on newer data, the original listings are not warranted.”)

As a result, because Non-Stainless-Steel Manufacturing – Electric Arc Furnace (EAF) Operation and the Stainless-Steel Manufacturing – Electric Arc Furnace (EAF) Operation categories were not “deleted from the source category list *pursuant to section 112(c)(9) of the Act*” (40 CFR §63.40(e)), these source categories do not appear to fall within the “deleted source categories” exemption to Section 112(g), and thus it appears that the EAFs associated with the Proposed Steel Mill Project triggers the need for a case-by-case MACT determination.

More specifically, the EAFs associated with the Proposed Steel Mill Project are subject to the general requirement to ensure that the requirements of MACT are satisfied for the construction of new major stationary sources of regulated HAPs in accordance with 40 C.F.R. § 63.43 (i.e., “The permitting authority has made a final and effective case-by-case determination pursuant to the provisions of 40 CFR Part 63.43 such that emissions from the constructed or reconstructed major source will be controlled to a level no less stringent than the maximum achievable control technology emission limitation for new sources.”).

Final Step – Case-by-Case MACT Determination – Proposed Steel Mill Project's Electric Arc Furnaces

The following general principles are to be followed in the selection of MACT on a case-by-case basis:

1. The MACT emission limit shall not be less stringent than the emission control which is achieved in practice by the best controlled similar sources;
2. The maximum degree of reduction in emissions of HAP which can be achieved by utilizing those control technologies that can be identified from the available information, taking into

consideration the costs of achieving such emission reduction and any non-air quality health and environmental impacts and energy requirements associated with the emission control; and

3. If EPA has either proposed a relevant emission standard pursuant to section 112(d) or section 112(g) of the Act or adopted a presumptive MACT determination for the source category which includes the constructed major source.

40 C.F.R. § 63.43(c). To define the control level that is no less stringent than the maximum achievable control technology emission limitation for the best controlled sources similar to the EAFs associated with the Proposed Steel Mill Project, BRS reviewed the following 1) applicable New Source Performance Standards, 2) NESHAP Subpart YYYYYY and 3) Best Available Control Technology (BACT) determinations for EAFs similar to the EAFs for the Proposed Steel Mill Project under the PSD new source construction permit program.

New Source Performance Standards (NSPS)

EPA promulgated a specific NSPS provision that required new EAFs at steelmaking facilities to meet specific emission limitations. This NSPS provision is defined as Subpart AAa “Standards of Performance for Steel Plants – Electric Arc Furnaces and Argon-Oxygen Decarburization Vessels Constructed After August 17, 1983”. The provision required that all new EAFs meet the following limitations:

- No EAF is allowed to discharge from a control device a particulate matter in excess of 0.0052 grains/dscf;
- No EAF is allowed to discharge from a control device opacity in excess of 3 percent or greater; and
- No Melt shop supporting operation of an EAF is allowed to exhibit opacity at 6 percent or greater exiting from that shop.
- These provision also contains specific emission monitoring and monitoring of operation requirements.

The EAFs associated with the Proposed Steel Mill Project are designed to meet the above applicable requirements, including visible emissions from the Melt Shop, as defined under NSPS Subpart AAa.

Non-Major Source NESHAP Provisions

As discussed above EPA has developed a non-major source NESHAP provision for area sources which is defined as Subpart YYYYYY. EPA defined the following control requirements for EAFs, emission limits for EAFs, and specific requirements related to the control of contaminants from scrap:

- Install, operate and maintain a capture system that collects those emissions from each EAF and conveys the collected emissions to a control device for the removal of particulate matter (PM);
- An EAF must not discharge from a control device and contain in excess of 0.0052 grains of PM per dry standard cubic foot (gr/dscf);
- Any exit from a Melt Shop using an EAF is not allowed to exhibit 6% opacity or greater; and

- Section 63.10685 identifies specific requirements for the control on contaminants from scrap. The primary requirement is to prepare / implement a plan to minimize scrap steel containing mercury.

Note that the provisions defined in Subpart YYYYYY incorporate some of the same limitations imposed by NSPS AAa. As noted above the proposed EAFs and Melt Shop are designed to meet those applicable requirements.

BACT Defined under the PSD Construction Permit Program

As discussed in the PSD air permit application submitted to the AEEDEQ, dated September 20, 2021, BRS performed a Top Down BACT evaluation and based on that evaluation defined BACT emission limits for the proposed EAFs. The BACT emission limits defined for the EAFs were as follows:

- Particulate Matter (PM) limit of 0.0018 grains/dscf;
- Particulate Matter (PM10) limit of 0.0024 grains/dscf; and
- Particulate Matter (PM2.5) limit of 0.0024 grains/dscf.

These limits are based on installing a control device (i.e., baghouse) to control particulate matter from each of the EAFs associated with the Proposed Steel Mill Project. These limits reflect the best level of control for particulate matter taking into account energy, environmental and economic impacts. These limits are reflective of the level of control and limits being established for EAFs used in the steelmaking industry to produce stainless and non-stainless steel. The limits being proposed by BRS are more restrictive than those limits established under NSPS AAa and NESHAP Subpart YYYYYY.

Case-by-Case MACT Determination for the Proposed Steel Mill Project's Electric Arc Furnaces

Based on the above information, BRS has determined that case-by-case MACT requirements for the EAFs associated with the Proposed Steel Mill Project should be set as follows:

- Install, operate and maintain a capture system that collects those emissions from each EAF and conveys the collected emissions to a control device for the removal of particulate matter (PM);
- An EAF must not discharge from a control device and contain in excess of 0.0018 grains of PM per dry standard cubic foot (gr/dscf);
- Any exit from a Melt Shop using an EAF is not allowed to exhibit 6% opacity or greater; and
- 40 C.F.R. § 63.10685 identifies specific requirements for the control on contaminants from scrap. The primary requirement is to prepare / implement a plan to minimize scrap steel containing mercury.

If you should have any questions regarding the content of this Supplement #1, please address all questions or comments to Mr. Steven Frey at (847) 278-7705 or by email at stevefrey@kennedyjenks.com. Mr. Frey is the primary point of contact for BRS's PSD major modification request on behalf of BRS.

Sincerely,
Kennedy/Jenks Consultants



Steven A. Frey
Principal, Community of Practice Leader Air Quality

Cc:

Mr. Dean Caldwell - Big River Steel LLC
Mr. Marty Booher Attorney - BakerHostetler

Appendix J

40 C.F.R. Part 63 Subpart B

***Requirements for Control Technology Determinations for Major Sources in Accordance With
Clean Air Act Sections, Sections 112(g) and 112(j)***

Subpart B - Requirements for Control Technology Determinations for Major Sources in Accordance With Clean Air Act Sections, Sections 112(g) and 112(j)

Source: [59 FR 26449](#), May 20, 1994, unless otherwise noted.

§ 63.40 Applicability of [§§ 63.40](#) through [63.44](#).

(a) **Applicability.** The requirements of [§§ 63.40](#) through [63.44 of this subpart](#) carry out section 112(g)(2)(B) of the 1990 Amendments.

(b) **Overall requirements.** The requirements of [§§ 63.40](#) through [63.44 of this subpart](#) apply to any owner or operator who constructs or reconstructs a major source of hazardous air pollutants after the effective date of section 112(g)(2)(B) (as defined in [§ 63.41](#)) and the effective date of a title V permit program in the State or local jurisdiction in which the major source is (or would be) located unless the major source in question has been specifically regulated or exempted from regulation under a standard issued pursuant to section 112(d), section 112(h), or section 112(j) and incorporated in another subpart of part 63, or the owner or operator of such major source has received all necessary air quality permits for such construction or reconstruction project before the effective date of section 112(g)(2)(B).

(c) **Exclusion for electric utility steam generating units.** The requirements of this subpart do not apply to electric utility steam generating units unless and until such time as these units are added to the source category list pursuant to section 112(c)(5) of the Act.

(d) **Relationship to State and local requirements.** Nothing in this subpart shall prevent a State or local agency from imposing more stringent requirements than those contained in this subpart.

(e) **Exclusion for stationary sources in deleted source categories.** The requirements of this subpart do not apply to stationary sources that are within a source category that has been deleted from the source category list pursuant to section 112(c)(9) of the Act.

(f) **Exclusion for research and development activities.** The requirements of this subpart do not apply to research and development activities, as defined in [§ 63.41](#).

[[61 FR 68399](#), Dec. 27, 1996]

§ 63.41 Definitions.

Terms used in this subpart that are not defined in this section have the meaning given to them in the Act and in subpart A.

Affected source means the stationary source or group of stationary sources which, when fabricated (on site), erected, or installed meets the definition of “construct a major source” or the definition of “reconstruct a major source” contained in this section.

Affected States are all States:

- (1) Whose air quality may be affected and that are contiguous to the State in which a MACT determination is made in accordance with this subpart; or
- (2) Whose air quality may be affected and that are within 50 miles of the major source for which a MACT determination is made in accordance with this subpart.

Available information means, for purposes of identifying control technology options for the affected source, information contained in the following information sources as of the date of approval of the MACT determination by the permitting authority:

- (1) A relevant proposed regulation, including all supporting information;
- (2) Background information documents for a draft or proposed regulation;
- (3) Data and information available for the Control Technology Center developed pursuant to section 113 of the Act;
- (4) Data and information contained in the Aerometric Informational Retrieval System including information in the MACT data base;
- (5) Any additional information that can be expeditiously provided by the Administrator; and
- (6) For the purpose of determinations by the permitting authority, any additional information provided by the applicant or others, and any additional information considered available by the permitting authority.

Construct a major source means:

- (1) To fabricate, erect, or install at any greenfield site a stationary source or group of stationary sources which is located within a contiguous area and under common control and which emits or has the potential to emit 10 tons per year of any HAP's or 25 tons per year of any combination of HAP, or
- (2) To fabricate, erect, or install at any developed site a new process or production unit which in and of itself emits or has the potential to emit 10 tons per year of any HAP or 25 tons per year of any combination of HAP, unless the process or production unit satisfies criteria in paragraphs (2) (i) through (vi) of this definition.
 - (i) All HAP emitted by the process or production unit that would otherwise be controlled under the requirements of this subpart will be controlled by emission control equipment which was previously installed at the same site as the process or production unit;
 - (ii)

(A) The permitting authority has determined within a period of 5 years prior to the fabrication, erection, or installation of the process or production unit that the existing emission control equipment represented best available control technology (BACT), lowest achievable emission rate (LAER) under [40 CFR part 51](#) or [52](#), toxics - best available control technology (T-BACT), or MACT based on State air toxic rules for the category of pollutants which includes those HAP's to be emitted by the process or production unit; or

(B) The permitting authority determines that the control of HAP emissions provided by the existing equipment will be equivalent to that level of control currently achieved by other well-controlled similar sources (i.e., equivalent to the level of control that would be provided by a current BACT, LAER, T-BACT, or State air toxic rule MACT determination);

(iii) The permitting authority determines that the percent control efficiency for emissions of HAP from all sources to be controlled by the existing control equipment will be equivalent to the percent control efficiency provided by the control equipment prior to the inclusion of the new process or production unit;

(iv) The permitting authority has provided notice and an opportunity for public comment concerning its determination that criteria in paragraphs (2)(i), (2)(ii), and (2)(iii) of this definition apply and concerning the continued adequacy of any prior LAER, BACT, T-BACT, or State air toxic rule MACT determination;

(v) If any commenter has asserted that a prior LAER, BACT, T-BACT, or State air toxic rule MACT determination is no longer adequate, the permitting authority has determined that the level of control required by that prior determination remains adequate; and

(vi) Any emission limitations, work practice requirements, or other terms and conditions upon which the above determinations by the permitting authority are applicable requirements under section 504(a) and either have been incorporated into any existing title V permit for the affected facility or will be incorporated into such permit upon issuance.

Control technology means measures, processes, methods, systems, or techniques to limit the emission of hazardous air pollutants through process changes, substitution of materials or other modifications;

(1) Reduce the quantity of, or eliminate emissions of, such pollutants through process changes, substitution of materials or other modifications;

(2) Enclose systems or processes to eliminate emissions;

(3) Collect, capture or treat such pollutants when released from a process, stack, storage or fugitive emissions point;

(4) Are design, equipment, work practice, or operational standards (including requirements for operator training or certification) as provided in [42 U.S.C. 7412\(h\)](#); or

(5) Are a combination of paragraphs (1) through (4) of this definition.

Effective date of section 112(g)(2)(B) in a State or local jurisdiction means the effective date specified by the permitting authority at the time the permitting authority adopts a program to implement section 112(g) with respect to construction or reconstruction or major sources of HAP, or June 29, 1998 whichever is earlier.

Electric utility steam generating unit means any fossil fuel fired combustion unit of more than 25 megawatts that serves a generator that produces electricity for sale. A unit that co-generates steam and electricity and supplies more than one-third of its potential electric output capacity and more than 25 megawatts electric output to any utility power distribution system for sale shall be considered an electric utility steam generating unit.

Greenfield suite means a contiguous area under common control that is an undeveloped site.

List of Source Categories means the Source Category List required by section 112(c) of the Act.

Maximum achievable control technology (MACT) emission limitation for new sources means the emission limitation which is not less stringent than the emission limitation achieved in practice by the best controlled similar source, and which reflects the maximum degree of deduction in emissions that the permitting authority, taking into consideration the cost of achieving such emission reduction, and any non-air quality health and environmental impacts and energy requirements, determines is achievable by the constructed or reconstructed major source.

Notice of MACT Approval means a document issued by a permitting authority containing all federally enforceable conditions necessary to enforce the application and operation of MACT or other control technologies such that the MACT emission limitation is met.

Permitting authority means the permitting authority as defined in [part 70](#) or [71 of this chapter](#).

Process or production unit means any collection of structures and/or equipment, that processes assembles, applies, or otherwise uses material inputs to produce or store an intermediate or final product. A single facility may contain more than one process or production unit.

Reconstruct a major source means the replacement of components at an existing process or production unit that in and of itself emits or has that potential to emit 10 tons per year of any HAP or 25 tons per year of any combination of HAP, whenever:

- (1) The fixed capital cost of the new components exceeds 50 percent of the fixed capital cost that would be required to construct a comparable process or production unit; and
- (2) It is technically and economically feasible for the reconstructed major source to meet the applicable maximum achievable control technology emission limitation for new sources established under this subpart.

Research and development activities means activities conducted at a research or laboratory facility whose primary purpose is to conduct research and development into new processes and products, where such source is operated under the close supervision of technically trained personnel and is not engaged in the manufacture of products for sale or exchange for commercial profit, except in a *de minimis* manner.

Similar source means a stationary source or process that has comparable emissions and is structurally similar in design and capacity to a constructed or reconstructed major source such that the source could be controlled using the same control technology.

[[61 FR 68399](#), Dec. 27, 1996]

§ 63.42 Program requirements governing construction or reconstruction of major sources.

(a) **Adoption of program.** Each permitting authority shall review its existing programs, procedures, and criteria for preconstruction review for conformity to the requirements established by [§§ 63.40](#) through [63.44](#), shall make any additions and revisions to its existing programs, procedures, and criteria that the permitting authority deems necessary to properly effectuate [§§ 63.40](#) through [63.44](#), and shall adopt a program to implement section 112(g) with respect to construction or reconstruction of major sources of HAP. As part of the adoption by the permitting authority of a program to implement section 112(g) with respect to construction or reconstruction of major sources of HAP, the chief executive officer of the permitting authority shall certify that the program satisfies all applicable requirements established by [§§ 63.40](#) through [63.44](#), and shall specify an effective date for that program which is not later than June 29, 1998. Prior to the specified effective date, the permitting authority shall publish a notice stating that the permitting authority has adopted a program to implement section 112(g) with respect to construction or reconstruction of major sources of HAP and stating the effective date, and shall provide a written description of the program to the Administrator through the appropriate EPA Regional Office. Nothing in this section shall be construed either:

(1) To require that any owner or operator of a stationary source comply with any requirement adopted by the permitting authority which is not intended to implement section 112(g) with respect to construction or reconstruction of major sources of HAP; or

(2) To preclude the permitting authority from enforcing any requirements not intended to implement section 112(g) with respect to construction or reconstruction of major sources of HAP under any other provision of applicable law.

(b) **Failure to adopt program.** In the event that the permitting authority fails to adopt a program to implement section 112(g) with respect to construction or reconstruction of major sources of HAP with an effective date on or before June 29, 1998, and the permitting authority concludes that it is able to make case-by-case MACT determinations which conform to the provisions of [§ 63.43](#) in the absence of such a program, the permitting authority may elect to make such determinations. However, in those instances where the permitting authority elects to

make case-by-case MACT determinations in the absence of a program to implement section 112(g) with respect to construction or reconstruction of major sources of HAP, no such case-by-case MACT determination shall take effect until after it has been submitted by the permitting authority in writing to the appropriate EPA Regional Administrator and the EPA Regional Administrator has concurred in writing that the case-by-case MACT determination by the permitting authority is in conformity with all requirements established by [§§ 63.40](#) through [63.44](#). In the event that the permitting authority fails to adopt a program to implement section 112(g) with respect to construction or reconstruction of major sources of HAP with an effective date on or before June 29, 1998, and the permitting authority concludes that it is unable to make case-by-case MACT determinations in the absence of such a program, the permitting authority may request that the EPA Regional Administrator implement a transitional program to implement section 112(g) with respect to construction or reconstruction of major sources of HAP in the affected State of local jurisdiction while the permitting authority completes development and adoption of a section 112(g) program. Any such transitional section 112(g) program implemented by the EPA Regional Administrator shall conform to all requirements established by [§§ 63.40](#) through [63.44](#), and shall remain in effect for no more than 30 months. Continued failure by the permitting authority to adopt a program to implement section 112(g) with respect to construction or reconstruction of major sources of HAP shall be construed as a failure by the permitting authority to adequately administer and enforce its title V permitting program and shall constitute cause by EPA to apply the sanctions and remedies set forth in the Clean Air Act section 502(I).

(c) **Prohibition.** After the effective date of section 112(g)(2)(B) (as defined in [§ 63.41](#)) in a State or local jurisdiction and the effective date of the title V permit program applicable to that State or local jurisdiction, no person may begin actual construction or reconstruction of a major source of HAP in such State or local jurisdiction unless:

(1) The major source in question has been specifically regulated or exempted from regulation under a standard issued pursuant to section 112(d), section 112(h) or section 112(j) in part 63, and the owner and operator has fully complied with all procedures and requirements for preconstruction review established by that standard, including any applicable requirements set forth in [subpart A of this part 63](#); or

(2) The permitting authority has made a final and effective case-by-case determination pursuant to the provisions of [§ 63.43](#) such that emissions from the constructed or reconstructed major source will be controlled to a level no less stringent than the maximum achievable control technology emission limitation for new sources.

[[61 FR 68400](#), Dec. 27, 1996, as amended at [64 FR 35032](#), June 30, 1999]

§ 63.43 Maximum achievable control technology (MACT) determinations for constructed and reconstructed major sources.

(a) **Applicability.** The requirements of this section apply to an owner or operator who constructs or reconstructs a major source of HAP subject to a case-by-case determination of maximum achievable control technology pursuant to [§ 63.42\(c\)](#).

(b) **Requirements for constructed and reconstructed major sources.** When a case-by-case determination of MACT is required by [§ 63.42\(c\)](#), the owner and operator shall obtain from the permitting authority an approved MACT determination according to one of the review options contained in [paragraph \(c\)](#) of this section.

(c) **Review options.**

(1) When the permitting authority requires the owner or operator to obtain, or revise, a permit issued pursuant to title V of the Act before construction or reconstruction of the major source, or when the permitting authority allows the owner or operator at its discretion to obtain or revise such a permit before construction or reconstruction, and the owner or operator elects that option, the owner or operator shall follow the administrative procedures in the program approved under title V of the Act (or in other regulations issued pursuant to title V of the Act, where applicable).

(2) When an owner or operator is not required to obtain or revise a title V permit (or other permit issued pursuant to title V of the Act) before construction or reconstruction, the owner or operator (unless the owner or operator voluntarily follows the process to obtain a title V permit) shall either, at the discretion of the permitting authority:

(i) Apply for and obtain a Notice of MACT Approval according to the procedures outlined in [paragraphs \(f\)](#) through [\(h\)](#) of this section; or

(ii) Apply for a MACT determination under any other administrative procedures for preconstruction review and approval established by the permitting authority for a State or local jurisdiction which provide for public participation in the determination, and ensure that no person may begin actual construction or reconstruction of a major source in that State or local jurisdiction unless the permitting authority determines that the MACT emission limitation for new sources will be met.

(3) When applying for a permit pursuant to title V of the Act, an owner or operator may request approval of case-by-case MACT determinations for alternative operating scenarios. Approval of such determinations satisfies the requirements of section 112(g) of each such scenario.

(4) Regardless of the review process, the MACT emission limitation and requirements established shall be effective as required by [paragraph \(j\)](#) of this section, consistent with the principles established in [paragraph \(d\)](#) of this section, and supported by the information listed in [paragraph \(e\)](#) of this section. The owner or operator shall comply with the requirements in [paragraphs \(k\)](#) and [\(l\)](#) of this section, and with all applicable requirements in [subpart A of this part](#).

(d) ***Principles of MACT determinations.*** The following general principles shall govern preparation by the owner or operator of each permit application or other application requiring a case-by-case MACT determination concerning construction or reconstruction of a major source, and all subsequent review of and actions taken concerning such an application by the permitting authority:

(1) The MACT emission limitation or MACT requirements recommended by the applicant and approved by the permitting authority shall not be less stringent than the emission control which is achieved in practice by the best controlled similar source, as determined by the permitting authority.

(2) Based upon available information, as defined in this subpart, the MACT emission limitation and control technology (including any requirements under [paragraph \(d\)\(3\)](#) of this section) recommended by the applicant and approved by the permitting authority shall achieve the maximum degree of reduction in emissions of HAP which can be achieved by utilizing those control technologies that can be identified from the available information, taking into consideration the costs of achieving such emission reduction and any non-air quality health and environmental impacts and energy requirements associated with the emission reduction.

(3) The applicant may recommend a specific design, equipment, work practice, or operational standard, or a combination thereof, and the permitting authority may approve such a standard if the permitting authority specifically determines that it is not feasible to prescribe or enforce an emission limitation under the criteria set forth in section 112(h)(2) of the Act.

(4) If the Administrator has either proposed a relevant emission standard pursuant to section 112(d) or section 112(h) of the Act or adopted a presumptive MACT determination for the source category which includes the constructed or reconstructed major source, then the MACT requirements applied to the constructed or reconstructed major source shall have considered those MACT emission limitations and requirements of the proposed standard or presumptive MACT determination.

(e) ***Application requirements for a case-by-case MACT determination.***

(1) An application for a MACT determination (whether a permit application under title V of the Act, an application for a Notice of MACT Approval, or other document specified by the permitting authority under [paragraph \(c\)\(2\)\(ii\)](#) of this section) shall specify a control technology selected by the owner or operator that, if properly operated and maintained, will meet the MACT emission limitation or standard as determined according to the principles set forth in [paragraph \(d\)](#) of this section.

(2) In each instance where a constructed or reconstructed major source would require additional control technology or a change in control technology, the application for a MACT determination shall contain the following information:

- (i) The name and address (physical location) of the major source to be constructed or reconstructed;
 - (ii) A brief description of the major source to be constructed or reconstructed and identification of any listed source category or categories in which it is included;
 - (iii) The expected commencement date for the construction or reconstruction of the major source;
 - (iv) The expected completion date for construction or reconstruction of the major source;
 - (v) the anticipated date of start-up for the constructed or reconstructed major source;
 - (vi) The HAP emitted by the constructed or reconstructed major source, and the estimated emission rate for each such HAP, to the extent this information is needed by the permitting authority to determine MACT;
 - (vii) Any federally enforceable emission limitations applicable to the constructed or reconstructed major source;
 - (viii) The maximum and expected utilization of capacity of the constructed or reconstructed major source, and the associated uncontrolled emission rates for that source, to the extent this information is needed by the permitting authority to determine MACT;
 - (ix) The controlled emissions for the constructed or reconstructed major source in tons/yr at expected and maximum utilization of capacity, to the extent this information is needed by the permitting authority to determine MACT;
 - (x) A recommended emission limitation for the constructed or reconstructed major source consistent with the principles set forth in [paragraph \(d\)](#) of this section;
 - (xi) The selected control technology to meet the recommended MACT emission limitation, including technical information on the design, operation, size, estimated control efficiency of the control technology (and the manufacturer's name, address, telephone number, and relevant specifications and drawings, if requested by the permitting authority);
 - (xii) Supporting documentation including identification of alternative control technologies considered by the applicant to meet the emission limitation, and analysis of cost and non-air quality health environmental impacts or energy requirements for the selected control technology; and
 - (xiii) Any other relevant information required pursuant to subpart A.
- (3) In each instance where the owner or operator contends that a constructed or reconstructed major source will be in compliance, upon startup, with case-by-case MACT under this

subpart without a change in control technology, the application for a MACT determination shall contain the following information:

- (i) The information described in [paragraphs \(e\)\(2\)\(i\)](#) through [\(e\)\(2\)\(x\)](#) of this section; and
- (ii) Documentation of the control technology in place.

(f) *Administrative procedures for review of the Notice of MACT Approval.*

(1) The permitting authority will notify the owner or operator in writing, within 45 days from the date the application is first received, as to whether the application for a MACT determination is complete or whether additional information is required.

(2) The permitting authority will initially approve the recommended MACT emission limitation and other terms set forth in the application, or the permitting authority will notify the owner or operator in writing of its intent to disapprove the application, within 30 calendar days after the owner or operator is notified in writing that the application is complete.

(3) The owner or operator may present, in writing, within 60 calendar days after receipt of notice of the permitting authority's intent to disapprove the application, additional information or arguments pertaining to, or amendments to, the application for consideration by the permitting authority before it decides whether to finally disapprove the application.

(4) The permitting authority will either initially approve or issue a final disapproval of the application within 90 days after it notifies the owner or operator of an intent to disapprove or within 30 days after the date additional information is received from the owner or operator; whichever is earlier.

(5) A final determination by the permitting authority to disapprove any application will be in writing and will specify the grounds on which the disapproval is based. If any application is finally disapproved, the owner or operator may submit a subsequent application concerning construction or reconstruction of the same major source, provided that the subsequent application has been amended in response to the stated grounds for the prior disapproval.

(6) An initial decision to approve an application for a MACT determination will be set forth in the Notice of MACT Approval as described in [paragraph \(g\)](#) of this section.

(g) *Notice of MACT Approval.*

(1) The Notice of MACT Approval will contain a MACT emission limitation (or a MACT work practice standard if the permitting authority determines it is not feasible to prescribe or enforce an emission standard) to control the emissions of HAP. The MACT emission limitation or standard will be determined by the permitting authority and will conform to the principles set forth in [paragraph \(d\)](#) of this section.

(2) The Notice of MACT Approval will specify any notification, operation and maintenance, performance testing, monitoring, reporting and record keeping requirements. The Notice of MACT Approval shall include:

(i) In addition to the MACT emission limitation or MACT work practice standard established under this subpart, additional emission limits, production limits, operational limits or other terms and conditions necessary to ensure Federal enforceability of the MACT emission limitation;

(ii) Compliance certifications, testing, monitoring, reporting and record keeping requirements that are consistent with the requirements of [§ 70.6\(c\) of this chapter](#);

(iii) In accordance with section 114(a)(3) of the Act, monitoring shall be capable of demonstrating continuous compliance during the applicable reporting period. Such monitoring data shall be of sufficient quality to be used as a basis for enforcing all applicable requirements established under this subpart, including emission limitations;

(iv) A statement requiring the owner or operator to comply with all applicable requirements contained in [subpart A of this part](#);

(3) All provisions contained in the Notice of MACT Approval shall be federally enforceable upon the effective date of issuance of such notice, as provided by [paragraph \(j\) of this section](#).

(4) The Notice of MACT Approval shall expire if construction or reconstruction has not commenced within 18 months of issuance, unless the permitting authority has granted an extension which shall not exceed an additional 12 months.

(h) *Opportunity for public comment on the Notice of MACT Approval.*

(1) The permitting authority will provide opportunity for public comment on the Notice of MACT Approval, including, at a minimum:

(i) Availability for public inspection in at least one location in the area affected of the information submitted by the owner or operator and of the permitting authority's initial decision to approve the application;

(ii) A 30-day period for submittal of public comment; and

(iii) A notice by prominent advertisement in the area affected of the location of the source information and initial decision specified in [paragraph \(h\)\(1\)\(i\) of this section](#).

(2) At the discretion of the permitting authority, the Notice of MACT Approval setting forth the initial decision to approve the application may become final automatically at the end of the comment period if no adverse comments are received. If adverse comments are received,

the permitting authority shall have 30 days after the end of the comment period to make any necessary revisions in its analysis and decide whether to finally approve the application.

(i) ***EPA notification.*** The permitting authority shall send a copy of the final Notice of MACT Approval, notice of approval of a title V permit application incorporating a MACT determination (in those instances where the owner or operator either is required or elects to obtain such a permit before construction or reconstruction), or other notice of approval issued pursuant to [paragraph \(c\)\(2\)\(ii\)](#) of this section to the Administrator through the appropriate Regional Office, and to all other State and local air pollution control agencies having jurisdiction in affected States.

(j) ***Effective date.*** The effective date of a MACT determination shall be the date the Notice of MACT Approval becomes final, the date of issuance of a title V permit incorporating a MACT determination (in those instances where the owner or operator either is required or elects to obtain such a permit before construction or reconstruction), or the date any other notice of approval issued pursuant to [paragraph \(c\)\(2\)\(ii\)](#) of this section becomes final.

(k) ***Compliance date.*** On and after the date of start-up, a constructed or reconstructed major source which is subject to the requirements of this subpart shall be in compliance with all applicable requirements specified in the MACT determination.

(l) ***Compliance with MACT determinations.***

(1) An owner or operator of a constructed or reconstructed major source that is subject to a MACT determination shall comply with all requirements in the final Notice of MACT Approval, the title V permit (in those instances where the owner or operator either is required or elects to obtain such a permit before construction or reconstruction), or any other final notice of approval issued pursuant to [paragraph \(c\)\(2\)\(ii\)](#) of this section, including but not limited to any MACT emission limitation or MACT work practice standard, and any notification, operation and maintenance, performance testing, monitoring, reporting, and recordkeeping requirements.

(2) An owner or operator of a constructed or reconstructed major source which has obtained a MACT determination shall be deemed to be in compliance with section 112(g)(2)(B) of the Act only to the extent that the constructed or reconstructed major source is in compliance with all requirements set forth in the final Notice of MACT Approval, the title V permit (in those instances where the owner or operator either is required or elects to obtain such a permit before construction or reconstruction), or any other final notice of approval issued pursuant to [paragraph \(c\)\(2\)\(ii\)](#) of this section. Any violation of such requirements by the owner or operator shall be deemed by the permitting authority and by EPA to be a violation of the prohibition on construction or reconstruction in section 112(g)(2)(B) for whatever period the owner or operator is determined to be in violation of such requirements, and shall subject the owner or operator to appropriate enforcement action under the Act.

(m) ***Reporting to the Administrator.*** Within 60 days of the issuance of a final Notice of MACT Approval, a title V permit incorporating a MACT determination (in those instances where the

owner or operator either is required or elects to obtain such a permit before construction or reconstruction), or any other final notice of approval issued pursuant to [paragraph \(c\)\(2\)\(ii\)](#) of this section, the permitting authority shall provide a copy of such notice to the Administrator, and shall provide a summary in a compatible electronic format for inclusion in the MACT data base.

[[61 FR 68401](#)], Dec. 27, 1996]

§ 63.44 Requirements for constructed or reconstructed major sources subject to a subsequently promulgated MACT standard or MACT requirement.

(a) If the Administrator promulgates an emission standard under section 112(d) or section 112(h) of the Act or the permitting authority issues a determination under section 112(j) of the Act that is applicable to a stationary source or group of sources which would be deemed to be a constructed or reconstructed major source under this subpart before the date that the owner or operator has obtained a final and legally effective MACT determination under any of the review options available pursuant to [§ 63.43](#), the owner or operator of the source(s) shall comply with the promulgated standard or determination rather than any MACT determination under section 112(g) by the permitting authority, and the owner or operator shall comply with the promulgated standard by the compliance date in the promulgated standard.

(b) If the Administrator promulgates an emission standard under section 112(d) or section 112(h) of the Act or the permitting authority makes a determination under section 112(j) of the Act that is applicable to a stationary source or group of sources which was deemed to be a constructed or reconstructed major source under this subpart and has been subject to a prior case-by-case MACT determination pursuant to [§ 63.43](#), and the owner and operator obtained a final and legally effective case-by-case MACT determination prior to the promulgation date of such emission standard, then the permitting authority shall (if the initial title V permit has not yet been issued) issue an initial operating permit which incorporates the emission standard or determination, or shall (if the initial title V permit has been issued) revise the operating permit according to the reopening procedures in [40 CFR part 70](#) or part 71, whichever is relevant, to incorporate the emission standard or determination.

(1) The EPA may include in the emission standard established under section 112(d) or section 112(h) of the Act a specific compliance date for those sources which have obtained a final and legally effective MACT determination under this subpart and which have submitted the information required by [§ 63.43](#) to the EPA before the close of the public comment period for the standard established under section 112(d) of the Act. Such date shall assure that the owner or operator shall comply with the promulgated standard as expeditiously as practicable, but not longer than 8 years after such standard is promulgated. In that event, the permitting authority shall incorporate the applicable compliance date in the title V operating permit.

(2) If no compliance date has been established in the promulgated 112(d) or 112(h) standard or section 112(j) determination, for those sources which have obtained a final and legally effective MACT determination under this subpart, then the permitting authority shall establish a compliance date in the permit that assures that the owner or operator shall comply with the promulgated standard or determination as expeditiously as practicable, but not longer than 8 years after such standard is promulgated or a section 112(j) determination is made.

(c) Notwithstanding the requirements of [paragraphs \(a\) and \(b\)](#) of this section, if the Administrator promulgates an emission standard under section 112(d) or section 112(h) of the Act or the permitting authority issues a determination under section 112(j) of the Act that is applicable to a stationary source or group of sources which was deemed to be a constructed or reconstructed major source under this subpart and which is the subject of a prior case-by-case MACT determination pursuant to [§ 63.43](#), and the level of control required by the emission standard issued under section 112(d) or section 112(h) or the determination issued under section 112(j) is less stringent than the level of control required by any emission limitation or standard in the prior MACT determination, the permitting authority is not required to incorporate any less stringent terms of the promulgated standard in the title V operating permit applicable to such source(s) and may in its discretion consider any more stringent provisions of the prior MACT determination to be applicable legal requirements when issuing or revising such an operating permit.

[\[61 FR 68404\]](#), Dec. 27, 1996]

§§ 63.45-63.49 [Reserved]

§ 63.50 Applicability.

(a) *General applicability.*

(1) The requirements of this section through § 63.56 implement section 112(j) of the Clean Air Act (as amended in 1990). The requirements of this section through § 63.56 apply in each State beginning on the effective date of an approved title V permit program in such State. The requirements of this section through § 63.56 do not apply to research or laboratory activities as defined in [§ 63.51](#).

(2) The requirements of this section through § 63.56 apply to:

(i) The owner or operator of affected sources within a source category or subcategory under this part that are located at a major source that is subject to an approved title V permit program and for which the Administrator has failed to promulgate emission standards by the section 112(j) deadlines. If title V applicability has been deferred for a source category, then section 112(j) is not applicable for sources in that category within that State, local or tribal jurisdiction until those sources become subject to title V permitting requirements; and

(ii) Permitting authorities with an approved title V permit program.

(b) Relationship to State and local requirements. Nothing in §§ 63.50 through 63.56 shall prevent a State or local regulatory agency from imposing more stringent requirements, as a matter of State or local law, than those contained in §§ 63.50 through 63.56.

(c) The procedures in §§ 63.50 through 63.56 apply for each affected source only after the section 112(j) deadline for the source category or subcategory in question has passed, and only until such time as a generally applicable Federal standard governing that source has been promulgated under section 112(d) or 112(h) of the Act. Once a generally applicable Federal standard governing that source has been promulgated, the owner or operator of the affected source and the permitting authority are not required to take any further actions to develop an equivalent emission limitation under section 112(j) of the Act.

(d) Any final equivalent emission limitation for an affected source which is issued by the permitting authority pursuant to §§ 63.50 through 63.56 prior to promulgation of a generally applicable Federal standard governing that source under section 112(d) or 112(h) of the Act shall be deemed an applicable Federal requirement adopted pursuant to section 112(j) of the Act. Each such equivalent emission limitation shall take effect upon issuance of the permit containing that limitation under section 112(j)(5) of the Act, and shall remain applicable to the source until such time as it may be revised or supplanted pursuant to the procedures established by §§ 63.50 through 63.56. Such a final equivalent emission limitation, and all associated requirements adopted pursuant to § 63.52(f)(2), are directly enforceable under Federal law regardless of whether or not any permit in which they may be contained remains in effect.

[59 FR 26449, May 20, 1994, as amended at 67 FR 16605, Apr. 5, 2002; 68 FR 32601, May 30, 2003]

§ 63.51 Definitions.

Terms used in §§ 63.50 through 63.56 that are not defined in this section have the meaning given to them in the Act, or in [subpart A of this part](#).

Affected source means the collection of equipment, activities, or both within a single contiguous area and under common control that is in a section 112(c) source category or subcategory for which the Administrator has failed to promulgate an emission standard by the section 112(j) deadline, and that is addressed by an applicable MACT emission limitation established pursuant to this subpart.

Available information means, for purposes of conducting a MACT floor finding and identifying control technology options under this subpart, any information that is available as of the date on which the first Part 2 MACT application is filed for a source in the relevant source category or subcategory in the State or jurisdiction; and, pursuant to the requirements of this subpart, is additional relevant information that can be expeditiously provided by the Administrator, is submitted by the applicant or others prior to or during the public comment period on the section

112(j) equivalent emission limitation for that source, or information contained in the information sources in paragraphs (1) through (5) of this definition.

- (1) A relevant proposed regulation, including all supporting information;
- (2) Relevant background information documents for a draft or proposed regulation.
- (3) Any relevant regulation, information or guidance collected by the Administrator establishing a MACT floor finding and/or MACT determination.
- (4) Relevant data and information available from the Clean Air Technology Center developed pursuant to section 112(1)(3) of the Act.
- (5) Relevant data and information contained in the Aerometric Information Retrieval System (AIRS).
- (6) Any additional information that can be expeditiously provided by the Administrator, and
- (7) Any information provided by applicants in an application for a permit, permit modification, administrative amendment, or Notice of MACT Approval pursuant to the requirements of this subpart.
- (8) Any additional relevant information provided by the applicant.

Control technology means measures, processes, methods, systems, or techniques to limit the emission of hazardous air pollutants including, but not limited to, measures which:

- (1) Reduce the quantity, or eliminate emissions, of such pollutants through process changes, substitution of materials or other modifications;
- (2) Enclose systems or processes to eliminate emissions;
- (3) Collect, capture, or treat such pollutants when released from a process, stack, storage or fugitive emissions point;
- (4) Are design, equipment, work practice, or operational standards (including requirements for operator training or certification) as provided in [42 U.S.C. 7412\(h\)](#); or
- (5) Are a combination of paragraphs (1) through (4) of this definition.

Enhanced review means a review process containing all administrative steps needed to ensure that the terms and conditions resulting from the review process can be incorporated using title V permitting procedures.

Equivalent emission limitation means an emission limitation, established under section 112(j) of the Act, which is equivalent to the MACT standard that EPA would have promulgated under section 112(d) or (h) of the Act.

Maximum achievable control technology (MACT) emission limitation for existing sources means the emission limitation reflecting the maximum degree of reduction in emissions of hazardous air pollutants (including a prohibition on such emissions, where achievable) that the Administrator, taking into consideration the cost of achieving such emission reductions, and any non-air quality health and environmental impacts and energy requirements, determines is achievable by sources in the category or subcategory to which such emission standard applies. This limitation shall not be less stringent than the MACT floor.

Maximum achievable control technology (MACT) emission limitation for new sources means the emission limitation which is not less stringent than the emission limitation achieved in practice by the best controlled similar source, and which reflects the maximum degree of reduction in emissions of hazardous air pollutants (including a prohibition on such emissions, where achievable) that the Administrator, taking into consideration the cost of achieving such emission reduction, and any non-air quality health and environmental impacts and energy requirements, determines is achievable by sources in the category or subcategory to which such emission standard applies.

Maximum Achievable Control Technology (MACT) floor means:

(1) For existing sources:

(i) The average emission limitation achieved by the best performing 12 percent of the existing sources in the United States (for which the Administrator has emissions information), excluding those sources that have, within 18 months before the emission standard is proposed or within 30 months before such standard is promulgated, whichever is later, first achieved a level of emission rate or emission reduction which complies, or would comply if the source is not subject to such standard, with the lowest achievable emission rate (as defined in section 171 of the Act) applicable to the source category and prevailing at the time, in the category or subcategory, for categories and subcategories of stationary sources with 30 or more sources; or

(ii) The average emission limitation achieved by the best performing five sources (for which the Administrator has or could reasonably obtain emissions information) in the category or subcategory, for categories or subcategories with fewer than 30 sources;

(2) For new sources, the emission limitation achieved in practice by the best controlled similar source.

New affected source means the collection of equipment, activities, or both, that if constructed after the issuance of a section 112(j) permit for the source pursuant to [§ 63.52](#), is subject to the applicable MACT emission limitation for new sources. Each permit must define the term “new

affected source,” which will be the same as the “affected source” unless a different collection is warranted based on consideration of factors including:

- (1) Emission reduction impacts of controlling individual sources versus groups of sources;
- (2) Cost effectiveness of controlling individual equipment;
- (3) Flexibility to accommodate common control strategies;
- (4) Cost/benefits of emissions averaging;
- (5) Incentives for pollution prevention;
- (6) Feasibility and cost of controlling processes that share common equipment (e.g., product recovery devices);
- (7) Feasibility and cost of monitoring; and
- (8) Other relevant factors.

Permitting authority means the permitting authority as defined in [part 70 of this chapter](#).

Research or laboratory activities means activities whose primary purpose is to conduct research and development into new processes and products where such activities are operated under the close supervision of technically trained personnel and are not engaged in the manufacture of products for commercial sale in commerce, except in a de minimis manner; and where the source is not in a source category, specifically addressing research or laboratory activities, that is listed pursuant to section 112(c)(7) of the Act.

Section 112(j) deadline means the date 18 months after the date for which a relevant standard is scheduled to be promulgated under this part, except that for all major sources listed in the source category schedule for which a relevant standard is scheduled to be promulgated by November 15, 1994, the section 112(j) deadline is November 15, 1996, and for all major sources listed in the source category schedule for which a relevant standard is scheduled to be promulgated by November 15, 1997, the section 112(j) deadline is December 15, 1999.

Similar source means that equipment or collection of equipment that, by virtue of its structure, operability, type of emissions and volume and concentration of emissions, is substantially equivalent to the new affected source and employs control technology for control of emissions of hazardous air pollutants that is practical for use on the new affected source.

Source category schedule for standards means the schedule for promulgating MACT standards issued pursuant to section 112(e) of the Act.

[[59 FR 26449](#), May 20, 1994, as amended at [61 FR 21372](#), May 10, 1996; [64 FR 26314](#), May 14, 1999; [67 FR 16605](#), Apr. 5, 2002]

§ 63.52 Approval process for new and existing affected sources.

(a) *Sources subject to section 112(j) as of the section 112(j) deadline.* The requirements of [paragraphs \(a\)\(1\)](#) and [\(2\)](#) of this section apply to major sources that include, as of the section 112(j) deadline, one or more sources in a category or subcategory for which the Administrator has failed to promulgate an emission standard under this part on or before an applicable section 112(j) deadline. Existing source MACT requirements (including relevant compliance deadlines), as specified in a title V permit issued to the source pursuant to the requirements of the subpart, must apply to such sources.

(1) The owner or operator must submit an application for a title V permit or for a revision to an existing title V permit or a pending title V permit meeting the requirements of [§ 63.53\(a\)](#) by the section 112(j) deadline if the owner or operator can reasonably determine that one or more sources at the major source belong in the category or subcategory subject to section 112(j).

(2) If an application was not submitted under [paragraph \(a\)\(1\)](#) of this section and if notified by the permitting authority, the owner or operator must submit an application for a title V permit or for a revision to an existing title V permit or a pending title V permit meeting the requirements of [§ 63.53\(a\)](#) within 30 days after being notified in writing by the permitting authority that one or more sources at the major source belong to such category or subcategory. Permitting authorities are not required to make such notification.

(3) The requirements in [paragraphs \(a\)\(3\)\(i\)](#) through [\(ii\)](#) of this section apply when the owner or operator has obtained a title V permit that incorporates a case-by-case MACT determination by the permitting authority under section 112(g) or has submitted a title V permit application for a revision that incorporates a case-by-case MACT determination under section 112(g), but has not submitted an application for a title V permit revision that addresses the emission limitation requirements of section 112(j).

(i) When the owner or operator has a title V permit that incorporates a case-by-case MACT determination by the permitting authority under section 112(g), the owner or operator must submit an application meeting the requirements of [§ 63.53\(a\)](#) for a title V permit revision within 30 days of the section 112(j) deadline or within 30 days of being notified in writing by the permitting authority that one or more sources at the major source belong in such category or subcategory. Using the procedures established in [paragraph \(e\)](#) of this section, the permitting authority must determine whether the emission limitations adopted pursuant to the prior case-by-case MACT determination under section 112(g) are substantially as effective as the emission limitations which the permitting authority would otherwise adopt pursuant to section 112(j) for the source in question. If the permitting authority determines that the emission limitations previously adopted to effectuate section 112(g) are substantially as effective as the emission limitations which the permitting authority would otherwise adopt to effectuate section 112(j) for the source, then the permitting authority must retain the existing emission limitations in the permit as the emission limitations to

effectuate section 112(j). The title V permit applicable to that source must be revised accordingly. If the permitting authority does not retain the existing emission limitations in the permit as the emission limitations to effectuate section 112(j), the MACT requirements of this subpart are satisfied upon issuance of a revised title V permit incorporating any additional section 112(j) requirements.

(ii) When the owner or operator has submitted a title V permit application that incorporates a case-by-case MACT determination by the permitting authority under section 112(g), but has not received the permit incorporating the section 112(g) requirements, the owner or operator must continue to pursue a title V permit that addresses the emission limitation requirements of section 112(g). Within 30 days of issuance of that title V permit, the owner or operator must submit an application meeting the requirements of [§ 63.53\(a\)](#) for a change to the existing title V permit. Using the procedures established in [paragraph \(e\)](#) of this section, the permitting authority must determine whether the emission limitations adopted pursuant to the prior case-by-case MACT determination under section 112(g) are substantially as effective as the emission limitations which the permitting authority would otherwise adopt pursuant to section 112(j) for the source in question. If the permitting authority determines that the emission limitations previously adopted to effectuate section 112(g) are substantially as effective as the emission limitations which the permitting authority would otherwise adopt to effectuate section 112(j) for the source, then the permitting authority must retain the existing emission limitations in the permit as the emission limitations to effectuate section 112(j). The title V permit applicable to that source must be revised accordingly. If the permitting authority does not retain the existing emission limitations in the permit as the emission limitations to effectuate section 112(j), the MACT requirements of this subpart are satisfied upon issuance of a revised title V permit incorporating any additional section 112(j) requirements.

(b) Sources that become subject to section 112(j) after the section 112(j) deadline and that do not have a title V permit addressing section 112(j) requirements. The requirements of [paragraphs \(b\)\(1\)](#) through [\(4\)](#) of this section apply to sources that do not meet the criteria in [paragraph \(a\)](#) of this section on the section 112(j) deadline and are, therefore, not subject to section 112(j) on that date, but where events occur subsequent to the section 112(j) deadline that would bring the source under the requirements of this subpart, and the source does not have a title V permit that addresses the requirements of section 112(j).

(1) When one or more sources in a category or subcategory subject to the requirements of this subpart are installed at a major source, or result in the source becoming a major source due to the installation, and the installation does not invoke section 112(g) requirements, the owner or operator must submit an application meeting the requirements of [§ 63.53\(a\)](#) within 30 days of startup of the source. This application shall be reviewed using the procedures established in [paragraph \(e\)](#) of this section. Existing source MACT requirements (including relevant compliance deadlines), as specified in a title V permit issued pursuant to the requirements of this subpart, shall apply to such sources.

(2) The requirements in this paragraph apply when one or more sources in a category or subcategory subject to this subpart are installed at a major source, or result in the source

becoming a major source due to the installation, and the installation does require emission limitations to be established and permitted under section 112(g), and the owner or operator has not submitted an application for a title V permit revision that addresses the emission limitation requirements of section 112(j). In this case, the owner or operator must apply for and obtain a title V permit that addresses the emission limitation requirements of section 112(g). Within 30 days of issuance of that title V permit, the owner or operator must submit an application meeting the requirements of [§ 63.53\(a\)](#) for a revision to the existing title V permit. Using the procedures established in [paragraph \(e\)](#) of this section, the permitting authority must determine whether the emission limitations adopted pursuant to the prior case-by-case MACT determination under section 112(g) are substantially as effective as the emission limitations which the permitting authority would otherwise adopt pursuant to section 112(j) for the source in question. If the permitting authority determines that the emission limitations previously adopted to effectuate section 112(g) are substantially as effective as the emission limitations which the permitting authority would otherwise adopt to effectuate section 112(j) for the source, then the permitting authority must retain the existing emission limitations in the permit as the emission limitations to effectuate section 112(j). The title V permit applicable to that source must be revised accordingly. If the permitting authority does not retain the existing emission limitations in the permit as the emission limitations to effectuate section 112(j), the MACT requirements of this subpart are satisfied upon issuance of a revised title V permit incorporating any additional section 112(j) requirements.

(3) The owner or operator of an area source that, due to a relaxation in any federally enforceable emission limitation (such as a restriction on hours of operation), increases its potential to emit hazardous air pollutants such that the source becomes a major source that is subject to this subpart, must submit an application meeting the requirements of [§ 63.53\(a\)](#) for a title V permit or for an application for a title V permit revision within 30 days after the date that such source becomes a major source. This application must be reviewed using the procedures established in [paragraph \(e\)](#) of this section. Existing source MACT requirements (including relevant compliance deadlines), as specified in a title V permit issued pursuant to the requirements of this subpart, must apply to such sources.

(4) On or after April 5, 2002, if the Administrator establishes a lesser quantity emission rate under section 112(a)(1) of the Act that results in an area source becoming a major source that is subject to this subpart, then the owner or operator of such a major source must submit an application meeting the requirements of [§ 63.53\(a\)](#) for a title V permit or for a change to an existing title V permit or pending title V permit on or before the date 6 months after the date that such source becomes a major source. Existing source MACT requirements (including relevant compliance deadlines), as specified in a title V permit issued pursuant to the requirements of this subpart, shall apply to such sources.

(c) **Sources that have a title V permit addressing section 112(j) requirements.** The requirements of [paragraphs \(c\)\(1\)](#) and [\(2\)](#) of this section apply to major sources that include one or more sources in a category or subcategory for which the Administrator fails to promulgate an emission standard under this part on or before an applicable section 112(j) deadline, and the owner or operator has a permit meeting the section 112(j) requirements, and

where changes occur at the major source to equipment, activities, or both, subsequent to the section 112(j) deadline.

(1) If the title V permit already provides the appropriate requirements that address the events that occur under [paragraph \(c\)](#) of this section subsequent to the section 112(j) deadline, then the source must comply with the applicable new source MACT or existing source MACT requirements as specified in the permit, and the section 112(j) requirements are thus satisfied.

(2) If the title V permit does not contain the appropriate requirements that address the events that occur under [paragraph \(c\)](#) of this section subsequent to the section 112(j) deadline, then the owner or operator must submit an application for a revision to the existing title V permit that meets the requirements of [§ 63.53\(a\)](#). The application must be submitted within 30 days of beginning construction and must be reviewed using the procedures established in [paragraph \(e\)](#) of this section. Existing source MACT requirements (including relevant compliance deadlines), as specified in a title V permit issued pursuant to the requirements of this subpart, shall apply to such sources.

(d) *Requests for applicability determination or notice of MACT approval.*

(1) An owner or operator who is unsure of whether one or more sources at a major source belong in a category or subcategory for which the Administrator has failed to promulgate an emission standard under this part may, on or before an applicable section 112(j) deadline, request an applicability determination from the permitting authority by submitting an application meeting the requirements of [§ 63.53\(a\)](#) by the applicable deadlines specified in [paragraphs \(a\), \(b\), or \(c\)](#) of this section.

(2) In addition to meeting the requirements of [paragraphs \(a\), \(b\), and \(c\)](#) of this section, the owner or operator of a new affected source may submit an application for a Notice of MACT Approval before construction, pursuant to [§ 63.54](#).

(e) *Permit application review.*

(1) Each owner or operator who is required to submit to the permitting authority a Part 1 MACT application which meets the requirements of [§ 63.53\(a\)](#) for one or more sources in a category or subcategory subject to section 112(j) must also submit to the permitting authority a timely Part 2 MACT application for the same sources which meets the requirements of [§ 63.53\(b\)](#). Each owner or operator shall submit the Part 2 MACT application for the sources in a particular category or subcategory no later than the applicable date specified in table 1 to this subpart. The submission date specified in table 1 to this subpart for Miscellaneous Organic Chemical Manufacturing shall apply to sources in each of the source categories listed in table 2 to this subpart. When the owner or operator is required by [§§ 63.50 through 63.56](#) to submit an application meeting the requirements of [§ 63.53\(a\)](#) by a date which is after the date for a Part 2 MACT application for sources in the category or subcategory in question established by table 1 to this subpart, the owner or operator shall submit a Part 2 MACT application meeting the requirements of [§ 63.53\(b\)](#) within 60 additional days after the applicable deadline for submission of the Part 1 MACT application.

Part 2 MACT applications must be reviewed by the permitting authority according to procedures established in [§ 63.55](#). The resulting MACT determination must be incorporated into the source's title V permit according to procedures established under title V, and any other regulations approved under title V in the jurisdiction in which the affected source is located.

(2) Notwithstanding [paragraph \(e\)\(1\)](#) of this section, the owner or operator may request either an applicability determination or an equivalency determination by the permitting authority as provided in [paragraphs \(e\)\(2\)\(i\)](#) and [\(ii\)](#) of this section.

(i) Each owner or operator who submitted a request for an applicability determination pursuant to [paragraph \(d\)\(1\)](#) of this section on or before May 15, 2002, which remains pending before the permitting authority on May 30, 2003, and who still wishes to obtain such a determination, must resubmit that request by July 29, 2003, or by the date which is 60 days after the Administrator publishes in the Federal Register a proposed standard under section 112(d) or 112(h) of the Act for the category or subcategory in question, whichever is later. Each request for an applicability determination which is resubmitted under this [paragraph \(e\)\(2\)\(i\)](#) must be supplemented to discuss the relation between the source(s) in question and the applicability provision in the proposed standard for the category or subcategory in question, and to explain why there may still be uncertainties that require a determination of applicability. The permitting authority must take action upon each properly resubmitted and supplemented request for an applicability determination within an additional 60 days after the applicable deadline for the resubmitted request. If the applicability determination is positive, the owner or operator must submit a Part 2 MACT application meeting the requirements of [§ 63.53\(b\)](#) by the date specified for the category or subcategory in question in Table 1 to this subpart. If the applicability determination is negative, then no further action by the owner or operator is necessary.

(ii) As specified in [paragraphs \(a\)](#) and [\(b\)](#) of this section, an owner or operator who has submitted an application meeting the requirements of [§ 63.53\(a\)](#) may request a determination by the permitting authority of whether emission limitations adopted pursuant to a prior case-by-case MACT determination under section 112(g) that apply to one or more sources at a major source in a relevant category or subcategory are substantially as effective as the emission limitations which the permitting authority would otherwise adopt pursuant to section 112(j) for the source in question. Such a request must be submitted by the date for the category or subcategory in question specified in Table 1 to this subpart. Any owner or operator who previously submitted such a request under a prior version of this [paragraph \(e\)\(2\)\(ii\)](#) need not resubmit the request. Each request for an equivalency determination under this [paragraph \(e\)\(2\)\(ii\)](#), regardless of when it was submitted, will be construed in the alternative as a complete application for an equivalent emission limitation under section 112(j). The process for determination by the permitting authority of whether the emission limitations in the prior case-by-case MACT determination are substantially as effective as the emission limitations which the permitting authority would otherwise adopt under section 112(j) must include the opportunity for full public, EPA, and affected State review prior to a final determination. If the permitting authority determines that the emission limitations in the prior case-by-case MACT determination are substantially as

effective as the emission limitations which the permitting authority would otherwise adopt under section 112(j), then the permitting authority must adopt the existing emission limitations in the permit as the emission limitations to effectuate section 112(j) for the source in question. If more than 3 years remain on the current title V permit, the owner or operator must submit an application for a title V permit revision to make any conforming changes in the permit required to adopt the existing emission limitations as the section 112(j) MACT emission limitations. If less than 3 years remain on the current title V permit, any required conforming changes must be made when the permit is renewed. If the permitting authority determines that the emission limitations in the prior case-by-case MACT determination under section 112(g) are not substantially as effective as the emission limitations which the permitting authority would otherwise adopt for the source in question under section 112(j), the permitting authority must make a new MACT determination and adopt a title V permit incorporating an appropriate equivalent emission limitation under section 112(j). Such a determination constitutes final action for purposes of judicial review under [40 CFR 70.4\(b\)\(3\)\(x\)](#) and corresponding State title V program provisions.

(3) Within 60 days of submittal of the Part 2 MACT application, the permitting authority must notify the owner or operator in writing whether the application is complete or incomplete. The Part 2 MACT application shall be deemed complete on the date it was submitted unless the permitting authority notifies the owner or operator in writing within 60 days of the submittal that the Part 2 MACT application is incomplete. A Part 2 MACT application is complete if it is sufficient to begin processing the application for a title V permit addressing section 112(j) requirements. In the event that the permitting authority disapproves a permit application or determines that the application is incomplete, the owner or operator must revise and resubmit the application to meet the objections of the permitting authority. The permitting authority must specify a reasonable period in which the owner or operator is required to remedy the deficiencies in the disapproved or incomplete application. This period may not exceed 6 months from the date the owner or operator is first notified that the application has been disapproved or is incomplete.

(4) Following submittal of a Part 1 or Part 2 MACT application, the permitting authority may request additional information from the owner or operator. The owner or operator must respond to such requests in a timely manner.

(5) If the owner or operator has submitted a timely and complete application as required by this section, any failure to have a title V permit addressing section 112(j) requirements shall not be a violation of section 112(j), unless the delay in final action is due to the failure of the applicant to submit, in a timely manner, information required or requested to process the application. Once a complete application is submitted, the owner or operator shall not be in violation of the requirement to have a title V permit addressing section 112(j) requirements.

(f) **Permit content.** The title V permit must contain an equivalent emission limitation (or limitations) for the relevant category or subcategory determined on a case-by-case basis by the permitting authority, or, if the applicable criteria in [subpart D of this part](#) are met, the title V permit may contain an alternative emission limitation. For the purposes of the preceding sentence, early reductions made pursuant to section 112(i)(5)(A) of the Act must be achieved

not later than the date on which the relevant standard should have been promulgated according to the source category schedule for standards.

(1) The title V permit must contain an emission standard or emission limitation that is equivalent to existing source MACT and an emission standard or emission limitation that is equivalent to new source MACT for control of emissions of hazardous air pollutants. The MACT emission standards or limitations must be determined by the permitting authority and must be based on the degree of emission reductions that can be achieved if the control technologies or work practices are installed, maintained, and operated properly. The permit must also specify the affected source and the new affected source. If construction of a new affected source or reconstruction of an affected source commences after a title V permit meeting the requirements of section 112(j) has been issued for the source, the new source MACT compliance dates must apply.

(2) The title V permit must specify any notification, operation and maintenance, performance testing, monitoring, and reporting and recordkeeping requirements. In developing the title V permit, the permitting authority must consider and specify the appropriate provisions of [subpart A of this part](#). The title V permit must also include the information in [paragraphs \(f\)\(2\)\(i\) through \(iii\)](#) of this section.

(i) In addition to the MACT emission limitation required by [paragraph \(f\)\(1\)](#) of this section, additional emission limits, production limits, operational limits or other terms and conditions necessary to ensure practicable enforceability of the MACT emission limitation.

(ii) Compliance certifications, testing, monitoring, reporting and recordkeeping requirements that are consistent with requirements established pursuant to title V and [paragraph \(h\)](#) of this section.

(iii) Compliance dates by which the owner or operator must be in compliance with the MACT emission limitation and all other applicable terms and conditions of the permit.

(A) The owner or operator of an affected source subject to the requirements of this subpart must comply with the emission limitation(s) by the date established in the source's title V permit. In no case shall such compliance date be later than 3 years after the issuance of the permit for that source, except where the permitting authority issues a permit that grants an additional year to comply in accordance with section 112(i)(3)(B) of the Act, or unless otherwise specified in section 112(i), or in [subpart D of this part](#).

(B) The owner or operator of a new affected source, as defined in the title V permit meeting the requirements of section 112(j), that is subject to the requirements of this subpart must comply with a new source MACT level of control immediately upon startup of the new affected source.

(g) **Permit issuance dates.** The permitting authority must issue a title V permit meeting section 112(j) requirements within 18 months after submittal of the complete Part 2 MACT application.

(h) **Enhanced monitoring.** In accordance with section 114(a)(3) of the Act, monitoring shall be capable of demonstrating continuous compliance for each compliance period during the applicable reporting period. Such monitoring data shall be of sufficient quality to be used as a basis for directly enforcing all applicable requirements established under this subpart, including emission limitations.

(i) **MACT emission limitations.**

(1) The owner or operator of affected sources subject to [paragraphs \(a\), \(b\), and \(c\)](#) of this section must comply with all requirements of this subpart that are applicable to affected sources, including the compliance date for affected sources established in [paragraph \(f\)\(2\)\(iii\)\(A\)](#) of this section.

(2) The owner or operator of new affected sources subject to [paragraph \(c\)\(1\)](#) of this section must comply with all requirements of this subpart that are applicable to new affected sources, including the compliance date for new affected sources established in [paragraph \(f\)\(2\)\(iii\)\(B\)](#) of this section.

[[67 FR 16606](#), Apr. 5, 2002; [68 FR 32602](#), May 30, 2003]

§ 63.53 Application content for case-by-case MACT determinations.

(a) **Part 1 MACT application.** The Part 1 application for a MACT determination must contain the information in [paragraphs \(a\)\(1\)](#) through [\(4\)](#) of this section.

(1) The name and address (physical location) of the major source.

(2) A brief description of the major source and an identification of the relevant source category.

(3) An identification of the types of emission points belonging to the relevant source category.

(4) An identification of any affected sources for which a section 112(g) MACT determination has been made.

(b) **Part 2 MACT application.**

(1) In compiling a Part 2 MACT application, the owner or operator may cross-reference specific information in any prior submission by the owner or operator to the permitting authority, but in cross-referencing such information the owner or operator may not presume favorable action on any prior application or request which is still pending. In compiling a Part 2 MACT application, the owner or operator may also cross-reference any part of a

standard proposed by the Administrator pursuant to section 112(d) or 112(h) of the Act for any category or subcategory which includes sources to which the Part 2 application applies.

(2) The Part 2 application for a MACT determination must contain the information in [paragraphs \(b\)\(2\)\(i\)](#) through [\(b\)\(2\)\(v\)](#) of this section.

(i) For a new affected source, the anticipated date of startup of operation.

(ii) Each emission point or group of emission points at the affected source which is part of a category or subcategory for which a Part 2 MACT application is required, and each of the hazardous air pollutants emitted at those emission points. When the Administrator has proposed a standard pursuant to section 112(d) or 112(h) of the Act for a category or subcategory, such information may be limited to those emission points and hazardous air pollutants which would be subject to control under the proposed standard.

(iii) Any existing Federal, State, or local limitations or requirements governing emissions of hazardous air pollutants from those emission points which are part of a category or subcategory for which a Part 2 application is required.

(iv) For each identified emission point or group of affected emission points, an identification of control technology in place.

(v) Any additional emission data or other information specifically requested by the permitting authority.

(3) The Part 2 application for a MACT determination may, but is not required to, contain the following information:

(i) Recommended emission limitations for the affected source and support information consistent with [§ 63.52\(f\)](#). The owner or operator may recommend a specific design, equipment, work practice, or operational standard, or combination thereof, as an emission limitation.

(ii) A description of the control technologies that would be applied to meet the emission limitation including technical information on the design, operation, size, estimated control efficiency and any other information deemed appropriate by the permitting authority, and identification of the affected sources to which the control technologies must be applied.

(iii) Relevant parameters to be monitored and frequency of monitoring to demonstrate continuous compliance with the MACT emission limitation over the applicable reporting period.

[[67 FR 16609](#), Apr. 5, 2002, as amended at [68 FR 32602](#), May 30, 2003]

§ 63.54 Preconstruction review procedures for new affected sources.

The requirements of this section apply to an owner or operator who constructs a new affected source subject to [§ 63.52\(c\)\(1\)](#). The purpose of this section is to describe alternative review processes that the permitting authority may use to make a MACT determination for the new affected source.

(a) *Review process for new affected sources.*

(1) If the permitting authority requires an owner or operator to obtain or revise a title V permit before construction of the new affected source, or when the owner or operator chooses to obtain or revise a title V permit before construction, the owner or operator must follow the procedures established under the applicable title V permit program before construction of the new affected source.

(2) If an owner or operator is not required to obtain or revise a title V permit before construction of the new affected source (and has not elected to do so), but the new affected source is covered by any preconstruction or preoperation review requirements established pursuant to section 112(g) of the Act, then the owner or operator must comply with those requirements in order to ensure that the requirements of section 112(j) and (g) are satisfied. If the new affected source is not covered by section 112(g), the permitting authority, in its discretion, may issue a Notice of MACT Approval, or the equivalent, in accordance with the procedures set forth in [paragraphs \(b\)](#) through [\(f\)](#) of this section, or an equivalent permit review process, before construction or operation of the new affected source.

(3) Regardless of the review process, the MACT determination shall be consistent with the principles established in [§ 63.55](#). The application for a Notice of MACT Approval or a title V permit, permit modification, or administrative amendment, whichever is applicable, shall include the documentation required by [§ 63.53](#).

(b) *Optional administrative procedures for preconstruction or preoperation review for new affected sources.* The permitting authority may provide for an enhanced review of section 112(j) MACT determinations for review procedures and compliance requirements equivalent to those set forth in [paragraphs \(b\)](#) through [\(f\)](#) of this section.

(1) The permitting authority will notify the owner or operator in writing as to whether the application for a MACT determination is complete or whether additional information is required.

(2) The permitting authority will approve an applicant's proposed control technology, or the permitting authority will notify the owner or operator in writing of its intention to disapprove a control technology.

- (3) The owner or operator may present in writing, within a time frame specified by the permitting authority, additional information, considerations, or amendments to the application before the permitting authority's issuance of a final disapproval.
- (4) The permitting authority will issue a preliminary approval or issue a disapproval of the application, taking into account additional information received from the owner or operator.
- (5) A determination to disapprove any application will be in writing and will specify the grounds on which the disapproval is based.
- (6) Approval of an applicant's proposed control technology must be set forth in a Notice of MACT Approval (or the equivalent) as described in [§ 63.52\(f\)](#).

(c) ***Opportunity for public comment on Notice of MACT Approval.*** The permitting authority will provide opportunity for public comment on the preliminary Notice of MACT Approval prior to issuance, including, at a minimum,

- (1) Availability for public inspection in at least one location in the area affected of the information submitted by the owner or operator and of the permitting authority's tentative determination;
- (2) A period for submittal of public comment of at least 30 days; and
- (3) A notice by prominent advertisement in the area affected of the location of the source information and analysis specified in [§ 63.52\(f\)](#). The form and content of the notice must be substantially equivalent to that found in [§ 70.7 of this chapter](#).
- (4) An opportunity for a public hearing, if one is requested. The permitting authority will give at least 30 days notice in advance of any hearing.

(d) ***Review by the EPA and affected States.*** The permitting authority must send copies of the preliminary notice (in time for comment) and final notice required by [paragraph \(c\)](#) of this section to the Administrator through the appropriate Regional Office, and to all other State and local air pollution control agencies having jurisdiction in affected States. The permitting authority must provide EPA with a review period for the final notice of at least 45 days and shall not issue a final Notice of MACT Approval until EPA objections are satisfied.

(e) ***Compliance with MACT determinations.*** An owner or operator of a major source that is subject to a MACT determination must comply with notification, operation and maintenance, performance testing, monitoring, reporting, and recordkeeping requirements established under [§ 63.52\(h\)](#), under title V, and at the discretion of the permitting authority, under [subpart A of this part](#). The permitting authority must provide the EPA with the opportunity to review compliance requirements for consistency with requirements established pursuant to title V during the review period under [paragraph \(d\)](#) of this section.

(f) *Equivalency under section 112(l)*. If a permitting authority requires preconstruction review for new source MACT determinations under this subpart, such requirement shall not necessitate a determination under [subpart E of this part](#).

[[59 FR 26449](#), May 20, 1994, as amended at [67 FR 16610](#), Apr. 5, 2002]

§ 63.55 Maximum achievable control technology (MACT) determinations for affected sources subject to case-by-case determination of equivalent emission limitations.

(a) *Requirements for permitting authorities*. The permitting authority must determine whether the [§ 63.53\(a\)](#) Part 1 and [§ 63.53\(b\)](#) Part 2 MACT application is complete or an application for a Notice of MACT Approval is approvable. In either case, when the application is complete or approvable, the permitting authority must establish hazardous air pollutant emissions limitations equivalent to the limitations that would apply if an emission standard had been issued in a timely manner under section 112(d) or (h) of the Act. The permitting authority must establish these emissions limitations consistent with the following requirements and principles:

- (1) Emission limitations must be established for the equipment and activities within the affected sources within a source category or subcategory for which the section 112(j) deadline has passed.
- (2) Each emission limitation for an existing affected source must reflect the maximum degree of reduction in emissions of hazardous air pollutants (including a prohibition on such emissions, where achievable) that the permitting authority, taking into consideration the cost of achieving such emission reduction and any non-air quality health and environmental impacts and energy requirements, determines is achievable by affected sources in the category or subcategory for which the section 112(j) deadline has passed. This limitation must not be less stringent than the MACT floor which must be established by the permitting authority according to the requirements of section 112(d)(3)(A) and (B) and must be based upon available information.
- (3) Each emission limitation for a new affected source must reflect the maximum degree of reduction in emissions of hazardous air pollutants (including a prohibition on such emissions, where achievable) that the permitting authority, taking into consideration the cost of achieving such emission reduction and any non-air quality health and environmental impacts and energy requirements, determines is achievable. This limitation must not be less stringent than the emission limitation achieved in practice by the best controlled similar source which must be established by the permitting authority according to the requirements of section 112(d)(3). This limitation must be based upon available information.
- (4) The permitting authority must select a specific design, equipment, work practice, or operational standard, or combination thereof, when it is not feasible to prescribe or enforce an equivalent emission limitation due to the nature of the process or pollutant. It is not feasible to prescribe or enforce a limitation when the Administrator determines that

hazardous air pollutants cannot be emitted through a conveyance designed and constructed to capture such pollutant, or that any requirement for, or use of, such a conveyance would be inconsistent with any Federal, State, or local law, or the application of measurement methodology to a particular class of sources is not practicable due to technological and economic limitations.

(5) Nothing in this subpart shall prevent a State or local permitting authority from establishing an emission limitation more stringent than required by Federal regulations.

(b) **Reporting to EPA.** The owner or operator must submit additional copies of its Part 1 and Part 2 MACT application for a title V permit, permit revision, or Notice of MACT Approval, whichever is applicable, to the EPA at the same time the material is submitted to the permitting authority.

[[67 FR 16610](#), Apr. 5, 2002]

§ 63.56 Requirements for case-by-case determination of equivalent emission limitations after promulgation of subsequent MACT standard.

(a) If the Administrator promulgates a relevant emission standard that is applicable to one or more affected sources within a major source before the date a permit application under this [paragraph \(a\)](#) is approved, the title V permit must contain the promulgated standard rather than the emission limitation determined under [§ 63.52](#), and the owner or operator must comply with the promulgated standard by the compliance date in the promulgated standard.

(b) If the Administrator promulgates a relevant emission standard under section 112(d) or (h) of the Act that is applicable to a source after the date a permit is issued pursuant to [§ 63.52](#) or [§ 63.54](#), the permitting authority must incorporate requirements of that standard in the title V permit upon its next renewal. The permitting authority must establish a compliance date in the revised permit that assures that the owner or operator must comply with the promulgated standard within a reasonable time, but not longer than 8 years after such standard is promulgated or 8 years after the date by which the owner or operator was first required to comply with the emission limitation established by the permit, whichever is earlier. However, in no event shall the period for compliance for existing sources be shorter than that provided for existing sources in the promulgated standard.

(c) Notwithstanding the requirements of [paragraph \(a\)](#) or [\(b\)](#) of this section, the requirements of [paragraphs \(c\)\(1\)](#) and [\(2\)](#) of this section shall apply.

(1) If the Administrator promulgates an emission standard under section 112(d) or (h) that is applicable to an affected source after the date a permit application under this paragraph is approved under [§ 63.52](#) or [§ 63.54](#), the permitting authority is not required to change the emission limitation in the permit to reflect the promulgated standard if the permitting authority determines that the level of control required by the emission limitation in the permit

is substantially as effective as that required by the promulgated standard pursuant to [§ 63.1\(e\)](#).

(2) If the Administrator promulgates an emission standard under section 112(d) or (h) of the Act that is applicable to an affected source after the date a permit application is approved under [§ 63.52](#) or [§ 63.54](#), and the level of control required by the promulgated standard is less stringent than the level of control required by any emission limitation in the prior MACT determination, the permitting authority is not required to incorporate any less stringent emission limitation of the promulgated standard in the title V permit and may in its discretion consider any more stringent provisions of the MACT determination to be applicable legal requirements when issuing or revising such a title V permit.

Table 1 to Subpart B of Part 63 - Section 112(j) Part 2 Application Due Dates

Due date	MACT standard
10/30/03	Combustion Turbines. Lime Manufacturing. Site Remediation. Iron and Steel Foundries. Taconite Iron Ore Processing. Miscellaneous Organic Chemical Manufacturing (MON). ¹
	Organic Liquids Distribution. Primary Magnesium Refining. Metal Can (Surface Coating). Plastic Parts and Products (Surface Coating). Chlorine Production. Miscellaneous Metal Parts and Products (Surface Coating) (and Asphalt/Coal Tar Application - Metal Pipes). ²
4/28/04	Industrial Boilers, Institutional/Commercial Boilers and Process Heaters. ³ Plywood and Composite Wood Products. Reciprocating Internal Combustion Engines. ⁴ Auto and Light-Duty Truck (Surface Coating).
11/14/05	Industrial Boilers, Institutional/Commercial Boilers, and Process Heaters. ⁵ Hydrochloric Acid Production. ⁶

¹ Covers 23 source categories, see Table 2 to this subpart.

² Two source categories.

³ Includes all sources in the three categories, Industrial Boilers, Institutional/Commercial Boilers, and Process Heaters that burn no hazardous waste.

⁴ Includes engines greater than 500 brake horsepower.

⁵ Includes all sources in the three categories, Industrial Boilers, Institutional/Commercial Boilers, and Process Heaters that burn hazardous waste.

⁶ Includes furnaces that produce acid from hazardous waste at sources in the category Hydrochloric Acid Production.

[[68 FR 32603](#), May 30, 2003, as amended at [70 FR 39664](#), July 11, 2005]

Table 2 to Subpart B of Part 63 - MON Source Categories

Manufacture of Paints, Coatings, and Adhesives.

Alkyd Resins Production.

Maleic Anhydride Copolymers Production.

Polyester Resins Production.

Polymerized Vinylidene Chloride Production.

Polymethyl Methacrylate Resins Production.

Polyvinyl Acetate Emulsions Production.

Polyvinyl Alcohol Production.

Polyvinyl Butyral Production.

Ammonium Sulfate Production-Caprolactam By-Product Plants.

Quaternary Ammonium Compounds Production.

Benzyltrimethylammonium Chloride Production.

Carbonyl Sulfide Production.

Chelating Agents Production.

Chlorinated Paraffins Production.

Ethylidene Norbornene Production.

Explosives Production.

Hydrazine Production.

OBPA/1,3-Diisocyanate Production.

Photographic Chemicals Production.

Phthalate Plasticizers Production.

Rubber Chemicals Manufacturing.

Symmetrical Tetrachloropyridine Production.

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